



HAL
open science

Two-Stage Alkaline-Enzymatic Pretreatments To Enhance Biohydrogen Production from Sunflower Stalks

Florian Monlau, Eric Trably, Abdellatif Barakat, Jérôme Hamelin, Jean-Philippe Steyer, Hélène Carrère

► **To cite this version:**

Florian Monlau, Eric Trably, Abdellatif Barakat, Jérôme Hamelin, Jean-Philippe Steyer, et al.. Two-Stage Alkaline-Enzymatic Pretreatments To Enhance Biohydrogen Production from Sunflower Stalks. *Environmental Science and Technology*, 2013, 47 (21), pp.12591 - 12599. <10.1021/es402863v>. <hal-02647473>

HAL Id: hal-02647473

<https://hal.inrae.fr/hal-02647473v1>

Submitted on 8 Aug 2023

HAL is a multi-disciplinary open access archive for the deposit and dissemination of scientific research documents, whether they are published or not. The documents may come from teaching and research institutions in France or abroad, or from public or private research centers.

L'archive ouverte pluridisciplinaire **HAL**, est destinée au dépôt et à la diffusion de documents scientifiques de niveau recherche, publiés ou non, émanant des établissements d'enseignement et de recherche français ou étrangers, des laboratoires publics ou privés.



HAL Authorization

Two-stage alkaline-enzymatic pretreatments to enhance biohydrogen production from sunflower stalks

Florian Monlau, Eric Trably*, Abdellatif Barakat¹, Jérôme Hamelin, Jean-Philippe Steyer, H  l  ne Carrere

INRA, UR0050, Laboratoire de Biotechnologie de l'Environnement, Avenue des Etangs, 11100 Narbonne, France

*eric.trably@supagro.inra.fr

¹ present address : INRA, UMR IATE 1208 Ing  nierie des Agropolym  res et Technologies Emergentes, 2, place Pierre Viala F- 34060 Montpellier, France,

Due to their rich composition in carbohydrates, lignocellulosic residues represent an interesting source of biomass to produce biohydrogen by dark fermentation. Nevertheless, pretreatments should be applied to enhance the solubilization of holocelluloses and increase their further conversion into biohydrogen. The aim of this study was to investigate the effect of thermo-alkaline pretreatment alone and combined with enzymatic hydrolysis to enhance biohydrogen production from sunflower stalks. Low increase of hydrogen potentials from 2.3 ± 0.9 mL $H_2 \cdot g^{-1}$ VS to 4.4 ± 2.6 mL $H_2 \cdot g^{-1}$ and 20.6 ± 5.6 mL $H_2 \cdot g^{-1}$ VS were observed with raw sunflower stalks and after thermo-alkaline pretreatment at 55  C, 24h, 4% NaOH and 170  C, 1 h, 4% NaOH, respectively. Enzymatic pretreatment alone showed an enhancement of the biohydrogen yields to 30.4 ml $H_2 g^{-1}$ initial VS whereas it led to 49 mL $H_2 g^{-1}$ initial VS and 59.5 mL $H_2 g^{-1}$ initial VS when combined with alkaline pretreatment at 55  C and 170  C, respectively. Interestingly, a diauxic effect was observed with sequential consumption of sugars by the mixed cultures during dark fermentation. Glucose was first consumed and, once glucose was completely exhausted, xylose was utilized by the microorganisms, mainly related to *Clostridium* species.

Graphical abstract

37 **Introduction:**

38 Development of renewable energy such as hydrogen has recently taken a considerable place in the scientific community due to oil crisis
39 and the wish of mitigating global warming by reducing greenhouse gas emission. Biohydrogen production by dark fermentation of
40 lignocellulosic substrates appears to be one of the most promising ways, especially when using agricultural residues since they are cheap,
41 abundant and provide new incomes to farmers through a profitable reuse of the residues.^{1,2} Among them, sunflower stalks are present in
42 large quantities and represent renewable and low-cost raw materials for the production of biofuels such as biohydrogen.³ In particular,
43 holocelluloses (hemicelluloses and cellulose) which are polymers of pentose and hexose simple sugars can be efficiently converted into
44 biohydrogen by dark fermentation.⁴ Fermentative biohydrogen can be produced by either pure or mixed bacterial cultures. Even though
45 pure cultures exhibit higher hydrogen yields, the high costs for maintaining these pure cultures restrict the development of industrial
46 applications. Mixed cultures such as anaerobic sludge are easier to be used since they do not require sterile conditions, present a high
47 metabolic flexibility and can therefore transform a wide range of feedstock.⁵ However, direct conversion of lignocellulosic substrates into
48 hydrogen is recalcitrant due to the intrinsic structure of the organic materials, and so far, only very low hydrogen yields of 1, 3 and 9 ml
49 H₂ g⁻¹VS have been reported for wheat straws, cornstalks and corn straws, respectively.¹ The main bottleneck of using lignocellulosic
50 biomass by dark fermentation is to convert holocelluloses into readily fermentable products as previously reported.^{2,6} Recent studies^{1,6}
51 suggested that hydrogen yields correlate strongly with the content in easily accessible sugars of the organic substrates. Hydrolysis of
52 cellulosic biomass is thus required since most of the hydrogen-producing bacteria find soluble substrates much easier to degrade.⁷
53 Among hydrolysis technologies that convert holocelluloses into soluble sugars, two conventional methods using mineral acids or
54 enzymes are commonly used. Enzymatic hydrolysis is considered as an efficient, energy saving and environment-friendly process.
55 Recently, hydrogen yields from poplar leaves were increased from 15.04 to 44.92 mL H₂ g⁻¹ dry materials after pretreatment with 2%
56 Vicozyme L (mixture of arabinase, cellulase, β-glucanase, hemicellulase and xylanase).⁸ However, the accessibility of holocelluloses to
57 the enzymes for further conversion into fermentable sugars is limited by the lignin content and the cellulose crystallinity.^{8,9,10}
58 Consequently, additional pretreatments need to be applied prior to the enzymatic attack to reduce this strong physical barrier and enhance
59 holocellulose hydrolysis.¹¹ Alkaline pretreatments are known to remove efficiently lignin and lignin-hemicellulose complex, and thus can
60 increase enzymatic hydrolysis of holocelluloses.^{9,10} Combining alkaline pretreatment with enzymatic hydrolysis appears to be a
61 promising approach to enhance hydrogen production from lignocellulosic residues. So far, alkaline pretreatment followed by enzymatic
62 hydrolysis has been widely investigated for bioethanol production^{3,12} and, to our knowledge, only one study investigated alkaline
63 pretreatment combined with enzymatic hydrolysis for biohydrogen production of lignocellulosic residues and using anaerobic mixed
64 cultures.¹³ In this study, alkaline pretreatment (4 % NaOH (w/v) at 100°C for 2h) was combined with enzymatic hydrolysis (cellulases
65 from *Trichoderma Reesei* at 20 U g⁻¹) to enhance biohydrogen production from bagasse.¹³ A hydrogen yield of 300 mL H₂ g⁻¹ VS
66 (Volatile Solids) was observed compared to 31 mL H₂ g⁻¹ VS with only enzymatic hydrolysis. Nevertheless, the use of hemicellulases
67 was not considered in their study although fermentative biohydrogen can be produced from both hemicelluloses and cellulose.
68 The objectives of our study were: (1) to investigate the effect of thermo-alkaline pretreatment (55°C, 24h, 4% NaOH or 170°C, 1h, 4%

69 NaOH) or two-stage thermo-alkaline and enzymatic pretreatments on biohydrogen production, (2) to monitor the dynamics of the
70 bacterial communities supporting the fermentation process of the sugars released from enzymatic hydrolysis.

71

72 **Experimental**

73 **Feedstocks:**

74 “Serin” sunflower stalks were dried at 37°C for 48 h and milled to a particle size of 2-3 mm using a SM-100 cutting mill. Total Solids
75 (TS) and Volatile Solids (VS) were analysed according to the APHA standard methods.¹⁴ All measurements were carried out in
76 duplicates.

77 **Thermo-alkaline and enzymatic pretreatments**

78 Thermo-alkaline pretreatments were performed on sunflower stalks at an initial solid organic load of 35 g_{TS} L⁻¹. At 55°C, pretreatment
79 was performed in 500 mL flasks with 4% NaOH (g/100g_{TS}) for 24 hours, in a “Edmund Butler” heating shaker series SM-30-control with
80 an agitation speed of 150 rpm. Pretreatment was performed at 170°C in a 1 L Zipperclave autoclave series 02-0378-1 (Autoclave France)
81 with 4% NaOH for 1 hour under an agitation speed of 150 rpm. After pretreatment, the liquors were separated from the solid fraction by
82 filtration through a 0.25 mm sieve. Biological Hydrogen Potentials (BHP) batch tests were carried out on total, liquid and solid fractions
83 of the residual solids after alkaline pretreatment (Fig. 1). The remaining liquors were kept at 4°C for further chemical analysis and the
84 solid fractions were washed several times with distilled water to remove water soluble compounds, and then dried at 40°C for 24 h. This
85 washing step allowed removing phenolic compounds which are known to inhibit or deactivate enzymes.¹⁵ Solid fractions were kept at
86 4°C for further chemical analysis and enzymatic hydrolysis. Concerning enzymatic hydrolysis, untreated and dried alkaline-pretreated
87 solid fractions of sunflower stalks were autoclaved during 20 min at 121°C. This sterilization step was required to avoid consumption of
88 the sugars released during enzymatic hydrolysis by indigenous microorganisms present naturally in lignocellulosic substrates.¹⁶
89 Enzymatic hydrolysis of the untreated and alkaline-pretreated solid fractions was performed at a solid organic load of 50 g remaining TS
90 L⁻¹ in flasks incubated at 35°C in an “Edmund Butler” heating shaker series SM-30-control under 150 rpm agitation. The pH was
91 buffered at 5 using 50 mM of 2-(N-morpholino) ethanesulfonic acid (MES) buffer. Cellulase from *Trichoderma reesei* (Sigma-Aldrich),
92 β-glucosidase from *Aspergillus niger* (Sigma-Aldrich) and xylanase from *Thermomyces lanuginosus* (Sigma-Aldrich) were added at a
93 concentration of 50 U g⁻¹ TS, 25 U g⁻¹ TS and 50 U g⁻¹ TS, respectively. After enzymatic hydrolysis, BHP tests were performed on the
94 total fraction (residual solids + liquor rich in xylose and glucose).

95 **Biochemical analysis:**

96 All samples were milled using a cutting miller Ika Werke MF 10 basic, and a 1 mm mesh. Total Kjeldahl Nitrogen (TKN) was titrated
97 using Buchi 370-K after mineralization of the samples. Proteins were determined by multiplying TKN by 6.25. The carbohydrate
98 composition of the untreated and solid fractions of pretreated sunflower stalks were measured using strong acid hydrolysis adapted from
99 Effland (1977).¹⁷ Samples (200 mg) were hydrolyzed with 12 M H₂SO₄ for 2h at room temperature. They were then diluted to reach an

100 acid concentration of 1.5 M and kept at 100°C for 3 h. The insoluble residues were separated from the supernatant by filtration with a
101 GFA-WHATMAN glass fiber filter. The insoluble residues were washed with 100 mL of deionised water and then placed in a crucible.
102 The crucible and the glass fiber filters were dried at 100°C during 24 h and then placed at 550°C during 2 h to determine the Klason
103 lignin content. The supernatant was filtrated with nylon filters (0.2 µm) and analyzed for quantification of sugars by High-Pressure
104 Liquid Chromatography (HPLC).

105 HPLC analysis was used to quantify monosaccharides (glucose, xylose, arabinose, glucuronic and galacturonic acids). The analysis was
106 performed with a combined Water/Dionex system, using a Biorad HPX-87H column at 50°C and a refractive index detector. The eluent
107 corresponded to a 0.005 M H₂SO₄ solution continuously pumped under a flow-rate of 0.3mL.min⁻¹. The system was calibrated with
108 glucose, xylose, arabinose, glucuronic and galacturonic acids standards (Sigma–Aldrich).

109 Cellulose and hemicellulose contents were estimated on the basis of monomeric sugar contents. Cellulose is a polymer of glucose while
110 hemicelluloses consist of branched chains of monomeric sugars composed mainly of pentoses such as xylose, arabinose. Consequently,
111 the cellulose and hemicellulose contents were estimated as follows:

$$112 \text{ Cellulose (\% TS)} = \text{Glucose (\%TS)} / 1.11 \quad (1)$$

$$113 \text{ Hemicelluloses (\% TS)} = [\text{Xylose (\%TS)} + \text{Arabinose (\%TS)}] / 1.13 \quad (2),$$

114 where 1.11 is the ratio of the molecular weights of glucose to glucan (180/162) and 1.13 is the ratio of the molecular weights of xylose
115 and arabinose to xylan (150/132).

116 **Metabolites and byproducts contents**

117 Volatile Fatty Acids (VFA) composition, *i.e.* acetic (C2), propionic (C3), butyric and iso-butyric (C4 and iC4), valeric and iso-valeric (C5
118 and iC5) and caproic (C6) acids were determined in the liquid phase using a gas chromatograph (GC-3900, Varian) equipped with a
119 flame ionization detector. The concentrations of non-VFA metabolic byproducts such as lactate and ethanol and other byproducts
120 (furfural, 5-hydroxymethylfurfural) were measured by HPLC analysis and refractometric detection (Waters R410). The components
121 were separated in an Aminex HPX-87H column (Biorad) maintained at 35°C. The eluent corresponded to 0.005 M H₂SO₄ and flow-rate
122 was 0.4 mL.min⁻¹. Total phenols in the liquid fraction of alkaline pretreated samples were determined using a microtube test
123 (Spectroquant, Merck) followed by a 4-aminoantipyrine colorimetric measurement after a two-hundred dilution.

124 **Accessible surface area and porosity**

125 Nitrogen adsorption–desorption was performed on a micromeritics ASAP 2010 volumetric apparatus at 77 K. Before adsorption
126 measurements, samples (0.5–0.3 g) were outgassed at 373 K under vacuum during 72 h. Specific surface area and porosity of the samples
127 were evaluated using the BET method.¹⁸

128 **Biochemical Hydrogen Potential (BHP) tests**

129 The H₂ production experiments were carried out in batch in 600 mL glass bottles. An anaerobically digested sludge was pretreated by
130 heat shock (90°C, 15 min) and then used as inoculum. One milliliter of the inoculum (final concentration around 250 mg-COD L⁻¹) was
131 added into a culture medium (final working volume of 200 mL) containing 100 mM of 2-(N-morpholino) ethanesulfonic acid (MES)

132 buffer, 5 g VS.L⁻¹ of untreated or pretreated sunflower stalks. The initial pH was adjusted to 5.5 using HCl 1 M. In a first series of
133 experiments, BHP tests were performed on thermoalkaline pretreated samples and on the separated liquid and solid fractions to determine
134 the part of hydrogen originating from both fractions. In a second series of experiments, BHP tests were performed only on the solid
135 residues after alkaline pretreatment with or with no enzymatic hydrolysis. All BHP tests were performed in duplicates. Once prepared,
136 the flasks were bubbled with nitrogen to obtain anaerobic conditions, and closed with air impermeable red butyl rubber septum-type
137 stoppers. Bottles were then incubated at 35°C. Two milliliters of the mixed cultures were periodically collected and centrifuged (13,000
138 rpm, 10 min). The supernatants were stored at 4°C for further metabolites analysis.

139 **DNA extraction, PCR amplification and CE-SSCP fingerprinting**

140 Two milliliters of the cultures were collected after 40 h and 92 h of incubation from all batch experiments. Microbial cells were then
141 centrifuged at 12,100 g for 15 min. Genomic DNA was extracted and purified using the Wizard Genomic DNA Purification kit
142 (Promega). DNA purity and quantity in the extracts were measured by spectrophotometry (Infinite NanoQuant M200, Tecan). 16S rRNA
143 genes were amplified for further fingerprinting analysis using Capillary Electrophoresis Single Strand Conformation Polymorphism (CE-
144 SSCP) as described elsewhere.¹⁹ Fingerprint normalization and comparison were performed using the StatFingerprint library²⁰ of the R
145 software version 2.10.1.²¹

146 **Identification of microbial communities by pyrosequencing**

147 Comparison of fingerprints led to the selection of one genomic DNA representative for each experimental condition. Identification of the
148 main dominant bacterial populations was performed by pyrosequencing of the V4-V5 regions of the 16S rRNA gene (Molecular
149 Research Laboratory, TX, USA). An average of 5161 sequences per sample was obtained, and sequence data derived from the
150 sequencing process was processed using a proprietary analysis pipeline (Molecular Research Laboratory, TX, USA). Sequences were
151 first clustered at 3% of divergence and then taxonomically classified using BLASTn against a curated GreenGenes database.

152

153 **Results and discussion:**

154 **Effect of thermo-alkaline and two-stage alkaline-enzymatic pretreatments on biochemical and structural features**

155 To investigate the biochemical changes induced by the thermo-alkaline pretreatment, variations in proteins, uronic acids, hemicelluloses,
156 cellulose and Klason lignin contents were estimated (Figure 1). Uronic acids which are constituents of hemicelluloses and pectins were
157 removed at 64% after alkali treatment at 55°C, and were totally removed at 170°C, as a consequence of the cleavage of the lignin-
158 hemicellulose linkages through uronic acids, so-called lignin-carbohydrate complexes (LCC). LCC remain the main obstacle for the
159 utilization of lignocellulosic biomass.⁴ Their cleavage makes holocelluloses more accessible for enzymatic hydrolysis and microbial
160 fermentation. Thermo-alkaline pretreatment at 170°C was found efficient to solubilize proteins since 54% were removed. Significant
161 hemicelluloses removals of 26% and 58% were observed after thermo-alkaline pretreatment at 55°C and 170°C, respectively. In contrast,

162 it was shown less than 8% of cellulose removal after thermo-alkaline pretreatment at both 55°C and 170°C. Finally, high lignin removals
163 of 22% and 36% were observed after thermo-alkaline pretreatment at 55°C and 170°C, respectively. Such results are in accordance with
164 previous studies reporting that alkaline pretreatment is efficient to delignify and remove partly lignin and hemicelluloses whereas
165 cellulose is preserved.^{9,10} As a result of such concomitant and similar removal of lignin and holocelluloses, no significant variation of the
166 lignin content ranging from 32.2 to 33.5 g/100g remaining VS was observed between alkaline pretreated solids and untreated sunflower
167 stalks. In contrast, a relative increase of 24% and 60.5% of the cellulose content compared to raw sunflower stalks was observed after
168 alkaline pretreatment at 55°C and 170°C, respectively. This result shows that cellulose was less removed compared to the other
169 compounds during thermo-alkaline pretreatments.

170 Table 1 shows the structural features such as accessible surface area (SA) and pore volume (Vp) of the untreated and alkaline-pretreated
171 solid fractions of the sunflower stalks. Low increase of SA and Vp was observed after thermo-alkaline pretreatment at 55°C. SA
172 increased from 1.55 m² g⁻¹ TS (sunflower stalks) to 1.59 m² g⁻¹ TS and Vp increased from 0.083 cm³ g⁻¹ TS (sunflower stalks) to 0.106
173 cm³ g⁻¹ TS. Thermo-alkaline pretreatment at 170°C was found more efficient in increasing SA and Vp with final values of 2.55 m² g⁻¹ TS
174 and 0.235 cm³ g⁻¹ TS, respectively. Similarly, Gharpuray et al. (1983) observed an increase of the accessible surface area from 0.64 to 1.7
175 m² g⁻¹ TS by pretreating wheat straw at 100°C with 10% NaOH (w/w) during 30 min.²²

176 In addition, enzymatic hydrolysis of the raw sunflower stalks and the residual solids obtained after alkaline pretreatment was further
177 investigated by estimating the solubilization of cellulose and hemicelluloses to glucose and xylose which are the two main monomeric
178 sugars found in holocelluloses (Figure 1). A low enzymatic hydrolysis of hemicelluloses (12%) and cellulose (35%) was observed on raw
179 sunflower stalks. After thermo-alkaline pretreatments, the enzymatic hydrolysis yields increased for both cellulose and hemicelluloses.
180 Indeed, after alkaline pretreatment at 55°C and enzymatic hydrolysis, an increase of 45% cellulose and 56% hemicelluloses
181 solubilization was observed. After alkaline pretreatment at 170°C and enzymatic hydrolysis, a higher increase of 51% and 82% was
182 observed for cellulose and hemicelluloses, respectively. Similar results were previously reported by combining alkaline-enzymatic
183 pretreatment on spruce and where enzymatic hydrolysis of both cellulose and hemicelluloses was substantially enhanced.²³ Several
184 factors may explain the increase of enzymatic hydrolysis after thermo-alkaline pretreatment. First, the increase of accessible surface area
185 and pore volume, as previously observed after thermo-alkaline pretreatment, can enhance the efficiency of enzymatic hydrolysis.
186 Consistently, good correlations between pore volume, accessible surface area and enzymatic digestibility of lignocellulosic residues were
187 previously reported.²⁴ Gharpuray et al. (1983) showed that the specific surface area can impact biomass digestibility: an increase of the
188 accessible surface area resulted in higher hydrolysis yields.²² However, the low increase of both accessible surface area and pore volumes
189 between raw sunflower stalks and sunflower stalks alkaline-pretreated at 55°C suggested that probably other factors were favorable for
190 enzymatic hydrolysis. Among them, removal of pectins (polymers of uronic acids) after thermo-alkaline pretreatment might explain the
191 increase of enzymatic hydrolysis efficiency. As described elsewhere, removal of pectins in hemp was shown to increase enzymatic
192 hydrolysis by 26%.²⁵ Even though thermo-alkaline pretreatment did not change the lignin content in the solid residues, a physical
193 redistribution of the lignin probably occurred with a cleavage of the LCC, that play a key role for enzyme accessibility and further
194 biomass digestibility.

196 Biohydrogen performances

197 Effect of thermo-alkaline and two-stage alkaline-enzymatic pretreatments on biohydrogen yields

198 Gas product analysis of Biological Hydrogen Potential (BHP) tests showed that only H₂ and CO₂ were produced during dark
199 fermentation, with no detectable CH₄ in the biogas. This suggests that heat shock treatment (90°C, 15 min) of the inoculum was efficient
200 to suppress methanogens from anaerobic sludge. A low hydrogen yield of 2.3 ± 0.9 mL H₂.g⁻¹ VS was observed for the raw sunflower
201 stalks (Table 1). A small increase in hydrogen yields to 4.4 ± 2.6 mL H₂.g⁻¹ VS and 20.6 ± 5.6 mL H₂.g⁻¹ VS were observed after thermo-
202 alkaline pretreatments at 55°C and 170°C, respectively. Similar results were obtained by pretreating grass with 0.5% NaOH (w/v) boiled
203 for 30 min with an increase of the hydrogen yield from 4.4 mL H₂.g⁻¹ dry grass for the untreated sample to 19.3 mL H₂.g⁻¹ dry grass after
204 treatment.¹¹ Alkaline pretreatment (0.4% NaOH, 24 h, room temperature) of sweet sorghum stalks led also to an increase of hydrogen
205 potentials (127 mL H₂.g⁻¹ VS compared to 52 mL H₂.g⁻¹ VS for untreated).²⁶ The enhancement of hydrogen yields coincided with an
206 increase in soluble sugars after alkali pretreatment compared to raw sweet sorghum stalks with a sugar concentration of 2.23 and 0.86
207 g.L⁻¹, respectively.²⁶

208 Biohydrogen potentials of separated liquid and solid fractions obtained after thermo-alkaline pretreatment at 55°C and 170°C were
209 further investigated to determine from which fraction the biohydrogen was produced (Table 1). At 55°C, biohydrogen production from
210 the liquid and solid fractions was similar with 2.6 and 2 mL H₂.g⁻¹ VS, respectively. In contrast, at 170°C, biohydrogen yield of the liquid
211 fraction was twice higher than solid fraction with 11.4 and 5.1 mL H₂.g⁻¹ VS, respectively. To analyze the performances of biohydrogen
212 production on these different fractions, biohydrogen yields were expressed in terms of initial sugar contents (glucose, xylose and
213 arabinose) according to the amount of holocelluloses present in the different fractions (total, solid and liquid) as shown in Table 1.
214 Concerning the liquid fractions, hydrogen yields of 0.344 and 0.865 mol H₂.mol⁻¹ hexose were obtained after 55°C and 170°C
215 pretreatments, respectively. Nevertheless, the hydrogen yields from the liquid phase remained lower than the values commonly reported
216 in the literature with simple sugars and mixed cultures, *i.e.* 2 mol H₂.mol⁻¹ glucose and 1.92–2.25 mol H₂.mol⁻¹ xylose.^{19, 27} Two
217 hypotheses can be formulated to explain these results. The first one is that soluble sugars released in the liquid phase are present in the
218 form of oligomeric and monomeric sugars. Recently, Quéméneur et al. (2011) showed the impact of the low carbohydrate structure
219 where di- and tri-saccharides affected significantly hydrogen production, and longer chains of oligomers lowered the hydrogen yields.²⁸
220 The second hypothesis is the generation of byproducts during thermo-alkaline pretreatments such as furfural, 5-HMF and phenol
221 compounds. Even though no byproducts of sugar degradation (furfural and 5-HMF) were detected in the liquid phase after thermo-
222 alkaline pretreatments, phenols coming from lignin degradation accumulated in the liquid phase at a low concentration of 25.7 mg L⁻¹
223 and 42.7 mg L⁻¹ at 55°C and 170°C, respectively (data not shown), and phenolic compounds were previously shown to negatively impact
224 biohydrogen production from xylose using mixed cultures^{15,19,29}.

225 Concerning the solid fractions, low hydrogen yields of 0.043 and 0.081 mol H₂.mol⁻¹ hexose were obtained, respectively, with raw
226 sunflower stalks and after alkaline pretreatment at 55°C. The increase of the hydrogen yields to 0.380 mol H₂.mol⁻¹ hexose after thermo-

227 alkaline pretreatment at 170°C on the solid fraction was likely due to the increase of the accessible surface area as shown in Table 1.
228 However, these hydrogen yields remained low likely because of the nature of the sugars present in the solid fractions which are in their
229 polymeric and not monomeric form. Since low hydrogen potentials were obtained whatever the solids, enzymatic hydrolysis was
230 performed on raw sunflower stalks as well as on the solid fractions after alkaline pretreatment of the straws at 55°C and 170°C to
231 enhance the solubilization of holocelluloses into monomeric sugars.

232

233 After enzymatic pretreatment of raw sunflower stalks, a maximal cumulative hydrogen production of 30.4 (\pm 3.8) mL H₂.g⁻¹ VS was
234 reached which was 13-fold higher than untreated sunflower stalks. Coupling alkaline-pretreatment with enzymatic hydrolysis led to a
235 significant increase of the hydrogen yields compared to enzymatic hydrolysis alone with 59.9 (\pm 2.6) mL H₂.g⁻¹ VS and 80.9 (\pm 3.0) mL
236 H₂.g⁻¹ VS at 55°C and 170°C, respectively. Such increase of hydrogen production was concomitant to the increase of enzymatic
237 hydrolysis through the release of soluble monomer sugars (ie glucose and xylose). Hydrogen yields of 0.562, 0.959 and 1.158 mol H₂.mol⁻¹
238 ¹ hexose were obtained after enzymatic hydrolysis ¹ of raw sunflower stalks and alkaline pretreated sunflower stalks at 55°C and 170°C,
239 respectively. Although a substantial increase was observed, these results remained lower than the average values of 2 mol H₂.mol⁻¹
240 glucose and 1.92–2.25 mol H₂.mol⁻¹ xylose commonly reported in the literature when using mixed cultures.^{19,27} These results suggest that
241 a part of holocelluloses was still not degraded during the dark fermentation process. Interestingly, if hydrogen potentials were expressed
242 by considering only the initial content in soluble sugars monomers (ie xylose and glucose) released after enzymatic pretreatment,
243 hydrogen yields ranged from 1.97 to 2.14 mol H₂.mol⁻¹ soluble sugars, in strict accordance with data previously published. Thus,
244 hydrogen was mainly produced from soluble sugar monomers released during enzymatic hydrolysis which is also in accordance with the
245 literature.^{6,26}

246 Furthermore, once the maximum cumulative hydrogen production was reached, microbial metabolites were also analyzed. The
247 fermentation metabolites produced with or without enzymatic hydrolysis of sunflower stalks and for the three conditions (raw, solid
248 residue from alkaline treatment at 55°C and 170°C) were only acetate and butyrate (data not shown). This suggests that H₂ was produced
249 only by the well described metabolic fermentative H₂-producing pathways of acetate and butyrate. Butyrate as well as acetate production
250 are indeed typical of a dark fermentation process when using substrates rich in carbohydrates.³⁰

251 **General remarks on biohydrogen potentials**

252 To assess the advantage of combining thermo-alkaline pretreatment with enzymatic hydrolysis, results were expressed according to the
253 initial VS, as shown in Figure 2. In the case of thermo-alkaline pretreated stalks, the hydrogen produced from the liquid fraction after
254 thermo alkaline pretreatment and the hydrogen produced from the solids alkaline-pretreated at 55°C and 170°C and with or without
255 enzymatic hydrolysis were considered separately. Moreover, a theoretical hydrogen potential (100 L H₂.kg⁻¹ initial VS) was calculated by
256 considering the content of holocelluloses in sunflower stalks and a hydrogen production of 2 mol H₂.mol⁻¹ eq glucose as commonly
257 observed with mixed cultures.¹⁶

258 As mentioned previously, a hydrogen yield of 30.4 mL H₂.g⁻¹ initial VS was obtained after enzymatic pretreatment of sunflower stalks,

259 which was 13-fold higher than raw sunflower stalks ($2.3 \pm 0.9 \text{ mL H}_2\text{.g}^{-1}$ initial VS). When considering combined thermo-alkaline
260 pretreatment at 55°C and 170°C with enzymatic hydrolysis, hydrogen potentials were respectively 21 to 26-fold higher than with untreated
261 stalks. In both cases, the main part of hydrogen was coming from the enzymatic-alkaline-pretreated solid fraction which corresponded
262 respectively to 81% and 95% of total biohydrogen production. When considering the initial VS content, coupling thermo-alkaline
263 pretreatment at 170°C with enzymatic hydrolysis was not substantially beneficial compared to 55°C since hydrogen yields increased only
264 from 49 to 59.5 mL H₂.g⁻¹ initial VS. Overall, hydrogen yields obtained after enzymatic hydrolysis with or without coupling with thermo-
265 alkaline pretreatments remained always lower than the highest hydrogen yields that can be expected if holocelluloses would have been
266 fully converted to H₂ during the dark fermentation process. In addition, and to make the process economically viable, the effluents of the
267 H₂ fermentation process should also be considered for further valorisation as either hydrogen by photo-fermentation or methane by
268 anaerobic digestion.^{4,31}

269

270 **Bacterial community analysis**

271 By investigating the metabolic routes of the dark fermentation process, a diauxic behavior of the mixed culture was observed on the
272 consumption of soluble sugars (ie glucose and xylose) released after enzymatic hydrolysis. Glucose was first consumed and, once glucose
273 was completely exhausted, xylose was utilized by the microorganisms (Fig. 3). Such diauxic effect has been well described with pure
274 cultures, but to our knowledge, no study reported such effect with complex mixed cultures. Diauxic growth usually occurs when bacterial
275 cells of an individual species are exposed to multiple carbon sources leading to a catabolic repressive effect that does not permit
276 simultaneous consumption of all sugars, *i.e.* sugars are sequentially consumed resulting in two successive exponential growth phases that
277 are separated by an intermediate lag phase. Glucose is a preferred substrate for many microorganisms, and is responsible of a common
278 catabolic repression which is commonly called the “glucose effect”.³² In mixed culture, several bacterial populations with different
279 substrate affinities can use indifferently all sugars, and various microbial populations can very probably use several carbon sources
280 simultaneously.³³ Therefore, a diauxic behaviour could result from a diauxic growth but also from a shift of highly specific microbial
281 populations. To support the hypothesis of a diauxic catabolic repression effect, a bacterial analysis of the H₂-producing bacteria present in
282 mixed culture was performed at two experimental times: 40 h and 92 h, corresponding to the end of glucose and xylose consumption,
283 respectively (red arrows in Figure 3). The number of sequences analyzed per sample ranged from 3980 to 6366 and the number of
284 identified species varied between 23 and 34 according to the sample. The bacterial species with a relative abundance above 1% at 40 h and
285 92 h in the dark H₂ fermentation batch are summarized in Table 2.

286

287 For all samples, the bacterial community was dominated by members of the *Clostridium* genus with an average of 92% of the total
288 abundance. The composition of the bacterial communities in this study was similar to the ones reported in previous studies carried out in
289 dark fermentation systems.^{19,34} For instance, in granular sludge of H₂-producing bioreactor using sucrose as substrate, 69.1% of the clones
290 were affiliated to four *Clostridium* species.³² Similarly, a proportion of *Clostridium* species of 85.8% was observed during dark

291 fermentation of xylose and after heat shock pretreatment (90°C, 10 min) of the anaerobic mixed culture inoculum.¹⁹
292 During the glucose phase consumption, a specific enrichment of *Clostridium butyricum* amongst the other *Clostridium* species was
293 observed with proportions varying from 80.3 % to 92.9%. In contrast, during xylose consumption, even though *Clostridium butyricum*
294 remained the main dominant species, other *Clostridium* species clearly outcompeted. More particularly, and except for *Clostridium*
295 *bifermantans*, the relative abundance of *Clostridium butyricum* decreased between 40 h and 92 h, while the abundance of minority species
296 such as *Clostridium roseum*, *Clostridium aciditolerans*, *Clostridium saccharoperbutylacetonicum* and *Clostridium tunisiense* increased
297 after 40 h. Consequently, the diauxic effect observed on glucose/xylose consumption was not only related to a diauxic growth of
298 *Clostridium butyricum* but also to the development of highly competitive *Clostridium* species during the change of sugar degradation
299 pathway. This result suggests that the diauxic effect could be common to the whole *Clostridium* genus. Diauxic effects were previously
300 reported on ethanol production from glucose/xylose mixture using pure cultures, ie. *Saccharomyces cerevisiae* and *E. coli*^{35,36}. So far, and
301 to our knowledge, such diauxic effect has not been so clearly reported with fermentative mixed cultures. In general, diauxic effect can be
302 avoided by the use of mixed cultures instead of pure cultures since the presence of various bacterial populations enhances the possibilities
303 to convert concomitantly a large range of substrates due to microbial diversity, metabolic flexibility, and the possibility of specific
304 individual ecological niches.³⁵ In this study, the heat shock pretreatment initially applied on anaerobic sludge led not only to the complete
305 suppression of *Archaea* methanogens, but also to a strong selection of *Clostridium* species with a low final number of bacteria species
306 ranging from 23 to 34 only. This observation is in accordance with Baghchehsaraee et al. (2008) who showed that heat pretreatment (80°C
307 or 95°C) of inocula led to a substantial decrease of bacterial diversity.³⁷ Comparatively, much higher numbers of bacteria ranging from
308 114 to 164 were reported on three granular and non-granular mesophilic cultures which were not heat treated.³⁸

309

310 Acknowledgements

311 The authors are grateful to ADEME, the French Environment and Energy Management Agency, for financial support in the form of F.
312 Monlau's PhD grant.

313

314 References

- 315 (1) Guo, X. M. Biohydrogen production and metabolic pathways in dark fermentation related to the composition of organic solid
316 waste. Ph.D. Thesis, University of Montpellier 2, 2012.
- 317 (2) Cheng, C. L.; Lo, Y. C.; Lee, K. S.; Lee, D. J.; Lin, C. Y.; Chang, J. S. Biohydrogen production from lignocellulosic feedstock.
318 *Bioresource Technol.* **2011**, 102, 8514–8523.
- 319 (3) Sharma, S.K.; Kalra, K.L; Grewal, H.S. Enzymatic saccharification of pretreated sunflower stalks. *Biomass Bioenerg.* **2002**,
320 23(3), 237-243.
- 321 (4) Monlau, F.; Barakat, A.; Trably, E.; Dumas, C.; Steyer, J.-P.; Carrere, H. Lignocellulosic materials into Biohydrogen and
322 Biomethane: impact of structural features and pretreatment. *Crit. Rev. Environ. Sci. Technol.* **2013**, 43, 260-322.

- 323 (5) Li, D. M.; Chen, H. Z. Biological hydrogen production from steam-exploded straw by simultaneous saccharification and
324 fermentation. *Int. J. Hydrogen Energ.* **2007**, 32, 1742–1748.
- 325 (6) Monlau, F.; Sambusiti, C.; Barakat, A.; Guo, X. M.; Latriille, E.; Trably, E.; Steyer, J.P.; Carrere, H. Predictive models of
326 biohydrogen and biomethane production based on the compositional and structural features of lignocellulosic materials.
327 *Environ. Sci. Technol.* **2012**, 46, 12217-12225.
- 328 (7) Pan, C. M.; Ma, H. C.; Fan, Y. T.; Hou, H. W. Bioaugmented cellulosic hydrogen production from cornstalk by integrating
329 dilute acid-enzyme hydrolysis and dark fermentation. *Int. J. Hydrogen Energ.* **2011**, 36, 4852–4862.
- 330 (8) Cui, M.; Yuan, Z.; Zhi, X.; Wei, L.; Shen, J. Biohydrogen production from poplar leaves pretreated by different methods using
331 anaerobic mixed bacteria. *Int. J. Hydrogen Energ.* **2010**, 35, 4041-4047.
- 332 (9) Taherzadeh, M.J.; Karimi, K. Pretreatment of lignocellulosic wastes to improve ethanol and biogas production: A review. *Int. J.*
333 *Mol. Sci.* **2008**, 9, 1621-1651.
- 334 (10) Monlau, F.; Barakat, A.; Steyer, J. P.; Carrère, H. Comparison of seven types of thermo-chemical pretreatments on the structural
335 features and anaerobic digestion of sunflower stalks. *Bioresource Technol.* **2012**, 120, 241–247.
- 336 (11) Cui, M.J.; Shen, J.Q. Effects of acid and alkaline pretreatments on the biohydrogen production from grass by anaerobic dark
337 fermentation. *Int. J. Hydrogen Energ.* **2011**, 37, 1120-1124.
- 338 (12) Rabelo, S.C.; Carrere, H.; Maciel Filho, R.; and Costa, A.C. Production of bioethanol, methane and heat from sugarcane bagasse
339 in a biorefinery concept. *Bioresource Technol.* **2011**, 102, 7887-7895.
- 340 (13) Chairattananokorn, P.; Penthamkeerati, P.; Reungsang, A.; Lo, Y. C.; Lu, W. B.; Chang, J. S. Production of biohydrogen
341 from hydrolyzed bagasse with thermally preheated sludge. *Int. J. Hydrogen Energ.* **2009**, 34, 7612-7617.
- 342 (14) A. P. H. A. *Standard Methods for the Examination of Water and Wastewater*, 20th ed., American Public Health Association,
343 1998.
- 344 (15) Kim, Y., Ximenes, E., Mosier, N.S., Ladisch M.R. Soluble inhibitors/deactivators of cellulose enzymes from lignocellulosic
345 biomass. *Enzyme Microb Technol.* **2011**, 48, 408-415
- 346 (16) Quemeneur, M.; Bittel, M.; Trably, E.; Dumas, C.; Fourage, L.; Ravot, G.; Steyer, J. P.; Carrere, H. Effect of enzyme addition
347 on fermentative hydrogen production from wheat straw. *Int. J. Hydrogen Energ.* **2012**, 37, 10639-10647.
- 348 (17) Effland, M. J. Modified procedure to determine acid-insoluble lignin in wood and pulp. *Tappi.* **1977**, 60, 143–144.
- 349 (18) Brunauer, S.; Emmett, P.H.; Teller, E. Adsorption of gases in multimolecular layers. *J Am Chem Soc.* **1938**, 60, 309-319.
- 350 (19) Quémeneur, M.; Hamelin, J.; Barakat, A.; Steyer, J.P.; Carrere, E.; Trably, E. Inhibition of fermentative hydrogen production by
351 lignocellulose-derived compounds in mixed cultures. *Int. J. Hydrogen Energ.* **2012**, 37, 3150-3159.
- 352 (20) Michelland, R.J.; Dejean, S.; Combes, S.; Fortun-Lamothe, L.; Cauquil, L. Stat Fingerprints: a friendly graphical interface
353 program for processing and analysis of microbial fingerprint profiles. *Mol Ecol Resources.* **2009**, 9, 1359-1363.
- 354 (21) R Development Core Team R: A language and environment for statistical computing. R Foundation for Statistical Computing,
355 Vienna, Austria. **2009**, ISBN 3-900051-07-0, URL <http://www.R-project.org>.
- 356 (22) Gharpuray, M.M.; Lee, Y.H.; Fan, L.T. Structural Modification of Lignocellulosics by Pretreatments to Enhance Enzymatic-
357 Hydrolysis. *Biotechnol. Bioeng.* **1983**, 25, 157-172.
- 358 (23) Zhao, Y.; Wang, Y.; Zhu, J.Y.; Ragauskas A; Deng, Y. Enhanced enzymatic hydrolysis of spruce by alkaline pretreatment at
359 low temperature. *Biotechnol. Bioeng.* **2007**, 99, 1320-1328
- 360 (24) Chang, V.S.; Holtzaple, M.T. Fundamental factors affecting biomass enzymatic reactivity. *Appl. Biochem. Biotechnol.* **2000**,
361 84, 5-37.
- 362 (25) Pakarinen, A.; Zhang, J.; Brock, T.; Maijala, P.; Viikari, L. Enzymatic accessibility of fiber hemp is enhanced by enzymatic or
363 chemical removal of pectin. *Bioresource Technol.* **2012**, 107, 275- 281.
- 364 (26) Shi, X. X.; Song, H. C.; Wang, C. R.; Tang, R. S.; Huang, Z. X.; Gao, T. R.; Xie, J. Enhanced bio-hydrogen production from
365 sweet sorghum stalk with alkalization pretreatment by mixed anaerobic cultures. *Int. J. Energ. Res.* **2010**, 34, 662–672.
- 366
367
368
369
370
371
372
373
374
375
376
377
378
379
380
381
382
383
384

- 385 (27) Lin C.Y.; Cheng, C.H. Fermentative hydrogen production from xylose using anaerobic mixed microflora. *Int. J. Hydrogen*
386 *Energ.* **2006**, 31, 832–40.
387
- 388 (28) Quemeneur, M.; Hamelin, J.; Benomar, S.; Guidici-Ortoni, M. T.; Latrille, E.; Steyer, J. P.; Trably, E. Changes in hydrogenase
389 genetic diversity and proteomic patterns in mixed-culture dark fermentation of mono-, di- and tri-saccharides. *Int. J. Hydrogen*
390 *Energ.* **2011**, 36, 11654-11665.
391
- 392 (29) Monlau, F.; Aemig, Q.; Trably, E.; Hamelin, J.; Steyer, J.P.; Carrere, H. Specific inhibition of biohydrogen-producing
393 *Clostridium* sp. after dilute-acid pretreatment of sunflower stalks. *Int. J. Hydrogen Energ.* **2013**, 38, 12273–12282.
394
- 395 (30) Guo, X. M.; Trably, E.; Latrille, E.; Carrere, H.; Steyer, J. P. Hydrogen production from agricultural waste by dark fermentation:
396 A review. *Int. J. Hydrogen Energ.* **2010**, 35, 10660–10673.
397
- 398 (31) Nath, K.; Das, D. Improvement of fermentative hydrogen production: various approaches. *Appl. Microbiol Biotechnol.* **2004**, 65,
399 520-529.
400
- 401 (32) Dellomonaco, C., Fava, F. and Gonzalez, R. The path to next generation biofuels: successes and challenges in the era of
402 synthetic biology. *Microbial Cell Factories.* **2010**, 9, 3.
403
- 404 (33) Kovarova-Kovar, K.; Egli, T. Growth kinetics of suspended microbial cells: from single-substrate-controlled growth to mixed
405 substrate kinetics. *Microbiol. Mol. Biol. Rev. a.* **1998**, 62, 646.
406
- 407 (34) Fang H.H.P.; Zhang T.; Liu H. Microbial diversity of a mesophilic hydrogen-producing sludge. *Appl. Microbiol. Biotechnol.*
408 **2002**, 58: 112–118.
409
- 410 (35) Hanly, T.J.; Henson, M.A. Dynamic Flux Balance Modeling of Microbial Co-Cultures for Efficient Batch Fermentation of
411 Glucose and Xylose Mixtures. *Biotechnol. Bioeng.* **2010**, 108, 376-385.
412
- 413 (36) Kuyper M.; Toirkens, M.J.; Diderich, J.A.; Winkler, A.A.; van Dijken, J.P.; Pronk, J.T. Evolutionary engineering of mixed-
414 sugar utilization by a xylose-fermenting *Saccharomyces cerevisiae* strain. *FEMS Yeast Res.* **2005**, 5, 925-934.
415
- 416 (37) Baghchehsaraee, B.; Nakhla, G.; Karamanev, D.; Margaritis, A.; Reid, G. The effect of heat pretreatment temperature on
417 fermentative hydrogen production using mixed cultures. *Int. J. Hydrogen Energ.* **2008**, 33, 4064-4073.
418
- 419 (38) Chaganti, S.R.; Lalman, J.A.; Heath, D.D., 16S rRNA gene based analysis of the microbial diversity and hydrogen production in
420 three mixed anaerobic cultures. *Int. J. Hydrogen Energ.* **2012**, 7, 9002-9017.
421

422 TABLES and FIGURES CAPTIONS

423
424
425 **Table 1** Accessible surface area (SA), Volume pores (Vp) Sugars contents in equivalent hexose (g eq hexose.g⁻¹ VS) and biohydrogen potentials originating
426 from total, liquid and solid fractions of raw sunflower stalks (SS) and alkaline-pretreated sunflower stalks at 55°C(SS 55°C) and 170°C (SS 170°C) with or
427 without enzymatic hydrolysis
428

429 **Table 2** Repartition of the bacterial population in % of order, genus and species during dark fermentation process at 40 h and 92 h after enzymatic
430 hydrolysis of raw sunflower stalks (SS), alkaline pretreated sunflower stalks at 55°C (SS, 55°C) and at 170°C (SS, 170°C).
431

432 **Figure 1** Scheme of pretreatment strategies used and biochemical composition of raw sunflower stalks (SS) expressed in g/100g initial VS and of the solid
433 fractions after thermo-alkaline pretreatments at 55°C (SS 55°C) and at 170°C (SS 170°C) expressed in g/100g initial VS and in g/100g remaining VS.
434 Values correspond to means of two replicates of independent values ± standard deviation.

435 **Figure 2** Impact of pretreatments on the origin of the biohydrogen production (ml H₂.g⁻¹ initial VS) for raw sunflower stalks and solid residue of alkaline
436 pretreated sunflower stalks at 55°C and 170°C with or without enzymatic hydrolysis. Values correspond to means of two replicates of independent values ±
437 standard deviations (error bars).
438

439 **Figure 3** Evolution of sugars monomers consumption (ie glucose and xylose) released from enzymatic hydrolysis during H₂ fermentation in mixed culture
440 (a) from raw sunflower stalks (b) from solid residue of sunflower stalks pretreated at 55°C, 24 h, 4% NaOH (c) from solid residue of sunflower stalks
441 pretreated at 170°C, 1 h, 4% NaOH. Values correspond to means of two replicates of independent values ± standard deviations (error bars).

443 **Table 1** Accessible surface area (SA), Volume pores (Vp) Sugars contents in equivalent hexose (g eq hexose.g⁻¹ VS) and biohydrogen potentials originating from total, liquid and solid fractions of raw sunflower
 444 stalks (SS) and alkaline-pretreated sunflower stalks at 55°C(SS 55°C) and 170°C (SS 170°C) with or without enzymatic hydrolysis

Conditions	Fractions	Structural features		Sugars content (g eq hexose. 100g ⁻¹ VS)	Biohydrogen potentials	
		SA (m ² .g ⁻¹ remaining TS)	Vp (cm ³ .g ⁻¹ remaining TS)		mL H ₂ .g ⁻¹ VS	mol H ₂ .mol ⁻¹ eq hexose
SS	Total	1.55	0.083	43.5	2.3 ± 0.9	0.043
SS (55°C)	Total			43.5	4.4 ± 2.6	0.081
	Liquid			6.1 (14%) ^a	2.6 ± 0.2 (57%) ^b	0.344
	Solid	1.59	0.106	37.4 (86%) ^a	2 ± 0 (43%) ^b	0.043
SS (170°C)	Total			43.5	20.6 ± 5.6	0.380
	Liquid			10.6 (24.3%) ^a	11.4 ± 0.3 (69%) ^b	0.865
	Solid	2.55	0.235	32.9 (75.7%) ^a	5.1 ± 0.4 (31%) ^b	0.125
SS + Enzymes	Total			43.5	30.4 ± 3.8	0.562
SS (55°C) + Enzymes	Total			50.2	59.9 ± 2.6 ^c	0.959
SS (170°C) + Enzymes	Total			56.1	80.9 ± 3.0 ^c	1.158

445 ^a Percentage of total glucose originating from the liquid and solid fractions. In the liquid fraction, sugar content in equivalent glucose was calculated according the removal of holocelluloses
 446 in the initial total fraction.

447 ^b Percentage of biohydrogen potentials originating from the liquid and solid fractions

448 ^c Biohydrogen potentials are expressed in ml H₂.g⁻¹ remaining VS

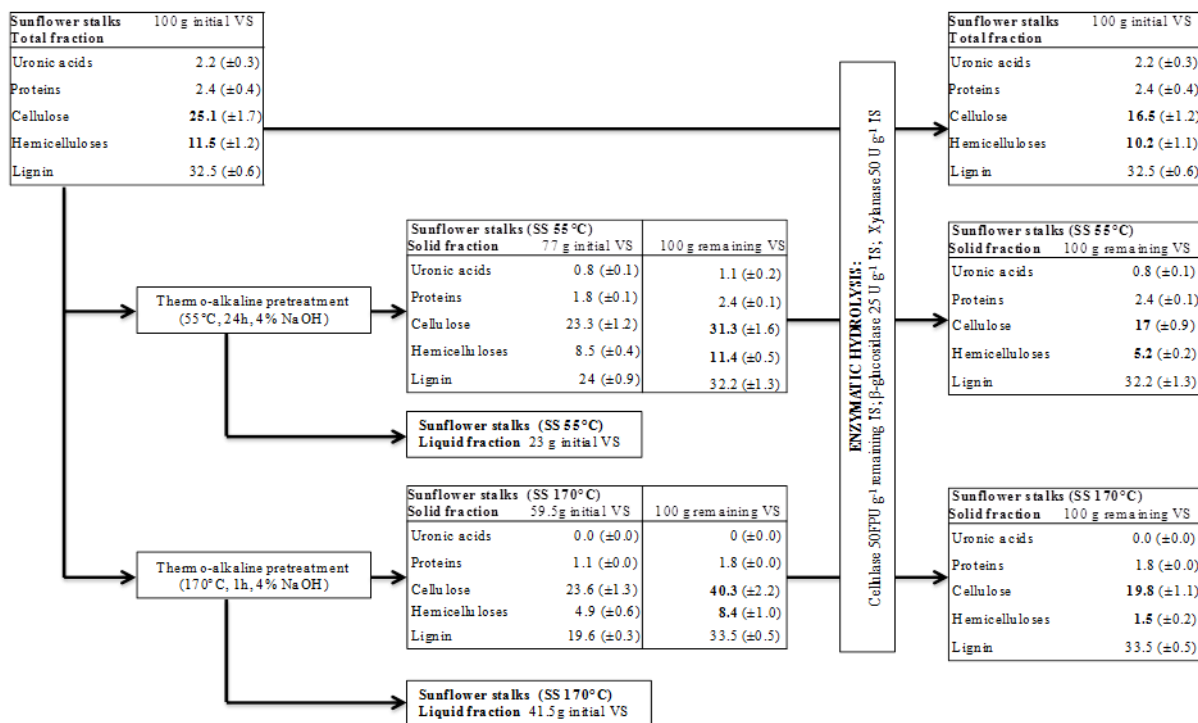
449

450

452 **Table 2** Repartition of the bacterial population in % of order, genus and species during dark fermentation process at 40 h and 92 h after enzymatic hydrolysis of raw sunflower stalks (SS), alkaline pretreated
 453 sunflower stalks at 55°C (SS, 55°C) and at 170°C (SS, 170°C).

	Conditions					
	SS 40 h	SS 92 h	SS (55°C) 40 h	SS (55°C) 92 h	SS (170°C) 40 h	SS (170°C) 92 h
Number of sequencing	6366	4715	4791	6172	3980	4940
Number of species	26	28	23	34	25	30
% ORDER / Genus species^a						
CLOSTRIDIALES	91	92	96	92	85	95
<i>Clostridium butyricum</i>	89.0	72.3	92.9	60.3	80.3	71.6
<i>Clostridium perfringens</i>	0.0	0.0	0.0	9.7	0.0	0.1
<i>Clostridium roseum</i>	0.4	6.2	0.7	6.7	0.7	13.5
<i>Clostridium aciditolerans</i>	0.9	1.5	0.5	6.5	1.5	1.5
<i>Clostridium saccharobutylicum</i>	0.0	0.0	0.0	2.7	0.0	0.1
<i>Clostridium tertium</i>	0.2	0.8	0.8	1.9	0.6	0.4
<i>Clostridium lundensis</i>	0.0	0.4	0.0	1.7	0.0	0.4
<i>Clostridium peptidivorans</i>	0.2	0.6	0.1	1.1	0.4	0.2
<i>Clostridium saccharoperbutylaceticum</i>	0.3	3.3	0.3	1.1	0.5	2.6
<i>Clostridium tunisiense</i>	0.1	1.0	0.1	0.3	0.0	3.5
<i>Clostridium bifermentans</i>	0.0	0.0	1.0	0.1	0.9	0.3
<i>Clostridium thiosulfatireducens</i>	0.0	3.2	0.0	0.0	0.0	0.2
<i>Clostridium botulinum</i>	0.0	1.7	0.0	0.0	0.0	0.4
<i>Clostridium paraputrificum</i>	0.0	1.0	0.0	0.0	0.0	0.1
BACILLALES	8	7	3	5	13	4
<i>Rummeliibacillus pycnus</i>	0.0	0.0	0.6	3.0	0.0	0.0
<i>Sporolactobacillus racemilacticus</i>	0.0	0.0	0.0	1.1	0.0	1.0
<i>Bacillus ginsengihumi</i>	7.9	7.0	2.0	0.6	13.3	3.0
Others	1	1	1	3	2	1

454 ^a Among the species observed, only species with a relative abundance above 1% are represented in the table

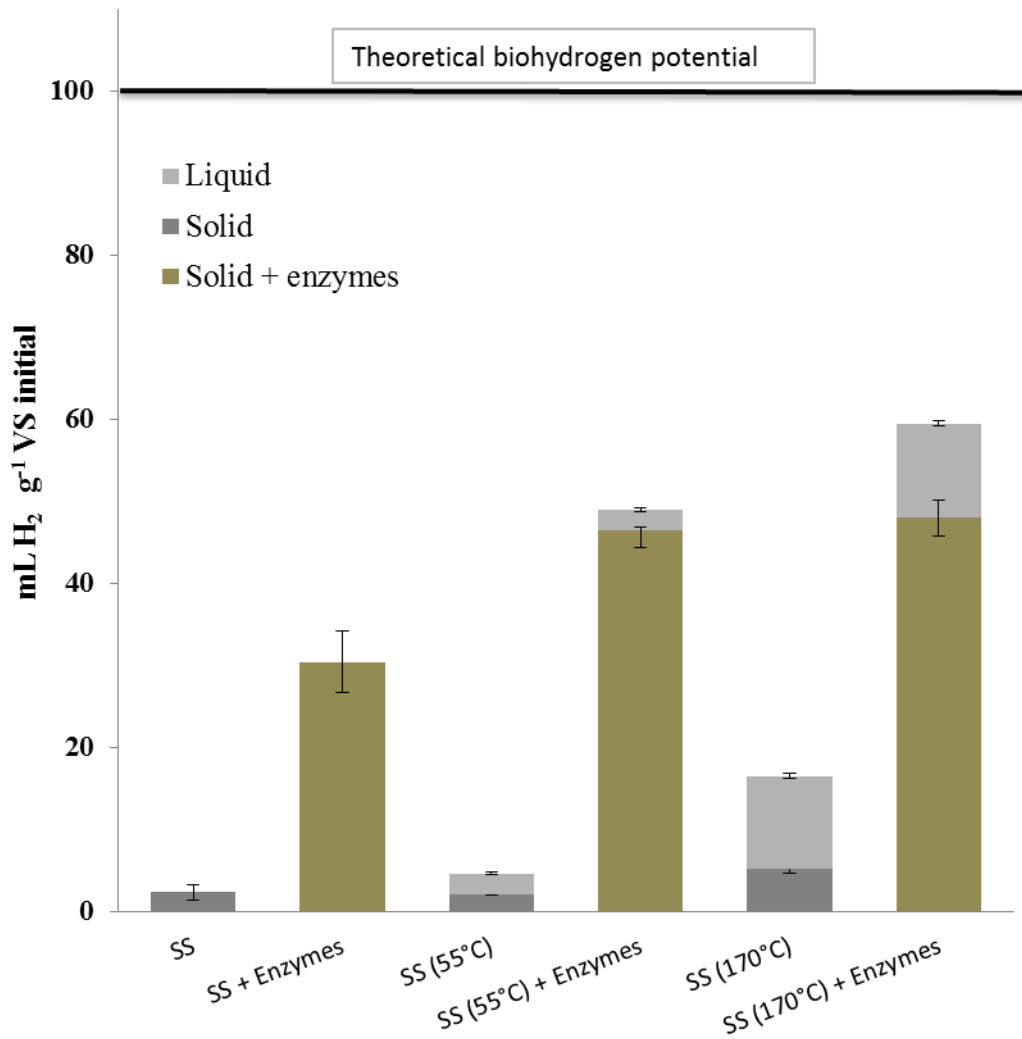


456

457

458 **Figure 1** Scheme of pretreatment strategies used and biochemical composition of raw sunflower stalks (SS) expressed in g/100g initial VS and of the solid
 459 fractions after thermo-alkaline pretreatments at 55°C (SS 55°C) and at 170°C (SS 170°C) expressed in g/100g initial VS and in g/100g remaining VS.
 460 Values correspond to means of two replicates of independent values ± standard deviation.

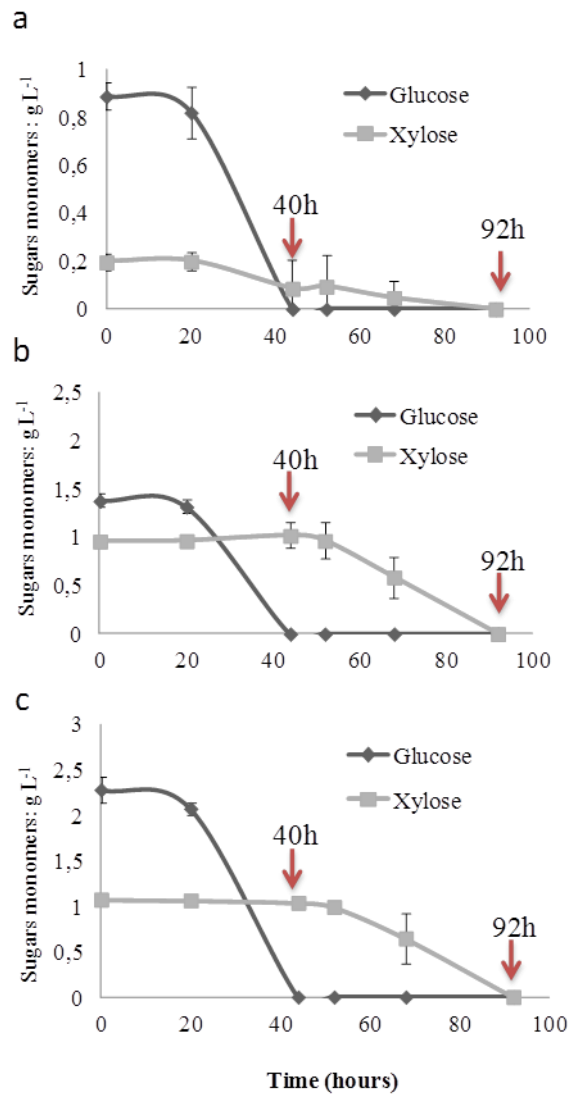
461



462
463

464 **Figure 2** Impact of pretreatments on the origin of the biohydrogen production (mL H₂·g⁻¹ initial VS) for raw sunflower stalks and solid residue of alkaline
465 pretreated sunflower stalks at 55°C and 170°C with or without enzymatic hydrolysis. Values correspond to means of two replicates of independent values ±
466 standard deviations (error bars).

467



468

469

470

471 **Figure 3** Evolution of consumption of monomeric sugars (ie glucose and xylose) released from enzymatic hydrolysis during H₂ fermentation in mixed
 472 cultures (a) from raw sunflower stalks (b) from solid residue of sunflower stalks pretreated at 55°C, 24 h, 4% NaOH (c) from solid residue of sunflower
 473 stalks pretreated at 170°C, 1 h, 4% NaOH. Values correspond to means of two replicates of independent values ± standard deviations (error bars).

474

475

476

477

478

479

480