

Comparative Life Cycle Assessment of two advanced treatment steps for wastewater micropollutants: How to determine whole-system environmental benefits?

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- 1 Comparative Life Cycle Assessment of two advanced treatment steps for wastewater micropollutants: how to
- 2 determine whole-system environmental benefits?
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9 Abstract

10 Advanced wastewater treatment (AWT) technologies are now considered to target urban micropollutants 11 (MPs) before discharge into receiving water bodies and to comply with specific criteria for reuse. Extra 12 energy and/or resources are necessary to achieve the elimination of MPs. Using the Life Cycle Assessment 13 framework, this study assesses net environmental efficiencies for two AWTs (i) ozone systems (air-fed and 14 pure oxygen-fed) and (ii) granular activated carbon filter. Sixty-five MPs with proven removal efficiency 15 values and toxicity and/or ecotoxicity potentials were included in this study building on results from recent 16 research. Consolidated Life Cycle Inventories with data guality and uncertainty characterization were 17 produced with an emphasis on operational inputs. Results show that the direct water quality benefits obtained from AWT are outweighed by greater increases in indirect impacts from energy and resource 18 19 demands. Future research should include water quality aspects not currently captured in life cycle impact 20 assessment, such as endocrine disruption and whole-effluent toxicity, in order to assess the complete policy 21 implications of MP removal strategies.

22

23 Keywords

24 Life Cycle Analysis; micropollutants; advanced wastewater treatment; removal efficiencies;

25 environmental impacts; granular activated carbon; ozone treatment

- 26
- Abbreviations: AWT, advanced wastewater treatment; LCA, life cycle assessment; LCI, life cycle inventory;
 LCIA, life cycle impact assessment; MP, micropollutant; GAC, granular activated carbon

29 1. Introduction

30 Several organic and inorganic micropollutants (MPs) are insufficiently eliminated in conventional 31 wastewater treatment plants (WWTPs) as they are designed to treat biodegradable carbon, nitrogen and 32 phosphorus, and they eliminate non-polar and large organic molecules (Zepon Tarpani and Azapagic, 2018) 33 or metals with affinity with organic matter (Choubert et al., 2011b). Therefore, discharges of MPs in aquatic 34 environments can lead to potential negative effects on living organisms. A large array of MPs found in very 35 low concentrations in treated wastewater make advanced wastewater treatment (AWT) processes technically 36 challenging. Intensive usage of treatment chemicals and energy in AWT processes have been associated 37 with increased life cycle toxicity and other environmental impacts (Dolar et al., 2012; Igos et al., 2012; Papa 38 et al., 2015, 2013; Pasgualino et al., 2011; Rahman et al., 2018). In order to find AWT technologies suited to 39 meeting targets on MPs, it is important to understand environmental benefits achieved by MP removal (e.g., 40 reduced toxicity) as well as unintended environmental impacts due to additional chemical, energy, and 41 materials requirements. Life cycle assessment (LCA) has been used extensively to characterize and quantify 42 the net environmental impacts of wastewater treatment plants, and to compare treatment options (Byrne et 43 al., 2017; Corominas et al., 2020). Nevertheless, few papers consider MPs due to the lack of toxicity and/or 44 ecotoxicity potentials (Arzate et al., 2019; Igos et al., 2021, 2012; Rahman et al., 2018). However, the effects 45 of MPs in the environment are yet to be fully understood (Eggen et al., 2014) and therefore affected by high 46 uncertainty and low coverage of impact pathways. Furthermore, the extensive identification and 47 quantification of all the MPs in wastewater is a complicated task both technically and economically. For this 48 reason, often just a few target compounds are reported in monitoring studies and potential impacts are 49 calculated with these incomplete data (Aemig et al., 2021; Alfonsín et al., 2014; Rahman et al., 2018). For 50 example, transformation products which arise from oxidative treatments and are not included in the LCA may 51 increase ecotoxicity of the treated effluent (Vogna et al., 2004).

52 Because the scope of LCA includes both direct emissions from WWTPs as well as indirect emissions 53 from producing and transporting all chemicals, energy, and infrastructure required for treatment, LCA can be 54 applied to study both environmental benefits and costs associated with AWT to meet stringent regulations.

55 The aim of this work was to determine the net environmental efficiencies for AWTs like oxidation by 56 ozone produced with pure oxygen or air, or adsorption by activated carbon.

57 2. Materials and methods

The steps leading to the environmental assessment of two types of wastewater management systems using the life cycle assessment (LCA) method are presented in this section. Thus, we will follow the recommended scheme of a standardized LCA (ISO, 2006a, 2006b): (i) goal and scope definition (Section 2.1), (ii) inventory analysis and uncertainty characterization (Sections 2.2 and 2.3), (iii) impact assessment (Section 2.4), (iv) interpretation of results and discussion of the most salient issues when considering MPs in LCA (Section 3).

64 2.1. Goal and scope definition

The objectives of this study were to assess and compare life cycle environmental impacts of two promising AWT processes targeting wastewater MPs (e.g. ozonation and adsorption on activated carbon), identifying their main environmental hotspots. Additionally, the ecotoxicity and toxicity impacts of MPs in the AWT effluent were estimated and compared to the equivalent impact of the effluent from conventional WWTPs without AWT. The scope of the study covers AWT effluent discharges and by-products generated during the AWT as well as the infrastructures of treatment units, and operational inputs (e.g. required electricity, chemicals or adsorption media).

72 2.1.1. Functional unit

Generally, LCA studies on wastewater treatment systems used a functional unit on assumed per capita loadings such as the population-equivalent (PE) defined in the European directive 91/271 (Corominas et al., 2020). Hence, the functional unit selected for this LCA study was "the AWT of an urban (biologically pretreated) wastewater effluent generated from 50 000 PE during one year". Such a treatment capacity can be estimated at 2,74.10⁶ m³.year⁻¹ based on the assumption that an average French PE discharges 0,15 m³ of wastewater daily (Mercoiret, 2010; Risch et al., 2011).

The rationale for this choice of functional unit was to ensure good representativeness with a LCA based on an existing full-scale French WWTP using biofiltration (secondary treatment) followed by ozonation and extensively monitored (Choubert et al., 2017b). In the following, different AWT processes were compared using this common functional unit of comparison since these systems were all designed for wastewater treatment.

84 2.1.2. <u>Scenarios</u>

85 This study considered two technologically proven AWT processes for the removal of organic MPs with 86 both proven removal efficiencies for use on urban wastewater. First, ozone treatment is currently the most 87 used oxidation process for organic MPs removal in drinking water production and is now recently considered 88 for the advanced treatment of wastewater effluents (Bertanza et al., 2011; Bourgin et al., 2018; Guillossou et 89 al., 2020; Margot et al., 2013; Schindler Wildhaber et al., 2015). Second, adsorption onto granular activated 90 carbon (GAC) has been proven to be a viable process to remove organic MPs (Benstoem et al., 2017; 91 Boehler et al., 2012; Mailler et al., 2016; Sbardella et al., 2018). Four scenarios were built to meet the 92 objectives of this LCA study on AWTs which included a reference scenario "baseline" without any AWT, two 93 ozone systems with different feed gas (a. with pure oxygen, b. with air) and adsorption on granular activated 94 carbon (Table 1). Previous steps of treatment consist of a primary settling and different stages of secondary 95 treatment by submerged biofilters operated to remove suspended solids, biodegradable carbon and 96 ammonium.

97

Table 1. AWT scenarios modelled to meet the objectives of this LCA

98 Insert Table 1 here.

99

100 2.1.3. System boundaries

The system boundaries included the materials for the construction of AWT infrastructures, as well as their final disposal, and the resources required for their operation. Outlet pipes for discharge of treated water from the WWTP to the receiving environment were assumed invariant in all scenarios therefore not modelled in the scenario comparisons (by the ceteris paribus condition). The schematic diagrams of four wastewater treatment scenarios with different AWT processes are shown in Figure 1.



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Figure 1. Flow diagram and system boundaries for the AWT scenarios modelled in this study. System boundaries include the discharge of secondary effluent in a baseline scenario with no advanced treatment (1), discharge of AWT effluent after ozonation treatment with different feed gas (2a, with pure oxygen and 2b, with air); and discharge of AWT effluent after adsorption on GAC (3) as well as the end-of life of the GAC filter, material demands for the infrastructure construction and end-of-life.

112 2.2. Inventory analysis

113 2.2.1. Infrastructure and operational inputs

Infrastructure requirements for AWTs were modelled after a reference plant with a treatment capacity of 100 000 PE (Larsen et al., 2010). Then infrastructure demands were scaled down to the 50 000 PE capacity in the chosen functional unit (Annex Table S1), using a power law function to account for the non-linear relationships between the equipment capacities and the respective material demands (Arzate et al., 2019; Gallego-Schmid and Tarpani, 2019).

A detailed source analysis was first performed on each data source for energy and chemical requirements 119 120 since these parameters showed a great variability across literature. The results from the source analysis 121 were used to filter the data to select representative values (Annex Table S2). Then life cycle inventories 122 (LCIs) were built for each scenarios using a horizontal weighted-averaging approach (Henriksson et al., 123 2013) which accounted for inherent uncertainties and spread, thereby guantifying data uncertainty. 124 Inventories of operational requirements are summarized in Table 2 with respect to infrastructure 125 (construction and disposal), energy, chemicals and emissions. Background data was sourced from the 126 Ecoinvent v3.6 database (Ecoinvent, 2019) using French (FR)-specific processes where possible and 127 modelled in the SimaPro 8.4 LCA software (Pré Consultants, 2017).

128 The operational energy demand for AWT scenarios were in the same order of magnitude and they represent 129 about 15-20% of the overall energy demand in a WWTP (Arzate et al., 2019). For ozonation this energy 130 demand is strongly dependent on the specific ozone dose, which was set at 6.22 gO₃/m³ i.e. 0.78 gO₃/gDOC 131 with a dissolved organic carbon load of 8 gDOC/m³ in this study (Choubert et al., 2017b). Hence for 132 ozonation with air, this energy demand is estimated at 1,2.10⁻¹ kWh/m³ or 3,2.10⁵ kWh/year with a total treated wastewater volume of 2,74.10⁶ m³/year based on the average French inhabitant wastewater 133 134 generation of 0,15 m³/(PE.d⁻¹). This energy demand is contingent to specific parameters such as nitrites and 135 DOC in the secondary effluent and the chosen value for the energy demand in the ozonation step should 136 represent the global consumption of electricity (including ozone destruction, air production, cooling etc.). 137 Replacing the feed-gas with pure oxygen reduces the energy demand of 25% (Choubert et al., 2017b) since 138 the energy demand for air production is then negligible. However, the average pure oxygen demand is 139 estimated at 8.8 gO₂/gO₃ (Annex Table S2) (Larsen et al., 2010; Muñoz et al., 2009; Remy, 2013). In all 140 scenarios the energy was modelled with the French electricity mix reported by ecoinvent v3.6.

Granular activated carbon (GAC) filter media requires fresh activated carbon and can be regenerated with spent media. The amount of fresh GAC used in a filter bed during its 5 years of operational lifetime was estimated with 20% of losses during a regeneration cycle. In this study, the GAC filter media underwent regeneration every 6 months before final disposal after 5 years (Rahman et al., 2018).

Table 2. Inventory data to treat secondary effluent from 50 000 PE during one year through the AWT processes under study
 Insert Table 2 here.

147

2.2.2. MP concentrations and loads in secondary effluent, and removal efficiencies in AWT

Among the broad range of MPs routinely found in wastewater (Pistocchi et al., 2019; Ternes et al., 2004; Verlicchi et al., 2012), 65 MPs from different chemical groups are selected for the current study. This shortlist includes 30 pharmaceuticals, 9 pesticides, 9 inorganics, 8 various industrial substances, 5 hormones, 3 fragrances and 1 polycyclic aromatic hydrocarbon (Annex Table S3a). These short-listed MPs were chosen considering (i) available monitoring data in secondary effluents and AWT effluents (i.e. with quantified removal efficiencies) and, (ii) available toxicity and/or ecotoxicity potentials in life cycle impact assessment (LCIA) methods.

155 Measured concentrations of MPs in secondary effluent may range widely from 1,7 ng.L⁻¹ and 29,7 156 μ g.L⁻¹ (Bruchet et al., 2015; Choubert et al., 2011a, 2017b; Coquery et al., 2011; Li et al., 2019; Martin Ruel 157 et al., 2012; Miège et al., 2008). The arithmetic means of the reported concentrations are used in the present 158 study as influent MP loads feeding to the AWT removal processes (Annex Table S3b). Removal efficiencies

achieved for ozonation and GAC processes were quantified using recent research (Bourgin et al., 2018; Choubert et al., 2014, 2017b; Guillossou et al., 2019, 2020; Li et al., 2019; Mailler et al., 2015; Martin Ruel et al., 2012; Rahman et al., 2018). A particular attention was given to the selection of reliable removal efficiencies in AWT effluents given the low MP concentrations and sampling measurement uncertainties to ensure unbiased MP analyses (Choubert et al., 2017a). MP loads in secondary effluent and average removal efficiencies for the two AWT processes are listed in Table 3.

Table 3. Selected MPs with average concentrations, estimated mass loadings in secondary treated effluents of WWTPs
 entering AWT and associated removal efficiencies

168 Insert Table 3 here.

In general both ozone and GAC demonstrate removal efficiencies greater than 75% on fragrances, industrial substances and hormones. Ozone treatment targets better pharmaceuticals, while GAC shows overall greater removal efficiencies on pesticides. As a rule, inorganics are not affected by ozone (Ruel et al., 2011) while GAC may partially adsorb (e.g. copper and chromium) or release (e.g. arsenic and vanadium) in treated effluent. Indeed, industrial-scale GAC filters use carbon extracted from coal which contains traces of metallic elements potentially leached from the GAC filter during the AWT (Choubert et al., 2014).

175 2.3. Uncertainty characterization

176 In order to ensure transparency and credibility of the LCA results obtained in this study, it is critical 177 that the uncertainty sources are quantified and their effects on results are communicated (Gavankar et al., 178 2015). Furthermore, the treatment of uncertainty will help interpret differences in the studied systems in the 179 comparative LCA (e.g. to determine whether the preference for one system can be questionable due to 180 result uncertainties) as shown in Igos et al. (2018). Uncertainty ranges for unit processes taken from the 181 Ecoinvent database (Ecoinvent, 2019; Wernet et al., 2016) were defined by the "data pedigree" algorithm 182 available in SimaPro (Pré Consultants, 2019) as proposed by Weidema and Wesnaes (1996). This algorithm 183 relates the datum uncertainty to its source characteristics - i.e. reliability of the source, representativeness of 184 the sample, currency of the period, geographical correlation, technological correlation and sample size. The 185 uncertainty ranges associated to infrastructure construction and AWT operation (e.g. amounts of building 186 materials, energy and ancillary chemicals used, MP discharges etc) are described in Table 4.

187Table 4. Data quality and uncertainty estimation for two life-cycle stages: construction and use (including operation,188maintenance and AWT effluent discharges)

189

190 Insert Table 4 here.

Based on uncertainty data in the LCI, uncertainty propagation in the modelled systems was estimated using a random sampling method i.e. the available Monte-Carlo routine in SimaPro with 1500 runs to yield mean and standard deviation values estimated with 95% confidence intervals (Annex Table S7b). Finally, the influences of uncertainty in two key parameters were studied using sensitivity analyses (See section 3.3).

195 **2.4. Life cycle impact assessment**

196 The Impact World+ method (Bulle et al., 2019) was selected for its robust assessment of human toxicity 197 and freshwater ecotoxicity potentials based on the consensual midpoint-level USEtox v2 model (Rosenbaum 198 et al., 2008). The library of the USEtox v2 model in SimaPro was complemented with 31 new 199 characterization factors (Alfonsín et al., 2014; Maillard et al., 2019) corresponding to the MP shortlist used in 200 this study (Annex Table S3a and Table S4). Detailed characterization factors are given after Maillard et al. 201 (2019) for 107 substances including organic MPs and pesticides in freshwater ecotoxicity (Table S8a and 202 S8b) and human toxicity (Table S9a and S9b). In Impact World+ at the damage level, some indicators 203 including long-term effects (climate change, marine acidification, toxicity cancer, toxicity non-cancer, and 204 freshwater, terrestrial, and marine ecotoxicity) are subdivided into separate mid-to-endpoint indicators for 205 short-term and long-term in order to differentiate impacts occurring in the short-term and long-term (after 100 years). Hence, added MPs were also characterized at the damage level (mid-to-endpoint) for the short-term 206 207 toxicity and ecotoxicity indicators (namely freshwater ecotoxicity and human toxicity cancer and non-cancer) 208 using conversion coefficients (Bulle et al., 2019; Huijbregts et al., 2005). However on long-term toxicity and 209 ecotoxicity indicators, characterization factors for organic MPs discharged in water were estimated to be nil 210 under the hypothese that organic MPs undergo complete degradation within 100 years after discharge.

211 3. Results and discussion

212 **3.1.** Environmental hotspots within AWT systems (midpoint level)

213 Contribution analyses for the baseline scenario and the three AWT scenarios are shown on 15 214 midpoint indicators (Figure 4). These results indicate that ozone with pure oxygen (scenario 2a) yields the 215 greatest impacts on 10/15 indicators due to feed-gas production and storage, with the exclusion of two 216 indicators with non-significant differences with another scenario (e.g. less than 10% difference). As 217 expected, reduction of MPs in the effluent (discharges, in blue) after AWT leads to reduced direct 218 environmental and health impacts. However, these reductions can hardly be seen as overall life cycle 219 impacts are dominated for most impact categories by indirect emissions from upstream production of energy,

- 220 chemicals, and (to a lesser extent) infrastructure materials. For example, AWTs reduce MPs concentration in
- the effluent locally as shown on midpoint toxicity impacts (i.e. freshwater ecotoxicity and human toxicity from
- the USEtox v2 model) yet their implementation lead to net increases in overall life cycle impacts.



Figure 2. Contribution analysis on the fifteen midpoint indicators of Impact World+ method (Bulle et al., 2019) for the four AWT scenarios which include baseline (1), ozone (2a and 2b) and

activated carbon (3). All scenarios are compared using the same functional unit, being the advanced wastewater treatment from 50 000 PE during one year. Relative contributions (in %) are indicated with the scenario having the greatest impact at 100%.

227

228 These findings are consistent with previous LCA studies (Arzate et al., 2019; Igos et al., 2012; Rahman et al., 2018) and this can be explained by low MP concentrations and low values of LCIA impact 229 230 factors for discharged MPs. However, the effects of these substances in the environment are yet to be fully 231 understood (Eggen et al., 2014) and therefore affected by high uncertainty and low coverage of impact 232 pathways. Furthermore, the extensive identification and guantification of all the MPs in wastewater is a complicated task both technically and economically. For this reason, often just a few target compounds are 233 234 reported in monitoring studies and potential impacts are calculated with these incomplete data (Aemig et al., 235 2021; Alfonsín et al., 2014; Rahman et al., 2018). For example, transformation products which arise from 236 oxidative treatments and are not included in the LCA may increase ecotoxicity of the treated effluent (Vogna 237 et al., 2004).

The breakdown of the freshwater ecotoxicity impact contributions demonstrate that copper and zinc are by far the greatest contributors (90%) in baseline and AWT effluents, with organic MPs accounting for less than 10% of the total impact (Annex Table 5a). These results on freshwater ecotoxicity impact also underline that five organic MPs ranked among the top ten contributors, estradiol, triclosan, cybutryne (irgarol), HHCB (Galaxolid), and 4-NP1EO which have significant ecotoxicity potentials (Figure 3).





Breakdown of major freshwater ecotoxicity contributors (% of the total impact)

244

245 Figure 3. Top ten contributors on freshwater ecotoxicity for AWT discharges, expressed in % of the total impact

Similarly, the breakdown of human toxicity impacts (respectively, cancer and non-cancer) proves once again that nickel and arsenic contribute almost single-handedly to the total impacts. Seven organic MPs rank among the top ten contributors on the human toxicity (cancer) impact: fluoranthene, oxazepam, ethinyl estradiol, metronidazole, atrazine, cyclophosphamide and acetaminophen. While on the human toxicity (noncancer), diclofenac, AHTN (tonalid) and ketoprofen are among the leading organic MPs (Annex Table S5b). Five novel organic MPs (HHCB, 4-NP1EO, AHTN and ketoprofen) that were added in the USEtox v2 model 252 appeared among the first ten contributors on these impacts, which highlights the importance of 253 complementing existing (eco)toxicity models to refine further the environmental assessment of AWT systems 254 (Figure 4).







256

Figure 4. Top ten contributors on human toxicity (a. cancer and b. non-cancer) for AWT discharges, expressed in % of the total
 impact.

259 On the whole, impacts of effluent discharges are generally reduced after GAC treatment except on 260 human toxicity non cancer, with arsenic release (Choubert et al., 2014) and on freshwater eutrophication due 261 to phosphates based on a pilot-scale study (Mailler et al., 2015). However, these removal efficiencies should 262 benefit from consolidated measurements to provide greater accuracy in scenario comparisons.

263 **3.2.** Long term vs short term impacts (mid-to-endpoint)

A distinction between long term and short term seems necessary to further analyse toxicity-related impacts with a strong dominance of inorganic MPs over organic MPs. Indeed, current impact assessment methods are not adequately mechanistic or capable of combining the potential impacts of organic compounds with those of metals (Pradinaud et al., 2019). Due to this limitation in LCIA methods, metals tend to significantly impact on toxicity and ecotoxicity indicators compared to degradable organic MPs due to their persistence in the environment in different dissolved or particulate forms (Aemig et al., 2021; Brudler et al., 2019; Lorenzo-Toja et al., 2016; Risch et al., 2018). With the temporal horizon distinction at the mid-toendpoint level in the Impact World+ method (Bulle et al., 2019), the impacts of metals and persistent organic pollutants can be differentiated into short-term (first 100 years) and longer-term impacts (beyond 100 years).

273 Results for the ozone scenarios effectively highlight significant organic MP removal and reduced 274 negative impacts of about an order of magnitude on the short-term horizon for aquatic ecosystems 275 (freshwater ecotoxicity short-term indicator) compared to baseline scenario as shown in logarithmic scale in 276 Figure 5. However, as shown in Figure 4 and more detailed in Annex Table S7, AWT effluent discharges 277 contributed modestly (respectively 10% and 7% for ozone scenarios and GAC) to the overall freshwater 278 ecotoxicity indicator, behind indirect resource demands (respectively 90% and 93%). Hence, the net 279 increases in freshwater ecotoxicity long-term indicators for AWT scenarios with metals emissions originate 280 mostly from background processes.



281

Figure 5. Temporal horizon distinction on freshwater ecotoxicity indicator (mid-to-endpoint level, IW+ method). Short-term impacts occur after emission until 100 years, while long-term impacts occur beyond 100 years. Impact results are expressed on a logarithmic scale to inform on the order of magnitude differences between short and long-term impacts. Detailed contributions on the short-term freshwater ecotoxicity indicator are given in Supplementary information (Table S6).

286 Conversely, benefits of organic MP removal are not evidenced on (human) health-related impacts 287 (See Annex Figure S1). As demonstrated in Aemig et al. (2021), the total impact of organic MPs released in 288 the aquatic environment through WWTP effluents on human health was low due to (i) no direct exposure 289 routes for organic MPs (e.g. to capture potential endocrine disruption effects), (ii) the buffer role of the 290 environment where the MP loads are diluted, and (iii) the low MP loads after AWT (Simazaki et al., 2015). 291 Unsurprisingly, metals are leading the long-term freshwater ecotoxicity impacts, with copper, zinc and nickel.

292 Detailed impact contributions on short-term freshwater ecotoxicity (Annex Table S6) reveal the most 293 potent ecotoxic MPs in baseline and AWT effluents which are hormones (estradiol), pesticides (triclosan), 294 industrial substances (alkylphenols group) and a fragrance (HHCB).

295 3.3. Comparative analysis of AWTs

296 In this section a comparative LCA is performed between three AWT systems and the baseline 297 scenario using the chosen functional unit. Given the four studied scenarios, in total six pair-wise comparisons were performed to rank the compared systems (Igos et al., 2018). However, as noted by Guérin-Schneider et al. (2018) the interpretation of results for different scenarios on the full range of 18 impact categories defined in Impact World+ is often complex due to cognitive obstacles. Hence, a decision tree (Guérin-Schneider et al., 2018) in Figure 6 helped structure the decision-making by proposing explicit simplification modalities to select relevant impact categories (Annex Table S11).

303



304

Figure 6. Decision-support procedure for the analysis of LCIA results leading to a choice backed on biophysical criteria
 among several scenarios (adapted from Guérin-Schneider et al, 2018)

307 Overall, the simplified interpretation of results leads to the following ranking of scenarios in order of

308 increasing environmental impacts: 1. Baseline < 2b. Ozone (air) < 3. GAC < 2a. Ozone (O2).



1. Baseline < 2b. Ozone (air) < 3. GAC < 2a. Ozone (O2)

Figure 7. Pairwise comparisons of scenarios using the simplified decision-support procedure (Guérin-Schneider et al. 2018)
Indeed results show that use of ozone produced with air and GAC are equivalent on ecosystems
quality with less impacts than oxygen-fed ozone. Also, ozone produced with air appears as a better AWT
choice compared with GAC or oxygen-fed ozone in terms of human health endpoints for the specific
operating conditions in this study (Figure 8 and Figure 9) accounting for inventory data quality and spread
(on the 65 MPs monitored in AWT discharges (See Annex Table S2). However, the baseline scenario (no
AWT) demonstrate clear increases in net environmental impacts for all AWT scenarios at this endpoint level.





Figure 8. Comparison of AWT scenarios at endpoint level (IW+ method) with detailed contribution breakdown in relative values
(%) on the damage indicators: a. Ecosystems quality and b. Human health.







Figure 9. Comparison of AWT scenarios at endpoint level (IW+ method) with detailed contribution breakdown in absolute
 values on the damage indicators: a. Ecosystems quality (PDF.m².yr) and b. Human health (DALY).

325

Uncertainties around impact results were estimated (Annex Table S7) with mean values and standard deviations with 95% confidence intervals using the Monte Carlo randomization on process parameters. Sensitivity analyses on selected parameters such as energy source and inputs used in the process which showed significant impact contributions at the endpoint level are important for wastewater systems in general (Igos et al., 2021; Rebello et al., 2020). Considering an European electricity mix (Wernet et al., 2016) instead of the French electricity mix with an important nuclear energy share, for the ozone scenarios (2a and 2b) greatly alters the results of the comparative LCA with now non-significant differences between air-fed ozone generators and oxygen-fed ozone generators (Annex Table S10). This result underlines the importance of specifying the geographical context of this study.

336 Under the modelling assumptions of this study oxygen-fed ozone did not show net environmental 337 benefits relative to air-fed ozone due to a significant increase in impacts from the extra energy demand, based on a weighted mean value across reviewed studies around 19 kWh/kgO3. However, using detailed 338 339 measurements on a full scale French WWTP with ozone treating 30 000 PE, the ozonation step (comprising 340 of air production, ozone generation, ozone destruction, ventilation and cooling) had a global energy demand 341 of 32 kWh/kgO3 (See Annex Table S2). A sensitivity analysis on this energy demand for ozone scenarios 342 showed that the latter value yielded impact increases of about 13% and 18% on human health and 343 ecosystems endpoints (See Annex Figure S2), which underlines the significance of this choice of parameter 344 value in the LCA in agreement with Igos et al. (2021).

Regarding inputs such as reagent production, the GAC scenario could benefit from a further reduction in impacts from activated carbon since its contributions to endpoints were significant despite the hypotheses on GAC reactivation with 20% of GAC lost during regeneration as an alternative of using fresh activated carbon after every breakthrough event (Igos et al., 2021; Rahman et al., 2018; Sbardella, 2019). A sensitivity analysis on the GAC regeneration rates shows that using 10% regeneration losses (compared to 20%) yielded moderate reductions in impacts at endpoint level of 5% on Human health and 8% on ecosystems guality (See Annex Figure S3).

352 4. Conclusions

The objective of this study was to carry out an environmental impact assessment of AWTs (e.g. ozone treatment and granular activated carbon adsorption) taking into account removal efficiencies on 65 MPs among different chemical groups. Major results are highlighted in the following, as well as recommendations and challenges on the way to conduct such a LCA:

Efficiencies of AWT systems were determined in this LCA study with 31 new toxicity and ecotoxicity
 potentials for MPs in the USEtox v2 model library. Metals (e.g. copper and zinc) contribute
 significantly to ecotoxicity impacts.

- Five novel organic MPs (HHCB, 4-NP1EO, AHTN and ketoprofen) that were added in the USEtox v2
 model library appeared among the first ten contributors on freshwater ecotoxicity and human toxicity
 impacts.
- Comparative LCA results reveal multiple environmental trade-offs of AWT when considered on a life
 cycle basis. The local water quality benefits achieved from the reduction of MPs in effluent are
 largely outweighed by the indirect toxicity at a regional level resulting from high resource use (e.g.
 electricity consumption and feed-gas).
- Hence it is important to develop detailed life cycle inventories and modelling assumptions concerning
 background processes, with uncertainty quantification on future LCA studies for AWT systems
 especially with comparative LCAs as some major parameters can alter the comparison outcomes;
- Results for the ozone scenarios effectively highlight significant organic MP removal and reduced
 negative impacts of about an order of magnitude on the short-term horizon for aquatic ecosystems.
- Most potent ecotoxic MPs in short-term freshwater ecotoxicity in all discharges were hormones
 (estradiol), pesticides (triclosan), industrial substances (alkylphenols group) and a fragrance
 (HHCB).
- Air-fed ozone and GAC are better AWT choices compared with oxygen-fed ozone on the ecosystems quality endpoint for the specific operating conditions in this study (using a French electricity mix). On human health, air-fed ozone is by far the best AWT choice, followed by GAC and finally pure oxygen-fed ozone. However these results must be interpreted carefully and provide an understanding of regionally distributed life cycle impacts which have to be complemented with knowledge of local water quality issues;
- More research on toxicity data and impact assessment models to improve organic/inorganic MP distinction in existing endpoints and to account for additional MP-relevant endpoints (e.g., endocrine disruption, synergistic effects of mixtures) and transformation products would improve the utility and representativeness of the LCA results, while process improvements may increase removal rates while lowering energy and chemical requirements. In light of the current results, however, life cycle environmental impacts should be considered while adopting management and risk mitigation strategies for MPs in combination with local risk assessment approaches.
- 388

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Table 1. AWT scenarios modelled to meet the objectives of this LCA

| Scenario | Advanced wastewater treatment (AWT) process |
|----------|---|
| 1 | Baseline (no advanced treatment) |
| 2a | Ozone (pure oxygen) |
| 2b | Ozone (air) |
| 3 | Granulated activated carbon (GAC) |

Table 2. Inventory data to treat secondary effluent from 50 000 PE during one year through the AWT processes under study

| Scenario | Ozone (air) | | Ozone (pure oxygen) | | GAC | |
|---|-------------|---------|---------------------|---------|---------|---------|
| Building materials, kg (1) | т | 2SD | т | 2SD | т | 2SD |
| Concrete | 2.6E+04 | 2.6E+03 | 2.6E+04 | 2.6E+03 | 4.9E+01 | 4.9E+00 |
| Plastics | 1.7E+00 | 1.7E-01 | 1.7E+00 | 1.7E-01 | 2.1E+01 | 2.1E+00 |
| Metals | 1.8E+03 | 1.8E+02 | 1.8E+03 | 1.8E+02 | 1.8E+02 | 1.8E+01 |
| Electricity consumption, kWh (2) | 3.2E+05 | 6.4E+04 | 2.4E+05 | 4.8E+04 | 7.3E+04 | 1.5E+04 |
| Ancillary chemicals consumption, kg (2) | | | | | | |
| Oxygen (pure) | | | 1.5E+05 | 3.0E+4 | | |
| Activated carbon (fresh) | | | | | 1.1E+04 | 2.2E+03 |
| Activated carbon (reactivated) | | | | | 2.8E+04 | 5.6E+03 |

Details in Supporting information: (1) Table S1, (2) Table S2

| | | · | | Removal efficiencies ^b of AWT processes (%) | |
|-----------------------|---------------------------------|---------------------------------------|--|---|------------------|
| | | manuful concentration ^d in | estimated mass loading in | | |
| Group | Compounds | secondary effluent (ng/l) | secondary effluent (g/L) with 50000 | ozonation | activated carbon |
| | | | PE capacity and 150L/(PE.d) | Ozonation | |
| | | | | | |
| F ue group and | ADBI (Celestolid) | 1.69E+03 | 1.27E+01 | 80.0 | 95.0 |
| Fragrances | AHIN (Ionalid) | 7.60E+02 2.06E+02 | 5.70E+00 2.20E+01 | 80.0 | 95.0 |
| | Estradiol | 2 23E+01 | 2.29E+01 1.68E-01 | 80.0 97 5 | 87.0 76.0 |
| | Estrone | 1.59E+01 | 1.20E-01 | 93.5 | 82.0 |
| Hormones | Ethinyl Estradiol | 1.67E+00 | 1.25E-02 | 92.5 | 95.1 |
| | Progesterone | 2.24E+01 | 1.68E-01 | 0 | 79.5 |
| | Testosterone | 2.90E+01 | 2.18E-01 | 95.0 | 80.0 |
| | 4-nonylphenol | 4.79E+02 | 3.59E+00 | 22.4 | 75.0 |
| | 4-tert-butylphenol | 1.42E+02 | 1.07E+00 | 50.0 | 90.0 |
| | Bisphenol A | 4.78E+02 | 3.58E+00 | 95.0 | 74.5 |
| | Ethylparaben | 1.40E+02 | 1.05E+00 | 99.0 | /1./ |
| (various) | | 5.07E+02 | 4.252+00 | 98.0 | 73.3 |
| | NP1EO NP2EO | 4.41E+02 3.40E+02 | 2 555+00 | 95.0 | 67.7 |
| | Propylparaben | 4.38E+02 | 3.29E+00 | 80.0 | 85.0 |
| | | | | 0010 | 0010 |
| Polycyclic Aromatic | Fluoranthene | 6.82E+01 | 5.12E-01 | | |
| Hydrocarbons | | | | 50.0 | 42.0 |
| | Acetaminophen | 3.71E+01 | 2.78E-01 | 90.4 | 89.7 |
| | Alprazolam | 3.48E+00 | 2.61E-02 | 79.0 | 0 |
| | Amitriptyline | 2.91E+01 | 2.19E-01 | 48.0 | 46.0 |
| | Atenolol | 1.27E+03 | 9.56E+00 | 93.4 | 95.9 |
| | Azithromycin | 2.30E+02 | 1.73E+00 | 84.5 | 69.0 80 F |
| | Carbamazepine | 7.89E+02 | 5.922+00 | 97.9 71 F | 80.5 |
| | Citalopram | 4.78L+02 1 70F+02 | 1 285+00 | 71.5 | 49.0 57 5 |
| | Clarithromycin | 5.10F+02 | 3.82E+00 | 96.3 | 92.0 |
| | Cyclophosphamide | 6.75E+00 | 5.06E-02 | 84.0 | 0 |
| | Diazepam | 8.79E+01 | 6.59E-01 | 86.5 | 71.5 |
| | Diclofenac | 8.57E+02 | 6.43E+00 | 97.4 | 78.3 |
| | Erythromycin | 2.22E+02 | 1.66E+00 | 89.9 | 68.4 |
| | lohexol | 1.52E+04 | 1.14E+02 | 38.0 | 49.8 |
| Pharmaceuticals | Ketoprofen | 1.11E+03 | 8.35E+00 | 73.3 | 68.5 |
| | Metoprolol | 1.17E+02 | 8.80E-01 | 92.5 | 97.0 |
| | Metronidazole | 7.88E+02 | 5.91E+00 | 72.0 | 79.0 |
| | Naproxen | 8.58E+02 | 6.43E+00 2.515±00 | 94.0 | 49.7 |
| | Oflovacin | 3.34E+02 1 56E±02 | 2.51E+00 1 17E+00 | 03.0 91.8 | 87.0 75.8 |
| | Oxazepam | 5.29F+02 | 3.97E+00 | 84.3 | 60.5 |
| | Propranolol | 1.92E+02 | 1.44E+00 | 97.5 | 95.8 |
| | Roxithromycin | 4.30E+01 | 3.22E-01 | 84.7 | 69.0 |
| | Simvastatine | 7.18E+02 | 5.39E+00 | 70.0 | 65.0 |
| | Sotalol | 1.84E+03 | 1.38E+01 | 98.0 | 90.0 |
| | Sulfamethoxazole | 3.86E+02 | 2.90E+00 | 96.1 | 64.9 |
| | Sulfapyridin | 4.92E+02 | 3.69E+00 | 91.0 | 82.2 |
| | Tetracycline | 2.50E+01 | 1.88E-01 | 77.5 | 54.9 |
| | rimetnoprim Venlafavino | 3.39E+02 | 2.54E+UU | 93.9 05 5 | 91.0 |
| | Arsenic | 2.30E+U2 5 68F±03 | 1.92C+00 1.92C+00 | د.ده ۲ ۸ | 04.U -107 |
| | Barium | 5.06E+02 | 4.200+00 5 13F+01 | 15.0 | -28.0 |
| | Chromium | 1.44E+03 | 1.08E+01 | -4.0 | 92.0 |
| | Copper | 5.72E+03 | 4.29E+01 | 4.0 | 84.0 |
| Inorganics | Lead | 5.03E+02 | 3.77E+00 | 35.0 | 97.0 |
| | Molybdenum | 4.20E+03 | 3.15E+01 | 8.5 | -1.0 |
| | Nickel | 9.83E+03 | 7.37E+01 | 10.5 | 56.0 |
| | Vanadium | 1.34E+03 | 1.00E+01 | 15.0 | -205.0 |
| | Zinc | 2.97E+04 | 2.22E+02 | 9.0 | 49.0 |
| | AMPA | 2.06E+03 | 1.55E+01 | 50.0 | 6.4 |
| | | 2.34±+01 | 1./0E-U1 2.255.01 | 42.U 22 2 | 80.8 50.0 |
| | | 3.00E+01 2.07E±02 | 2.23E-U1 1 55F±00 | 55.5 88 7 | 50.0 Q2 1 |
| Pesticides | Imidaclopride ("Neonicotinoid") | 6 94F+01 | 5,21F-01 | 67.0 | 89.0 |
| | Isoproturon | 4.34E+01 | 3.25E-01 | 68.0 | 87.0 |
| | Simazine | 2.18E+01 | 1.64E-01 | 50.0 | 91.0 |
| | Terbutryn | 3.80E+01 | 2.85E-01 | 85.0 | 80.0 |
| | Triclosan | 9.83E+02 | 7.37E+00 | 75.0 | 56.3 |
| _ | | | | | |
| Classical pollutants | Nitrite (NO2-) | 1.35E+05 | 1.01E+03 | 78.0 | 94.2 |
| | Phosphate (PO4-) | 8.30E+05 | 6.23E+03 | /8.0 | -26.3 |

Table 3. Selected MPs with measured concentrations, estimated mass loadings in secondary effluents from WWTPs entering advanced treatment processes and associated removal efficie

^{*a*} Sources of MP concentrations: AMPERES project (Martin Ruel et al., 2012; Bruchet et al., 2015), MICROPOLIS-PROCEDES project (Choubert et al., 2017b), Li et al. (2019) ^{*b*} Sources of MP removal efficiencies: Li et al., 2019; Guillossou et al., 2019, 2020; Mailler et al., 2015; Rahman et al., 2018; Choubert et al., 2014, 2017b; Bourgin et al., 2018. ncies

Table 4. Data quality and uncertainty estimation for two life-cycle stages: construction and use (including operation, maintenance and AWT effluent discharges)

| Life cycle stage | Inventory (LCI) component | Distribution type | Uncertainty characterisation (1) | Uncertainty source | | | |
|---|---|----------------------|----------------------------------|---------------------------|--|--|--|
| Construction stage | Materials manufacturing (kg) | | Ecoinvent (2) | | | | |
| (infrastructure) | Amount of material used (kg) | Normal | CV=5% | see (3) | | | |
| | Electricity production (kWh) | | Ecoinvent (2) | | | | |
| Use stage | Amount of electricity consumption (kWh) | Normal | CV=10% | see (3) | | | |
| (Operation & | Ancillary chemicals production (kg) | | Ecoinvent (2) | | | | |
| discharges) | Amount of ancillary chemicals used (kg) | Normal | CV=10% | see (3) | | | |
| | Micropollutants load discharged in effluents (g) | Normal | CV=20% | (Versini et al., 2016) | | | |
| (1) CV= coefficien | (1) CV= coefficient of variation. Uncertainty information is provided with mean average values and standard | | | | | | |
| deviation. | | | | | | | |
| (2) Uncertainty from the Ecoinvent database when defined, assessment of data quality based on a pedigree | | | | | | | |
| matrix (Weidema and Wesnaes, 1996). For our system, up to 70% of the Ecoinvent processes have available uncertainty information. | | | | | | | |
| (3) Estimated uncertainty (SD) based on expert judgement | | | | | | | |