

# Pectin degradation accounts for apple tissue fragmentation during thermomechanical-mediated puree production

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1	Pectin degradation accounts for apple tissue fragmentation during thermomechanical-
2	mediated puree production
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16	
17	Abstract
18	The relationship between fruit and puree's characteristics is still poorly understood. In
19	particular, it is not understood how pectin solubilisation and degradation alter the texture of
20	plant-cell dispersions and how a targeted application of processing conditions can be used to
21	design naturally textured food products. Systematic combinations of thermal and mechanical
22	treatments with three different temperatures (70, 83, 95 °C) and grinding speeds (300, 1000,
23	3000 rpm), applied on one-month (T1) and six-months stored (T6) apples, were used to
24	generate apple purees with contrasted structural and textural characteristics. For T1, serum
25	viscosity increased with increasing temperature (8 to 104 mPa.s) with a marked increase in

26 pectin solubilisation (1 to 6 mg/g serum). Pectin macromolecular size and

27 (arabinose+galactose)/rhamnose ratio, estimating pectin side chain branching, decreased with 28 temperature. For T6, pectin showed decreased galactose, leading to facilitated cell separation, 29 low serum viscosity (~16 mPa.s) and restricted impact of process conditions on pectin 30 composition and structure. Grinding had limited impact on pectin solubilisation for T1 and T6 31 but strongly impacted particle size (498–1096 µm for T1 or 320–1068 µm for T6) and puree's 32 viscosity (871-1475 mPa.s for T1 or 853-1453 mPa.s for T6). Tissue fragmentation was 33 favoured by temperature increase for T1 and by the maturation of raw apples. Process 34 parameters induced differences in the puree's structure and texture depending on the 35 maturation level of raw apples. The observed changes were linked to pectin degradation and 36 substantial side chain loss.

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*Malus x domestica* Borkh.; Texture; Rheology; Particle size; Cell separation; Polysaccharide
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# 40 **1. Introduction**

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42 Plant-based purees are suspensions of individual cells and cell clusters (pulp) dispersed in an 43 aqueous phase (serum) (Rao, 1992). The texture is an important quality characteristic of plant-44 based dispersions (Szczesniak & Kahn, 1971) driven by particle size distribution, pulp content 45 and serum viscosity (Espinosa et al., 2011: Leverrier, Almeida, Espinosa-Munoz, & Cuvelier, 46 2016; Rao, 1992). These factors can be modulated by applying particular thermal and 47 mechanical treatments on raw material in order to optimise pureed food's textural 48 characteristics without the addition of texture-controlling agents such as starches, gums, and 49 stabilisers. Many studies focused either on the effect of thermal (Anthon, Diaz, & Barrett, 50 2008; Christiaens et al., 2012) or mechanical (Espinosa et al., 2011; Moelants et al., 2012; 51 Moelants et al., 2014) treatments. However, both heating and grinding are complementary 52 during processing since both treatments alter the puree's structure.

The structural characteristics are linked to modifications in pectin structure and composition (Sila et al., 2009). Pectins contribute to intercellular adhesion and cell wall porosity and strength (Carpita & Gibeaut, 1993; Jarvis, 1984). However, these plant cell wall polysaccharides are especially vulnerable to enzymatic and chemical degradation. Indeed, pectin solubilisation during processing induces tissue softening during processing (Van Buren, 1979), thus facilitating subsequent tissue disruption via mechanical treatments.

59 Pectins are complex groups of polysaccharides, comprising homogalacturonan (HG), 60 rhamnogalacturonan I (RG I) and II (RG II). HG is composed of a linear chain of α-1,4-linked 61 galacturonic acids, which can be methyl-esterified at the C6 position. The degree of 62 methylation (DM) and the distribution of ester groups over the HG backbone are crucial since 63 sequences of several consecutive non-esterified galacturonic acids can induce cross-links with 64 calcium ions (Kohn & Luknár, 1977). This mechanism may contribute to cell-cell adhesion in 65 the middle lamella. Endogenous pectin methylesterase (PME) can demethoxylate the HG backbone, which can be cross-linked by calcium ions and cause an increase in cell adhesion 66 67 and texture (Waldron, Smith, Parr, Ng, & Parker, 1997) or be further degraded by 68 polygalacturonase (PG) (Sila et al., 2009), resulting in texture loss. While enzyme activity is 69 rapidly inactivated by heat, chemical reactions are generally promoted. Pectins are susceptible 70 to acid hydrolysis due to the acidic pH of apples (around 3.7) and other fruits. On the other 71 hand, β-elimination is less critical during fruit-based food production (Waldron, Parker, & 72 Smith, 2003).

Although the most studied changes are reported for HG pectins, RG I domains are also sensitive to heat treatment. RG I consists of a backbone with alternating rhamnose and galacturonic acid residues. Rhamnose residues can be decorated by neutral sugar side chains composed of galactose and/or arabinose (Ridley, O'Neill, & Mohnen, 2001). Arabinans are particularly susceptible to acid hydrolysis, followed by galactans (Green, 1967; Thibault, Renard, Axelos, Roger, & Crepeau, 1993). Interestingly, "debranching" (i.e., loss of arabinans and galactans) was associated with attenuated cell adhesion in apple fruits (Nara, Kato, &
Motomura, 2001; Pena & Carpita, 2004). Additionally, RG II, which accounts for less than
10% of the pectin content, has a galacturonic acid backbone with several complex
oligosaccharide side chains attached to it (Mohnen, 2008; Ndeh et al., 2017).

83 Only a few studies have systematically analysed the combined effect of thermal and 84 mechanical processes on puree's texture (Day, Xu, Oiseth, Lundin, & Hemar, 2010; Lopez-85 Sanchez et al., 2011). Furthermore, no extensive studies have investigated the consequences 86 of pectin degradation (thermal degradation) on mechanical processing. However, 87 modifications in pectin composition and structure are crucial in understanding the impact of 88 processing on plant-based food structure and texture. Herein, we evaluated particle size, pulp 89 wet mass and serum viscosity following the application of different temperature and grinding 90 regimes and elucidated the process-structure-function relationship of pectins and their 91 influence on apple puree texture. As pectin modifications in the raw material linked to post-92 harvest storage alter puree's texture (Buergy, Rolland-Sabaté, Leca, & Renard, 2020), the 93 impact of processing conditions was compared between apples stored for one and six months.

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#### 95 2. Material and Methods

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Apple (*Malus x domestica* Borkh.) cultivar Golden Delicious was grown in Mallemort, France and harvested in September 2018 and 2019, corresponding to the commercial harvest dates. In 2018, apples were chemically thinned using 3 L/ha PRM 12® RP (ethephon, 17 April 2018), 2 L/ha PRM 12® RP (24 April 2018), 3.5 L/ha MaxCel® (6-Benzylaminopurine) and 1.5 kg/ha Rhodofix® (1-naphthalenacetic acid, 30 April 2018) and 3.5 L/ha MaxCel® (4 May 2018). In 2019, apples were thinned with 18 L/ha ATS

<sup>97 2.1.</sup> Plant material

105 (ammonium thiosulphate, 20 April 2019), 0.15 kg/hL Rhodofix® (27 April 2019) and 5 L/ha
106 MaxCel® (4 May 2019).

Apples harvested in 2018 and 2019 were stored for six months (T6) and one month (T1), respectively, at 4 °C in a normal atmosphere. One day before processing, apples were divided into two equal groups. The first batch was used to isolate the alcohol-insoluble solids (AIS) (see section 2.4.1), the second batch was processed into a puree.

111

# 112 2.2. Puree preparation

113

Approximately 3 kg of apples were cored, cut into 12 pieces and processed under vacuum using a cooker-cutter (RoboQbo Qb8-3, RoboQbo, Bentivoglio, Italy), equipped with two micro-serrated cutting blades and a mixing blade. T1 and T6 apples were processed under identical conditions (Supplementary Fig. S1). Each temperature (70, 83, 95 °C) was combined with a blade rotation speed (300, 1000, 3000 rpm), resulting in nine different treatments. Each process was conducted in triplicate, and each repetition was spaced by one week due to the time needed for sample characterisation.

Since the temperature increase was longer for higher temperatures (difference of 140 s between 70 and 95 °C), a low blade rotation speed of 100 rpm was applied during this period. This step was employed to mix the apples without grinding them. Upon reaching the working temperature, we increased the blade rotation speed and maintained this speed for 30 min. The heating effects caused by blending were counteracted by the cooling system of the cookercutter, guaranteeing a constant value ( $\pm 1$  °C) around the indicated process temperature. Purees were not refined, and physicochemical characterisations were carried out directly after

processing once the purees reached room temperature. Analytical measurements were
conducted on thawed samples previously stored at -20 °C.

#### 131 2.3. *Physico-chemical characterisation*

132

#### 133 2.3.1. Rheology of the purees and sera

134 Rheological analyses of both purees and sera were conducted at 22.5 °C as reported 135 previously (Buergy et al., 2020), a stress-controlled rheometer (Physica MCR301) equipped 136 with a Peltier cell (CPTD-200) and a measuring cylinder (CC27/S) from Anton Paar (Graz, 137 Austria). For purees, the flow curve and amplitude sweep were measured using a vane 138 measuring system (FL100/6W). Rheological analyses were not theoretically adapted for 139 purees containing particles larger than 1 mm, since the measuring system gap was 3.46 mm. 140 Thus, rheological values obtained for purees prepared at 70 and 83 °C and 300 rpm should be 141 treated cautiously.

142 Serum viscosity was measured with a flow curve using a double gap cylinder geometry set143 (DG27).

144

145 2.3.2. Particle size distribution

146 Laser granulometry (Mastersizer 2000, Malvern Instruments, Malvern, UK) was employed to 147 measure the particle size distribution in the puree as described by Buergy et al. (2020). The 148 Malvern's software was used to calculate the averaged size distribution over three repeated 149 measurements on the same sample. Each puree was analysed twice.

150

151 2.3.3. Pulp wet mass (PWM) and water retention capacity (WRC)

Each puree (3 repetitions  $\times$  9 processes) was centrifuged (7690  $\times$  g, 15 min at 15 °C) and separated into pulp and serum. The ratio of the pulp weight to the initial weight of the puree was defined as the PWM and expressed in g/100 g (Espinosa et al., 2011). The WRC of the pulp was defined as the amount of water retained by the pulp's cell wall polysaccharides and expressed in g/g dry weight (Robertson et al., 2000). The ratio of the PWM to the pulp's dry weight was estimated after AIS isolation. The WRC was only analysed for samples processed
at 3000 rpm since these purees represented individual cells. One sample at each temperature
was measured, both for T1 and T6.

160

161 2.4. Analytical

- 162
- 163 2.4.1. Cell wall isolation and serum precipitation

164 Cell wall polysaccharides were extracted as AIS, using the protocol established by Le 165 Bourvellec et al. (2011). This method involves adding 700 mL of ethanol per litre of raw 166 apples to extract the AIS. Three replicates using 10 representative apples were performed, and 167 AIS yields were expressed in mg/g fresh weight (FW).

168 The pulp was washed with water and the AIS were isolated as previously described by Buergy 169 et al. (2020). The pulp's AIS yield was calculated by dividing the dry pulp weight by the 170 initial pulp weight after water-washing and expressed as mg/g FW.

The serum AIS were isolated by alcohol precipitation according to the method of Buergy et al. (2020). The dry sample weight and the initial serum weight ratio provides a rough estimate of the soluble pectin content in the continuous phase. Serum AIS yields are expressed in mg/g serum FW. Since the present study focused on apples stored for one month, the AIS extraction was conducted with all three T1 replicates, but only one T6 sample.

176

# 177 2.4.2. Cell wall polysaccharide analysis

178 After the acid hydrolysis of neutral sugars and the internal standard myo-inositol (Saeman, 179 Moore, Mitchell, & Millett, 1954), the free sugars were derivatised to volatile alditol acetates 180 (Englyst, Wiggins, & Cummings, 1982). Then the samples were applied to a Clarus 500 gas 181 chromatograph (PerkinElmer, Waltham, USA) equipped with a flame ionisation detector 182 (FID) and an OPTIMA® capillary column (30 m  $\times$  0.25 mm i.d., 0.25 µm film thickness, 183 Macherey-Nagel, Düren, Germany), and analysed at 230 °C. Helium was used as the carrier
184 gas.

185 Galacturonic acid (GalA) content in the acid hydrolysate was determined
186 spectrophotometrically using the *m*-hydroxydiphenyl assay (Blumenkrantz & Asboe-Hansen,
187 1973).

188 Methanol was quantified using the stable isotope dilution assay after saponification (Renard 189 & Ginies, 2009). Samples were analysed on a Trace 1300 gas chromatograph (Thermo 190 Scientific, Waltham, USA), equipped with a TG-WaxMS capillary column (30 m  $\times$  0.25 mm 191 i.d., 0.5 µm film thickness, Thermo Scientific, Waltham, USA) and coupled to a ISQ LT 192 single quadrupole mass spectrometer (Thermo Scientific, Waltham, USA).

193 The molar ratio of methanol to GalA gave the degree of methylation (DM) is expressed as a194 percentage (%).

195

#### 196 2.4.3. Starch determination

We used the total starch assay kit K-TSTA (Megazyme, Wicklow, Ireland) to quantify the starch content in the AIS of serum and raw apples. The specified enzyme concentrations were doubled since residual polyphenols in the AIS might reduce enzyme activity. Each sample was analysed in duplicate. All values for AIS, neutral sugars, GalA and methanol were adjusted according to the respective starch content.

202

203 2.4.4. High-performance size-exclusion chromatography coupled to multi-angle laser light
 204 scattering (HPSEC-MALLS) and online viscometry

As described by Buergy et al. (2020), the molar mass and size distribution of soluble pectins were determined on a high-performance size-exclusion chromatography (HPSEC) system coupled to a multi-angle laser light scattering detector (DAWN HELEOS 8+ (Wyatt Technology, Santa Barbara, USA) fitted with a K5 flow cell and a GaAs laser,  $\lambda = 660$  nm), a 209 differential refractive index detector (Shimadzu, Tokyo, Japan), an online viscometer 210 (Viscostar III, Wyatt Technology) and a prominence diode array detector (DAD). Initial 211 concentrations of 2.5 mg AIS/mL (serum) or 10 mg AIS/mL (raw apples) were used to extract 212 soluble pectins directly into the eluent (acetate buffer, 0.2 M, pH 3.6). Samples were eluted at 213 a flow rate of 0.6 mL/min at 40 °C and separated by three PolySep-GFC columns (P3000, 214 P5000 and P6000,  $300 \times 7.8$  mm) and a guard column, all from Phenomenex (Le Pecq, 215 France). The ASTRA® software (Wyatt Technology, version 7.3.2.19 for PC) was used for 216 data treatment as described by Buergy et al. (2020). The weight-average molar mass  $\overline{M}_{w}$ , the z-average intrinsic viscosity  $\overline{[\eta]}_z$  and the z-average viscometric hydrodynamic radius  $\overline{R}_{hz}(v)$ 217 218 were obtained at the summit of the main peak. Each sample was injected once. For T1, 219 samples of the first repetition were not considered since molar mass distribution was 220 significantly different from the other repetitions. This discrepancy was likely due to 221 incomplete starch degradation in these samples.

222

# 223 2.4.5. Nuclear magnetic resonance spectroscopy (NMR)

224 <sup>1</sup>H-NMR was employed to visualise  $\beta$ -elimination products in the serum AIS and was performed according to Tjan, Voragen, and Pilnik (1974). At 4 °C, AIS (5 mg/mL) were 225 solubilised for 1 h in distilled water before adjusting the pH to 6 with NaOH. The samples 226 were centrifuged (4272  $\times$  g, 15 min at 4 °C) to remove possible cell wall remnants. The 227 228 supernatant was freeze-dried before the sample was suspended in D<sub>2</sub>O (0.75 mL) over night at 229 4 °C. The following day, the sample was freeze-dried and suspended in D<sub>2</sub>O as before. The 230 samples obtained were analysed at all of the temperatures (3000 rpm, T1). As a positive 231 control, serum AIS, obtained at 95 °C, 3000 rpm and diluted to 5 mg/mL with distilled water, was heated for 30 min at 100 °C at pH 6. Afterwards, the control sample's pH was readjusted 232 233 to pH 6 and treated in the same way as the samples. Samples and the control were analysed in 234 D<sub>2</sub>O on an NMR spectrometer (Avance III 400 NB, Bruker, Wissembourg, France) equipped with a BBO 5 mm probe. We recorded 1D <sup>1</sup>H spectra at 70 °C. The most significant acquisition parameters included a <sup>1</sup>H 90° pulse of 10.2  $\mu$ s, 128 scans and a recycle delay of 10 s. Water signal presaturation was used to minimise the residual HDO signal.

NMR relaxation was used to monitor the interactions between the <sup>1</sup>H of water and the AIS in samples ground at 3000 rpm for all temperatures. These interactions can be related to the porosity of the system. For these experiments, samples from both T1 and T6 were utilised since they all presented individual cells.

Transverse relaxation ( $T_2$ ) of pulp AIS (100 mg) rehydrated in distilled water and excess water gently removed, was measured at 4 °C on a Bruker Minispec mq20 (0.47 T), equipped with a thermostated <sup>1</sup>H probe, using the Carr-Purcell-Meiboom-Gill pulse sequence. Echo time was 1 ms, 2000 even echoes were collected, and 128 scans were acquired with a recycle delay of 7 s. An inverse Laplace transformation (ILT) was applied to convert the relaxation signals into a continuous distribution of the  $T_2$  relaxation components (Lahaye, Bouin, Barbacci, Le Gall, & Foucat, 2018; Saunders, Bunggyoo, Maes, Akle, & Zahr, 2012).

249

250 2.5. Statistical analysis

251

252 The technological repetitions were spaced by one week, and a complete protocol (temperature 253 × grinding speed) was carried out each week. Analyses were generally conducted once for 254 each of the three repetitions. Exceptions are stated in the text. The Shapiro-Wilk test was used 255 to determine if the results were normally distributed. The Kruskal-Wallis non-parametric test 256 (Kruskal & Wallis, 1952) was employed to assess differences between the samples at the 95% 257 level of significance, using the Microsoft Excel XLSTAT package (Addinsoft, 2020). Pooled 258 standard deviations (PSD) were calculated for each series of repeated measurements using the 259 sum of individual variances weighted by the individual degrees of freedom (Box, Hunter, & 260 Hunter, 1978). The R statistical software (R Core Team, 2018) was used to perform principal

261 component analysis (PCA) and linear regression, using the "FactoMineR" (Lê, Josse, &
262 Husson, 2008) and "stats" packages included in the R statistical software, respectively.

263

#### 264 **3. Results and discussion**

265

266 In a preliminary test (data not shown), purees were prepared at 50 and 70 °C and yielded 267 purees with equivalent textures. It was concluded that the apple enzymes did not sufficiently 268 degrade pectins during processing. Indeed, PG is only present in minimal amounts in apples 269 (Wu, Szakacsdobozi, Hemmat, & Hrazdina, 1993) and is unlikely to impact apple puree's 270 texture. Additionally, apple PME has low activity at pH 3.7 and a D-value of 0.7 min at 60°C 271  $(Z = 9.2^{\circ})$  (Denes, Baron, & Drilleau, 2000), which means that it is inactivated during the 272 come-up time, and at least partially accounts for the unaltered textures of the purees in the 273 preliminary test. Notably, 70 °C was the lowest processing temperature at which we could 274 unequivocally evaluate the impact of the chemical reactions on apple purees. Moreover, since 275 the heat increase speed was identical for all samples during puree processing, PME would 276 have been able to demethylate pectins equally in all purees.

277

# 278 *3.1. Textural characteristics of apple purees*

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Different process conditions led to contrasted textural characteristics of apple purees. Apparent viscosity (Fig. 1A) obtained at 70 °C and 300 rpm had a high standard deviation. This result was due to large apple cell clusters (Supplementary Fig. S2) that were not sufficiently separated by slow grinding. Consequently, the altered rheological values for the purees obtained under these conditions have limited reliability. When these results were not considered, the data show that increasing the grinding speed significantly reduced the puree's viscosity (Supplementary Table S1). While temperature did not have a significant impact, high temperatures increased viscosity, especially at 3000 rpm. Other textural characteristics
such as yield stress, G' and G'' (Supplementary Table S1) were also significantly attenuated
with increased grinding but were not influenced by temperature. The same trend was observed
for T6 (Supplementary Table S1), and the effect of grinding on apparent viscosity was more
pronounced since even slow grinding speeds led to homogenous puree textures (Fig. 1B).
Hence, the range of apparent viscosity values was slightly reduced compared to T1. However,
the storage duration did not significantly alter textural characteristics in this experiment.



295 296

Fig. 1. Apparent puree viscosity at 50 s<sup>-1</sup> (A, B), pulp wet mass (C, D) and serum viscosity at 100 s<sup>-1</sup> (E, F) for purees obtained with different temperatures and grinding speeds for T1 (A, 297 C, E) and T6 (B, D, F). White bars represent purees ground at 300 rpm, grey bars purees 298 299 ground at 1000 rpm and black bars purees ground at 3000 rpm.

- 301 3.2. Determinants of apple puree's texture
- 302
- 303 3.2.1. Particle size distribution

For T1 and T6, particle size decreased with increased grinding speed (Fig. 2). This observation was correlated with puree's viscosity (Fig. 3A), which also decreased with grinding.

307



308

Fig. 2. Particle size distribution of purees obtained with different temperatures and grinding
speeds for T1 (A) and T6 (B). Dotted lines represent purees ground at 300 rpm, dashed lines
purees ground at 1000 rpm, and continuous lines purees ground at 3000 rpm.

For T1, particle size was also influenced by temperature (Fig. 2A). Purees prepared at low grinding speeds (300 and 1000 rpm) and moderate temperatures (70 and 83 °C) showed a bimodal distribution with the main peak around 950  $\mu$ m and a shoulder, indicative of smaller particles. After grinding at 3000 rpm, particles showed a monomodal distribution around 480

317 µm at 70 °C and 360 µm at 83 °C. Particle size distributions for purees heated at 95 °C were 318 more narrow and exhibited smaller sizes at all grinding speeds: 630 µm, 315 µm and 210 µm 319 for purees ground at 300, 1000 and 3000 rpm, respectively. Since apple cells are around 200 um in size (Khan & Vincent, 1990; Leverrier et al., 2016), only purees produced at 95 °C and 320 321 3000 rpm led to individualised cells for T1. Although these purees showed the smallest 322 particle sizes, they were more viscous than purees prepared at lower temperatures, even at the 323 same grinding speed (Fig. 1A). In this sense, grinding alone cannot account for the puree's 324 texture.

For T6 (Fig. 2B), particle size depended only on grinding speed (Supplementary Table S1). Whereas purees ground at 300 rpm showed a prominent peak with a small shoulder, purees prepared with grinding speeds of 1000 and 3000 rpm presented large quantities of individual cells at all temperatures tested. Even though the same procedures produced smaller particles than T1, this did not always result in less viscous purees (Fig. 1B).



**Fig. 3.** Scatterplots of particle size (d 0.9) in the puree (A), pulp wet mass (B) and serum viscosity at 100 s<sup>-1</sup> (C) as a function of apparent puree viscosity at 50 s<sup>-1</sup>. Empty symbols represent samples for T1 and filled symbols samples for T6. 70 °C, 300 rpm (circle); 70 °C, 1000 rpm (half-circle downwards); 70 °C, 3000 rpm (half-circle upwards); 83 °C, 3000 rpm (triangle); 83 °C, 1000 rpm (triangle with the apex pointing downwards); 83 °C, 3000 rpm

337 (triangle with the apex pointing to the right); 95 °C, 300 rpm (square); 95 °C, 1000 rpm
338 (diamond); 95 °C, 3000 rpm (pentagon).

339

# 340 *3.2.2. Pulp wet mass, water retention capacity and cell wall porosity*

PWM for T1 (Fig. 1C) was similar for purees obtained at 70 and 83 °C. On the other hand, this value was significantly increased in in purees prepared at 95 °C. Since the pulp's WRC (Fig. 4A) were also higher for purees heated at 95 °C, higher temperatures probably increased cell wall degradation, suggesting that the cell wall was retaining water. A similar observation was reported previously with heat-treated dietary fibres (Guillon, Barry, & Thibault, 1992) and apple cell wall material (Müller & Kunzek, 1998).

Grinding speed did not induce significant differences (Supplementary Table S1). The higher PWM of the purees obtained at 300 rpm (70 and 83 °C) resulted from intact cell clusters, which did not pack during centrifugation. These cell clusters are more rigid and occupy more volume (Leverrier et al., 2016; Lopez-Sanchez, Chapara, Schumm, & Farr, 2012).

351 For T6, the temperature did not affect the PWM values (Fig. 1D). It is plausible that the fruit 352 maturation damaged the cell wall structure, limiting the impact of temperature. Grinding 353 showed a slightly significant impact on PWM for T6 but no trend could be observed. Overall, 354 the PWM was not significantly altered with storage. However, the PWM of aged cells seemed 355 to be higher when moderate temperatures (70 and 83 °C) and higher grinding speeds (1000 356 and 3000 rpm) were applied. The results obtained under these conditions were similar to T1 357 subjected to low grinding (300 rpm) or high temperature (95 °C). This result is supported by 358 the pulp's WRC (Fig. 4A) and could be explained by cell walls' porosity.

The  $T_2$  relaxation times (Fig. 4B) showed water mobility distribution in the rehydrated pulp AIS. For these types of experiments, longer  $T_2$  relaxation values are indicative of greater water mobility. This relationship can be roughly linked to the meso-porosity of the material since an increase in  $T_2$  relaxation times involve, among others, an increase in average pore 363 size (Meng & Ragauskas, 2014). For T1, five  $T_2$  relaxation domains were identified. In 364 contrast, only four domains were detected in T6. These domains were slightly more narrow, 365 particularly at the two highest temperatures, including a relative T6 sample "homogenisation". 366 The slowest water mobility centred on a  $T_2$  value of about 4 ms, corresponding to pore sizes 367 ranging between 5 and 7.5 nm (Barron et al., 2021), could be associated with water molecules 368 involved in strong interaction with macromolecules. These values tended to decrease with 369 increased temperature, indicating reduced pore size with higher temperatures. Environments 370 with higher relaxation times (45-340 ms) all tended to increase with temperature. This 371 observation is partly due to an increase in pore size of 15-120 nm with temperature and 372 accounts for augmented WRC and PWM values. In general, higher  $T_2$  relaxation times were 373 observed in aged cells, indicating more porous cell walls and higher PWM. The exact values 374 are presented in Supplementary Table S2.



375

Fig. 4. Water retention capacity of the pulp (A) and relaxation times  $T_2$  (B) for purees obtained at different temperatures and ground at 3000 rpm for T1 (white bars or continuous lines) and T6 (black bars or dashed lines).

379

380 Similar results were obtained with fresh purees (data not shown). However, other 381 measurements, such as Simons' stain or NMR cryoporometry (Meng & Ragauskas, 2014), 382 should be conducted to confirm the impact of temperature and storage on cell wall porosity. 383 Although the T1 purees prepared at higher temperatures exhibited smaller particle sizes, the 384 purees were slightly more viscous (Fig. 1A). This result was probably due to the higher PWM 385 values being correlated with more viscous purees (Fig. 3B). Additionally, while the T6 386 particles were significantly smaller (Supplementary Table S1), the purees' textural 387 characteristics (apparent viscosity, yield stress, G' and G'') were similar for T1 and T6. The 388 higher PWM values in the older apples may have a smoothing effect on particle size. These results demonstrate the complex interactions between different texture determinants. 389 390 Furthermore, altering these interactions by mechanical or thermal treatments can influence the 391 puree texture.

392

393 *3.2.3. Serum viscosity* 

394 Serum viscosity was significantly altered by temperature increase for T1 (Fig. 1E) but not for 395 T6 (Fig. 1F). This effect was especially apparent for T1, in which the colour of the sera was 396 more intense with increased grinding speed (Supplementary Fig. S3). This result might be due 397 to small particle fragments in the serum. However, this did not alter serum viscosity since the 398 grinding speed had no significant effect on this parameter. Overall, the storage duration did 399 not significantly modify serum viscosity (Supplementary Table S1). It should be pointed out 400 that the interaction between storage duration and temperature had a major impact, with T1 401 displaying lower serum viscosity values at 70 °C and impressively higher values at 95 °C than 402 T6.

The purees' serum viscosity was found to be poorly correlated with their apparent viscosity (Fig. 3C). Additionally, serum viscosity did not vary significantly between the samples, except for T1 purees heated at 95 °C. These high serum viscosities might modify the sensory perception of consistency, resulting in a smoother texture in the mouth (Espinosa-Munoz, Symoneaux, Renard, Biau, & Cuvelier, 2012).

410

411 Principal component analysis (PCA, Fig. 5) was conducted with textural characteristics 412 (apparent viscosity; yield stress; G'; G''), and possible determinants of puree's texture (particle 413 size; PWM, i.e. the amount of liquid phase bound by insoluble particles; serum viscosity) for 414 T1 and T6 were evaluated. Together, the first two principal components (PC1 and PC2) 415 explained more than 80% of the total variance. Yield stress, G' and G'' were grouped at PC1, 416 together with particle size, indicating a strong dependence. T1 samples (Fig. 5B) were more 417 variable than T6 since they were more dispersed in the sample map. In conclusion, the impact 418 of processing on the puree's texture and its determinants was reduced by prolonged post-419 harvest storage. Indeed, NMR relaxation experiments (Fig. 4B) and previous results (Buergy 420 et al., 2020) confirmed this conclusion.

T1 samples produced at 70 and 83 °C were placed together at PC1, while purees prepared at
95 °C were explained by PC2. This result led to two extremes, one at PC1 that accounted for
samples ground at 300 rpm and heated at moderate temperatures (70 and 83 °C) and one at
PC2, samples heated at 95 °C.

Samples were separated according to the grinding speed along PC1 (Fig. 5B). Thus, large particles were related to high yield stress, G' and G". Cell clusters deform less easily than individual cells and occupy more volume in the puree, consequently increasing the rheological characteristics (Leverrier et al., 2016; Lopez-Sanchez et al., 2012). Moreover, PWM and serum viscosity were placed near PC2 and perpendicular to the parameters mentioned above. These results suggest that the two input variables temperature and grinding, produce different effects.

Indeed, in the sample map (Fig. 5B), PC2 separated T1 purees produced at 95 °C, which were
characterised by high PWM and high serum viscosities (Fig. 1C and E), from T1 purees
produced at moderate temperatures (70 °C and 83 °C). On the other hand, the T6 purees were

intermediate. Apparent viscosity was less well explained in the PCA and stood alone between
PC1 and PC2. This observation indicated some co-dependence with particle size (along PC1)
and PWM and serum viscosity (along PC2). Hence, texture formation was influenced by
grinding, a step that highly affected particle size, and temperature, which facilitated tissue
separation in synergy with grinding, increased PWM, and serum viscosity.



442 **Fig. 5.** Principal component analysis (PCA) of rheological characteristics ( $n_{app}$ : apparent puree viscosity at 50 s<sup>-1</sup>, YS: yield stress, G' and G'': puree's storage and loss modulus, 443 444 respectively, at an angular frequency of 10 rad/s) and texture determinants (Particle size: particle size d 0.9, PWM: pulp wet mass,  $\eta_{serum}$ : serum viscosity at 100 s<sup>-1</sup>) of purees prepared 445 446 with apples stored for one and six months before processing. Correlation circle of variables 447 loadings on PC1 and PC2 (A). Sample maps of scores on PC1 and PC2 (B). For more 448 legibility, PCA was conducted on the mean value of three replications as the same patterns 449 were obtained as for PCA with all values. Empty symbols represent samples for T1 and filled 450 symbols samples for T6. 70 °C, 300 rpm (circle); 70 °C, 1000 rpm (half-circle downwards); 451 70 °C, 3000 rpm (half-circle upwards); 83 °C, 300 rpm (triangle); 83 °C, 1000 rpm (triangle 452 with the apex pointing downwards); 83 °C, 3000 rpm (triangle with the apex pointing to the 453 right); 95 °C, 300 rpm (square); 95 °C, 1000 rpm (diamond); 95 °C, 3000 rpm (pentagon).

454

### 455 3.4. Serum pectins can help to explain texture determinants

456

457 Mechanical and thermal treatment act synergistically during puree processing, affecting 458 texture determinants to different extents because temperature favours pectin degradation and 459 solubilisation (Sila et al., 2009). The detailed structural and compositional characterisation of 460 the pectins solubilised during processing (serum pectins) could provide insight into the 461 chemical processes that occur during apple processing. This knowledge could help elucidate 462 the complex interactions between texture determinants and lead to a specific puree's texture, 463 depending on post-harvest storage. Serum pectins were solubilised from the middle lamella or 464 the primary cell wall (Sila et al., 2009), thus facilitating tissue fragmentation (i.e., reduced 465 particle size) or increasing porosity and consequently the pulp's WRC (i.e., increased PWM). 466 The amount of solubilised pectins would, in turn, explain serum viscosity.

#### 468 *3.4.1. Chemical composition of serum pectins*

469 For T1, the amount and chemical composition of serum pectins was significantly altered by 470 temperature but not by grinding (Table 1). Serum AIS values were significantly increased 471 with elevated temperature, indicating improved pectin solubilisation from the cell wall and 472 middle lamella. This effect might weaken the cell wall structure and intercellular adhesion, 473 facilitating cell separation during grinding at elevated temperatures. Previous studies showed 474 that heating raw apple, carrot or broccoli tissue before grinding aided separation (Day et al., 475 2010; Lopez-Sanchez et al., 2011; Müller & Kunzek, 1998) but the results were not 476 corroborated with pectin analysis. Increased pectin solubilisation might also increase the pore 477 sizes in the cell wall (Fig. 4B), leading to improved WRC of the pulp (Fig. 4A) and PWM 478 (Fig. 1C). The amount of solubilised pectins was also correlated with the temperature-479 dependent increase in serum viscosity (Fig. 6A). Starch solubilisation might additionally 480 increase serum viscosity. The amount of starch in the serum significantly increased with 481 temperature and slightly with grinding speed until reaching a concentration of about 13 g/L at 482 95 °C and 3000 rpm. Considering that the gelatinisation temperature of starch in excess water 483 is around 60 °C, temperatures above 70 °C might solubilise starch better (Singh, Inouchi, & 484 Nishinari, 2005). Increased grinding also seemed to enhance starch solubilisation and was 485 probably due to increased cell wall rupture. Although amylose gels at less than 10 g/L 486 (Doublier & Choplin, 1989) and a 20 g/L amylopectin solution provides a viscosity increase 487 of 5 mPa.s (Matignon et al., 2014), these relatively low concentrations cannot account for the 488 high serum viscosity increase.

The GalA content in serum AIS also increased with temperature, confirming improved pectin solubilisation at high temperatures. The GalA/rhamnose ratio estimated the proportion of HG to RG I pectins. It was not altered either by temperature or by grinding, indicating that HG and RG I pectins were similarly solubilised. Although arabinan side chains are generally more susceptible to temperature than galactans (Green, 1967; Thibault et al., 1993), the 494 galactan/arabinan ratio decreased with increasing temperature. Pectin RG I fractions rich in 495 arabinans thus seemed to be more tightly bound to the cell wall and required more 496 degradation for solubilisation. The ratio of (arabinose+galactose)/rhamnose also decreased 497 with increasing temperature, revealing attenuated RG I side chain branching. Since RG I side 498 chains were shown to be linked to the cellulose-xyloglucan network in the cell wall (Popper & 499 Fry, 2005; Zykwinska, Ralet, Garnier, & Thibault, 2005), pectins seemed to be less attached 400 and thus more susceptible to solubilisation during processing.

501 All serum pectins were highly methylated, and the DM was not affected by temperature 502 (results not shown), attesting limited impact of PME activity during apple processing.

503 Compared to T1, the amount and composition of serum pectins for T6 were less affected by 504 thermomechanical processes (Table 1) during puree production. This observation could be 505 because endogenous enzymes already degraded pectins. The serum AIS content at  $70^{\circ}$  C was 506 higher for T6 than T1 but remained constant at any temperature, thus accounting for T6's 507 constant serum viscosity regardless of the processing conditions (Fig. 1F). Starch was not 508 detected. The AIS composition of serum pectins was stable for T6, whatever the grinding or 509 temperature. As an exception, the galactan/arabinan ratio was slightly decreased with 510 increased temperature, but the values were less dispersed than for T1 and the overall 511 (arabinose+galactose)/rhamnose ratio was not modified. Compared to T1, the latter ratio was 512 less critical and indicated reduced RG I side chain branching in T6 serum pectins. This 513 substantial decrease in RG I side chains (i.e., arabinose and galactose) probably contributed to 514 the higher relative GalA content in the T6 samples. Concerning T1, the HG to RG I ratio, 515 expressed as GalA/rhamnose, was not altered by temperature or grinding. However, this ratio 516 showed that, although the GalA content was higher for T6, more RG I was extracted, 517 especially with grinding. This result may be due to reduced RG I side chains, leading to a 518 weakened cell wall structure, as explained before. As observed by Nara et al. (2001) or Pena 519 and Carpita (2004), reduced RG I side chains were probably linked to reduced cell adhesion.

520 Indeed, cell separation was easy for T6 and purees prepared with aged apples showed 521 significantly smaller particles (Supplementary Table S1). Additionally, grinding generated 522 similar particle sizes independent of temperature. As previously stated by Buergy et al. 523 (2020), ageing facilitated cell separation for T6. As hypothesised before, the weakening of the 524 cell wall in aged apples probably increased cell wall porosity (Fig. 4B), leading to increased 525 WRC (Fig. 4A) and PWM (Fig. 1D).

526 Since raw apples also displayed RG I side chain loss, GalA increase and more RG I during

- 527 post-harvest storage (Supplementary Table S3), it is plausible that storage could be exploited
- 528 for producing a desired puree's texture.

Storage (months)	Temp. (°C)	Grinding (rpm)	AIS (mg/g FW)	Starch (mg/g FW)	GalA (mg/g AIS)	GalA Rha	$\frac{\text{Ara} + \text{Gal}}{\text{Rha}}$	Gal Ara	$\overline{M}_{w} \ge 10^{3}$ (g/mol)	$\frac{\overline{[\eta]}_z}{(mL/g)}$	d <sub>happ</sub> (g nm <sup>3</sup> /mol)
1	70	300	0.9	0.1	527	73	24	1.4	311	1903	0.8
		1000	1.1	0.2	556	94	24	1.4	545	1869	0.8
		3000	1.6	0.5	470	60	26	1.3	480	1811	0.8
	83	300	2.1	0.4	554	117	22	1.2	493	1609	0.9
		1000	1.7	0.4	539	88	25	1.2	522	1760	0.9
		3000	3.0	0.6	543	93	25	1.0	455	1783	0.8
	95	300	5.3	0.5	646	74	17	0.8	406	1229	1.2
		1000	5.8	1.0	602	82	21	0.8	425	1272	1.2
		3000	6.2	1.3	577	81	22	0.8	409	1268	1.2
6*	70	300	2.1	ND	683	52	8	1.1	157	510	3.0
		1000	1.8	ND	593	26	6	1.2	188	488	3.1
		3000	3.0	ND	605	30	7	1.0	273	579	2.6
	83	300	2.4	ND	663	48	7	1.0	166	583	2.6
		1000	2.5	ND	601	26	6	0.9	204	650	2.3
		3000	3.1	ND	605	27	6	1.0	229	620	2.4
	95	300	3.9	ND	689	67	10	0.8	159	507	3.0
		1000	3.4	ND	636	31	6	0.8	217	607	2.5
		3000	4.5	ND	619	28	6	0.8	250	636	2.4
PSD			0.8	0.5	49	28	3	0.1	50	162	0.1

**Table 1.** AIS yield, composition, and macromolecular characteristics of serum pectins, followed by Kruskal-Wallis *H*- and *P*-values.

1	Temperature H	20.9	10.6	9.6	3.4	7.5	22.6	5.5	18.6	18.3
	Temperature P	<0.001	0.005	0.008	0.184	0.023	<0.001	0.064	<0.001	0.000
	Grinding H	1.1	3.3	2.0	0.4	3.0	0.5	4.8	1.0	1.2
	Grinding P	0.572	0.190	0.361	0.804	0.220	0.798	0.089	0.614	0.556
6*	Temperature H	6.0	-	1.7	1.2	1.2	7.2	2.4	3.2	4.6
	Temperature P	0.051	-	0.430	0.561	0.561	0.027	0.301	0.202	0.099
	Grinding H	1.7	-	5.6	5.6	5.6	0.1	2.4	2.5	0.3
	Grinding P	0.430	-	0.061	0.061	0.061	0.957	0.301	0.288	0.875
Storage H		0.3	-	10.7	15.7	19.7	2.4	19.1	19.7	11.9
Storage P		0.596	-	0.001	<0.001	<0.001	0.121	<0.001	<0.001	0.001

531 \* Only one repetition per sample.

The ratio GalA/Rha estimated the relative amount of HG versus RG I, (Ara+Gal)/Rha estimated RG I branching and Gal/Ara the proportion of RG I side chains. Ratios were calculated using the yields of galacturonic acid (GalA) and neutral sugars arabinose (Ara), galactose (Gal) and rhamnose (Rha) content, expressed in mg/g AIS (Supplementary Table S4). AIS and chemical composition of serum pectins were corrected for the starch content. PSD: Pooled standard deviations; ND: Not detected; FW: Fresh weight (serum); AIS: Alcohol insoluble solids;  $\overline{M}_w$ : Weightaverage molar mass;  $\overline{[\eta]}_z$ : z-average intrinsic viscosity; d<sub>happ</sub>: Apparent molecular density, calculated as  $\overline{M}_w/(\frac{4}{3} \cdot \pi \cdot \overline{R}_{hz}(v)^3)$  with  $\overline{R}_{hz}(v)$ : zaverage viscometric hydrodynamic radius. Macromolecular characteristics were taken at the apex of the main peak.



539

**Fig. 6.** Scatterplots of serum viscosity at 100 s<sup>-1</sup> against serum AIS (A) and molar mass of serum pectins at the apex of the main peak (B). Empty symbols represent samples for T1 and filled symbols samples for T6. 70 °C, 300 rpm (circle); 70 °C, 1000 rpm (half-circle downwards); 70 °C, 3000 rpm (half-circle upwards); 83 °C, 300 rpm (triangle); 83 °C, 1000 rpm (triangle with the apex pointing downwards); 83 °C, 3000 rpm (triangle with the apex pointing to the right); 95 °C, 300 rpm (square); 95 °C, 1000 rpm (diamond); 95 °C, 3000 rpm 546 (pentagon).

547

# 548 3.4.2. Macromolecular characteristics of serum pectins

549 Macromolecular characteristics of soluble serum pectins give information about their 550 molecular structure and density. For T1, molar mass (Table 1) was not significantly altered by 551 temperature but showed an overall decrease when higher temperatures were applied. For T6, 552 molar mass was not altered by processing, but values were significantly lower than for T1. 553 The molar mass distributions of serum pectins (Fig. 7) are presented for samples prepared at 554 3000 rpm and different temperatures. For T1 purees (Fig. 7A) processed at moderate 555 temperatures (70 °C and 83 °C), the main fraction of serum pectin eluted at the same elution 556 volume (~19 mL), whereas the main peak was shifted to higher elution volumes after heating 557 at 95 °C. This result indicated a smaller pectin size for the samples obtained at 95 °C. A

558 second peak eluting at higher elution volumes (~25 mL), which represented smaller pectin 559 fractions, was also present, and its proportion decreased with increased temperature. However,  $\overline{M}_{w}$  (90–105 x 10<sup>3</sup> g/mol) and  $\overline{R}_{hz}(v)$  (10–16 nm) were similar in all samples and 560 could not be differentiated. For T6 (Fig. 7B), processing temperature did not affect the serum 561 562 pectins' macromolecular size. Compared with T1, the main peak of all pectin chromatograms 563 was shifted to higher elution volumes, and the second peak was smaller, indicating pectin 564 degradation during storage as observed before (Buergy et al., 2020). Hence, both increased 565 temperature (95 °C, for T1) and post-harvest storage induced pectin degradation, thus favouring pectin solubilisation. A reduction in RG I side chains weakened the cell wall 566 567 structure, leading to reduced cell adhesion and more porous cell walls. However, no trend was 568 observed between serum viscosity and molar mass (Fig. 6B).

569 It has been reported that pectin conformation can significantly impact serum viscosity (Diaz, 570 Anthon, & Barrett, 2009). Herein, intrinsic viscosity was significantly affected by temperature 571 increase (Table 1), leading to reduced values at 95 °C despite higher pectin concentrations. 572 Lower intrinsic viscosities at 95 °C for comparable molar mass at 70 and 83 °C indicted a 573 more compact pectin structure. This observation was confirmed by  $\overline{R}_{hz}(v)$  conformation plots 574 (Supplementary Fig. S4) and the apparent polymer density d<sub>happ</sub> (Table 1). The latter was 575 similar at 70 and 83 °C but significantly higher for 95 °C. Intrinsic viscosity was significantly 576 lower for T6, roughly half that of T1, whereas d<sub>happ</sub> increased by more than 2-fold. Since 577 serum pectins in purees from aged apples have more GalA and less arabinose and galactose 578 (Table 1), this higher density could result from more properly folded pectins because of 579 reduced steric hindrance. Although the conformation of serum pectins was altered, it could 580 not be linked to serum viscosity (data not shown).

581 Grinding had no impact on the macromolecular characteristics of the T1 serum pectins. In 582 contrast, molar mass and intrinsic viscosity of T6 pectins increased with grinding, although this trend was not statistically significant. Macromolecular characteristics of soluble pectins
extracted from raw apples showed the same trend as serum pectins during post-harvest
storage (i.e., smaller molar mass and intrinsic viscosity but higher d<sub>happ</sub>) (Supplementary
Table S3).

587



Fig. 7. Normalised chain concentration and molar mass versus elution volume (mL) pectins for T1 (A) and T6 (B) for purees prepared at 70 °C (continuous lines), 83 °C (dashed lines) and 95 °C (dotted lines) and a grinding speed of 3000 rpm. The signal (mV) obtained by the differential refractive index detector was normalised by dividing all data points by the signal at the peak's apex.

594

# 595 3.4.3. Mechanisms of pectin degradation during processing

596 At the natural pH of apples (~3.7), pectin degradation is minimal and might be due to either 597 acid hydrolysis or  $\beta$ -elimination (Liu, Renard, Rolland-Sabaté, Bureau, & Le Bourvellec, 598 2021). For T1 (Table 1), serum pectins showed higher amounts of GalA and the RG I side 599 chains arabinan and galactan were hydrolysed by temperature increase, which probably 600 favoured the extractability of pectins from the cell wall. Moreover, T1 serum pectins showed 601 reduced molar mass, macromolecular size and intrinsic viscosity (Table 1 and Fig. 7A) when temperature increased from 83 to 95 °C, attesting pectin degradation. To investigate the 602 mechanisms leading to pectin degradation at 95 °C, NMR was used to detect β-elimination 603

604 products in serum pectins, since the 235 nm wavelength in the DAD signal after sample 605 separation by HPSEC was not enough to detect β-elimination (data not shown). A small 606 signal in the <sup>1</sup>H-NMR spectrum around 6 ppm indicated the presence of β-elimination 607 products (Tjan et al., 1974). This signal was visible in the positive control and, slightly, in the 608 serum AIS obtained from purees heated at 95 °C (Fig. 8). In conclusion, only little β-609 elimination occurred, even at 95 °C, and acid hydrolysis seemed to be the predominant 610 reaction causing pectin degradation during apple processing.

611



612

613 **Fig. 8.** <sup>1</sup>H-NMR spectra of control and serum pectins extracted from the purees at 3000 rpm 614 with different temperatures for T1. The control (serum pectin 95 °C, 3000 rpm) was heated at 615 100 °C for 30 min at pH 6 to enhance β-elimination.

616

# 617 **5. Conclusions**

618

619 Both elevated temperature (95 °C) and apple maturation led to pectin degradation, resulting in

620 facilitated tissue fragmentation during processing. This treatment affected particle size, an

621 important determinant of puree's texture, and other parameters such as PWM and serum 622 viscosity. Since pectin and puree's structures were significantly altered by increasing 623 temperature in fresh (T1) but not in older (T6) apples, the combination of storage duration and 624 temperature had a significant impact. Although mechanical treatments were the predominant 625 factor for texture formation, they did not alter the pectin composition or structure, in T1 or 626 T6. The temperature had only a limited impact on the apple puree's texture. However, it 627 strongly affected PWM and serum viscosity, which counteracted the effect of smaller 628 particles produced by grinding. This study highlighted the importance of pectin analysis in 629 explaining the impact of thermomechanical processes on puree's texture. A detailed 630 characterisation of the pulp's cell wall composition and structure should be performed in 631 future work. It would also be interesting to conduct detailed kinetics, over short periods of 5 632 to 15 min, at different temperatures and grinding speeds to precisely identify the moment 633 structural alterations occur.

634

# 635 CRediT authorship contribution statement

636

Alexandra Buergy: Conceptualization, Investigation, Formal analysis, Data curation,
Writing - original draft. Agnès Rolland-Sabaté: Conceptualization, Supervision, Validation,
Writing - review & editing. Alexandre Leca: Conceptualization, Investigation, Supervision,
Writing - review & editing. Xavier Falourd: Investigation, Formal analysis, Writing - review
& editing. Loïc Foucat: Investigation, Formal analysis, Writing - review & editing.
Catherine M. G. C. Renard: Conceptualization, Funding acquisition, Project administration,
Validation, Writing - review & editing.

644

#### 645 **Declaration of competing interest**

646	
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648	
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650	
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