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1 **Mid-infrared technique to forecast cooked puree properties from raw apples: a**  
2 **potential strategy towards sustainability and precision processing**

3

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28

29 **Highlights**

30 MIRS discriminated purees cooked from different apples and processing conditions.

31 MIRS on purees gave robust predictions of soluble solids and acidity ( $RPD \geq 3.1$ ).

32 Spectra of purees could be calculated from spectra of homogenized raw apples.

33 The calculated spectra allowed acceptable predictions of puree viscosity ( $RPD \geq 2.5$ ).

34

35 **Abstract**

36 The potential of MIRS was investigated to: i) differentiate cooked purees issued from  
37 different apples and process conditions, and ii) predict the puree quality characteristics  
38 from the spectra of homogenized raw apples. Partial least squares (PLS) regression was  
39 tested both, on the real spectra of cooked purees and their reconstructed spectra  
40 calculated from the spectra of homogenized raw apples by direct standardization. The  
41 cooked purees were well-classified according to apple thinning practices and cold  
42 storage durations, and to different heating and grinding conditions. PLS models using  
43 the spectra of homogenized raw apples can anticipate the titratable acidity (the residual  
44 predictive deviation (RPD) = 2.9), soluble solid content (RPD = 2.8), particle averaged  
45 size (RPD = 2.6) and viscosity (RPD  $\geq$  2.5) of cooked purees. MIR technique can  
46 provide sustainable evaluations of puree quality, and even forecast texture and taste of  
47 purees based on the prior information of raw materials.

48

49 **Key words:** *Malus x domestica* Borkh.; Mid infrared spectroscopy; PLS models; Direct  
50 standardization; Discriminant analysis.

51

52 **Introduction**

53 Apple puree is one of the major industrially processed fruit products (over 0.3  
54 million tons consumed per year in France and the world market value about 2000  
55 million USD annually) (FranceAgriMer, 2017; Market Research Future, 2019), and can  
56 be used as the basic ingredient of jams, preserves or compotes (Defernez, Kemsley, &  
57 Wilson, 1995). The quality of apple purees is systematically influenced by both raw  
58 material characteristics (Buergy, Rolland-Sabaté, Leca, & Renard, 2020; Lan, Bureau,  
59 Chen, Leca, Renard, & Jaillais, 2021; Lan, Jaillais, Leca, Renard, & Bureau, 2020;  
60 Rembiałkowska, Hallmann, & Rusaczonok, 2007) and cooking strategies (heating,  
61 grinding speed and refining levels etc.) (Espinosa, To, Symoneaux, Renard, Biau, &  
62 Cuvelier, 2011; Oszmiański, Wolniak, Wojdyło, & Wawer, 2008; Picouet, Landl,  
63 Abadias, Castellari, & Viñas, 2009). In practical apple processing, industrial  
64 manufactures have to face the variability and heterogeneity of raw apples, optimize  
65 their processing strategies to maintain the sustainable and expected quality level of final  
66 puree products. Thus, developing rapid, efficient and integrated methods is needed to  
67 guide suitable fruit processing procedures, even to design innovative foods by using the  
68 raw material variability, and to reduce fruit wastes all along the processing chain.

69 Mid infrared spectroscopy (MIRS) is one of the main candidates for both the  
70 quantification and qualification of agricultural commodities and processed food  
71 (Bureau, Cozzolino, & Clark, 2019; Downey, 1998). Although MIRS presents a  
72 relatively lower ability for quantification than that of chromatography or mass  
73 spectrometry, it has the advantage of a rapid data acquisition and can provide  
74 informative fundamental vibrations of molecular bonds (Karoui, Mazerolles, & Dufour,  
75 2003). It does require a minimal sample preparation as the measurement must be done  
76 on homogeneous samples as liquid, puree or powder due to the very low penetration of  
77 radiation into the samples. Direct MIR characterizations of raw and processed fruits  
78 have shown considerable aptitudes to evaluate soluble solids content (SSC), dry matter  
79 content (DMC), titratable acidity (TA), some individual sugars, organic acids,  
80 rheological (viscosity and viscoelasticity) and structural (particle averaged size and  
81 volume) properties (Ayvaz, Sierra-Cadavid, Aykas, Mulqueeney, Sullivan, &

82 [Rodriguez-Saona, 2016; Lan, Renard, Jaillais, Leca, & Bureau, 2020](#)). These studied  
83 parameters are related to the taste (SSC, DMC, TA, malic acid), the texture (viscosity,  
84 viscoelasticity, particles and cell wall contents) and the basic nutrients (fructose,  
85 sucrose and glucose) impacting in a large amount puree quality ([Bureau, Ścibisz, Le  
86 Bourvellec, & Renard, 2012; Espinosa-Muñoz, Renard, Symoneaux, Biau, & Cuvelier,  
87 2013; Fügél, Carle, & Schieber, 2005](#)).

88 Currently, our interest is to determine the possibility of using this technique to  
89 anticipate the characteristics of processed materials from the data acquired on  
90 homogenized raw fruit. According to our previous studies, strong correlations of  
91 spectral, chemical and textural properties between raw apples and the corresponding  
92 purees have been pointed out ([Lan, Jaillais, Leca, Renard, & Bureau, 2020; Lan, Renard,  
93 Jaillais, Leca, & Bureau, 2020](#)). Based on that, the quality of final processed purees  
94 could be predicted by the infrared spectral information acquired on raw apples using  
95 partial least square (PLS) regression ([Lan, Jaillais, Leca, Renard, & Bureau, 2020](#)). The  
96 main drawback of this strategy is the need, for modelling, to systematically acquire the  
97 corresponding spectra on both raw and processed materials with a large number of  
98 conditions representative of the variability, giving often only rough assessments. In  
99 addition, the internal correlations of quality traits during puree processing were only  
100 confirmed under one of the most commonly used processing conditions ([Lan, Jaillais,  
101 Leca, Renard, & Bureau, 2020](#)).

102 Direct standardization (DS) is a simple and efficient chemometric tool for the  
103 calibration transfer between spectral measurements or between two different sets of  
104 conditions, such as the spectral calibration from the off-line to on-line spectra of olive  
105 fruits ([Salguero-Chaparro, Palagos, Peña-Rodríguez, & Roger, 2013](#)). As far as we  
106 know, this method has never been considered to bridge the spectral variations along the  
107 fruit processing chain. Our interest of this method is thus to find the spectra  
108 relationships of all processed purees and their corresponding spectral information  
109 acquired on homogenized apples, and to calculate the reconstructed processed puree  
110 spectra according to their relative spectral information acquired on apples by DS, taking  
111 into account both the variability of raw materials and of commonly used processing

112 conditions. If so, the predictive models of puree quality traits (biochemical and physical)  
113 using their reconstructed spectra dataset open the possibility to i) predict the properties  
114 of processed apples based on the prior information of raw materials; ii) provide  
115 sustainable and precise processing strategies to estimate the quality potential of final  
116 products, and iii) to compare *in silico* the prediction results of different processing  
117 approaches to better control the quality of fruit products.

118 Accordingly, this work aimed to assess the potential of MIRS to: i) detect the  
119 variability of the cooked apple purees according to the pre- and post-harvest conditions  
120 (fruit thinning and storage periods) and the main processing conditions (heating  
121 temperature and grinding speed); ii) calculate reconstructed spectra of purees taking  
122 into account the variability of raw fruits and processing conditions; and iii) characterize  
123 and anticipate the biochemical (SSC, DMC, TA, individual sugars and malic acid),  
124 rheological (viscosity and viscoelasticity) and textural (particle size and volume)  
125 properties of the processed purees.

## 126 **Materials and methods**

### 127 **2.1 Apples and purees**

#### 128 **2.1.1 Apples**

129 The experiment was conducted on the cultivar ‘Golden Delicious’ in 2017 and 2019.  
130 All apples were harvested at commercial maturity from La Pugère experimental orchard  
131 (Mallemort, Bouches du Rhône, France) (**Figure 1**).

132 - In 2017, half of the ‘Golden Delicious’ apples were subjected to a commercial  
133 chemical fruit thinning (Th+) with standard fruit load (50-100 fruits/tree), the other  
134 half was not thinned (Th-), resulting in a high fruit load (150-200 fruits/tree). After  
135 harvesting, apples were processed into purees the day after harvest (T0), and after  
136 one (T1), three (T3) and six months (T6) of cold storage at 4°C.

137 - In 2019, the commercially thinned ‘Golden Delicious’ apples (Th+) were stored  
138 for up to one month (T1) at 4 °C until starch regression, then processed into purees  
139 under different processing conditions.

#### 140 **2.1.2 Puree processing**

141 Before processing, and for each condition, around 2 kg apples were homogenized

142 at 11000 rpm with an Ultraturrax T-25 (IKA, Labortechnik, GmbH, Staufen, Germany)  
143 as raw apple homogenates. Three batches of apples (3 kg each) were used to produce  
144 three puree lots for each condition. After sorting and washing, Golden Delicious apples  
145 were cored and cut in 8 portions, then processed in a multi-functional processing system  
146 (Roboqbo, Qb8-3, Bentivoglio, Italy) by different conditions (**Figure 1**):

147 - In 2017, all apple groups (2 thinning practices  $\times$  4 storage periods) were  
148 cooked with a standard Hot Break recipe of 95°C for 5 min at a 1500 rpm grinding  
149 speed, then cooled down to 65°C while maintaining the grinding speed. Finally, 24  
150 different cooked purees (2 thinning practices  $\times$  4 storage periods  $\times$  3 lots) were prepared.

151 - In 2019, each apple group was processed with three different heating  
152 temperatures of 70°C, 83°C and 95°C for 30 min, while ground at three speed levels of  
153 300 rpm, 1000 rpm and 3000 rpm, respectively. Totally, 27 different cooked purees (3  
154 heating temperatures  $\times$  3 grinding speeds  $\times$  3 lots) were prepared.

155 Finally, all cooked purees were conditioned in two hermetically sealing plastic bags:  
156 one was cooled at room temperature (22.5 °C) before the next-day measurements of  
157 rheological, structural and some biochemical (SSC, TA, fructose, sucrose, glucose and  
158 malic acid) properties. And the other one was freeze-dried (FD) and stored at -20 °C  
159 for the determination of the content of cell wall, which are known to be a major  
160 contributor of rheological properties of apple purees ([Espinosa-Muñoz, Renard,](#)  
161 [Symoneaux, Biau, & Cuvelier, 2013](#)).

## 162 **2.2 Determination of puree quality traits**

### 163 **2.2.1 Rheological and structural characterizations on cooked purees**

164 The cooked puree rheological measurements were carried out using a Physica  
165 MCR-301 controlled stress rheometer (Anton Paar, Graz, Austria) and a 6-vane  
166 geometry (FL100/6W) with a gap of 3.46 mm, at 22.5 °C. The flow curves were  
167 performed after a pre-shearing period of 1 minute at a shear rate of 50 s<sup>-1</sup>, followed by  
168 5 minutes at rest. The viscosity was then measured at a controlled shear rate range of  
169 [10; 250] s<sup>-1</sup> on a logarithmic ramp. The values of viscosity at 50 s<sup>-1</sup> and 100 s<sup>-1</sup> ( $\eta_{50}$   
170 and  $\eta_{100}$  respectively) were kept as final indicators of the puree viscosity linked to  
171 sensory characteristics during consumption ([Engelen & de Wijk, 2012](#)). Amplitude



172 Sweep (AS) tests were performed at an angular frequency of 10 rad./s in the  
173 deformation range of [0.01; 100] %, in order to determine the linear viscoelastic range  
174 of the purees and the yield stress, defined as the crossing point between the storage  
175 modulus ( $G'$ ) and the loss modulus ( $G''$ ) curves.

176 Cooked purees were diluted in distilled water to separate particles, stained with  
177 calcofluor (0.1 g/L) and highlighted with a 365 nm UV lamp (Soukup, 2014). The  
178 particle sizes averaged over volume  $d(4:3)$  (de Brouckere mean) and over surface area  
179  $d(3:2)$  (Sauter mean) were measured by a laser granulometer (Rawle, 2003)  
180 (Mastersizer 2000, Malvern Instruments, Malvern, UK).

### 181 **2.2.2 Biochemical analyses on cooked purees**

182 SSC was determined with a digital refractometer (PR-101 ATAGO, Norfolk, VA,  
183 USA) and expressed in °Brix at 20 °C. TA was determined by titration up to pH 8.1  
184 with 0.1 mol/L NaOH and expressed in mmol  $H^+$ /kg of fresh weight (FW) using an  
185 autotitrator (Methrom, Herisau, Switzerland). Individual sugars and malic acid were  
186 quantified using colorimetric enzymatic kits, according to the manufacturer's  
187 instructions (R-biopharm, Darmstadt, Germany). The content of glucose, fructose,  
188 sucrose and malic acid were expressed in g/kg FW. These measurements were  
189 performed with a SAFAS flx-Xenius XM spectrofluorimeter (SAFAS, Monaco) at 570  
190 nm for the sugars and 450 nm for malic acid. The DMC was estimated from the weight  
191 of freeze-dried samples upon reaching a constant weight (freeze-drier, 5 days). Cell  
192 wall materials of purees were isolated using the alcohol insoluble solids method  
193 proposed by Renard (2005) and the cell wall contents (AIS contents) were expressed in  
194 both FW and dry matter weight (DW).

### 195 **2.3 Spectrum acquisition on raw apple homogenates and cooked purees**

196 The MIR spectra were acquired at 23 °C using a Tensor 27 FTIR spectrometer  
197 (Bruker Optics®, Wissembourg, France) equipped with a horizontal attenuated total  
198 reflectance (ATR) sampling accessory and a deuterated triglycine sulphate (DTGS)  
199 detector. The samples were placed at the surface of a zinc selenide crystal (ATR-ZnSe)  
200 with six internal reflections. Spectra with 32 scans for ATR-ZnSe were collected from  
201 4000  $cm^{-1}$  to 650  $cm^{-1}$  with a 4  $cm^{-1}$  resolution and were corrected against the

202 background spectrum of air. Three replications of spectral measurement were done for  
203 each homogenized raw apples and each cooked apple puree.

204 The whole spectral dataset of MIR is described in **Figure S1**. It included i) 81  
205 spectra of raw apple homogenates, of which 72 spectra acquired in 2017 (3 apple  
206 batches  $\times$  2 fruit thinning conditions  $\times$  4 storage times  $\times$  3 spectral replicates) and 9  
207 spectra acquired in 2019 (3 apple batches  $\times$  3 spectral replicates); and ii) 153 spectra of  
208 cooked apple purees, containing 72 spectra acquired in 2017 (2 fruit thinning conditions  
209  $\times$  4 storage times  $\times$  3 processing lots  $\times$  3 spectral replicates) and 81 spectra acquired in  
210 2019 (3 heating temperatures  $\times$  3 grinding levels  $\times$  3 processing lots  $\times$  3 spectral  
211 replicates).

#### 212 **2.4 Statistical analyses of reference data**

213 The reference data of cooked purees processed in 2017 and 2019 are presented as  
214 the mean values and the data dispersion within our experimental dataset expressed as  
215 standard deviation values (SD). After the Shapiro-Wilk tests, the references data of  
216 processed purees affected by fruit thinning and storage times were normal distributed  
217 ( $\alpha=0.05$ ), but not for the dataset of heating temperature and grinding effects during  
218 puree processing. Thus, analysis of variance (ANOVA) was carried out to determine  
219 the significant differences of cooked purees due to fruit thinning and storage times  
220 applied on raw apples (**Table S1**) using XLSTAT (version 2018.5.52037, Addinsoft  
221 SARL, Paris, France) data analysis toolbox. Kruskal-Wallis tests were performed to  
222 evaluate the effects of heating temperature and grinding levels during puree processing  
223 (**Table S2**).

#### 224 **2.5 Spectra transferred by direct standardization (DS)**

225 In this study, DS was used to find the relationship between the spectra matrices of  
226 all cooked purees (***P***) and their corresponding spectra of raw apple homogenates (***F***),  
227 taking into account the effects of raw material variability and processing conditions.  
228 The DS transfer works were performed in R software (version 4.0.2) ([R Core Team,](#)  
229 [2019](#)) following a previous report ([Ji, Viscarra Rossel, & Shi, 2015](#)):

$$230 \quad \mathbf{P} = \mathbf{FB} + \mathbf{E} \quad (1)$$

231 where ***B*** is the transfer matrix ( $\lambda \times \lambda$ ) presenting the variations in both ***F*** and ***P***,

232  $E$  is the residual matrix used to correct the baseline difference.  $F$ ,  $P$  and  $E$  matrices  
 233 have the same size  $n \times \lambda$ , where  $n$  presents the numbers of transfer spectra and  $\lambda$  is the  
 234 number of wavenumbers between 1800 and 900  $\text{cm}^{-1}$ .

235 First, to compute the transfer  $B$  and error  $E$  matrices, the whole MIR spectral  
 236 dataset ( $P$  and  $F$ ) was divided into: the calibration matrices, presenting the first two  
 237 batches of raw apple homogenates ( $Fc$ ) and the first two lots of cooked purees ( $Pc$ ),  
 238 and the validation matrices with the third batch of raw apple homogenates ( $Fv$ ) and the  
 239 third lot of cooked purees ( $Pv$ ) (Figure S1).

240 In a second step, DS was performed separately on the calibration matrices of raw  
 241 apple homogenates ( $Fc$ ) and cooked purees ( $Pc$ ) in 2017 ( $Fc_{2017}$  and  $Pc_{2017}$ ) and  
 242 2019 ( $Fc_{2019}$  and  $Pc_{2019}$ ) (Figures S1 and 2):

243 - the calibration matrices of apples ( $Fc_{2017}$ ) and purees ( $Pc_{2017}$ ) were processed  
 244 to obtain the  $B_0$  and  $E_0$  related to the effects of raw materials on the processed  
 245 purees as follows:

$$246 \quad Pc_{2017} = Fc_{2017}B_0 + E_0 \quad (2)$$

247 Both ( $Fc_{2017}$ ) and ( $Pc_{2017}$ ) have the same size  $n \times \lambda$ , where  $n = 48$ ; (2 thinning  
 248 practices  $\times$  4 storage periods  $\times$  2 apple batches/ puree lots  $\times$  3 spectral replicates.

249 - the calibration matrices of apples ( $Fc_{2019}$ ) and purees ( $Pc_{2019}$ ) were performed  
 250 for each puree processing condition, as follows:

$$251 \quad Pc_{2019}^{(i)} = Fc_{2019}B_i + E_i \quad (3)$$

252 where  $i$  from 1 to 9, corresponding to 9 different processing conditions (3 heating  
 253 temperatures  $\times$  3 grinding speeds). To each spectral replicate of  $Fc_{2019}$  corresponds  
 254 nine spectra according to each processing condition ( $Pc_{2019}$ ). All the spectra of  $Pc_{2019}$   
 255 matrix corresponding to the same processing conditions were gathered in a specific  
 256 matrix  $Pc_{2019}^{(i)}$ . The size of this matrix (one for each processing condition) is equal to  
 257 that of raw apple homogenates  $Fc_{2019}$  ( $n = 6$  spectra (2 apple batches  $\times$  3 spectral  
 258 replicates)  $\times$   $\lambda$ ).

259 Thirdly, once all the transfer  $B$  ( $B_0$  and  $B_i$ ) and error  $E$  ( $E_0$  and  $E_i$ ) matrices  
 260 were computed, they were used to calculate the cooked puree reconstructed calibration

261 and validation spectra matrices, as follows (**Figure 2**):

$$262 \quad \mathbf{Tc}_{2017} = \mathbf{Fc}_{2017}\mathbf{B}_0 + \mathbf{E}_0 \quad (4)$$

$$263 \quad \mathbf{Tv}_{2017} = \mathbf{Fv}_{2017}\mathbf{B}_0 + \mathbf{E}_0 \quad (5)$$

$$264 \quad \mathbf{Tc}_{2019} = \mathbf{Fc}_{2019}\mathbf{B}_i + \mathbf{E}_i \quad (6)$$

$$265 \quad \mathbf{Tv}_{2019} = \mathbf{Fv}_{2019}\mathbf{B}_i + \mathbf{E}_i \quad (7)$$

266 Finally, the reconstructed calibration and validation spectral matrices of cooked  
267 puree,  $\mathbf{Tc}$  ( $\mathbf{Tc}_{2017} + \mathbf{Tc}_{2019}$ ) and  $\mathbf{Tv}$  ( $\mathbf{Tv}_{2017} + \mathbf{Tv}_{2019}$ ) of the two years (2017  
268 and 2019) were obtained with the same sizes of the real spectral matrices of cooked  
269 puree,  $\mathbf{Pc}$  and  $\mathbf{Pv}$ , for the further multivariate regressions.

## 270 **2.6 Multivariate regression**

271 Spectral pre-processing and multivariate data analysis were performed with Matlab  
272 7.5 (Mathworks Inc. Natick, MA, USA) software using the SAISIR package ([Cordella](#)  
273 [& Bertrand, 2014](#)). After pretests of several pre-processing treatments (baseline  
274 correction, standard normal variate (SNV) and a derivative transform calculation using  
275 Savitzky–Golay method (window size = 11, 21, 31) applied on several different spectral  
276 regions, the best results of prediction and discrimination were obtained on the range  
277 1800-900  $\text{cm}^{-1}$ , which has been already highlighted ([Lan, Renard, Jaillais, Leca, &](#)  
278 [Bureau, 2020](#)). Principal Component Analysis (PCA) and Factorial Discriminant  
279 Analysis (FDA) were applied on SNV pre-treated spectra of cooked purees to detect  
280 their differences related to the variability of both, raw apples and processing conditions.  
281 The specificity and sensitivity values of FDA discriminations were calculated by the  
282 already reported method of Nargis et al. ([2019](#)).

283 PLS models were developed using the SNV pre-processed puree spectra (1800-900  
284  $\text{cm}^{-1}$ ) of the calibration set  $\mathbf{Pc}$  and the DS transferred spectra of purees ( $\mathbf{Tc}$ ),  
285 corresponding to the same reference dataset. The two calibration matrices of cooked  
286 purees included a total of 102 spectra (48 spectra in 2017: 2 thinning practices  $\times$  4  
287 storage periods  $\times$  2 lots  $\times$  3 spectral replicates, and 54 spectra in 2019: 3 heating  
288 temperatures  $\times$  3 grinding speeds  $\times$  2 lots  $\times$  3 spectral replicates). Then, the developed  
289 PLS models were applied on their corresponding validation spectra sets of  $\mathbf{Pv}$  and  
290  $\mathbf{Tv}$ , with a total of 51 spectra in 2017: 2 thinning practices  $\times$  4 storage periods  $\times$  1 lot

291 × 3 spectral replicates and in 2019: 3 heating temperatures × 3 grinding speeds × 1 lot  
292 × 3 spectral replicates. PLS model performance was assessed using the determination  
293 coefficient of calibration ( $R_c^2$ ) and validation ( $R_v^2$ ), the root-mean-square error of  
294 validation (RMSEV), the number of latent variables for calibration (LVs), the residual  
295 predictive deviation of validation set (RPD), as described by Nicolai et al. (2007). The  
296 linkable spectral regions of the acceptable PLS models presenting RPD values higher  
297 than 2.5 (Nicolai, Beullens, Bobelyn, Peirs, Saeys, Theron, et al., 2007) were displayed  
298 based on their  $\beta$ - coefficients (Tables 1 and 2).

### 299 3. Results and discussion

#### 300 3.1 Variability of cooked purees based on their MIR Spectra

##### 301 3.1.1 Variability induced by the raw materials

302 According to ANOVA (F-values), fruit thinning applied on apples during their  
303 growth in orchard resulted in a significant variation ( $p < 0.001$ ) of viscosity ( $\eta_{50}$  and  
304  $\eta_{100}$ ), viscoelasticity ( $G'$ ,  $G''$ , yield stress), particle sizes (d4:3 and d3:2) and  
305 biochemical compositions (DMC, SSC, TA, pH, malic acid, sucrose, fructose and AIS)  
306 of the cooked purees. Particularly, the impact of thinning on the viscosity, DMC and  
307 SSC of purees was higher than the effect of post-harvest storage at 4°C (Table S1).  
308 Purees processed from thinned apples (Th+) had higher viscosity values ( $\eta_{50}$  and  $\eta_{100}$ )  
309 and bigger particle sizes (d4:3) than those from the non-thinned apples (Th-), observed  
310 after the three months of cold storage (T3 and T6) (Buegy, Rolland-Sabaté, Leca, &  
311 Renard, 2020). Moreover, an intensive decrease of average particle sizes (d 4:3) was  
312 observed in the purees cooked with the apples stored one month at 4°C (T1) for both  
313 ‘thinning’ (Th+) and ‘non-thinning’ (Th-) treatments. PCA applied on the spectra of  
314 cooked purees in 2017 showed a good ability to detect the effects of treatments applied  
315 on raw apples (fruit thinning and storage periods) (Figure 3a and 3b). The effect of  
316 thinning on the first principal component (PC1 90.1%) was much higher than that of  
317 storage on the second principal component (PC2 6.9%), which was in line with our  
318 previous results (Lan, Renard, Jaillais, Leca, & Bureau, 2020). In addition, the increase  
319 of the band at 1022  $\text{cm}^{-1}$  and the decrease of the bands at 1061-1065  $\text{cm}^{-1}$ , attributed to  
320 sucrose and fructose respectively (Bureau, Cozzolino, & Clark, 2019), were the major

321 contributors of the observed discriminations on the two PCs (**Figure 3c and 3d**).

### 322 3.1.2 Variability induced by processing conditions

323 The different grinding speeds affected significantly ( $p < 0.05$ ) the viscosity ( $\eta_{50}$   
324 and  $\eta_{100}$ ), viscoelasticity ( $G'$  and  $G''$ ) and particle size (d4:3 and d3:2) of the cooked  
325 purees (**Table S2**). Particularly, the increase of grinding speed significantly ( $p < 0.001$ )  
326 decreased viscosity ( $\eta_{50}$  and  $\eta_{100}$ ), viscoelasticity (yield stress,  $G'$  and  $G''$ ) and particle  
327 sizes (d4:3) which was observed at each tested temperature. From macroscopic images  
328 of purees (data not shown), the larger particles disappeared with increasing grinding  
329 speeds, which was enough to cause a decrease in the puree viscosity ([Espinosa-Muñoz,](#)  
330 [Renard, Symoneaux, Biau, & Cuvelier, 2013](#)). Inversely, the increasing heating  
331 temperatures induced no significant ( $p > 0.05$ ) changes of puree viscosity ( $\eta_{50}$  and  $\eta_{100}$ )  
332 and viscoelasticity (yield stress,  $G'$  and  $G''$ ). The highest heating temperature (95°C)  
333 resulted in a significant ( $p < 0.05$ ) increase of DMC and SSC and a decrease of TA and  
334 malic acid. Consequently, the changes of grinding speed during the puree processing  
335 significantly modified the structural properties and viscoelastic behaviors of purees,  
336 whereas heating temperature affected strongly the biochemical composition of purees.

337 FDA performed on the cooked puree spectra in 2019 successfully classified the  
338 processing changes induced at the different heating temperatures (**Figure 4a**) and  
339 grinding speeds (**Figure 4b**). The samples cooked at 95 °C were well-separated from  
340 the other two conditions (4 factors, 100% of sensitivity and specificity in **Table S3a**),  
341 according to the first factorial component (F1) (**Figure 4a**). The specific bands at 1745  
342  $\text{cm}^{-1}$  and 1539  $\text{cm}^{-1}$  were attributed to the increase of soluble pectins, probably in  
343 relationship with their solubilization in puree serum from apple cell walls, enhanced  
344 with the increasing heating temperature ([Liu, Renard, Rolland-Sabaté, Bureau, & Le](#)  
345 [Bourvellec, 2020](#)). Moreover, the negative peaks at 1057  $\text{cm}^{-1}$  and 998  $\text{cm}^{-1}$  could be  
346 due to the hydrolysis of sucrose during thermal processing, thus resulting in the increase  
347 of fructose (1022  $\text{cm}^{-1}$ ) and glucose (1107  $\text{cm}^{-1}$ ) contents.

348 The three different grinding levels could be discriminated according to the first two  
349 factorial components (F1 and F2) (**Figure 4b**), especially for the highest grinding speed  
350 at 3000 rpm ('G3' in **Figure 4b**) (4 factors, over 85.19% of specificity and sensitivity

351 in **Table S3b**). The intensive negative spectral peaks at 1558, 1539-1541, 1508 and  
352 1458  $\text{cm}^{-1}$  along both the two discriminant factors (F1 and F2 in **Figure 4d and 4e**)  
353 were all located in the region between 1450  $\text{cm}^{-1}$  and 1600  $\text{cm}^{-1}$ , which has been already  
354 attributed to the changes of particle size and rheological behavior after apple puree  
355 mechanical refining in a previous experiment (Lan, Renard, Jaillais, Leca, & Bureau,  
356 2020). These peaks indicated the decrease of particle size (d4:3 and d3:2) and viscosity  
357 of purees with increasing grinding speeds, which was in line with our reference  
358 measurements (**Table S2**) and Espinosa et al. (2011).

359 Briefly, MIR technique could detect several kinds of variability sources such as  
360 thinning practices during fruit cultivation, cold storage and processing conditions  
361 (temperature and grinding) in the cooked purees. In addition, the spectral region 1450-  
362 1750  $\text{cm}^{-1}$  was validated as being a reliable analytical signal of processing linked to the  
363 textural and rheological changes in purees.

### 364 **3.2 Prediction of quality traits of cooked purees by MIRS**

365 For all developed PLS models, as expected the decreases of determination  
366 coefficients between the calibration set ( $R_c^2$ ) and the validation set ( $R_v^2$ ) were observed  
367 in **Table 1**. According to RPD values over 2.5 (Nicolai, Beullens, Bobelyn, Peirs, Saeys,  
368 Theron, et al., 2007), prediction was acceptable to good (RPD from 2.6 to 3.3) for  
369 viscosity ( $\eta_{50}$  and  $\eta_{100}$ ), average particle sizes (d4:3), SSC, TA, pH values and malic  
370 acid were content in cooked purees by MIRS, taking into account a large variability of  
371 raw apple materials and processing conditions.

372 Apparent puree viscosity at a shear rate value of 50  $\text{s}^{-1}$  ( $\eta_{50}$ ), which has been  
373 described to be the highly correlated with the in-mouth texture perception of fluid food  
374 (Chen & Engelen, 2012), could be predicted by MIRS with a  $R_v^2$  of 0.87 and a RPD of  
375 3.2. MIR prediction of apparent puree viscosity at a single shear rate value of 100  $\text{s}^{-1}$   
376 ( $\eta_{100}$ ) ( $R_v^2 = 0.85$ , RPD= 3.0) observed here were much better than its prediction by  
377 NIRS (RPD = 1.3) (Lan, Jaillais, Leca, Renard, & Bureau, 2020), These results  
378 evidenced the possibility of MIRS to estimate puree viscosity. For the two apparent  
379 puree viscosity values measured at  $\eta_{50}$  and  $\eta_{100}$ , the main wavenumber regions at 1718-  
380 1730  $\text{cm}^{-1}$  and 1618-1678  $\text{cm}^{-1}$  were still observed in our previous work (Lan, Renard,



381 [Jaillais, Leca, & Bureau, 2020](#)). This could validate the application of MIRS to predict  
382 puree viscosity by taking into account not only the raw fruit variability but also the  
383 complex effects of processing conditions. However, the predictions ( $R_v^2 < 0.81$ , RPD  
384  $< 2.1$ ) of the viscoelastic parameters of purees ( $G'$ ,  $G''$  and yield stress) were not precise  
385 enough to estimate the viscoelastic behaviors and the moment when puree starts to flow.  
386 Indeed, heating and grinding affected puree viscoelasticity (SD values of 2362 Pa for  
387  $G'$ , 595 Pa for  $G''$ , 27.1 Pa for yield stress) and resulted in more than twice higher  
388 variations of these parameters than those induced by thinning and cold storage on raw  
389 materials (SD values of 1001 Pa for  $G'$ , 234 Pa for  $G''$  and 12.9 Pa for yield stress).  
390 These new prediction accuracies of the viscoelastic parameters of purees ( $G'$ ,  $G''$  and  
391 yield stress) were not as good as our previous ones by MIRS ([Lan, Renard, Jaillais,](#)  
392 [Leca, & Bureau, 2020](#)), but could be more robust to be considered for future  
393 applications. MIR coupled with the linear regression (PLS) showed a good performance  
394 ( $R_v^2 = 0.87$ , RPD= 3.1) to evaluate the volume average particle size of purees (d4:3),  
395 but not the surface average particle size (d3:2). Particularly, the most informative  
396 wavenumbers to evaluate puree particle size at 1701-1713  $\text{cm}^{-1}$ , 1655-1668  $\text{cm}^{-1}$  and  
397 1537-1541  $\text{cm}^{-1}$  have been already observed previously to predict puree viscosity, to  
398 discriminate the purees prepared with different grinding speeds (mentioned in **part 3.1**)  
399 and with different refining levels ([Lan, Renard, Jaillais, Leca, & Bureau, 2020](#)). Such  
400 good prediction of puree average particle size (d4:3) could not come from internal  
401 correlations with puree composition such as SSC, DMC or AIS contents because of  
402 their poor correlation ( $R^2 < 0.48$ ), but probably some specific signals needing to be  
403 identified and confirmed. Moreover, we confirmed here the impossibility to predict the  
404 cell wall content directly in puree by MIRS, without any preparation such as freeze-  
405 drying ([Lan, Renard, Jaillais, Leca, & Bureau, 2020](#))

406 A good prediction of global puree quality traits, SSC (RPD= 3.1) and DMC (RPD=  
407 2.9), was obtained with 5 LVs (**Table 1**). The variation of SSC and DMC in purees were  
408 highly correlated ( $R^2 = 0.76$ ), which explained the good estimations of these two  
409 parameters. Their respective fingerprint wavenumbers of SSC and DMC prediction  
410 were similar and detected at 996-1001  $\text{cm}^{-1}$ , 1048-1057  $\text{cm}^{-1}$  and 1109-1112  $\text{cm}^{-1}$ ,



411 corresponding to the variations of sucrose, fructose and glucose in purees (Bureau,  
412 Cozzolino, & Clark, 2019). Moreover, the prediction of TA was excellent (RPD = 3.2),  
413 with a limited RMSEV of 7.6 mmol H<sup>+</sup>/kg FW. The typical wavenumber region at  
414 1709-1720 cm<sup>-1</sup> in TA prediction has already been attributed to the C=O vibration of  
415 acid group (Bureau, Quilot-Turion, Signoret, Renaud, Maucourt, Bancel, et al., 2013;  
416 Clark, 2016). Depending on the good correlations between the different contributors of  
417 apple acidity (R<sup>2</sup> = 0.81 between TA and malic acid, R<sup>2</sup> = 0.76 between TA and pH),  
418 MIRS provided an acceptable prediction of pH (R<sub>v</sub><sup>2</sup> = 0.83 and RPD = 2.5) and malic  
419 acid content (R<sub>v</sub><sup>2</sup> = 0.85 and RPD= 2.7). Despite the similar typical fingerprints  
420 observed in the β-coefficients of PLS models of malic acid and pH, the relative lower  
421 RPD values and R<sub>v</sub><sup>2</sup> of pH compared to malic acid were probably due to the low pH  
422 variation. Concerning the main individual sugars, acceptable prediction was obtained  
423 only for fructose (RPD = 2.6), but neither for sucrose (RPD= 1.3) nor for glucose (RPD  
424 = 1.5), which was in line with our previous results (Lan, Renard, Jaillais, Leca, &  
425 Bureau, 2020). The lower concentration of glucose (10.4-25.4 g/kg FW) than the other  
426 individual sugars (34.9-98.7 g/kg FW of fructose, 39.1-118.5 g/kg FW of sucrose) led  
427 to its worse prediction by MIR results. A higher internal biochemical correlation  
428 between the major compounds (SSC, TA) and fructose (R<sup>2</sup> = 0.79 for SSC and fructose,  
429 R<sup>2</sup> = 0.76 for TA and fructose) in apple purees might explain the better prediction of  
430 fructose than the one of sucrose (R<sup>2</sup> = 0.58 for SSC and sucrose, R<sup>2</sup> = 0.44 for sucrose  
431 and TA).

432 Briefly, MIR technique can provide a simultaneous and robust estimation of  
433 biochemical compositions (dry matter, soluble solids, titratable acidity, pH, malic acid  
434 and fructose), rheological behaviors (viscosity at η<sub>50</sub> and η<sub>100</sub>) and particle size (d<sub>4:3</sub>)  
435 of apple purees, taking into account the large variability along the apple puree  
436 production chain (agricultural practices, post-harvest storage and processing  
437 conditions).

### 438 **3.3 Reconstructed spectra for prediction of puree quality traits**

439 In this part, MIR prediction models were developed using the reconstructed spectra  
440 of the calibration set of cooked purees (**Tc**), only done for the well-predicted parameters

441 mentioned in **part 3.2**, which were  $\eta_{50}$  and  $\eta_{100}$ , d4:3, SSC, DMC, TA, pH, malic acid  
442 and fructose. Then, these models were applied on the validation reconstructed spectra  
443 of the cooked purees (***Tv***).

444 Overall, based on the PLS regression applied on the puree reconstructed spectra,  
445 acceptable predictions were obtained ( $RPD > 2.5$ ) for rheological ( $\eta_{50}$ ,  $\eta_{100}$ ), structural  
446 (d4:3) and global biochemical (SSC, DMC, TA) parameters (**Table 2**). In contrast,  
447 predictions appeared not acceptable for malic acid ( $RPD = 2.3$ ), fructose ( $RPD = 1.7$ )  
448 and pH ( $RPD = 2.1$ ). Compared to the previous prediction from the real puree spectra  
449 (**Table 1**), lower  $R_v^2$  and higher LVs have been generally obtained for all parameters  
450 giving some lower prediction performance (**Table 2**). Particularly, the use of the  
451 reconstructed spectra showed a good ability to predict puree viscosity parameters ( $\eta_{50}$   
452 and  $\eta_{100}$ ) with  $R_v^2 > 0.82$ ,  $RPD > 2.5$  and prediction errors (RMSEV) of 0.21 Pa.s and  
453 0.10 Pa.s for  $\eta_{50}$  and  $\eta_{100}$ , respectively. These results were close to those from the real  
454 spectra of purees (**Table 1**). The fingerprint wavenumbers used in the PLS models were  
455 similar for both reconstructed and real spectra, mainly 1718-1734  $\text{cm}^{-1}$ , 1616-1336  $\text{cm}^{-1}$   
456 and 1547-1553  $\text{cm}^{-1}$  as described in **Part 3.2**. Although a relative lower  $R_v^2$  and RPD  
457 ( $R_v^2 = 0.84$  and  $RPD = 2.6$ ) were obtained for particle size (d4:3) compared to the results  
458 on the real puree spectra (**Table 1**), the consistent fingerprints were highly related to  
459 the puree texture such as 1701-1715  $\text{cm}^{-1}$ , 1537-1541  $\text{cm}^{-1}$  and 1101-1107  $\text{cm}^{-1}$ . These  
460 prediction performances revealed for the first time the possibility to evaluate the  
461 variation of averaged particle sizes in the cooked purees based on the MIR information  
462 of the corresponding raw apple homogenates. Considering the other global quality  
463 parameters, acceptable predictions were obtained for SSC ( $R_v^2 = 0.85$  and  $RPD = 2.8$ )  
464 and DMC ( $R_v^2 = 0.84$  and  $RPD = 2.6$ ) contents. The specific wavenumbers in the ranges  
465 997-1001  $\text{cm}^{-1}$  and 1048-1057  $\text{cm}^{-1}$  for sucrose and in the ranges 1009-1112  $\text{cm}^{-1}$  for  
466 fructose mainly contributed to the PLS models for both reconstructed and real spectra.  
467 These ranges have been already mentioned to be linked to these sugars ([Bureau,  
468 Cozzolino, & Clark, 2019](#)), which are the main ones in apples. For acidity, the  
469 reconstructed spectra gave an excellent prediction of TA ( $R_v^2 = 0.86$  and  $RPD = 2.9$ ),  
470 using the spectral regions between 1709-1720  $\text{cm}^{-1}$  of the typical C=O absorption

471 (Clark, 2016). Consequently, PLS applied on the reconstructed MIR spectra calculated  
472 from the spectra of raw apple homogenates showed the possibility to directly predict  
473 the viscosity, averaged particle sizes, SSC, DMC and TA of cooked purees.

474 Several initial attempts have been tested to monitor the quality of cooked food from  
475 infrared information of their raw materials with the objectives to predict the texture of  
476 cooked poultry pectoralis major muscles (Meullenet, Jonville, Grezes, & Owens, 2004),  
477 of cooked rice (Windham, Lyon, Champagne, Barton, Webb, McClung, et al., 1997)  
478 and of apple purees (Lan, Jaillais, Leca, Renard, & Bureau, 2020). In these studies, the  
479 spectra matrix of the raw materials and the reference data of the corresponding  
480 processed materials were used to calibrate models. The predictions thus obtained are  
481 mainly due to the strong internal correlations of quality traits between materials before  
482 and after processing, which could provide semi-quantitative prediction accuracy for  
483 practical uses. However, the internal correlations of quality traits during fruit processing  
484 still remain unreliable when using a large variability of raw materials and various  
485 industrial processing systems (Lan, Jaillais, Leca, Renard, & Bureau, 2020). Further,  
486 such a direct modelling method requires a necessary step of acquisition of the infrared  
487 information on raw material batches for each processing condition, in order to obtain  
488 the same matrix sizes of spectra and reference data for calibration.

489 Here, a potential strategy has been firstly proposed to build reconstructed MIR  
490 spectra of processed purees from the spectra of raw apple homogenates using a spectral  
491 transfer method. The high consistency of the specific fingerprints used in the PLS  
492 models obtained for both the real spectra and the reconstructed spectra, confirmed our  
493 choice for this modelling strategy. Compared to the direct modelling method, a great  
494 advantage of using spectral transfer strategy is that the calibration dataset only needs  
495 the infrared information and reference data of several processed purees and just a  
496 limited number of spectra of corresponding raw apples. For example, in our dataset of  
497 2019, the reconstructed spectra of 27 different processed purees could be transferred  
498 from only 3 corresponding spectra of the same apple batches.

499 After a simple scanning of raw apple homogenates by MIRS, our models revealed  
500 the possibility to i) predict the quality of apple purees, such as viscosity, SSC and TA

501 using a standard processing recipe (95 °C for 5 mins and grinding at 1500 rpm), even  
502 though a large variability of raw apples was used (different fruit thinning and cold  
503 storage periods); and ii) to monitor and anticipate the organoleptic properties of cooked  
504 purees under different processing strategies, which is relevant for the processors and  
505 market. For example, a higher viscosity and acidity in-mouth feeling (predicted  $\eta_{50} =$   
506  $1.42 \pm 0.09$  Pa.s, predicted TA =  $65.8 \pm 3.5$  meq/kg FW) were predicted with the recipe  
507 at 83 °C for 30 min and grinding speed of 1000 rpm than with the recipe at 95 °C for  
508 30 min and grinding speed of 3000 rpm (predicted  $\eta_{50} = 0.98 \pm 0.14$  Pa.s, predicted  
509 TA =  $56.4 \pm 4.5$  meq/kg FW).

## 510 **Conclusion**

511 As far as we know, this is the first study that shows the ability of MIRS to estimate  
512 the quality of processed fruit products taking into account a large variability coming  
513 from agricultural practices, post-harvest storage and processing conditions along the  
514 whole processing chain. MIR technique provided reliable assessment of viscosity,  
515 averaged particle sizes and major compositions (SSC, DMC, TA and malic acid) of  
516 apple purees.

517 Further, a simple spectroscopic transfer method (direct standardization) was  
518 applied for the first time to develop the reconstructed spectra of purees from their  
519 corresponding spectra of raw apple homogenates. MIRS coupled with PLS regression  
520 obtained acceptable predictions of TA, DMC, SSC, viscosity ( $\eta_{50}$  and  $\eta_{100}$ ) and  
521 averaged particle sizes of the final puree based on their reconstructed spectra. With a  
522 simple scanning of raw apple homogenates, MIR technique opens the possibility to i)  
523 predict the quality of final purees under a standard processing procedure, which is  
524 beneficial for fruit processing sustainability; and even ii) to monitor the texture and  
525 tastes of purees under different processing conditions for a better management.

526

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534

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- 634



635 **Figure captions:**

636 **Figure 1.** Experimental scheme for apple production, puree preparation and the sample  
637 characterization by infrared spectroscopy and reference measurements.

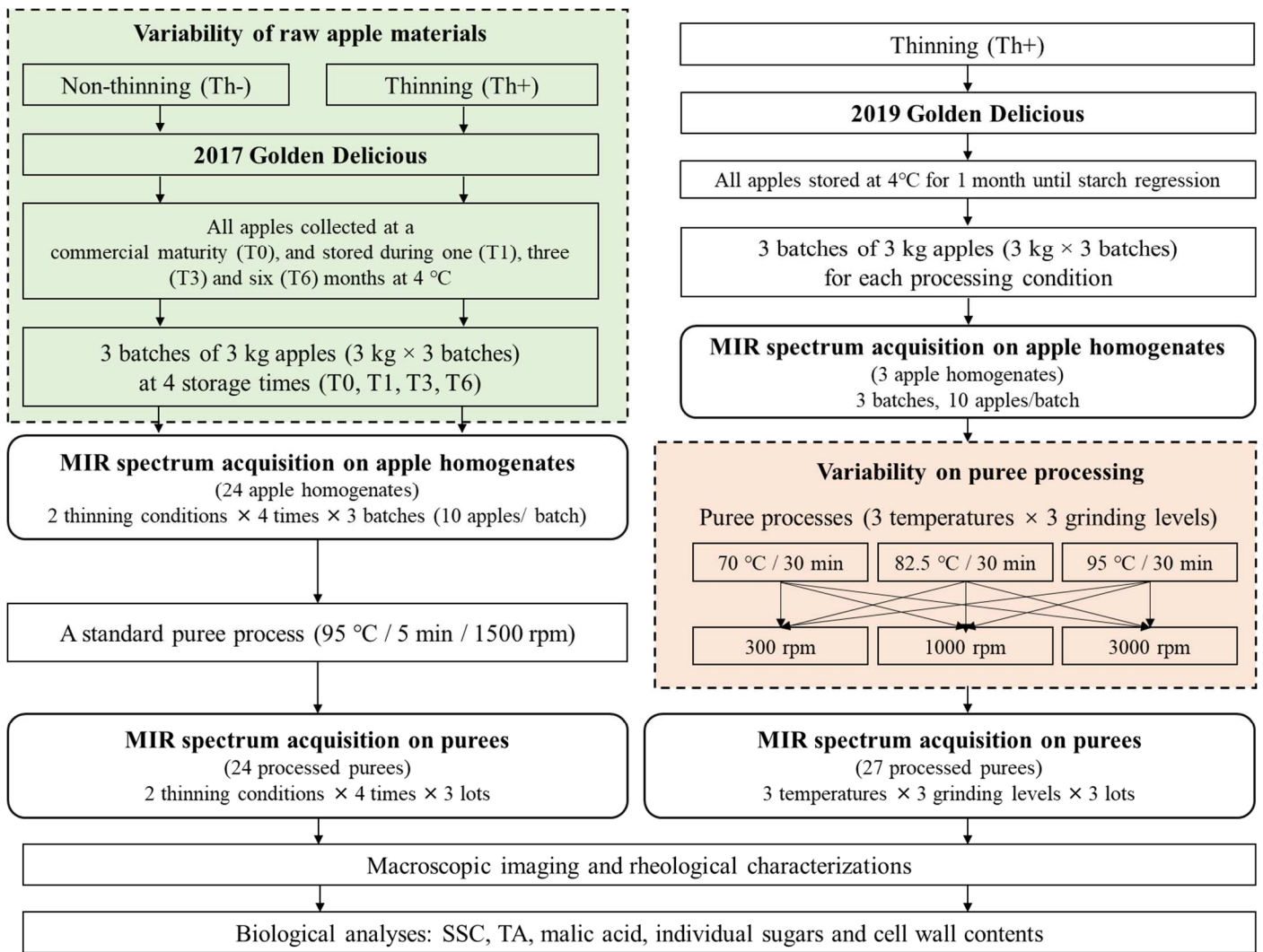
638 **Figure 2.** Overview of the applied methodology to exploit reconstructed MIR spectra  
639 of purees and multivariate regression.

640 **Figure 3.** Principal Component Analysis on the SNV pre-treated MIR spectra (900-  
641 1800  $\text{cm}^{-1}$ ) of purees cooked with thinned (Th+) and non-thinned (Th-) ‘Golden  
642 Delicious’ apples stored at 4°C during 0, 1, 3 and 6 months (T0, T1, T3 and T6): **(a)** the  
643 scores plot of the first two components (PC1 and PC2) related to fruit thinning; **(b)** the  
644 scores plot of the first two components (PC1 and PC2) related to storage periods; **(c)**  
645 the loading plot of PC1; **(d)** the loading plot of PC2.

646 **Figure 4.** Maps of Factorial Discriminant Analysis (FDA) performed on the SNV pre-  
647 treated MIR spectra (900-1800  $\text{cm}^{-1}$ ) of purees cooked with: **(a)** three different  
648 temperatures (70 °C, 83 °C and 95 °C) and **(b)** three grinding speeds (G0 at 300 rpm,  
649 G1 at 1000 rpm and G3 at 3000 rpm); **(c)** the first factorial score (‘F1’) of heating  
650 temperature discrimination; **(d)** the first factorial score (‘F1’) of grinding discrimination;  
651 **(e)** the second factorial score (‘F2’) of grinding discrimination.

652 **Figure S1.** Overview of MIR spectra pre-processing, direct standardization (SD) and  
653 multivariate regression

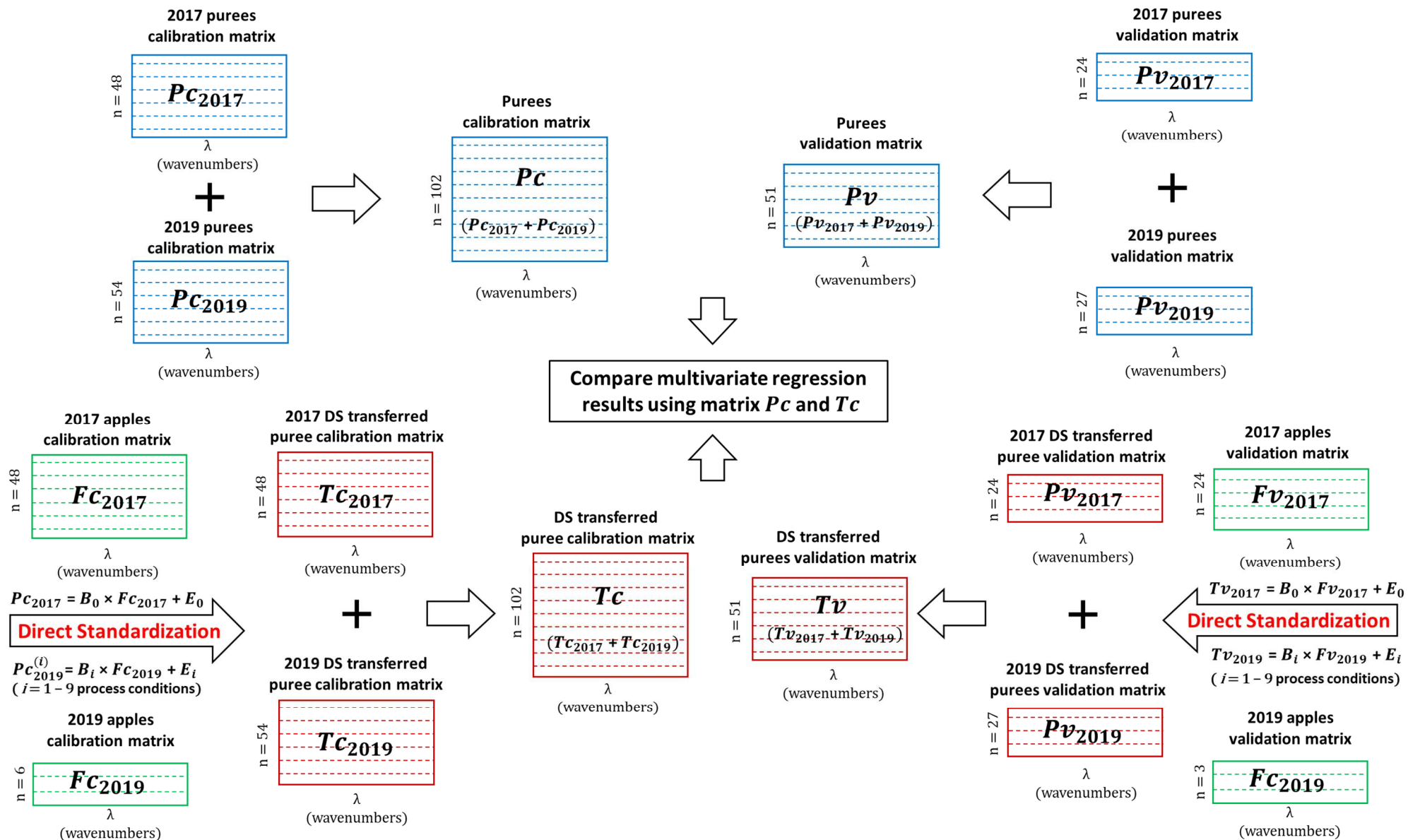
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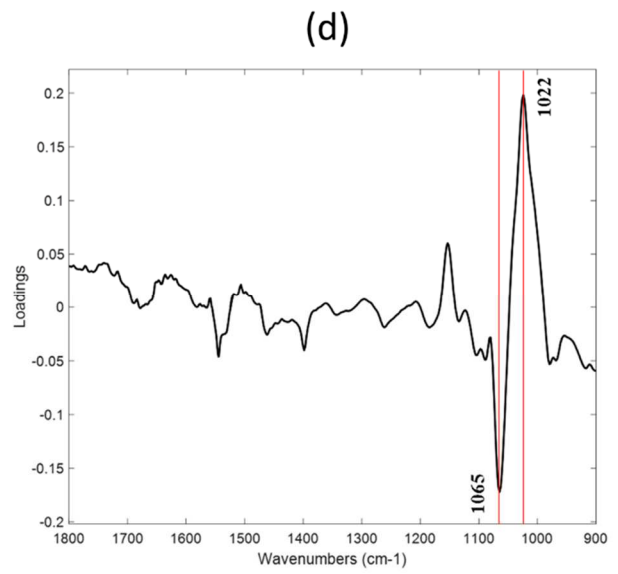
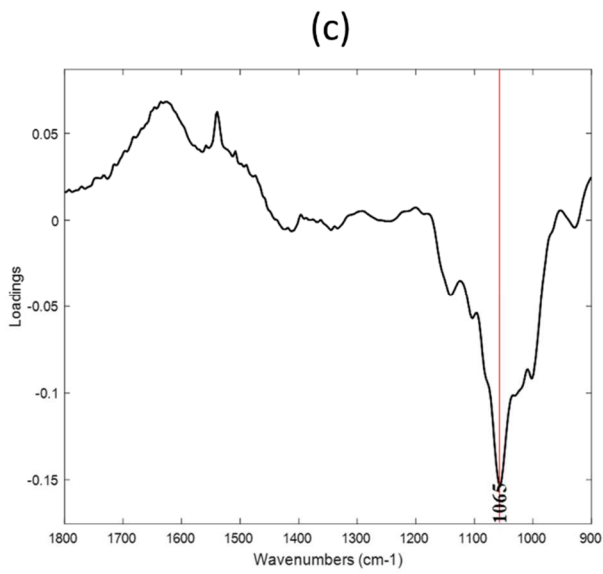
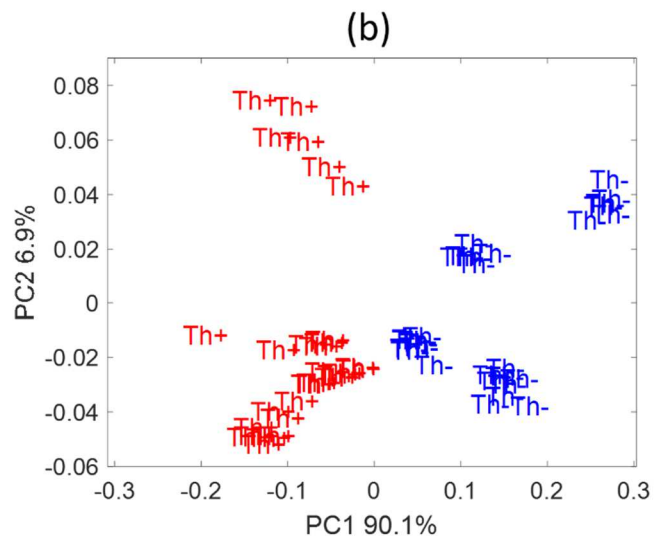
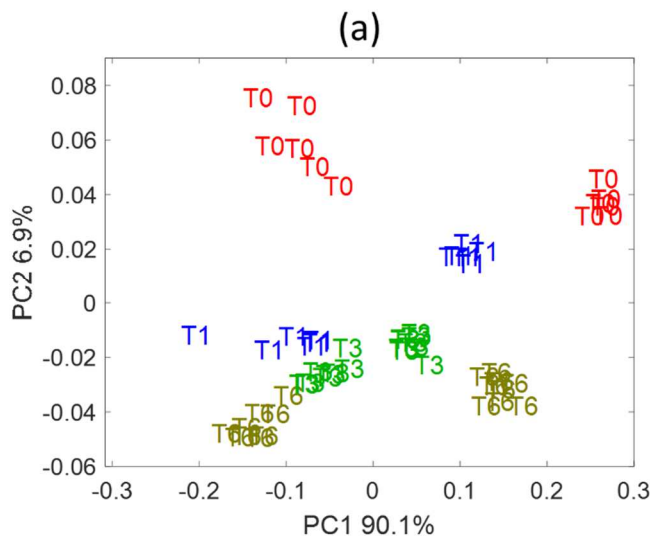
**Figure 1**



657

658

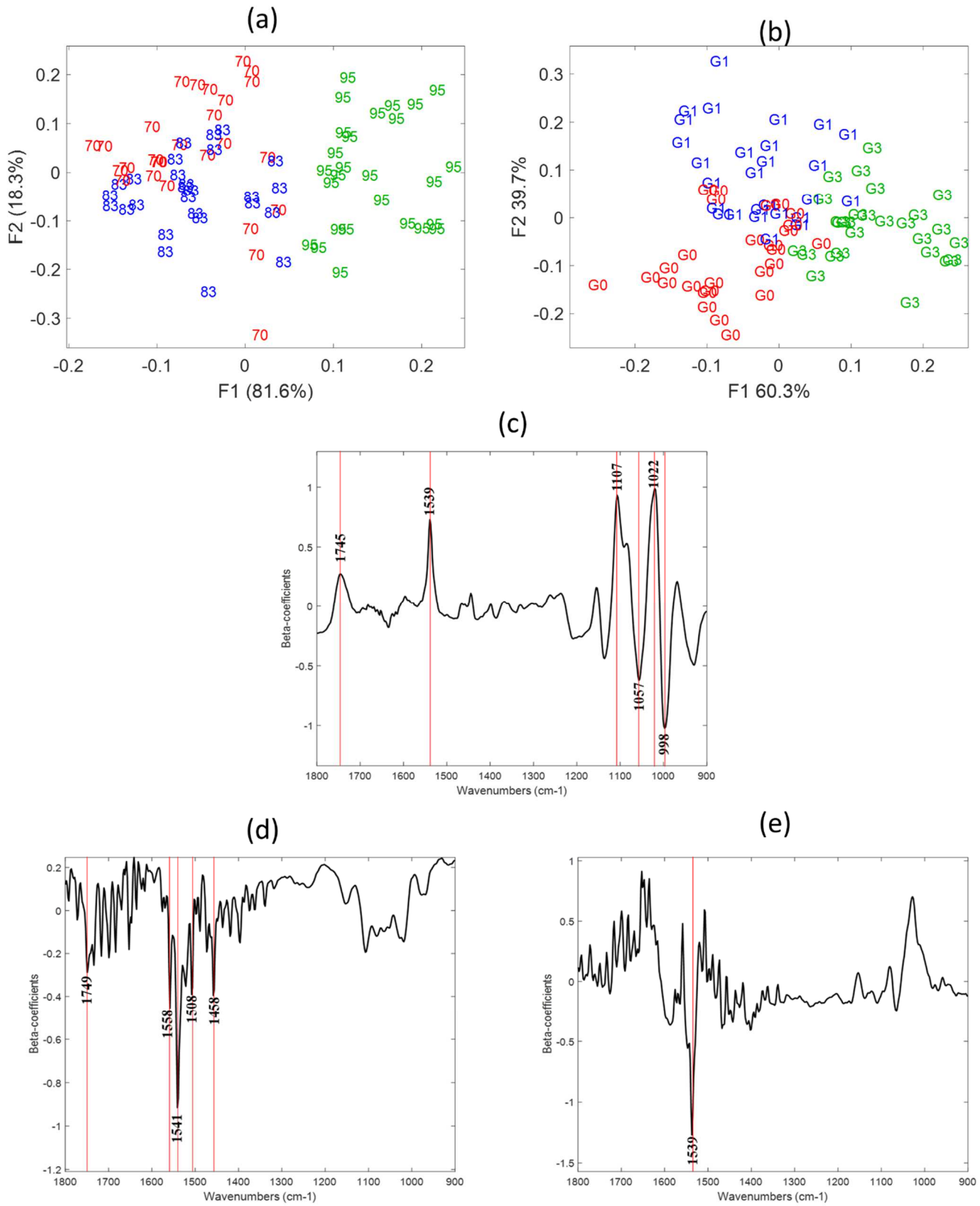
Figure 2



659

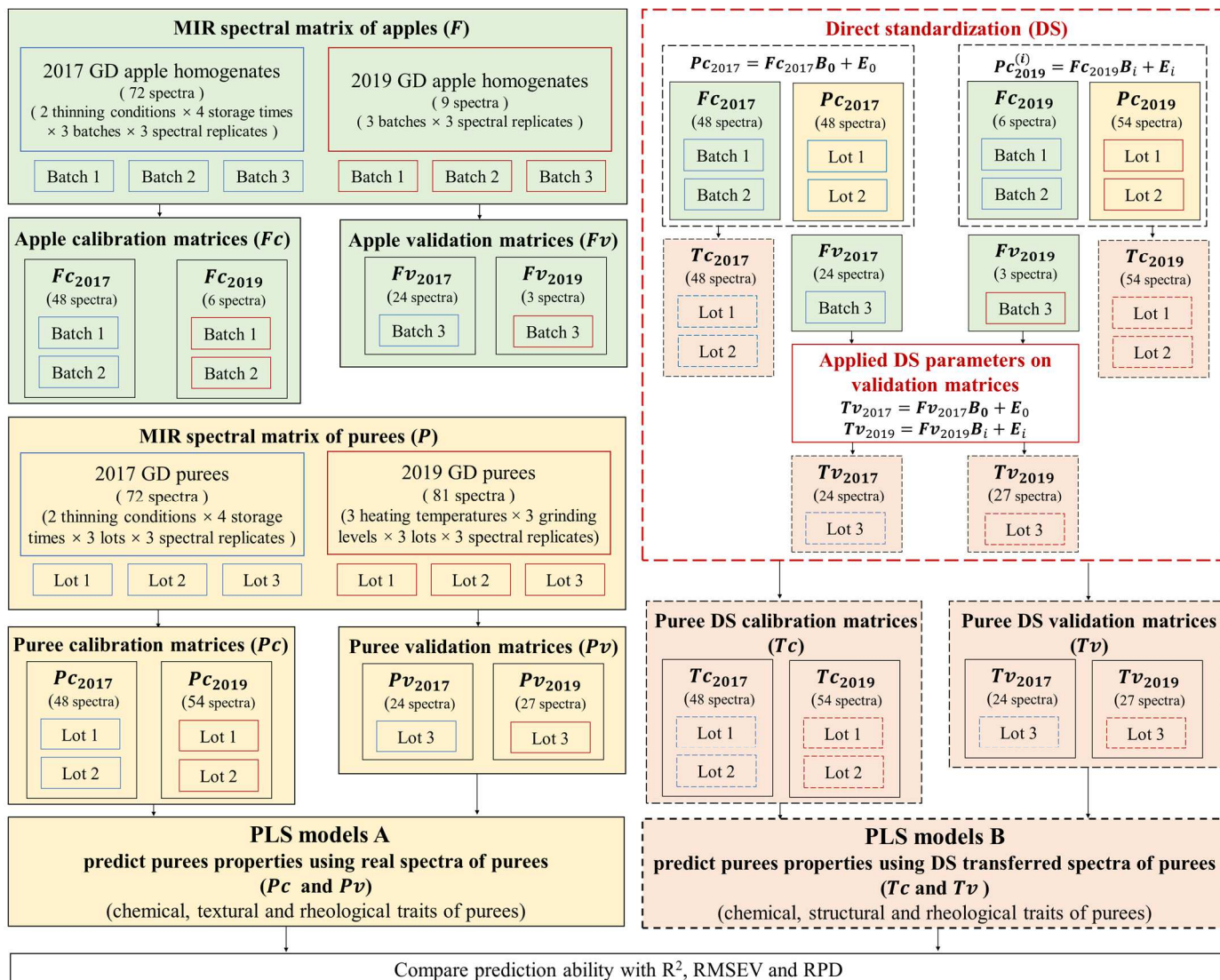
660

**Figure 3**



661

662 **Figure 4**



663

664

Figure S1

665 **Table 1** Prediction of biochemical, structural and rheological properties of apple purees using PLS regression based on their MIR spectra between 900-1800 cm<sup>-1</sup>  
 666 <sup>1</sup>.

Parameter	Range	SD	R <sub>c</sub> <sup>2</sup>	R <sub>v</sub> <sup>2</sup>	RMSEV	RPD	LVs	Linkable regions (cm <sup>-1</sup> )
η 50	0.57-2.28	0.39	0.91	0.87	0.19	3.2	7	1780-1788, 1718-1734, 1659-1678, 1636-1616, 1549-1558, 1157-1163
η 100	0.26-1.22	0.27	0.89	0.85	0.07	3.0	8	1780-1788, 1718-1734, 1659-1678, 1636-1616, 1549-1558, 1157-1163
AS-G' (Pa)	1069-11154	2362	0.85	0.75	854	2.0	12	/
AS-G'' (Pa)	210-2707	595	0.87	0.73	298	1.9	12	/
yield stress	8.7-131	27.1	0.86	0.81	12.8	2.1	11	/
d 4:3	196-920	197	0.90	0.87	65	3.1	8	1780-1788, 1701-1713, 1649-1653, 1537-1541, 1101-1107, 1032-1043 1011-1026
d 3:2	44-360	60.1	0.76	0.62	41.7	1.4	11	/
AIS (DM)	133.1-193.6	12.4	0.79	0.50	7.6	1.4	10	/
AIS (FW)	21.8-14.1	3.4	0.80	0.50	2.2	1.5	6	/
DMC (g/g FW)	0.15-0.23	0.02	0.87	0.84	0.01	2.9	5	997-1001,1051-1057, 1101-1109
SSC (°Brix)	12.6-18.6	1.9	0.91	0.86	0.6	3.1	5	997-1001,1051-1057, 1101-1109
TA (mmol H <sup>+</sup> /kg FW)	5.1-73.5	25.5	0.89	0.86	7.6	3.2	6	1713-1709, 1105-1109, 1016-1018, 1074-1072, 1038-1042
pH	3.6-4.4	0.2	0.89	0.83	0.1	2.6	7	1713-1709, 1105-1109, 1016-1018, 1074-1072, 1038-1042
malic (g/kg FW)	2.4-7.0	1.2	0.88	0.85	0.4	2.7	6	1721-1709, 1105-1109, 1016-1018, 1074-1072
fructose (g/kg FW)	34.9-98.7	16.0	0.89	0.84	6.1	2.6	9	1709-1713, 1259-1265, 1105-1109, 1074-1080,1038-1042, 1016-1020, 970-974
sucrose (g/kg FW)	39.1-118.5	18.5	0.79	0.64	14.0	1.3	9	/
glucose (g/kg FW)	10.4-25.4	3.6	0.74	0.68	2.4	1.5	7	/

667 Note: Puree spectra and references data from ‘Golden Delicious’ apples, including variability of two different thinning conditions, cold storage (during 0, 1, 3  
 668 and 6 months), three heating temperatures (70, 83 and 95 °C) and three grinding levels (300, 1000, 3000 rpm). All results based on the SNV pre-treated MIR  
 669 spectra at 900-1800 cm<sup>-1</sup>. R<sub>c</sub><sup>2</sup>: determination coefficient of the calibration set; R<sub>v</sub><sup>2</sup>: determination coefficient of the validation set; RPD: the residual predictive  
 670 deviation of validation set; the linkable regions based on the β-coefficients of PLS models with the RPD values higher than 2.5; “/” presented the unacceptable  
 671 results with the RPD values lower than 2.5.

672

673 **Table 2** Prediction of biochemical, structural and rheological properties of apple purees using PLS regression based on their reconstructed MIR spectra of raw  
 674 apple homogenates between 900-1800 cm<sup>-1</sup>.

Parameter	Range	SD	R <sub>c</sub> <sup>2</sup>	R <sub>v</sub> <sup>2</sup>	RMSEV	RPD	LVs	Linkable regions (cm <sup>-1</sup> )
η 50	0.57-2.28	0.39	0.85	0.82	0.21	2.5	8	1720-1734, 1636-1614, 1556-1560, 1547-1533, 1506-1510, 1448-1470, 1157-1169
η 100	0.26-1.22	0.27	0.86	0.83	0.10	2.6	9	1720-1734, 1661-1675, 1636-1616, 1549-1558, 1507-1512, 1445-1468, 1157-1163
d 4:3	196-920	197	0.89	0.84	76	2.6	9	1740-1745, 1701-1715, 1645-1659, 1583-1587, 1537--1541, 1508-1510, 1452-1470, 1100-1112
DMC (g/g FW)	0.15-0.23	0.02	0.87	0.84	0.01	2.6	6	1161-1165, 1101-1107, 1084-1090, 1051-1063, 989-1001
SSC (°Brix)	12.6-18.6	1.9	0.89	0.85	0.7	2.8	5	1101-1112, 1084-1090, 1051-1069, 997-1001
TA (mmol H <sup>+</sup> /kg FW)	5.1-73.5	25.5	0.88	0.86	8.9	2.9	7	1715-1710, 1107-1113, 1082-1086, 1059-1063, 1038-1042, 1001-993
pH	3.6-4.4	0.2	0.84	0.79	0.1	2.1	8	1715-1709, 1105-1110, 1016-1018, 1074-1072, 1038-1042
malic (g/kg FW)	2.4-7.0	1.2	0.87	0.82	0.6	2.3	9	1713-1709, 1105-1109, 1080-1088, 1058-1064, 1016-1018, 1001-998
fructose (g/kg FW)	34.9-98.7	15.0	0.82	0.72	8.9	1.7	11	/

675 Note: Puree spectra and references data from ‘Golden Delicious’ apples, including variability of two different thinning conditions, cold storage (during 0, 1, 3  
 676 and 6 months), three heating temperatures (70, 83 and 95 °C) and three grinding levels (300, 1000, 3000 rpm). All results based on the SNV pre-treated MIR  
 677 spectra at 900-1800cm<sup>-1</sup>. R<sub>c</sub><sup>2</sup>: determination coefficient of the calibration set; R<sub>v</sub><sup>2</sup>: determination coefficient of the validation set; RPD: the residual predictive  
 678 deviation of validation set; the linkable regions based on the β-coefficients of PLS models with the RPD values higher than 2.5; “/” presented the unacceptable  
 679 results with the RPD values lower than 2.5.

680



**Table S1** Biochemical, structural and rheological data of apple purees and ANOVA results.

Fruit thinning	Storage periods	$\eta_{50}$ Pa.s	$\eta_{100}$ Pa.s	G' Pa	G'' Pa	Yield stress Pa	d 4:3 -	d 3:2 -	DMC g/g FW	SSC °Brix	TA mmol H+/kg FW	glucose g/kg FW	fructose g/kg FW	sucrose g/kg FW	malic acid g/kg FW	pH	AIS mg/g FW	AIS mg/g DW	
Th-	T0	1.28	0.77	3127.8	626.7	47.5	909.9	251.5	0.19	13.4	58.1	18.9	50.5	66.7	4.5	3.7	164.5	31.6	
	T1	1.13	0.70	1960.2	466.7	21.9	694	351.9	0.19	15.0	54.4	15.4	49.4	59.1	2.8	3.8	147.2	27.6	
	T3	0.87	0.55	1849	453	13.9	339.8	205.9	0.20	14.1	46.7	18.6	84.1	84.8	3.6	4.0	140.0	27.3	
	T6	0.92	0.50	1816	427	14	316.1	223.6	0.19	13.8	26.8	23.0	85.1	77.3	2.7	4.4	145.7	27.6	
Th+	T0	1.75	0.97	3375.1	816.4	52.1	831.6	231.6	0.21	15.5	70.9	23.5	85.3	64.4	5.5	3.6	163.3	33.9	
	T1	1.54	0.94	2783.7	639.5	25.2	489	261.8	0.21	17.6	69.3	16.8	80.3	115.9	5.6	3.8	150.9	31.9	
	T3	1.25	0.70	2517.6	609	22.3	405.1	228.3	0.22	16.9	59.9	13.8	88.0	102.5	4.9	3.8	143.3	31.6	
	T6	1.60	0.88	3168.2	751.7	33.9	393.5	255.1	0.23	17.5	34.7	23.8	95.7	44.0	3.6	4.3	150.3	34.8	
Storage time	significance	***	***	***	***	***	***	***	**	**	***	***	***	***	***	***	***	ns	*
	F-values	20.4	13.6	24.7	15.0	72.8	216.1	41.5	6.6	8.3	279.4	74.7	76.2	38.5	13.8	436.3	1.8	4.3	
Fruit thinning	significance	***	***	***	***	***	***	*	***	***	***	ns	***	**	***	***	**	**	
	F-values	138.2	61.5	67.3	91.5	29.6	47.2	5.5	157.7	115.7	176.9	1.3	187.8	13.8	57.9	48.8	15.9	10.3	

Data expressed in fresh weight (FW) or dry weight (DW); values correspond to the mean of 3 puree replications (3 kg per replication). Raw apples were stored at 4°C: from harvest (T0)

and during one (T1), three (T3) and six months (T6). Two conditions of fruit load during cultivation: non-thinning with 100% number of apples (Th-) and thinning with 50% number of

apples (Th+) per tree. In grey, two way- ANOVA results obtained for Golden Delicious purees. ns, \*, \*\*, \*\*\*: Non significant or significant at P < 0.05, 0.01, 0.001 respectively.

**Table S2** Biochemical, textural and rheological data of apple purees and results of Kruskal-Wallis non-parametric test.

Temperatures	Grinding speeds	$\eta_{50}$	$\eta_{100}$	G'	G''	Yield stress	d 4:3	d 3:2	DMC	SSC	TA	glucose	fructose	sucrose	malic acid	pH	AIS	AIS
°C	rpm	Pa.s	Pa.s	Pa	Pa	Pa	-	-	g/g FW	°Brix	mmol H+/kg FW	g/kg FW	g/kg FW	g/kg FW	g/kg FW		mg/g FW	mg/g DW
70	300	1.27	0.89	9629.8	2389.5	97.7	583.8	103.6	0.17	13.8	63.6	16.1	67.9	70.9	6.3	3.9	26.8	158.0
	1000	1.42	0.91	3295.4	768.8	38.8	633.7	274.8	0.16	13.8	67.8	18.0	66.2	76.6	6.4	3.9	28.0	171.4
	3000	0.64	0.40	1111.3	215.6	10.2	353.5	207.6	0.17	14.4	69.1	17.3	65.5	86.0	6.6	3.9	28.1	165.1
83	300	1.23	0.93	8437.5	2078.9	97.9	553.0	212.8	0.18	14.9	59.9	14.6	67.7	70.6	5.8	3.8	29.5	166.7
	1000	1.38	0.87	3036.9	764.4	35.6	647.8	324.8	0.16	13.4	69.8	17.4	71.9	75.2	5.2	3.9	25.6	159.6
	3000	0.91	0.54	1312.2	259.9	11.8	297.4	192.4	0.17	14.8	70.3	16.6	66.8	76.1	5.7	3.9	28.2	162.6
95	300	1.93	1.16	3708.2	1101.3	30.0	492.9	262.1	0.17	14.9	60.2	17.0	72.6	66.9	4.8	3.9	27.9	160.8
	1000	1.44	0.84	1955.4	522.2	16.6	332.9	209.8	0.17	14.9	64.1	17.8	71.3	64.5	5.1	3.9	26.2	157.3
	3000	1.07	0.63	1399.4	362.2	14.0	206.4	153.2	0.17	14.8	62.0	18.9	69.2	65.8	5.4	3.8	26.2	154.1
Temperature	significances	<i>ns</i>	<i>ns</i>	<i>ns</i>	<i>ns</i>	<i>ns</i>	*	<i>ns</i>	*	*	*	*	*	**	**	<i>ns</i>	<i>ns</i>	<i>ns</i>
	F-values	<i>4.1</i>	<i>1.3</i>	<i>0.9</i>	<i>0.4</i>	<i>1.5</i>	<i>7.0</i>	<i>1.2</i>	<i>6.3</i>	<i>6.8</i>	<i>8.4</i>	<i>6.1</i>	<i>8.9</i>	<i>9.1</i>	<i>10.2</i>	<i>2.1</i>	<i>2.3</i>	<i>4.2</i>
Grinding speeds	significances	**	***	***	***	***	**	**	<i>ns</i>	<i>ns</i>	<i>ns</i>	<i>ns</i>	<i>ns</i>	<i>ns</i>	<i>ns</i>	<i>ns</i>	<i>ns</i>	<i>ns</i>
	F-values	<i>10.9</i>	<i>17.2</i>	<i>21.6</i>	<i>22.6</i>	<i>19.4</i>	<i>13.7</i>	<i>9.2</i>	<i>1.1</i>	<i>2.8</i>	<i>1.4</i>	<i>0.4</i>	<i>0.1</i>	<i>1.4</i>	<i>0.2</i>	<i>1.3</i>	<i>0.4</i>	<i>0.2</i>

687 Data expressed in fresh weight (FW) or dry weight (DW); values correspond to the mean of 3 puree replications (3 kg per replication). Processing conditions variations were: three  
688 heating temperatures at 70°C, 83°C and 95°C for 30 min, and three grinding speeds at 300, 1000 and 3000 rpm at each temperature. In grey, Kruskal-Wallis results obtained on Golden  
689 Delicious purees. ns, \*, \*\*, \*\*\*: Non significant or significant at P < 0.05, 0.01, 0.001 respectively.

690 **Table S3** The results of sensitivity (in blue cells) and specificity (in yellow cells) from: **(a)** the FDA discrimination (4 factors) of three different heating  
 691 temperatures; and **(b)** the FDA discrimination (4 factors) of three different grinding speeds.

692 **(a)**

Temperatures (°C)	70	83	95
70	/	76.67%	100%
83	83.33%	/	100%
95	100%	100%	/

693 **(b)**

Grinding speeds (rpm)	300	1000	3000
300	/	75.00%	85.19%
1000	76.92%	/	87.10%
3000	85.19%	100%	/

694

695