

Extrusion technology as a promising tool for vegetable oil extraction: Biorefinery of Apiaceae fruits

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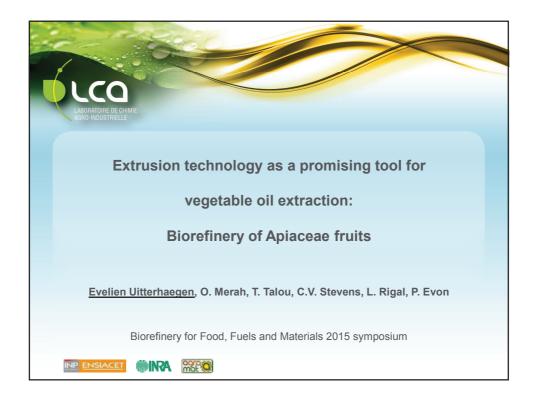
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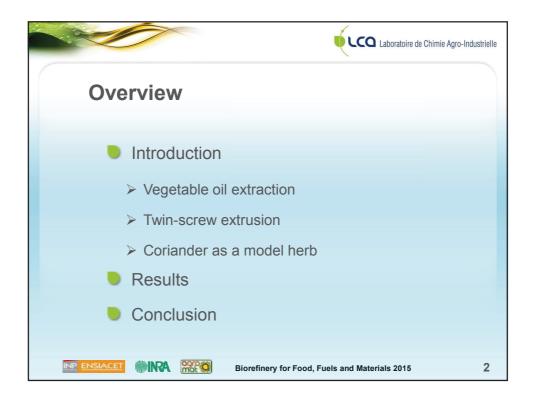
EXTRUSION TECHNOLOGY AS A PROMISING TOOL FOR VEGETABLE OIL EXTRACTION: BIOREFINERY OF APIACEAE FRUITS

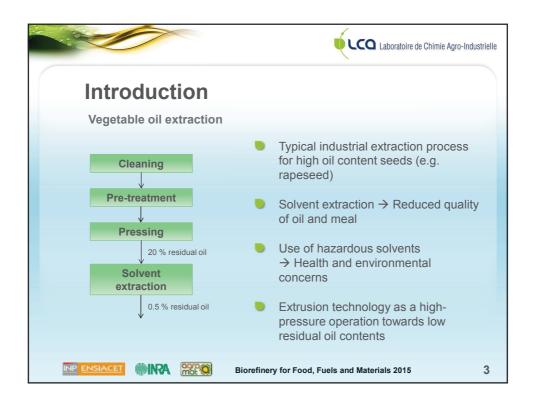
Evelien Uitterhaegen^{1,2}, O. Merah^{1,2}, T. Talou^{1,2}, C.V. Stevens³, L. Rigal^{1,2}, P. Evon^{1,2}

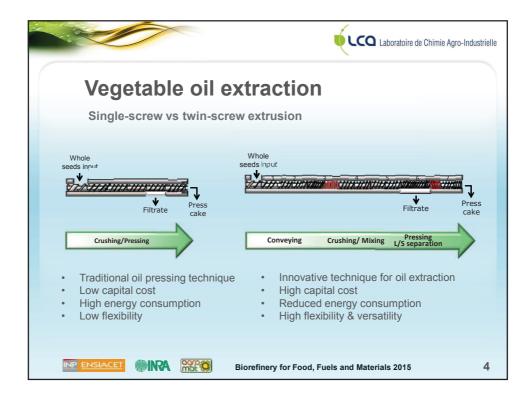
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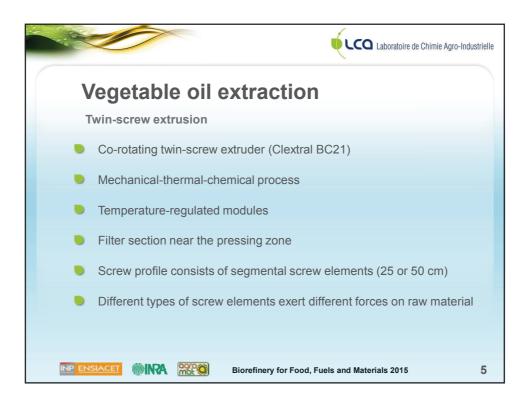
As fossil resources are steadily depleting and environmental concerns have developed into one of the main discussion points in public and political agendas, sustainability and an ecological viewpoint have become indispensable terms in modern society. This critical pressure towards 'greener' alternatives has led to a progressive application of renewable resources by the chemical industry. Vegetable oils present an interesting class of bioresources, with a market comprising both food and non-food applications. Their extraction is a key process as it will exert a strong impact on the resulting oil characteristics and quality. It is most frequently executed through solvent extraction, although mechanical pressing may present an interesting alternative as it represents a generally safer and more sustainable process. Furthermore, oils obtained through pressing are considered to be of superior quality and do not contain any solvent traces. The main drawback to this process involves the extraction yield, which is typically lower than for solvent extraction. Therefore, research has recently focused on continuous oil extraction through extrusion technology and its process optimization in order to increase extraction yields. Single-screw, as well as twin-screw extrusion was employed to efficiently extract vegetable oil from Apiaceae fruits, with Coriandrum sativum L. as a model herb. Coriander vegetable oil is particularly interesting as it has recently been approved as Novel Food Ingredient and is rich in petroselinic acid, allowing applications in oleochemistry. Simultaneously, this allowed coriander fruit biorefinery, as the press cakes may be transformed into agromaterials through thermopressing or be incorporated into a thermoplastic matrix such as PLA for injection molding. This represents a key advancement in the overall process economics and an important waste reduction. The oil extraction efficiency was significantly enhanced through the application of pre-treatments of the fruits prior to the extrusion process. Specifically, the fruit moisture content was shown to exhibit a key impact on their crushing behavior and oil extraction yields. As an example, when mechanical pressing is conducted in a Clextral BC 21 twin-screw extruder, an extraction yield of 68% is reached, representing a 44% increase, when the fruit moisture content is reduced from 9.8 to 0.3%, further leading to a significant decrease in the residual oil content of the obtained press cake.

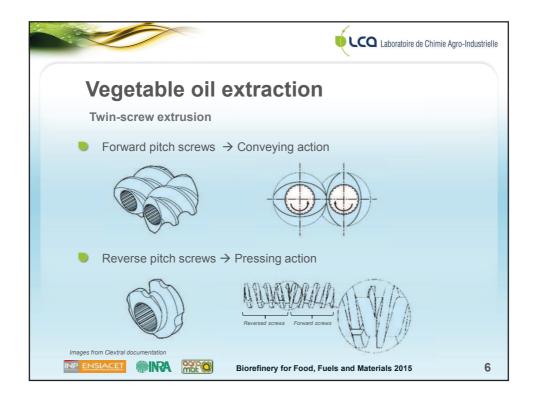




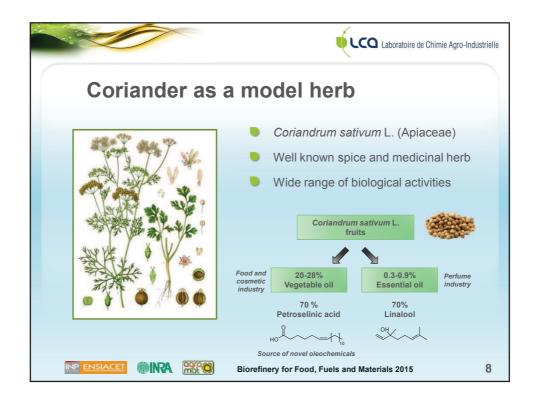


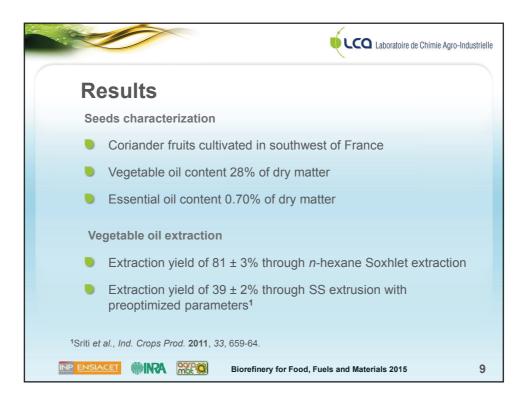




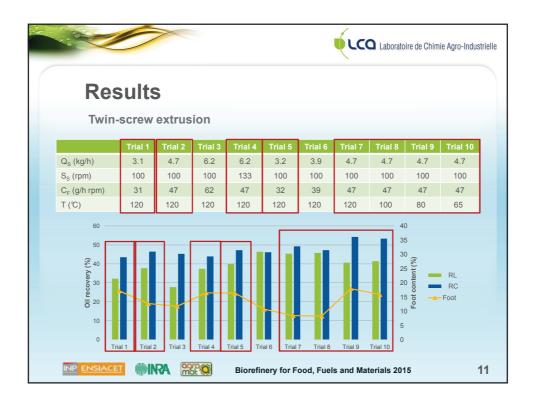


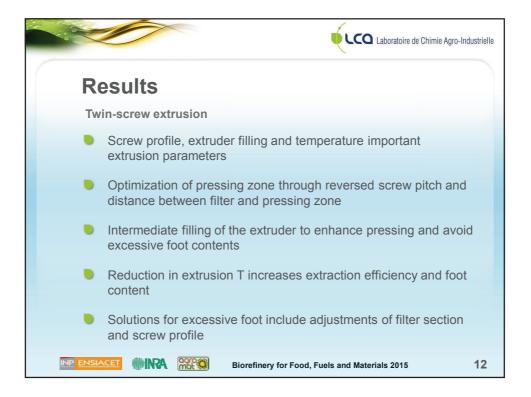






Res	sults	5								
Twin-	screw	extrus	ion							
S	crew p	orofile	alterati	ons ne	ear the	press	ing ma	dule		
	rofile 1 ariatio		ŕ	let flov	v rate a	and ex	trusior	n temp	erature	e on
• V	′ariatioi crew p	n of se rofile 2	eds in 2 (Trial	s 5-10)					
• V	ariatio	n of se	eds in			and ex Trial 6	trusior Trial 7	tempo Trial 8	erature Trial 9	e ON Trial 10
• V	ariation crew p	n of se rofile 2 Trial	eeds in 2 (Trial Trial	s 5-10 Trial) Trial	Trial	Trial	Trial	Trial	Trial
● V S	′ariatioi crew p Trial	n of se rofile 2 Trial 2	eeds in 2 (Trial Trial 3	s 5-10 Trial 4) Trial 5	Trial 6	Trial 7	Trial 8	Trial 9	Trial 10
Q _s (kg/h)	/ariation crew p Trial 1 3.1	n of se rofile 2 Trial 2 4.7	eds in 2 (Trial Trial 3 6.2	s 5-10 Trial 4 6.2) Trial 5 3.2	Trial 6 3.9	Trial 7 4.7	Trial 8 4.7	Trial 9 4.7	Trial 10 4.7







Quality cor	ວ nsideration:	s			
Quanty ool	loidoration				
	Trial 2	Trial 4	Trial 7	Trial 8	Trial 10
PA content (%)	72.8 ± 0.2	72.9 ± 0.2	73.4 ± 0.2	73.3 ± 0.1	73.3 ± 0.2
FFA (%)	1.46 ± 0.04	1.47 ± 0.01	1.41 ± 0.07	1.46 ± 0.01	1.52 ± 0.08
Essential oil content (% db)	0.14 ± 0.01	0.14 ± 0.01	0.14 ± 0.01	0.18 ± 0.01	0.31 ± 0.02
Signific		ch in petros se in essent ion T			cake with

