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## Assessment of evaporative cooling efficiency in greenhouses equipped with wetted porous plates

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### Abstract

The main objective of this study was to experimentally validate a mechanistic model for predicting the cooling efficiency ( $\eta$ ) of wetted porous plates built with expanded clay. The expanded clay material was physically characterized by specific mass, surface area, and volume. The model was validated with dry bulb temperature ( $T_{db}$ , °C) and air relative humidity (RH, %) data, which were continuously monitored in two different points, upstream and downstream the direction of the air passing through the porous plate. Data collection was carried out consecutively for a period of 10 days, between 11:00 a.m. and 4:00 p.m. Average values for  $\eta$ , simulated and observed, were  $74.8 \pm 7.4\%$  and  $68.3 \pm 8.3\%$ , respectively. Based on the developed model, it was observed that  $\eta$  was higher than 40% for  $T_{db} > 30$  °C and constant RH at 45%. The simulation for predictions indicates that the increase in the air temperature greater than 20 °C may affect negatively the production in greenhouses from states located in tropical and subtropical countries as Minas Gerais, Brazil, if some design criteria in the evaporative cooling system are not revised.

**Keywords:** Greenhouse; mathematical modeling; simulation; heat and mass transfer.

## Evaluación de la eficiencia de equipos de enfriamiento evaporativo usando placas porosas en invernaderos

### Resumen

El objetivo principal de este estudio fue validar experimentalmente un modelo mecánico para predecir la eficacia de enfriamiento ( $\eta$ ) de placas porosas construidas con arcilla expandida. El material de arcilla expandida fue físicamente caracterizado encontrando su masa específica, área superficial y volumen. El modelo fue validado con datos de temperatura de bulbo seco ( $T_{db}$ , °C) y humedad relativa del aire (humedad relativa, %) que fueron continuamente monitoreados en dos puntos diferentes, en contra y a favor de la dirección del aire que pasa a través de la placa porosa. La recolección de datos se llevó a cabo de forma consecutiva durante un período de 10 días entre las 11:00 y 4:00 p.m. Los valores medios de  $\eta$ , simulados y observados, fueron  $74,8 \pm 7,4\%$  y  $68,3 \pm 8,3\%$ , respectivamente. Basado en el modelo desarrollado, se observó que  $\eta$  fue mayor del 40% para  $T_{db} > 30$  °C y HR constante en 45%. La simulación indicó que el aumento de la temperatura del aire puede afectar negativamente la producción en invernaderos en Estados como Minas Gerais, Brazil, si no se revisan algunos criterios de diseño en el sistema de enfriamiento por evaporación.

**Palabras clave:** Invernadero; modelo matemático; simulación; transferencia de calor y masa.

### 1. Introduction

Climate change is no longer considered a questionable scientific hypothesis, but an inevitable paradigm [1]. One of its consequences is that some regions of the globe are being

exposed to extreme (high or low) temperatures. Specifically, tropical regions are facing abnormally warm summers, impacting both natural ecosystems and human intervened environments. In the latter, agriculture may be the sector of society that is mostly sensitive to extreme temperatures.

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Production efficiency in greenhouse systems are inherently dependent on external factors such as climatic agents (dry bulb temperature -  $T_{db}$ , relative humidity - RH, solar radiation, etc.), and design factors such as the roofing and walls materials and the presence of insect protection screens [2,3]. Climate control mechanisms, such as the ventilation and evaporative cooling systems [4], are essential for allowing optimum convective transfer of water vapor, gases and heat, keeping the internal environment at healthy levels.

Typical forms of evaporative cooling systems for protected environments consist of misting systems (low and high pressure), or forced passage of air through wetted porous plates by means of a ventilation system. According to [5], depending on the climatic conditions of the region where the evaporative cooling system is developed,  $T_{db}$  may be reduced up to 11°C. In tropical regions such as in Brazil, the average temperature drop is about 6°C.

The operating principle of evaporative cooling systems involves processes induced by heat and mass transfer, where water (either in its liquid or vapor state) and air are the working fluids. This process consists in evaporating water induced by the passage of an airflow, thus decreasing the  $T_{db}$  [6-8].

In order to evaluate and compare different evaporative cooling systems, various research studies have been conducted in the field [9-11]. However, limitations such as insufficient number of greenhouses with similar systems at the same location, and the high costs for conducting experimental research, have hampered the conduction of field studies covering a significant number of variables and factors.

A possible solution to this problem can be the use of models and computer simulations, followed by field validations. Subsequently, such validated models may be used to indicate the most relevant factors or variables, which, ultimately, are to be tested experimentally. Currently, a number of modeling techniques have been applied to simulate evaporative cooling systems in greenhouses [12,13]. These modeling approaches are still labor-intensive and require the acquisition of expensive specific commercial packages.

The development or adaptation of a mechanistic model for evaporative cooling systems that is relatively simpler but still able to accurately represent reality needs to be further evaluated. Evaporative coolers have been widely used for crop production in greenhouses due to their relatively good cost/benefit ratio. In these systems, the quantification of the efficiency ( $\eta$ ) is of great importance.

The aim of the present work was: a) to describe and validate a mechanistic model developed to predict the evaporative cooling efficiency ( $\eta$ ) of a wetted porous plate (PAD) system applied to a greenhouse, and b) present some experimental results in future scenarios of climate change.

## 2. Material and methods

### 2.1. Model description

The evaporative cooling efficiency ( $\eta$ ) is calculated from the variables dry bulb temperature ( $T_{db}$ ) and wet bulb temperature ( $T_{wb}$ ) of the air, measured both upstream and

downstream the pads, according to Eq.1 [14].

$$\eta = \left[ \frac{T_{db,i} - T_{db,o}}{T_{db,i} - T_{wb,i}} \right] \cdot 100 \quad (1)$$

Where:  $\eta$  - evaporative cooling efficiency (%);  $T_{db,i}$  and  $T_{db,o}$  - dry bulb temperature of the air upstream and downstream the pad cooling system, respectively (°C); and  $T_{wb,i}$  - wet bulb temperature of the air upstream the pad cooling system, (°C).

Fig. 1 can be observed the schematic representation of an evaporative cooling system of the wetted porous material type, where: a) Variable of air upstream the PAD cooling system:  $T_{db,i}$  - dry bulb temperature (°C),  $\omega_{a,i}$  - mixing ratio gradient ( $\text{kg kg}^{-1}$ );  $P_{atm}$  - Atmospheric pressure (kPa),  $\dot{m}_a$  - flow of water passing through the cooling plate ( $\text{kg s}^{-1}$ ); b) Variable of water:  $T_{water,i}$  - water temperature used to wet the cooling plate (°C) and  $\dot{m}_w$  - water flow through the cooling plate ( $\text{kg s}^{-1}$ ); c) Variable of PAD cooling:  $W$  - cooling plate width (m);  $H$  - cooling plate height (m) and  $L$  - thickness of the cooling plate (m); d) Variable of air downstream the PAD cooling system:  $T_{db,o}$  - dry bulb temperature of the air upstream (°C) and  $\omega_{a,o}$  - air mixture ratio after going through the cooling plate ( $\text{kg kg}^{-1}$ ).

Hence, a mathematical model for predicting  $\eta$  in pad cooling systems was developed, based on the heat and mass transfer equations proposed by [15]. The transfer of sensible heat between the air and the existing water film of the porous material can be expressed by Eq. 2, which, after integration (Eq. 3), resulted in Eq. 4, that predicts the temperature of the air after crossing the cooler ( $T_{bs,o}$ ).

$$dq_{a,s} = \dot{m}_a \cdot c_{p,a} \cdot dT_{db} = h \cdot (T_{water} - T_{db}) \cdot dA \quad (2)$$

Where:  $dq_{a,s}$  - sensible heat gradient (W);  $\dot{m}_a$  - mass flow of air across the cooling plate ( $\text{kg s}^{-1}$ );  $c_{p,a}$  - specific heat of air ( $\text{kJ kg}^{-1} \text{K}^{-1}$ );  $dT_{bs}$  - dry bulb air temperature gradient (°C);  $h$  - convective heat transfer coefficient ( $\text{W m}^{-2} \text{K}^{-1}$ );  $T_{water}$  -

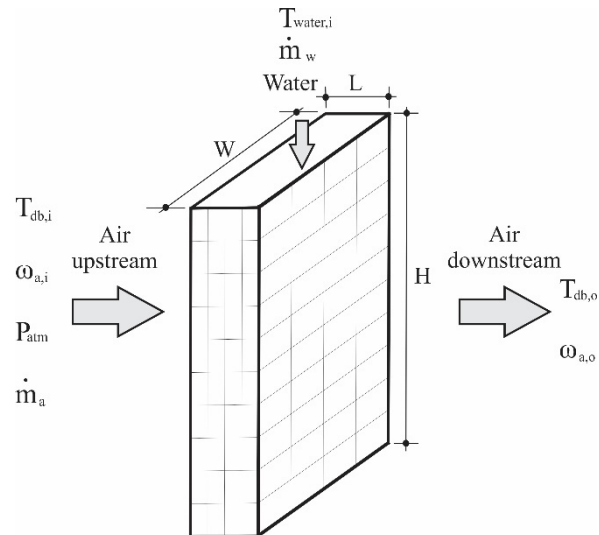


Figure 1. Schematic representation of an evaporative cooling system. Source: The authors.

temperature of the water used in the cooling plate wetting ( $^{\circ}\text{C}$ ); and  $dA$  - area gradient ( $\text{m}^2$ ).

$$\int_{T_{db,i}}^{T_{db,o}} \frac{1}{(T_{\text{water}} - T_{db})} dT_{db} = \frac{h}{m_a \cdot c_{p,a}} \cdot \alpha \cdot W \cdot H \cdot \int_0^L dx \quad (3)$$

Where:  $\alpha$  - surface area of wetted porous plate, per unit volume ( $\text{m}^2 \text{m}^{-3}$ );  $W$  - cooling plate width (m);  $H$  - cooling plate height (m);  $L$  - thickness of the cooling plate (m); and  $dx$  - infinitesimal variation of the cooling plate thickness (m).

$$T_{db,o} = T_{\text{water}} + (T_{db,i} - T_{\text{water}}) \cdot e^{-\left(\frac{h}{m_a \cdot c_{p,a}}\right) \cdot \alpha \cdot W \cdot H \cdot L} \quad (4)$$

Where:  $T_{db,o}$  - air temperature before crossing the plate ( $^{\circ}\text{C}$ ).

Similar to the heat balance performed in equations 1 through 4, a mass balance was performed for water vapor (Eq. 5), which, after substitutions and subsequent incorporation into (Eq. 6) resulted in Eq. 7, used for the prediction of air mixing ratio after crossing the plate ( $\omega_{a,o}$ ).

$$\dot{m} \cdot d\omega_a = k_d \cdot [\omega_{A,s} \cdot T_{\text{water}} - \omega_A] \cdot dA \quad (5)$$

Where:  $d\omega_a$  - mixing ratio gradient ( $\text{kg kg}^{-1}$ );  $k_d$  - mass transfer coefficient based on the use of the mixing ratio ( $\text{kg m}^{-2} \text{s}^{-1}$ );  $\omega_{A,s} \cdot (T_w)$  - mixing ratio to saturation conditions, depending on water temperature ( $\text{kg kg}^{-1}$ ); and  $\omega_A$  - mixing ratio in saturation conditions, depending on the water temperature ( $\text{kg kg}^{-1}$ ).

$$\int_{\omega_{a,i}}^{\omega_{a,o}} \frac{1}{\omega_{a,s} \cdot T_{\text{water}} - \omega_a} d\omega_a = \frac{h_m \cdot \rho_a}{\dot{m}_a} \cdot \alpha \cdot W \cdot H \cdot \int_0^L dx \quad (6)$$

Where:  $\omega_{a,i}$  - air mixture ratio that passes through the cooling plate ( $\text{kg kg}^{-1}$ );  $\omega_{a,o}$  - air mixture ratio after going through the cooling plate ( $\text{kg kg}^{-1}$ );  $h_m$  - mass transfer coefficient ( $\text{m s}^{-1}$ ); and  $\rho_a$  - air density ( $\text{kg m}^{-3}$ ).

$$\omega_{a,o} = \omega_{a,s} \cdot T_{\text{water}} - (\omega_{a,s} \cdot T_{\text{water}} - \omega_{a,i}) \cdot e^{-\left(\frac{h_m \cdot \rho_a}{\dot{m}_a}\right) \cdot \alpha \cdot W \cdot H \cdot L} \quad (7)$$

For the calculation of the mass transfer coefficient ( $h_m$ ), Eq. 8 was used, and the Colburn factor  $j_h$  was calculated by Eq. 9, as proposed by [16]. Eq. 9 is valid for the Prandtl number of about 0.7 and a Reynolds number between 90 and 4000.

$$h_m = 0.929 \cdot j_h \cdot v \quad (8)$$

Where:  $j_h$  - J factor of Colburn (dimensionless); and  $v$  - mass flow of air across the cooling plate ( $\text{kg s}^{-1}$ ).

$$j_h = \frac{2.06 \cdot \text{Re}_D^{-0.575}}{\varepsilon} \quad (9)$$

Where:  $\text{Re}_D$  - Reynolds number defined according to the

diameter of the spheres (dimensionless); and  $\varepsilon$  - porosity of the cooling plate filling material (decimal).

Based on temperature and relative humidity inputs before crossing the wet porous plate ( $T_{db,i}$  and  $\text{RH}_{i,i}$  respectively), wet bulb temperature was calculated ( $T_{wb,i}$ ). With the values of  $T_{db,i}$  and  $T_{wb,i}$  associated with  $T_{db,o}$ , obtained by Eq. 4, the  $\eta_{\text{simulated}}$  was obtained with Eq. 10. For the calculation of these and other psychrometric properties, the methodology proposed by [17] was used.

$$\eta_{\text{simulated}} = \frac{\left[ T_{db,i} - T_{\text{water}} + (T_{db,i} - T_{\text{water}}) \cdot e^{-\left(\frac{h}{m_a \cdot c_{p,a}}\right) \cdot \alpha \cdot W \cdot H \cdot L} \right]}{\left[ T_{db,i} - T_{wb,i} \right]} \cdot 100 \quad (10)$$

The equations demonstrated above were implemented into MS Excel®, where all calculations and simulations of this study were performed.

## 2.2. Characterization of the porous material

It was used expanded clay pebbles as the porous material in this experiment. It was physically characterized by determining the bulk density, porosity, average diameter, average volume and surface area. Each sample consisted of 50 expanded clay pebbles collected randomly from the porous plate. The density of the porous material, Eq. 11, was determined using the methodology of volume complementation, similar to that adopted for determining the bulk density of grain [18].

$$\rho = \frac{m}{V} \quad (11)$$

Where:  $\rho$  - density of the porous material ( $\text{g cm}^{-3}$ );  $m$  - mass of porous material (g); and  $V$  - volume of the porous material ( $\text{cm}^3$ ).

The porosity, Eq. 12, was determined indirectly, by filling the pores of the expanded clay sample with a fluid until saturation, and from the measured volume of the liquid and the sample, determining the total porosity [19].

$$P = \frac{V}{V_{\text{total}}} \cdot 100 \quad (12)$$

Where:  $P$  - total porosity of clays (%);  $V$  - porous volume ( $\text{cm}^3$ ); and  $V_{\text{total}}$  - total volume of the container ( $\text{cm}^3$ ).

The average diameter, volume and the surface area of the samples were obtained by taking photographs of 50 expanded clay with a digital camera (4.0 Mega-pixels) at different angles. These images were processed via Autocad program® 2012 (Autodesk). The results were used to calibrate the equations in order to characterize the modeled porous material as expanded clay.

## 2.3. Experimental setup and data collection for model validation

In order to check whether or not the model was able to realistically represent the cooling process of porous plates

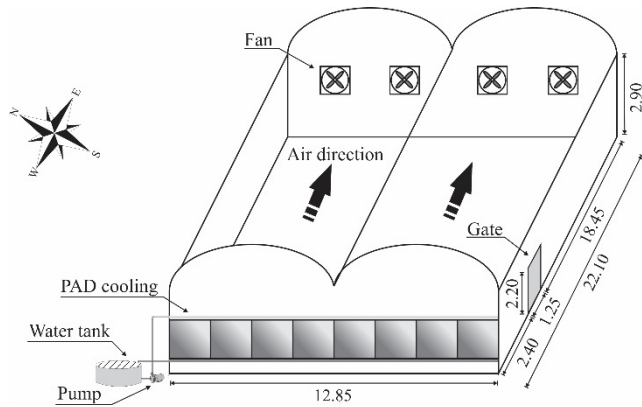


Figure 2. Schematic representation of the greenhouse performed in this study. Unit: meters (m).  
Source: The authors.

made of expanded clay, field measurements were performed at a greenhouse equipped with such a cooling system. The greenhouse was located in the Department of Plant Pathology, Federal University of Lavras (UFLA), in Lavras, Minas Gerais state, Brazil. Local geographical coordinates were 21° 14' south latitude, 45° 00' latitude west of Greenwich and 918 m above sea level. Measurements took place for ten consecutive days, between 11:00 a.m. and 4:00 p.m.

The greenhouse had dimensions of 22.1 m Length × 12.8 m Width × 2.9 m Height, covered with two arches of transparent plastic, east-west orientated, with four hoods. It was equipped with negative pressure tunnel ventilation system, and a series of 8 wetted porous pads measuring in total 12.8 m Length × 1.6 m Height × 0.1 m Depth, made of expanded clay. Fig. 2 shows the representation of the greenhouse studied.

Portable recorders were installed and pre-programmed to collect  $T_{bs}$  and relative humidity (RH) (Hobo®, mod. U12-012, resolution: temperature of 0.03°C and RH of 0.03%) next to the two sides of the wetted porous plate at two-second intervals. In order to assure accuracy of measurements, the sensors were calibrated using a weather station following the manufacturer's instructions.

The variable  $T_{water}$  was monitored at the water reservoir with a digital thermometer (Instrutherm®, mod. TH-060, resolution of ± 0.1°C and precision of 0.1%), at intervals of 30 minutes.

In order to determine the airflow rate through the wetted porous plate, one of the plates (dimensions 1.6 m Height × 1.5 m Length) was randomly selected and divided into nine equidistant sampling points according to the scheme of Fig. 3. Air velocity measurements were made via a digital propeller anemometer (Kestrel®, mod. 4000, precision of ± 3%), at 12 locations. The airflow values used in the simulations was obtained by the product of measured air velocity and area of the plate.

#### 2.4. Prediction of evaporative cooling efficiency for future scenarios

The composition of the future scenarios was developed in accordance to the forecast reported from [1], adding to the air

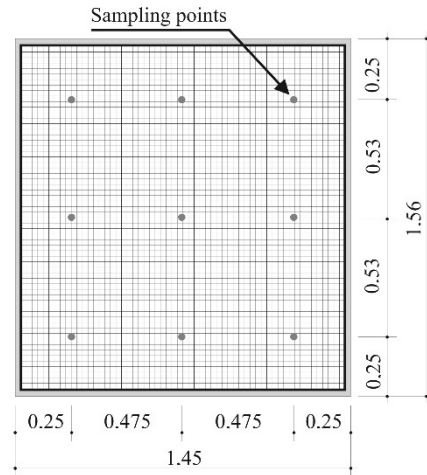


Figure 3. Schematic representation of equidistant points used to collect air velocity in wetted porous plate. Unit: meters (m).  
Source: The authors.

Table 1. Physical properties of the cooling pads (mean ± standard error).

Volume (cm <sup>3</sup> )	1.74 ± 0.88
Superficial area (cm <sup>2</sup> )	7.14 ± 2.39
Diameter (cm)	1.43 ± 0.23
Density (g cm <sup>-3</sup> )	0.36 ± 0.03
Pososity (%)	68 ± 0.7
Surface area of the wetted porous plate (m <sup>2</sup> )	12,8
Water temperature at top of plate (°C)	16.8 ± 0.5
Water temperature at bottom of plate (°C)	16.4 ± 0.5
Mean flow rate per linear meter (L s <sup>-1</sup> m <sup>-1</sup> )	0.050 ± 0.03

Source: The authors.

temperature 2.0°C and 2.5°C to the scenario B2 (more optimistic) in 2050 and 2100, respectively. For the composition of the scenario A2 (less optimistic) it was added 3.0°C e 8.0°C for the years of 2050 and 2100 respectively.

The simulations were performed considering the dimensions of the cooling pad used for validation. The relative humidity, average temperature, maximum temperature and maximum atmospheric pressure were obtained from official climatologic maps for Minas Gerais state, in the period of 1961-1990 [20]. The simulations via mathematical model were performed using the empirical equations adjusted in this experiment in order to estimate the efficiency of the pad cooling.

### 3. Results and discussion

#### 3.1. Summary of experimental data

Table 1 shows the average values of the main physical properties of the porous materials (volume, surface area, mean diameter, density and porosity), and variables from the cooling pads.

The diameter of the porous material was found to be (1.43 ± 0.23) cm, a result inferior to that described by [21], who found an average diameter of 2.7 cm for expanded clay. When evaluating different materials in wetted porous plates [22] found the best cooling efficiency with expanded clay

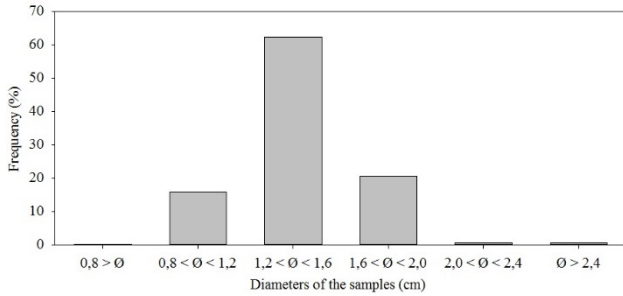


Figure 4. Values of relative frequencies for the diameters ( $\varnothing$ , cm) of the samples.  
Source: The authors.

average diameter of 2.4 cm. In Fig. 4, it is observed the values of the histogram for the diameter of the sampled expanded clay pebbles, with the largest occurrence lying between the diameters of 1.2 and 1.6 cm.

The density of expanded clay characterized in this study showed the average calculated value of  $0.36 \pm 0.03 \text{ g cm}^{-3}$ , which was lower than that found by [23], of  $0.45 \text{ g cm}^{-3}$ . In addition, the found value for porosity of  $(68 \pm 0.7) \%$ , did not coincide with the value of 50% found by [23].

To the extent that the thickness of the porous material increases, resistance to airflow usually increases and therefore the air contact time with the moist porous material increases. If, for a given thickness, porosity and capillary action of the porous material is increased, the water distribution will be more uniform; however, a larger volume of water is necessary, thereby increasing the resistance to the ventilation of the air [24].

The measured water flow rates of  $(0.05 \pm 0.03) \text{ L s}^{-1} \text{ m}^{-1}$  was much lower value than that described by [21],  $0.14 \text{ L s}^{-1} \text{ m}^{-1}$  adopted for cellulose plates 10 and 15 cm thick. According to [21], the flow of water passing through the plate should be high enough to clean the dirt and mineral salts, without allowing their accumulation. Relatively lower flow value could cause clogging of pipes and holes due to algae growth as observed in their system. These algae can also grow within the porous material, thereby increasing resistance to airflow and decreasing the cooling efficiency.

The average air speed of  $(0.9 \pm 0.31) \text{ ms}^{-1}$  was similar to that found by [22], which varied between 0.74 to  $1.09 \text{ ms}^{-1}$  for expanded clay plates with 120 mm thick. According to [22], the evaporative cooling efficiency is greater for any air velocity between 0.44 and  $1.28 \text{ ms}^{-1}$ .

The mean airflow rate calculated by the product of average speed and area of the porous plate was  $2.04 \text{ m}^3 \text{ s}^{-1}$ , which was higher than that found by [23] which ranged between 0.85 and  $1.25 \text{ m}^3 \text{ s}^{-1}$ .

### 3.2. Heat transfer coefficient and evaporative cooling efficiency

The heat transfer coefficient by convection ( $h$ ) is corrected ( $h'$ ) in Eq. 13 as a function of a set factor ( $F_1$ ) which is the difference between the simulated and observed values of  $h$  as a function of the air temperature as shown in Eq. (14),  $r^2 = 0.8005$ .

This correction was required because the original equation used to calculate the convective heat transfer coefficient was

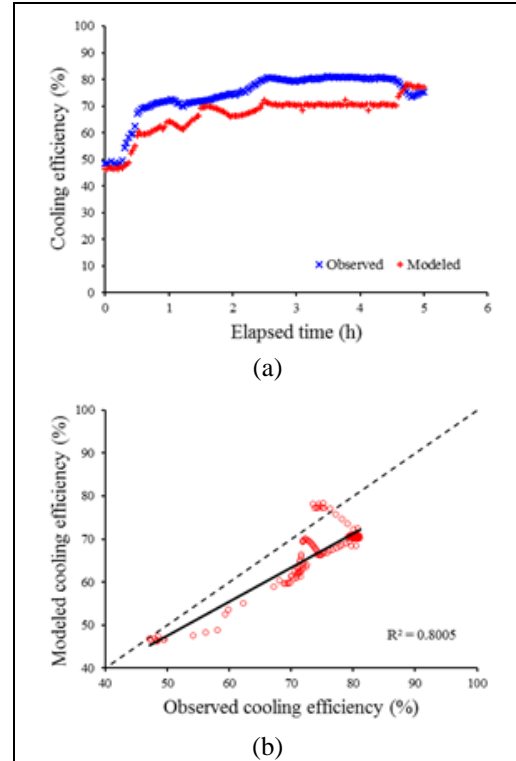


Figure 5. Simulated and observed cooling efficiencies ( $\eta$ , %) over time (a) and (b) plotted against one another as compared to a 45° slope line.  
Source: The authors.

set to porous plates with spherical materials and expanded clay has an irregular shape approaching spherical, and has a roughened, porous surface.

$$h' = F_1 + h \tag{13}$$

$$F_1 = -2627.14 + 171.05 \cdot T_{db,i} - 2.75 \cdot T_{db,i}^2 \tag{14}$$

To determine the independent variable that most influenced the  $F_1$  values, we proceeded to the regression analysis based on the maximum coefficient of determination ( $r^2$ ) using the PROC REG of SAS® [24].

After applying the correction factor in heat and mass transfer coefficient, cooling efficiency results improved, whose mean values, observed and simulated, were  $74.8 \pm 7.4\%$  and  $68.3 \pm 8.3\%$ , respectively. Fig. 5 shows the behavior of the observed efficiency as a function of time, and it is further observed that in general the simulated values underestimated the real efficiency.

In Fig. 5a, it is observed graphically the behavior of the average of air temperature before crossing the plate and cooling efficiency observed and simulated throughout the day. Little variation was observed in the efficiencies values, more variation occurring at the start of data collection, during which the evaporative cooling system is on and off frequently, staying on for approximately 1-3 minutes, not therefore reaching state balance (Fig. 5b). In turn, the next 16 hours, the system was kept engaged for longer periods, 30 to 120 minutes, providing better equilibrium conditions.

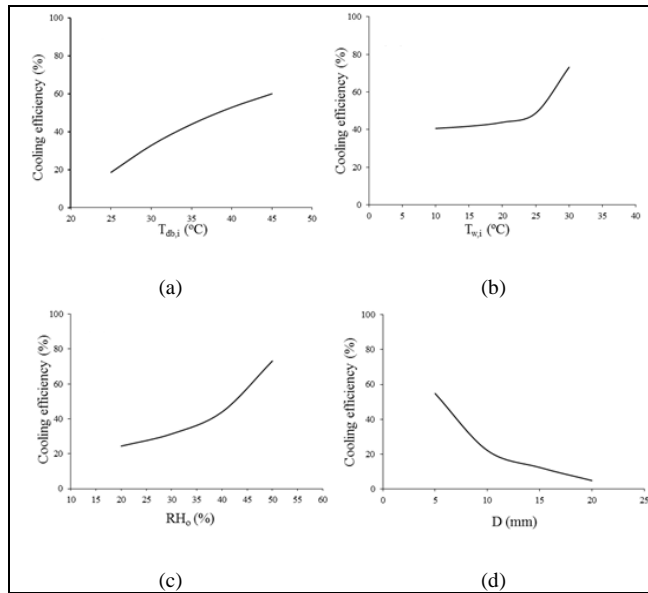


Figure 6. Sensitivity of cooling efficiency ( $\eta$ , °C) to inlet dry bulb temperature ( $T_{db,i}$ , °C, A), inlet water temperature ( $T_{w,i}$ , °C, B), inlet air relative humidity ( $RH_i$ , %, C) and expanded clay average diameter ( $D$ , mm). Source: The authors.

### 3.3. Model sensitivity

Simulations were performed for prediction of the behavior of  $T_{db,o}$ ,  $RH_o$  and  $\eta$  in function of air temperature before crossing the pad ( $T_{db,i}$  of 25 °C to 45°C), as can be seen in Fig. 6. The dimensions of the evaporative cooling plate were considered to be 11.70 m x 2.00 m x 0.075 m, diameter of the material used to fill the evaporative cooling plate ( $D$ ) of 10 mm, external relative humidity ( $RH_e$ ) 45%, atmospheric pressure ( $P_{atm}$ ) 101.32 kPa, mean air velocity inside the shed ( $V$ ) 1.2 m s<sup>-1</sup>, mass flow of air across the pad ( $m_a$ ) 41 kg s<sup>-1</sup>, water temperature applied to the porous plate ( $T_{water}$ ) of 20 °C and the relationship between surface area and volume of the porous material ( $\alpha$ ) of 170 m<sup>2</sup> m<sup>-3</sup>.

From Fig. 6 the capacity for reducing temperature and variation of  $RH_o$  can be seen as  $T_{db,i}$  increases causing the increase in  $\eta$ . Later, adopting  $T_{db,i}$  equal to 35 °C,  $D = 5, 10, 15$  and 20 mm, corresponding to values of 157.08 m<sup>2</sup> m<sup>-3</sup>, 78.54 m<sup>2</sup> m<sup>-3</sup>, 52.36 m<sup>2</sup> m<sup>-3</sup> and 23.56 m<sup>2</sup> m<sup>-3</sup> respectively, and assuming the values of the other variables described above, the behavior of  $T_{db,o}$ ,  $RH_o$  and  $\eta$  were simulated.

As it can be seen in Fig. 6, as the  $D$  increases it reduces the cooling capacity of the air  $RH_o$  and  $\eta$  (Fig. 6c and 6d). The calculated evaporative cooling efficiency was 54%. This value is in accordance to [25], who found  $\eta$  values of from 43% to 55% for plates with 5 cm thick and velocity ranging from 1.0 to 1.3 m s<sup>-1</sup>.

### 3.4. Prediction of evaporative cooling efficiency for future scenarios

It can be observed in Fig. 7, the behavior of the average air temperature ( $T_{db,i}$ ) and ( $T_{db,o}$ ), and the evaporative cooling system efficiency ( $\eta$ ) according to average temperature of the period 1961-1990 and the scenarios B2 and A2 for the years of 2050 and 2100.

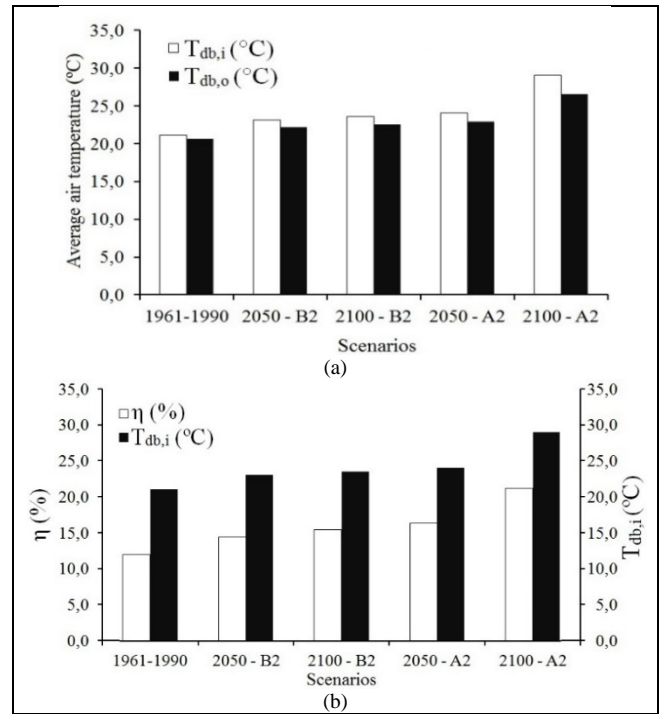


Figure 7. Behavior of average air temperature before ( $T_{db,i}$ ) and after ( $T_{db,o}$ ) crossing the wetted porous plate (a) and evaporative cooling efficiency ( $\eta$ ) due to the variation of the air temperature ( $T_{db,i}$ ) before crossing the wetted porous plate (b) according to the estimated average air temperature for the period of 1961-1990 and according to the B2 and A2 scenarios (IPCC, 2013), for the years 2050 and 2100. Source: The authors.

The simulation results for ( $T_{db,i}$ ) and ( $T_{db,o}$ ) are shown in Fig. 7a, which indicates the gradual increase of  $T_{db,o}$  in time into the greenhouse. The simulations indicate the need of dimensioning the evaporative cooling systems in order to adequate the internal environment of the greenhouse to the plants needs. The simulation results present general tendencies that might be important in the definition of strategies for ventilation projects.

Evaluating predictions of climate changes, it could be observed negative impacts in the agriculture production (Fig. 7b) [26-28]. If no precaution is taken, there might occur the migration of plant production to regions in order to achieve better thermal environment [29]. It can be harmful to the Brazilian economy, once Brazil is one of the countries most susceptible to the impacts of climate changes [30].

## 4. Conclusions

1. The mathematical model developed is suitable to simulate the PAD cooling systems, allowing the simulation of different system configurations, and may thus be used as a tool in the decision making process during the phase of design and dimensioning of evaporative cooling systems of the wetted porous plate type built with expanded clay;
2. With the variation of the diameter of the expanded clay filler used in the evaporative cooling plate, it was detected reduction of the capacity and efficiency of air cooling; and
3. The increase in the air temperature predicted in future

scenarios can affect negatively the plant production in greenhouses from Minas Gerais state, especially during the warmest period in the year.

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