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1 Traction open boundary condition for incompressible,
2 turbulent, single- or multi-phase flows, and surface wave
3 simulations

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9 **Abstract**

In simulations, artificial boundaries need to be introduced to limit the size of computational domains and thereby lower computational cost. At these boundaries, flow variables need to be calculated in a way that will not induce any perturbation of the interior solution, which poses a great challenge in incompressible flows. In this paper, we demonstrate the potential of a new traction open boundary condition to address the classical problems encountered in simulations with open boundary conditions: backflow instability, wave reflections, and confinement caused by the proximity of the outlet. This novel boundary treatment, based on a Lagrangian estimation of the traction in the outlet section coupled to a stabilization term, is shown to provide accuracy and stability for turbulent, single- or multi-phase flows, test cases. Using a simulation of surface gravity waves, we show that if special care is given to the computation of the estimated traction, it is possible to get a fully non-reflective open boundary condition.

10 *Keywords:* Outflow, non-reflective boundary, backflow instability

11 **1. Introduction**

12 Due to the finite nature of numerical simulations, it is often necessary
13 to truncate computational domains. This requires imposing artificial bound-
14 aries along with the associated mathematical conditions that close the system
15 of equations to be solved. The primary goal of such boundaries is to restrict

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16 the computation to a given region of interest without perturbing the solution
17 inside the domain, thereby limiting cost. In the case of outflow boundaries,
18 the flow should be allowed to leave the computational domain in the most
19 natural way possible without undergoing any perturbations that could prop-
20 agate upstream and thus pollute the upstream solution. Moreover, complex
21 dynamics may occur at the artificial boundary and the flow may contain re-
22 gions of both outflow and backflow, i.e., regions of flow reversal where the
23 outlet boundary acts as an inlet, potentially polluting the solution [1].

24 The definition of an ideal open boundary condition (OBC) for incompress-
25 ible fluid dynamic simulations is still an unresolved topic, as demonstrated by
26 Sani and Gresho after the “Open boundary condition minisymposium” [2],
27 or by other authors in recent reviews [1, 3]. However, one can describe the
28 effect of a non-ideal OBC on a simulation result. In wave-like simulations,
29 the phenomena of wave reflection can create unrealistic flows, instabilities
30 and prevent the flow from reaching a statistical equilibrium over a long com-
31 putational time [4]. In turbulent flows, the presence of backflow can cause
32 the system to experience an uncontrolled growth in kinetic energy, which has
33 for example been evidenced in biofluids simulations [5].

34 More generally, the choice of OBC can severely influence the size of the
35 computational domain due to the difficulty of finding a condition that does
36 not durably affect the upstream flow, the most famous example being the
37 impact of the outflow position on a cylinder drag and lift coefficients [6].
38 Indeed, the incompressibility constraint and the unphysical nature of domain
39 truncations may prevent finding a perfect OBC. However, in this paper,
40 we endeavor to present a novel boundary treatment that reduces the error
41 induced by outlet position on severely truncated domains and is stable to
42 backflow, in addition to satisfying the incompressibility constraint.

43 In the next section, the main types of outflow treatments are discussed.
44 The new proposed strategy is then presented. In section 3, the numerical im-
45 plementations of these boundary conditions are presented in the context of a
46 fractional step method with pressure projection method. Section 4 is devoted
47 to single phase test cases, consisting of the Kovasznay flow for measuring spa-
48 tial convergence, a time-dependent manufactured solution test for measuring
49 temporal convergence, and a flow past a square and a turbulent plane jet
50 to explore the stability and accuracy of the method. Finally, multiphase
51 test cases are considered in section 5, with the convection of a high density
52 droplet, a turbulent swirling liquid jet, and the transport of surface gravity
53 waves. All of the work presented hereafter is applied to outlet boundary con-

54 ditions where the flow is expected to be mostly leaving the computational
55 domain, but it can be applied as well on lateral and inlet boundaries.

56 2. Existing methods and present work

57 Before giving a short review of existing methods we introduce here some
58 useful notations. The computational domain will be referred to as Ω . This
59 domain is bounded by real and artificial (open) boundaries. The firsts ones are
60 denoted $\partial\Omega_d$ and the others $\partial\Omega_o$. $\partial\Omega$ will refer to both types of boundaries,
61 i.e., $\partial\Omega = \partial\Omega_d \cup \partial\Omega_o$. The vector \mathbf{n} is defined as the unit normal to those
62 boundaries, always oriented toward the exterior of the domain.

63 2.1. Existing methods

64 Apart from classical Dirichlet and Neumann conditions, one of the most
65 widely used boundary conditions is the convective boundary condition,

$$\frac{\partial\phi}{\partial t} + c \frac{\partial\phi}{\partial n} = 0. \quad (1)$$

66 This equation represents the transport of a quantity ϕ through a boundary
67 of normal \mathbf{n} with a phase speed c , where n is the coordinate in the \mathbf{n} direc-
68 tion. This condition, known as the Sommerfeld equation, or the radiation
69 condition, is in fact an exact absorbing condition, i.e., specification of the
70 incoming characteristic to zero, for a 1D wave equation with a constant wave
71 speed [1]. The most famous choice of phase speed comes from the work of
72 Orlandi [7]: c is computed locally based on known values of ϕ in the vicinity
73 of the boundary. This solution has been shown to result in a phase velocity
74 close to white noise [8]. Despite some improvements of Orlandi's method
75 [9], it seems that no satisfying method has emerged to obtain an accurate
76 estimation of the phase velocity without *a priori* knowledge of it [1, 10].

77 A general mathematical approach to obtain exact absorbing boundary
78 conditions has been derived [11]. However, to our knowledge, no applications
79 of this method to Navier-Stokes equations have been presented, the closest
80 being recent progress on shallow-water equations [1]. It has been applied to
81 a 2D wave equation whose coefficients are then identified using the Navier-
82 Stokes equations [12]. It results in a condition similar to Eq. (1) with the
83 phase velocity evaluated as the local speed and the presence of a viscous term
84 on the right hand side. More generally, a whole family of OBCs relies on the
85 method of characteristics [1].

86 On the other hand, another type of boundary condition can be directly
 87 derived from the Navier-Stokes equation in its weak form [13]: the traction
 88 boundary condition. It consists of applying a condition on the normal stress
 89 at the artificial boundary,

$$\bar{\boldsymbol{\sigma}} \cdot \mathbf{n} = (-p\mathbf{I} + \mu(\nabla\mathbf{u} + \nabla\mathbf{u}^T)) \cdot \mathbf{n} = \mathbf{t}, \quad (2)$$

90 where $\bar{\boldsymbol{\sigma}}$, p , μ and \mathbf{u} are the stress tensor, the pressure, the dynamic viscosity,
 91 and the velocity, respectively. \mathbf{t} is a traction vector that must be prescribed.
 92 No clear guidelines exist for the choice of this vector. The most widespread
 93 choice is $\mathbf{t} = \mathbf{0}$, giving the well-known “traction-free” boundary condition
 94 [14, 15]. The traction \mathbf{t} has also been computed locally and iteratively [13],
 95 based on previous runs on longer domains [2], or defined analytically with a
 96 Stokes solution [16].

97 As stated previously, the presence of backflow at an outlet boundary could
 98 lead to an instability due to an uncontrolled growth of kinetic energy. To
 99 understand it, the energy balance in the overall computational domain, Ω ,
 100 can be considered [17, 18],

$$\begin{aligned} \frac{\partial}{\partial t} \int_{\Omega} \frac{1}{2} \rho |\mathbf{u}|^2 &= - \int_{\Omega} \frac{\mu}{2} \|\mathbf{D}(\mathbf{u})\|^2 + \int_{\Omega} (\rho \mathbf{g} + \mathbf{T}_{\sigma}) \cdot \mathbf{u} \\ &+ \int_{\partial\Omega_d} \left(\bar{\boldsymbol{\sigma}} \cdot \mathbf{n} - \frac{1}{2} \rho |\mathbf{u}|^2 \mathbf{n} \right) \cdot \mathbf{u} \\ &+ \int_{\partial\Omega_o} \left(\bar{\boldsymbol{\sigma}} \cdot \mathbf{n} - \frac{1}{2} \rho |\mathbf{u}|^2 \mathbf{n} \right) \cdot \mathbf{u}, \end{aligned} \quad (3)$$

101 Where ρ is the density, \mathbf{g} is the gravity vector, $\mathbf{D}(\mathbf{u})$ is the shear rate tensor
 102 and \mathbf{T}_{σ} represents surface tension forces. It results that the rate of change
 103 of kinetic energy is controlled by viscous dissipation (exchange with internal
 104 energy), gravity (exchange with potential energy), surface tension (exchange
 105 with surface energy) and by two surface terms. The first one is expressed
 106 on $\partial\Omega_d$, the Dirichlet boundaries, where variables are known. The second
 107 surface term is expressed on $\partial\Omega_o$, the outflow boundary, where all variables
 108 have to be computed. In case of backflow, the convective part of this term
 109 becomes positive and can lead to a global increase of kinetic energy, leading
 110 to the instability of the system.

111 Following Eq. (3), one possible backflow treatment is to ensure that the
 112 last term is zero, preventing backflow from causing an unstable growth of

113 kinetic energy. It leads to the following OBC

$$\bar{\bar{\boldsymbol{\sigma}}} \cdot \mathbf{n} = (-p\mathbf{I} + \mu(\nabla\mathbf{u} + \nabla\mathbf{u}^T)) \cdot \mathbf{n} = \frac{\rho}{2}f(\mathbf{u})\mathbf{n}, \quad (4)$$

114 with $f(\mathbf{u})$ chosen so that it cancels the last term of Eq. (3) in case of backflow,
115 for example

$$f(\mathbf{u}) = \begin{cases} (\mathbf{u} \cdot \mathbf{n})^2 & \text{if } \mathbf{u} \cdot \mathbf{n} < 0, \\ 0 & \text{otherwise.} \end{cases} \quad (5)$$

116 This condition is similar to the stabilized traction-free condition used for
117 single phase flows [17, 19] and for multiphase flows [18, 20]. In case of back-
118 flow, the normal stress will compensate the normal influx of kinetic energy,
119 whereas it will vanish in case of outflow. Different forms for $f(\mathbf{u})$ along with
120 other types of backflow treatments have been reviewed [3].

121 The traction boundary condition, when used as the stabilized traction-
122 free condition as in Eq. (4), requires the flow to be well-developed before
123 reaching the boundary [13]. Several methods have already been proposed to
124 combine stability and accuracy even at high Reynolds number, such as the
125 “convective-like” traction boundary condition [21],

$$\bar{\bar{\boldsymbol{\sigma}}} \cdot \mathbf{n} = -\mu D_0 \frac{\partial \mathbf{u}}{\partial t} + \frac{\rho}{2} \Theta(\mathbf{u} \cdot \mathbf{n}) ((\mathbf{u} \cdot \mathbf{n})\mathbf{u} + |\mathbf{u}|^2 \mathbf{n}), \quad (6)$$

126 where D_0 is computed using a characteristic velocity, and the function $\Theta(x)$
127 is essentially equal to 1 for negative value of x and 0 otherwise, see [21]
128 for more details. The value of D_0 is found to have little effect on the overall
129 flow, except on the flow patterns near the outlet boundary. An earlier method
130 developed by Bruneau and Fabrie [16] combines a stabilization to backflow
131 and a non-zero traction,

$$\bar{\bar{\boldsymbol{\sigma}}} \cdot \mathbf{n} = \bar{\bar{\boldsymbol{\sigma}}}^{ref} \cdot \mathbf{n} + \frac{\rho}{2} (\mathbf{u} \cdot \mathbf{n})^- (\mathbf{u} - \mathbf{u}^{ref}), \quad (7)$$

132 where the reference values are computed using an analytical solution, or eval-
133 uated from known values inside the domain [22], and $(\mathbf{u} \cdot \mathbf{n})^- = \max(0, -\mathbf{u} \cdot \mathbf{n})$.
134 Note that this condition leads to a well-posed problem [23]. It has, to the
135 best of our knowledge, not been applied to projection methods.

136 Another potential backflow treatment is to simply force all velocities such
137 that $\mathbf{u} \cdot \mathbf{n} < 0$ to zero, thus preventing any influx of kinetic energy. This
138 solution provides energy stability of the system, but we will show in section

139 5.1 that it can lead to severe inaccuracies in multiphase flows. In [4], when
 140 the phase velocity is computed as $\mathbf{u} \cdot \mathbf{n} < 0$, the use of external data allows
 141 to limit the occurrence of the backflow instability.

142 As said in the introduction, the main difficulties encountered by out-
 143 flow treatments are associated with the proper transmission of perturbations
 144 through the artificial boundary, and to the presence of inflow/backflow re-
 145 gions on it. One common way to overcome those issues is to try to dissipate,
 146 or damp, the fluctuating energy of the flow before the outlet using artifi-
 147 cial zones called sponge layers or nudging layers. Sponge layers consist in
 148 the introduction of a dissipative source term in Navier-Stokes equations that
 149 becomes stronger when getting closer to the boundary [24]. Nudging layers
 150 consist of the relaxation of the flow towards prescribed external data [4].
 151 These solutions are intentionally excluded from our study to focus on the
 152 improvements of an accurate OBC.

153 Finally, most efforts to get non-reflective and accurate boundaries have
 154 been focused on convective-like OBCs, often requiring the use of external
 155 data that is consistent with the backflow treatment [4], whereas traction
 156 boundary conditions present an easier way to deal with backflow without
 157 the need for external data. As said previously, the stabilized traction-free
 158 condition, Eq. (4), requires the flow to be well-developed before reaching
 159 the boundary [13]. Traction boundary conditions have, to our knowledge,
 160 never been applied to problems of wave reflections.

161 2.2. Generalized traction boundary condition

162 We propose a new traction boundary condition, inspired from the Bruneau
 163 and Fabrie condition Eq. (7), that combines the two following characteristics.
 164 Firstly, the flow will not be required to be well-developed at the boundary,
 165 which will be achieved by applying a non-zero traction at the boundary. Sec-
 166 ondly, this OBC will be stable to influxes of kinetic energy due to backflow,
 167 which will be achieved by the inclusion of a stabilization term.

168 We express the traction at the boundary as

$$(-p\mathbf{I} + \mu(\nabla\mathbf{u} + \nabla\mathbf{u}^T)) \cdot \mathbf{n} = \mathbf{t}^{stab} + \alpha\mathbf{t}^{est}. \quad (8)$$

169 \mathbf{t}^{stab} is a numerical treatment to ensure stability to backflow. \mathbf{t}^{est} is an esti-
 170 mation of the traction at the outlet boundary and $\alpha = [0; 1]$ is an adjustable
 171 parameter. The accuracy of the present boundary treatment will depend on
 172 the choice of the last two terms.

173 Following Eq. (3), the stabilization term is taken such that it cancels the
 174 term responsible for the backflow instability in case of backflow,

$$\mathbf{t}^{stab} = \frac{\rho}{2} f(\mathbf{u}) \mathbf{n}, \quad (9)$$

175 with $f(\mathbf{u})$ defined as in Eq. (5). Thus, the kinetic energy variation at the
 176 open boundary is not equal to zero, as with Eq. (4), but depends on the value
 177 of $\alpha \mathbf{t}^{est}$. The results presented in this paper show that this novel boundary
 178 condition is sufficient to ensure the stability of the system in the presence of
 179 backflow at the open boundary. If α is equal to zero, one can see that we
 180 recover the stabilized traction-free condition presented in [17].

181 To obtain the best possible traction estimate we introduce here the gener-
 182 al idea behind our work. We propose \mathbf{t}^{est} , the estimated traction at the
 183 boundary, to be considered as a Lagrangian quantity. Its value can therefore
 184 be evaluated using an advection equation,

$$\frac{\partial \mathbf{t}^{est}}{\partial t} + \mathbf{u}_{ad} \cdot \nabla \mathbf{t}^{est} = \mathbf{0}, \quad (10)$$

185 where \mathbf{u}_{ad} is an advection velocity that can be computed using an analytical
 186 expression, an averaged or a local velocity.

187 2.3. Scope of this work

188 The previous method to estimate the traction is very general and studying
 189 all possible ways to resolve it is beyond the scope of the present paper.
 190 Thus, we restrict our study to a few particular cases. We first assume a
 191 one dimensional advection velocity of the estimated traction in the outlet
 192 boundary normal direction. Then, we assume a first order explicit temporal
 193 resolution of Eq. (10) on a cartesian grid. The choice of an explicit resolution
 194 is a consequence of the algorithm used to solve the coupling between velocity
 195 and pressure, as we detail in the next section. Finally, we use a first order
 196 upwind discretization of the spatial term in order to use values inside the
 197 computational domain.

198 The traction estimation is therefore expressed as

$$\mathbf{t}^{est} = [\phi \bar{\bar{\sigma}}_{BC-1} \cdot \mathbf{n} + (1 - \phi) \bar{\bar{\sigma}}_{BC} \cdot \mathbf{n}], \quad (11)$$

199 where the notations $BC - 1$ and BC refer to the point just before the
 200 boundary and the boundary point, respectively. ϕ is an interpolation coef-
 201 ficient computed using numerical parameters and the one dimensional ad-
 202 vection velocity. ϕ can be considered as a CFL condition and therefore has

203 here to be kept in the range $[0; 1]$ as the advection is only done between the
 204 boundary point and its closest neighbour.

205 The previous choices of resolution for Eq. (10) are not suitable in case
 206 of discontinuities in the traction field. This latter point is limiting in case
 207 of multiphase flows due to the effect of surface tension. The presence of a
 208 pressure jump can thus deteriorate the traction estimation and create un-
 209 physical velocities, or even stability issues. Therefore, in case of multiphase
 210 flows we limit our study to high Weber number. A way to get around that
 211 difficulty would be to use, for example, a semi-Lagrangian advection method
 212 [25] for \mathbf{t}^{est} . Other aspects may have to be considered, such as the curvature
 213 computation in the vicinity of the open boundary, or the density boundary
 214 condition. Note that the use of multiphase traction-free condition in phase
 215 field method provides a natural way to get around that difficulty as a surface
 216 tension term appears in the outlet boundary energy flux [18].

217 For $\alpha = 0$, the generalized traction boundary condition, Eq. (8), reduces
 218 to

$$(-p\mathbf{I} + \mu(\nabla\mathbf{u} + \nabla\mathbf{u}^T)) \cdot \mathbf{n} = \frac{\rho}{2}f(\mathbf{u})\mathbf{n}, \quad (12)$$

219 which will be referred to as the stabilized traction-free condition (TF) in the
 220 following. TF is the same condition as used in [17]. For $\alpha = 1$ and $\phi = 1$,
 221 Eq. (8) reduces to

$$(-p\mathbf{I} + \mu(\nabla\mathbf{u} + \nabla\mathbf{u}^T)) \cdot \mathbf{n} = \frac{\rho}{2}f(\mathbf{u})\mathbf{n} + \bar{\sigma}_{BC-1} \cdot \mathbf{n}, \quad (13)$$

222 which will be referred to as the estimated traction boundary condition (ET).
 223 This condition resembles the Bruneau and Fabrie condition, Eq. (7). The
 224 choice $\phi = 1$ raises the question of the dependence of the accuracy to nu-
 225 merical parameters, as the traction at the point just before the boundary
 226 may not always be a good estimation. In the final part of the article, we will
 227 consider the $\phi \neq 1$ case, where Eq. (8) reduces to

$$(-p\mathbf{I} + \mu(\nabla\mathbf{u} + \nabla\mathbf{u}^T)) \cdot \mathbf{n} = \frac{\rho}{2}f(\mathbf{u})\mathbf{n} + [\phi\bar{\sigma}_{BC-1} \cdot \mathbf{n} + (1 - \phi)\bar{\sigma}_{BC} \cdot \mathbf{n}], \quad (14)$$

228 which will be referred to as the convected traction boundary condition (CT).
 229 Note that in the previous three boundary conditions $f(\mathbf{u})$ is computed using
 230 Eq. (5).

231 In the rest of the paper we also use classic OBCs, such as the Neumann
 232 boundary condition (NM),

$$\frac{\partial \mathbf{u}}{\partial n} = 0, \quad (15)$$

233 or the convective boundary condition (CV),

$$\frac{\partial \mathbf{u}}{\partial t} + c \frac{\partial \mathbf{u}}{\partial n} = 0. \quad (16)$$

234 As mentioned previously the performance of such condition will be strongly
 235 linked to the choice of the convective velocity, which will be detailed later.

236 Finally, the main objectives of the present paper are, for each of the
 237 OBCs under consideration, to give a detailed description of the algorithm
 238 allowing to their use in the context of projection methods and VOF/Level Set
 239 methods, to demonstrate the importance of backflow stabilization in single- or
 240 multiphase flows, and to demonstrate the stability and accuracy of the non-
 241 zero traction methods, such as ET or CT. CT will only be used in the end of
 242 the paper, where the level of accuracy obtained with ET is not satisfactory.

243 3. Mathematical formulation and algorithms

244 3.1. General framework

245 Fluid dynamics are governed by conservation laws, forming the Navier-
 246 Stokes system of equations. Conservation of mass is, providing that the flow
 247 is incompressible ($\nabla \cdot \mathbf{u} = 0$),

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = \frac{\partial \rho}{\partial t} + \mathbf{u} \cdot \nabla \rho = 0. \quad (17)$$

248 Multiphase momentum conservation is written in the framework of the one
 249 fluid formulation [26]: a single equation with space varying material proper-
 250 ties is used to describe the dynamics of both phases. The effect of surface
 251 tension is added through a singular force, \mathbf{T}_σ , acting on the interface,

$$\frac{\partial \rho \mathbf{u}}{\partial t} + \nabla \cdot (\rho \mathbf{u} \mathbf{u}) = -\nabla p + \nabla \cdot (\mu [\nabla \mathbf{u} + \nabla \mathbf{u}^T]) + \mathbf{T}_\sigma + \rho \mathbf{g}. \quad (18)$$

252 In absence of phase change, the application of the momentum equation on
 253 the interface results in the classical jump condition for normal stress,

$$[p]_\Gamma = \sigma \kappa + 2 [\mu]_\Gamma \mathbf{n}_\Gamma^T \cdot \nabla \mathbf{u} \cdot \mathbf{n}_\Gamma, \quad (19)$$

254 where σ , κ and \mathbf{n}_Γ are the surface tension, the curvature and the normal vec-
 255 tor to the interface Γ respectively. The notation $[\cdot]_\Gamma$ represents the interfacial
 256 jump from liquid to gas.

257 These equations are solved using NGA, a finite volume, staggered-grid,
 258 second order flow solver [27]. Mass conservation, Eq. (17), is ensured through
 259 an unsplit semi-Lagrangian VOF advection method [25]. Momentum conser-
 260 vation, Eq. (18), is computed in a way consistent with mass transport and
 261 with the presence of interfacial discontinuities [28]. It is to be noted that
 262 all OBC methods presented are usable with any sharp interface-capturing
 263 method (VOF/Level-Set). For an application to diffuse interface methods,
 264 we refer the reader to a work for phase field method [18]. Interface boundary
 265 conditions, Eq. (19), are included in the pressure through the use of the ghost
 266 fluid method [29], with a curvature computed using a least-squares curve fit-
 267 ting method [30]. The coupling between velocity and pressure, required due
 268 to the incompressibility constraint, is enforced using an incremental pres-
 269 sure projection method [31]. In the following equations, superscripts n and
 270 $n + 1$ refer to previous and new time steps, respectively, whereas subscript
 271 k refers to the subiterations of the iterative Crank-Nicolson time advance-
 272 ment scheme [32] used in the present solver. Note that we use an implicit
 273 resolution of the linearized problem at each subiteration, see [27] for more
 274 details. Second order centered schemes are used for spatial discretization on
 275 all terms but the convective term at the interface, where a consistent mass
 276 and momentum advection strategy is employed (see [28] for more details). In
 277 case of single phase flows the same solver is used but the physical properties
 278 are taken as constant and surface tension effects are not present. First, a
 279 non-solenoidal velocity field, \mathbf{u}^*_{k+1} , is computed as

$$\begin{aligned}
 \frac{\rho_{k+1}^{n+1} \mathbf{u}^*_{k+1} - \rho^n \mathbf{u}^n}{\Delta t} &= -\nabla p_k^{n+1} - \nabla \cdot \left(\rho^n \mathbf{u}_k^{n+1/2} \left(\frac{\mathbf{u}^n + \mathbf{u}^*_{k+1}}{2} \right) \right) \\
 &+ \nabla \cdot \left[\mu^{n+1} \left(\nabla \left(\frac{\mathbf{u}^n + \mathbf{u}^*_{k+1}}{2} \right) + \nabla \left(\frac{\mathbf{u}^n + \mathbf{u}^*_{k+1}}{2} \right) \Big| \Big|^T \right) \right] \\
 &+ \rho_{k+1}^{n+1} \mathbf{g},
 \end{aligned} \tag{20}$$

280 where the intermediate velocity field is

$$\mathbf{u}_k^{n+1/2} = \frac{1}{2} (\mathbf{u}_k^{n+1} + \mathbf{u}^n). \tag{21}$$

281 Then, a Poisson equation is solved for the pressure increment Φ^{n+1} ,

$$\nabla \cdot \left(\frac{\Delta t}{\rho_{k+1}^{n+1}} \nabla (\Phi^{n+1}) \right) = \nabla \cdot \mathbf{u}_{k+1}^*. \quad (22)$$

282 Finally, the velocity and the pressure at the next time step are obtained using
283 Φ^{n+1} ,

$$\mathbf{u}_{k+1}^{n+1} = \mathbf{u}_{k+1}^* - \frac{\Delta t}{\rho_{k+1}^{n+1}} \nabla (\Phi^{n+1}), \quad (23)$$

284

$$p_{k+1}^{n+1} = p_k^{n+1} + \Phi^{n+1}. \quad (24)$$

285 Eqs. (20), (22) and (23)-(24) are referred to as *estimation*, *projection*,
286 and *correction*. Δt is the time step size. In the case of multiphase flows, ρ^n
287 and μ^{n+1} values are computed from the old and new VOF field, respectively,
288 whereas ρ_{k+1}^{n+1} is computed in a way that ensures consistency between mass
289 and momentum transport [28]. More details can be found in [33].

290 At all of these steps, boundary conditions have to be provided: velocity
291 boundary condition after estimation and correction, and pressure boundary
292 condition during projection. At the inflow and on the walls, those steps are
293 straightforward and well documented [34]. For the velocity it simply consists
294 of setting the corresponding values in the velocity vector. As these values
295 will not change during estimation and correction, this step is only necessary
296 after estimation, Eq. (20),

$$\mathbf{u}_{k+1}^* \Big|_{\partial\Omega_d} = \mathbf{u}_D^{n+1}, \quad (25)$$

297 where \mathbf{u}_D^{n+1} is an imposed velocity value given by the physics, i.e., inflow or
298 walls. The definition of the pressure boundary condition is directly obtained
299 from the application of Eq. (23) on those boundaries,

$$\frac{\partial \Phi^{n+1}}{\partial n} \Big|_{\partial\Omega_d} = 0. \quad (26)$$

300 The expression of outlet boundary conditions for velocities and pressure at
301 each step of the projection algorithm, resulting in the application of the
302 OBCs presented in section 2, is detailed in the next subsections.

303 *3.2. Implementation of convective/Neumann OBC*

304 Neumann (NM) and convective (CV) boundary conditions can be directly
 305 used to compute outlet velocities at the estimation step. In the CV boundary
 306 condition, Eq. (16), a wave velocity c has to be prescribed. In the present
 307 work, it is going to be taken as the maximal velocity in the plane just before
 308 the exit,

$$c = c_{max} = \max(\mathbf{u}_{k+1}^* \cdot \mathbf{n})_{BC-1}, \quad (27)$$

309 or as a theoretical wave speed, if available,

$$c = c_{th}. \quad (28)$$

310 The theoretical expression for the phase velocity will be detailed in the re-
 311 sults when used. Except if otherwise stated, the phase velocity will be taken
 312 as $c = c_{max}$. What is of interest here is the definition of the pressure bound-
 313 ary condition that will allow to obtain a solution to the Poisson equation,
 314 Eq. (22). This comes from the integration of Eq. (22) over the computational
 315 domain:

$$\int_{\partial\Omega} \frac{\Delta t}{\rho^{n+1}} \nabla \Phi^{n+1} \cdot \mathbf{n} dS = \int_{\partial\Omega} \mathbf{u}_{k+1}^* \cdot \mathbf{n} dS \quad (29)$$

316 Applying Eq. (26) will directly lead to the following pressure outlet boundary
 317 condition,

$$\int_{\partial\Omega} \frac{\Delta t}{\rho^{n+1}} \frac{\partial \Phi^{n+1}}{\partial n} \Big|_{\partial\Omega_o} dS = Q_{in} - Q_{out}, \quad (30)$$

318 where Q_{in} and Q_{out} are the inlet and outlet flow rates, respectively. Thus, if
 319 inlet and outlet flow rates are forced to be the same (including the clipping
 320 of negative velocities, as explained in section 2) when considering the appli-
 321 cation of the velocity OBC and the resolution of the Poisson equation, the
 322 pressure outlet boundary condition can simply be a Neumann BC,

$$\frac{\partial \Phi^{n+1}}{\partial n} \Big|_{\partial\Omega_o} = 0, \quad (31)$$

323 thus ensuring that the integral on the left hand side of Eq. (30) is equal to
 324 zero. Finally, as the gradient of pressure on all boundaries is equal to zero,
 325 there is no need to correct outlet velocities during the correction step. The
 326 overall algorithm is presented in algorithm 1.

Input: $\mathbf{u}^n, p^n, \rho^n$ in Ω and on $\partial\Omega$
1 Solve Eq. (17) using VOF advection $\rightarrow \kappa^{n+1}, \mu^{n+1}$ in Ω
2 **for** $k = 0$ **to** $k_{max} - 1$ **do**
3 Compute ρ_{k+1}^{n+1}
4 Solve Eq. (20) $\rightarrow \mathbf{u}_{k+1}^*$ in Ω
5 Apply Eq. (25) and Neumann or convective OBC on \mathbf{u}_{k+1}^*
6 Set all velocities such that $\mathbf{u}_{k+1}^* \cdot \mathbf{n} < 0$ to zero in the outlet section
7 Correct outlet flow rate
8 Solve Eq. (22) with Eq. (26) and Eq. (31) $\rightarrow \Phi^{n+1}$ in Ω
9 Correct velocities Eq. (23) and pressure Eq. (24) $\rightarrow \mathbf{u}_{k+1}^{n+1}$ and p_{k+1}^{n+1}
 in Ω
10 **end**
Output: $\mathbf{u}^{n+1}, p^{n+1}, \rho^{n+1}$ in Ω and on $\partial\Omega$
Algorithm 1: Algorithm for Neumann and convective OBCs

3.3. Implementation of traction-free and estimated traction OBC

The implementation of traction boundary conditions in pressure projection methods has been the subject of many publications in recent years [35, 14, 19, 36]. See also [37] in the context of vector penalty method and [38] for an extension to curved artificial boundaries. Note furthermore that all algorithms presented herein may be adapted to velocity correction methods starting from the work presented in [39].

The main difficulty is to ensure the validity of the relation,

$$(-p_{k+1}^{n+1}\mathbf{I} + \mu^{n+1}(\nabla\mathbf{u}_{k+1}^{n+1} + \nabla\mathbf{u}_{k+1}^{n+1T})) \cdot \mathbf{n} = \mathbf{t}^{n+1} \quad (32)$$

along with the incompressibility constraint at the end of the correction step. The form of the vector \mathbf{t}^{n+1} will depend on the type of traction boundary condition (TF, ET, or CT, see section 2) and will be explained below. A first strategy consists in simply setting the pressure increment to zero at the outlet [14], but this strategy is known to limit the order of convergence of the overall method [36]. An improvement is found with an update of the outlet pressure through a rotational pressure correction method [17, 18, 19]. It is known with those methods that the use of a rotational pressure correction will significantly improve the convergence order of the overall algorithm. However, in multiphase flows, there is, to our knowledge, only one example of a rotational pressure-correction [20], which involves the resolution of a second linear system due to the absence of an analytical solution for the

347 pressure increment. Thus, we choose to employ the method presented in [35],
 348 extended for multiphase flow and non-zero traction.

349 The method presented in [35] starts by applying the normal, i.e., perpen-
 350 dicular, projection of the traction boundary condition just after the estima-
 351 tion step, Eq. (20), using the available variables, namely p_k^{n+1} and \mathbf{u}_{k+1}^* . To
 352 simplify the understanding of the method, the coordinate system is taken to
 353 be cartesian (x, y, z) with an artificial boundary oriented along x . This first
 354 step is then,

$$-p_k^{n+1} + 2\mu^{n+1} \frac{\partial u_{k+1}^*}{\partial x} = t_x^{n+1}, \quad (33)$$

355 where t_x^{n+1} is assumed to be known. The final step will be the application of
 356 the traction outlet boundary condition on the new variables \mathbf{u}_{k+1}^{n+1} and p_{k+1}^{n+1} ,

$$-p_{k+1}^{n+1} + 2\mu^{n+1} \frac{\partial u_{k+1}^{n+1}}{\partial x} = t_x^{n+1}. \quad (34)$$

357 We are then looking for the pressure increment that will ensure the validity
 358 of Eq. (34) as well as satisfy the incompressibility condition. We first take
 359 the incompressibility condition in the cell just before the boundary,

$$\nabla \cdot \mathbf{u}_{k+1}^{n+1} = \frac{\partial u_{k+1}^{n+1}}{\partial x} + \frac{\partial v_{k+1}^{n+1}}{\partial y} + \frac{\partial w_{k+1}^{n+1}}{\partial z} = 0, \quad (35)$$

360 where we express $\partial u_{k+1}^{n+1}/\partial x$ using Eq. (33) and Eq. (34), and $\partial v_{k+1}^{n+1}/\partial y$ and
 361 $\partial w_{k+1}^{n+1}/\partial z$ using Eq. (23). It leads to

$$\nabla \cdot \mathbf{u}_{k+1}^{n+1} = \frac{p_{k+1}^{n+1} - p_k^{n+1}}{2\mu^{n+1}} + \nabla \cdot \mathbf{u}_{k+1}^* - \frac{\partial}{\partial y} \left(\frac{\Delta t}{\rho_{k+1}^{n+1}} \frac{\partial}{\partial y} \Phi^{n+1} \right) - \frac{\partial}{\partial z} \left(\frac{\Delta t}{\rho_{k+1}^{n+1}} \frac{\partial}{\partial z} \Phi^{n+1} \right). \quad (36)$$

362 Finally, as the flow is incompressible, the pressure boundary condition is

$$\frac{\partial}{\partial y} \left(\frac{1}{\rho_{k+1}^{n+1}} \frac{\partial}{\partial y} \Phi^{n+1} \right) + \frac{\partial}{\partial z} \left(\frac{1}{\rho_{k+1}^{n+1}} \frac{\partial}{\partial z} \Phi^{n+1} \right) - \frac{1}{2\mu^{n+1} \Delta t} \Phi^{n+1} = \frac{\nabla \cdot \mathbf{u}_{k+1}^*}{\Delta t}, \quad (37)$$

363 which is the pressure boundary condition derived in [35] adapted to a variable
 364 density flow. Previous equations are forming the algorithm used to compute
 365 and couple the x -velocity and the pressure at the outflow, and to satisfy
 366 exactly the relation Eq. (34) along with the incompressibility constraint.
 367 Concerning the tangential components of the velocity, the outflow condition
 368 is simply a Neumann condition,

$$\frac{\partial v_{k+1}^{*,n+1}}{\partial x} = \frac{\partial w_{k+1}^{*,n+1}}{\partial x} = 0. \quad (38)$$

369 This choice, rather than the use of a constraint on the tangential traction
 370 value, is motivated by the well-known fact that a tangential traction-free
 371 condition is not compatible with a parallel flow [40] and by the fact that
 372 several results are reported as better with a Neumann condition on tangential
 373 velocities rather than a tangential traction condition, even with non-zero
 374 traction [34].

375 It should be noted that the pressure boundary condition, Eq. (37), is only
 376 valid if t_x^{n+1} does not change between the estimation and correction steps.
 377 Otherwise, any change will have to be taken into account into the pressure
 378 OBC, Eq. (37). Thus, the traction t_x^{n+1} can be given depending on the type
 379 of open boundary condition. For TF, it is

$$t_x^{n+1} = \frac{\rho^n}{2} f(\mathbf{u}^n), \quad (39)$$

380 and for non-zero traction conditions (ET and CT),

$$t_x^{n+1} = \frac{\rho^n}{2} f(\mathbf{u}^n) + t_x^{est,n+1}. \quad (40)$$

381 The density is taken at the previous time step to be coherent with the
 382 choice of the velocity. The backflow stabilization is thus not instantaneous
 383 but delayed by one time step. As stated previously, the estimated normal
 384 traction is computed using interior values and at the previous iteration to
 385 ensure the validity of the pressure boundary condition. For ET,

$$t_x^{est,n+1} = \left(-p + 2\mu \frac{\partial u}{\partial x} \right)_{BC-1}^n, \quad (41)$$

386 and for CT,

$$t_x^{est,n+1} = \phi \left(-p + 2\mu \frac{\partial u}{\partial x} \right)_{BC-1}^n + (1 - \phi) \left(-p + 2\mu \frac{\partial u}{\partial x} \right)_{BC}^n, \quad (42)$$

387 with ϕ to be prescribed later. The overall algorithm is presented in algorithm
 388 2.

Input: $\mathbf{u}^n, p^n, \rho^n$ in Ω and on $\partial\Omega$
1 Solve Eq. (17) using VOF advection $\rightarrow \kappa^{n+1}, \mu^{n+1}$ in Ω
2 **for** $k = 0$ **to** $k_{max} - 1$ **do**
3 Compute ρ_{k+1}^{n+1}
4 Solve Eq. (20) $\rightarrow \mathbf{u}_{k+1}^*$ in Ω
5 Apply Eqs. (25)-(33) and (38) on \mathbf{u}_{k+1}^*
6 Solve Eq. (22) with Eq. (26) and Eq. (37) $\rightarrow \Phi^{n+1}$ in Ω
7 Correct velocities Eq. (23) and pressure Eq. (24) $\rightarrow \mathbf{u}_{k+1}^{n+1}$ and p_{k+1}^{n+1}
 in Ω
8 Apply Eqs. (34) and (38) on \mathbf{u}_{k+1}^{n+1}
9 **end**
Output: $\mathbf{u}^{n+1}, p^{n+1}, \rho^{n+1}$ in Ω and on $\partial\Omega$
Algorithm 2: Algorithm for traction OBCs

389 4. Single phase test cases

390 The improvements obtained using our novel outlet treatment are first
391 illustrated on single phase test cases. The first test case, the Kovaszny flow,
392 allows to see the spatial order of convergence of the overall method, while
393 the second test case, a time-dependent manufactured solution test, allows to
394 study the temporal order of convergence of the present algorithm. The third
395 test case, the flow around a square, shows both qualitative and quantitative
396 improvements thanks to ET. The last case, a turbulent plane jet, shows the
397 stability and accuracy of ET in the presence of a fully turbulent flow.

398 4.1. Kovaszny flow

399 The Kovaszny flow is a steady state flow used to mimic the flow behind a
400 cylinder [41]. This configuration is a 2D domain, periodic along the vertical
401 axis, with an inflow on its left boundary and an OBC on its right. The
402 analytical solution of the Kovaszny flow is given by

$$u = 1 - e^{\lambda x} \cos(2\pi y), \quad (43)$$

$$v = \frac{\lambda}{2\pi} e^{\lambda x} \sin(2\pi y), \quad (44)$$

$$p = \frac{1}{2} (1 - e^{2\lambda x}), \quad (45)$$

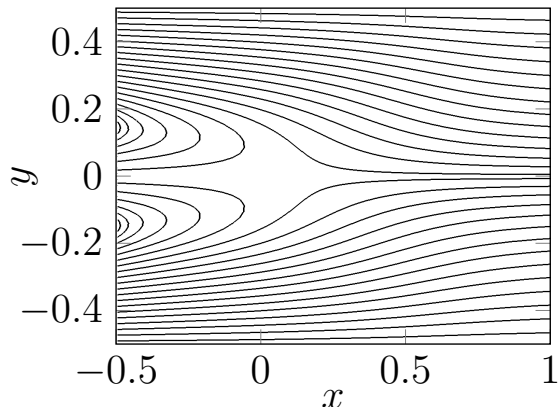


Figure 1: Streamlines of the Kovaszny flow

405 where $\lambda = \frac{Re}{2} - \sqrt{\frac{Re^2}{4} + 4\pi^2}$. We choose here $Re = 1/40$. Thus, this test
 406 case can be used to study the effect of the type of OBC and its position on
 407 the error level compared to the analytical solution [17]. The domain is a two-
 408 dimensional domain of size $-0.5 \leq x \leq L_x$ and $-0.5 \leq y \leq 0.5$, with L_x the
 409 position of the OBC. The mesh is uniform and Cartesian with a cell size Δ ,
 410 with Δ to be specified later. In all cases presented below, $\Delta t = 0.001$. The
 411 inflow is defined using the analytical solution in $x = -0.5$. The streamlines
 412 of this flow are shown in figure 1.

413 Hereafter we study the effect of the OBC choice on the error compared
 414 to the theoretical solution. Considered OBCs are NM, TF and ET. CV
 415 is intentionally excluded from this test case to avoid any discussion on the
 416 choice of the convective velocity at this point.

417 In a first comparative test, the domain length is kept constant with $L_x =$
 418 4.5 and the mesh is progressively refined in order to check the convergence of
 419 the error depending on the type of OBC. In figure 2a) we show the evolution of
 420 the L_2 error norm of the x -velocity and the pressure, for differents OBCs and
 421 depending on mesh resolution. One can first observe two differents behaviors:
 422 for coarser meshes, the same level of error is obtained for all three OBCs,
 423 which decreases with mesh resolution (with order 2, i.e., the order of used
 424 numerical methods). For finer meshes, and for NM and TF OBCs, the error
 425 progressively saturates at a constant value, indicating that outflow error is
 426 dominating. Note that this deviation occurs later for TF than for NM and
 427 stabilizes also at a lower value, meaning that TF gives a lower error than

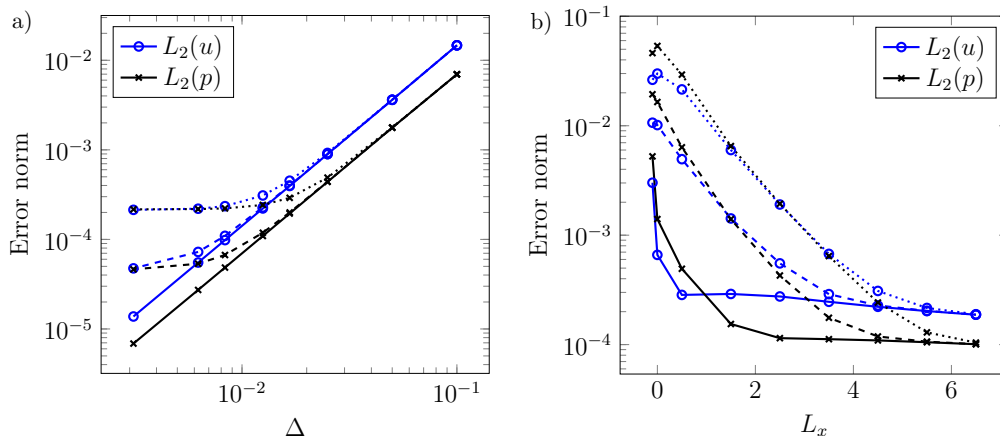


Figure 2: Error levels for different OBCs: a) Mesh convergence, b) Effect of domain truncation. Continuous line: ET - Dashed line: TF - Dotted line: NM

428 NM on that test case. On the other hand, with ET, no deviation is observed
 429 from the second order slope, meaning that in that range of mesh resolutions,
 430 the error due to the outflow is never dominating. With finer meshes and
 431 ET, one will necessarily observe a saturation of the error as the choice of
 432 the estimated traction is not perfect. Note that one can also compute the
 433 estimated traction using the analytical solution [17], which is not possible in
 434 real flow simulations. Note that second order convergence is also obtained in
 435 L_{inf} error norm.

436 In a second comparative test, the mesh is kept constant ($\Delta = 1/80$)
 437 and the domain is progressively truncated. Similarly to the previous test,
 438 we show on figure 2b) the evolution of the L_2 error norm of the x -velocity
 439 and the pressure, for different OBCs and depending on the position of the
 440 artificial boundary. It is seen in figure 2b) that on a sufficiently long domain
 441 all OBCs produce the same level of error. It is also seen that with NM the
 442 truncation of the domain has a much stronger effect than with other OBCs.
 443 The result is, for the range of L_x considered here and using NM, barely
 444 independent of the artificial boundary position. This point is improved with
 445 TF, which provides a better independence of the result with the position of
 446 the outlet. With ET the result is independent of L_x for a large range of
 447 domain size, even though a small increase of $L_2(u)$ is noticeable. Note that
 448 all OBCs are stable for the smallest domain ($L_x = -0.1$), where the outflow
 449 boundary is located in a recirculation zone, which is not possible without

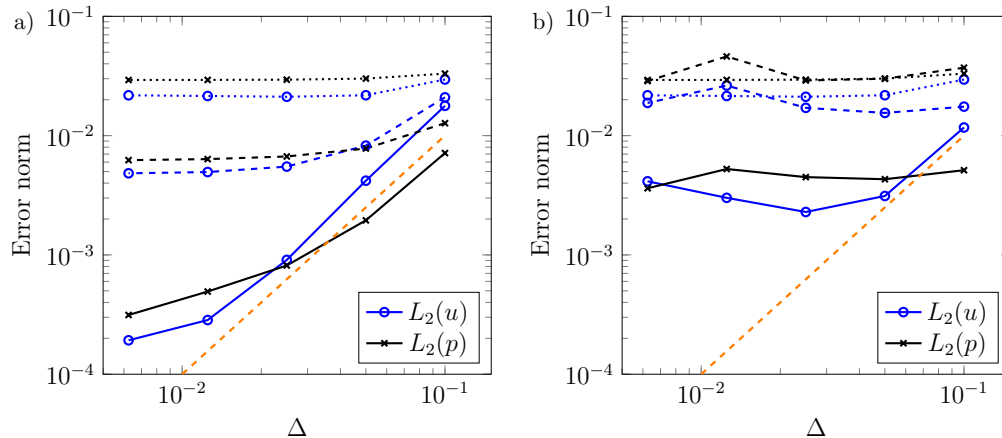


Figure 3: Error levels for different OBCs and two domain lengths: a) $L_x = 0.5$, b) $L_x = -0.1$. Continuous line: ET - Dashed line: TF - Dotted line: NM. The orange dashed line in both plots shows second order spatial convergence.

450 backflow treatment such as clipping or stabilization. But, in case of the
 451 durable presence of a backflow, even the traction condition will not provide
 452 a perfectly accurate solution as the stabilization term only makes sense in
 453 terms of kinetic energy conservation. In order to examine how the order
 454 of spatial convergence is deteriorated with domain truncation, we show in
 455 figure 3, two additional convergence tests with domains shorter than the one
 456 used for the test presented in figure 2a). For $L_x = 0.5$, see figure 3a), second
 457 order convergence is only obtained for $L_2(u)$ using ET and for a shorter
 458 range of resolution than previously. For $L_x = -0.1$, see figure 3b), the outlet
 459 boundary is located in the recirculation zone, and no clear convergence of the
 460 error with resolution can be observed, even using ET. For all resolutions and
 461 domain lengths tested, ET has the lowest level of error. The same results are
 462 obtained on L_{inf} error norm.

463 Those tests demonstrate the interest of the non-zero traction OBC on
 464 a steady state problem in terms of error level and independence to outlet
 465 position.

466 4.2. Time-dependent manufactured solution

467 In order to study the temporal order of convergence of the proposed
 468 method, we use the time-dependent manufactured solution of [17],

$$u = 2 \cos(\pi y) \sin(\pi x) \sin(t), \quad (46)$$

469

$$v = -2 \cos(\pi x) \sin(\pi y) \sin(t), \quad (47)$$

470

$$p = 2 \sin(\pi x) \sin(\pi y) \cos(t), \quad (48)$$

471 which satisfies the incompressibility condition ($\nabla \cdot \mathbf{u} = 0$). In order to sat-
 472 isfy Eq. (18), unsteady body forces have to be added to the Navier-Stokes
 473 equations.

474 The computational domain is two-dimensional, of size $0 \leq x \leq 2$ and
 475 $-1 \leq y \leq 1$, with 256 uniform cells in both directions. Eqs. (46) and (47)
 476 are enforced as Dirichlet boundary conditions on three boundaries of the
 477 computational domain, whereas the traction condition Eq. (32) is used on the
 478 last one. Similarly to [17, 20, 35], the right hand side of Eq. (32) is computed
 479 using the manufactured solution. Imposing the analytical traction value at
 480 the open boundary is needed to avoid the domination of spatial error over
 481 temporal error. No stabilization term is included as it becomes meaningless
 482 when one imposes the exact traction at the open boundary, i.e., when the
 483 open boundary is transformed into a Dirichlet boundary. The initial velocity
 484 field is set to zero, in agreement with the manufactured solution. For this
 485 test case we use $\rho = 1$ and $\mu = 0.01$.

486 The simulation is advanced in time with a fixed time step, Δt , to be
 487 specified, until a fixed final time $t_f = 0.5$. The L_2 error norm on different
 488 flow variables at this final time is computed with respect to the manufactured
 489 solution. The test is then repeated with various time steps.

490 The results are shown on figure 4. One can see that the error norm
 491 convergence for all flow variables is approximately of second order until a
 492 progressive saturation of the temporal error by the spatial error. Note that
 493 the convergence of the error seems to be faster for the velocities than for
 494 the pressure, which may be due to the presence of splitting errors [35]. A
 495 rotational pressure correction would be a solution to resolve this discrepancy
 496 [35, 17], but for the reason cited in section 3.3 we chose not to use this
 497 strategy. Note that the same results are obtained in L_{inf} error norm. In
 498 agreement with [35], these results suggest that the present algorithm for
 499 the implementation of traction conditions does not deteriorate the order of
 500 temporal convergence.

501 The choice of manufactured solution and computational domain we made
 502 involves $\mathbf{u} \cdot \mathbf{n} = 0$ and $p = 0$ at the boundaries (same test case as [17]). In
 503 order to prove that the results are not affected by these choices, we use the
 504 same manufactured solution on a computational domain shifted along x , i.e.,

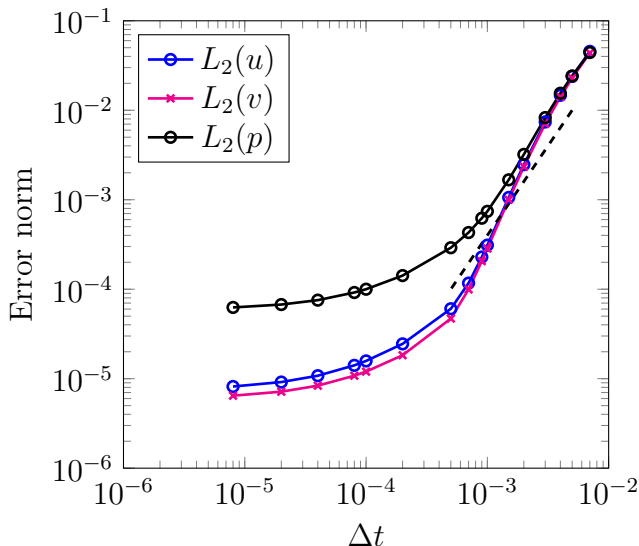


Figure 4: Method of manufactured solution. Convergence of the error level with respect to the time step. The dashed black line shows second order convergence.

505 with $-0.5 \leq x \leq 1.5$ and $-1 \leq y \leq 1$. This way, there is backflow and
 506 non-zero pressure at the open boundary at the final time ($t_f = 0.5$). The
 507 resolution is the same as previously.

508 The results are shown in figure 5a). Similarly to the previous results,
 509 second order temporal convergence is obtained, though with an error slightly
 510 higher than for the previous computational domain. This demonstrates once
 511 again that the present algorithm for traction condition does not deteriorate
 512 the order of temporal convergence. When we add the stabilization term to
 513 the analytical traction value, as done for the results presented in figure 5b),
 514 we observe degraded temporal convergence leading to an error plateau. We
 515 emphasize that this plateau is fully expected, as the stabilization term is
 516 purely ad-hoc and represents a numerical error when added to the analytical
 517 traction at the open boundary.

518 4.3. Flow around a square

519 We now compare the different OBCs on an unsteady case: the flow over
 520 a two-dimensional square. This test case presents two main interests from
 521 the point of view of OBC performance. Firstly, we study their ability to
 522 convect the vortices generated by the von Kármán instability through the

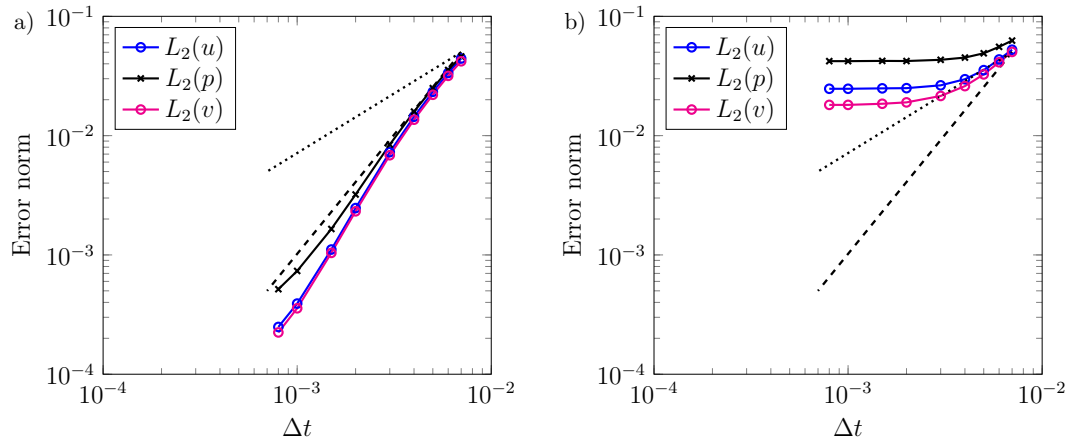


Figure 5: Method of manufactured solution for the shifted domain. Convergence of the error at the final time with respect to the time step, a) imposing the analytical traction at the open boundary, and b) imposing the analytical traction and the stabilization term at the open boundary. The dotted and dashed black lines show first and second order convergence, respectively.

523 artificial boundary. Secondly, we investigate the impact of the OBC position
 524 and type on aerodynamic quantities such as drag and lift coefficients and
 525 vortex shedding frequency

526 In a first test, we use the square as a vortex generator and we compare
 527 qualitatively TF and ET on their ability to properly convect vortices through
 528 the artificial boundary. The test case is a two dimensional domain of size
 529 $-5H \leq x \leq 5H$ and $-5H \leq y \leq 5H$ where H is the size of the square
 530 located in the middle of the domain. The Reynolds number $Re = \rho U H / \mu$
 531 is equal to 1000. U is the velocity uniformly imposed at the inflow ($x = -5H$)
 532 and the outflow is located at $x = 5H$. Symmetry boundary conditions are
 533 used at $y = \pm 5H$ and the domain is uniformly discretized with a cell size
 534 $\Delta = H/40$. The time step is chosen such that the CFL number stays equal to
 535 1. Under those conditions a strongly unsteady flow is generated downstream
 536 of the obstacle. It should be noted that this flow is unphysical given the
 537 three-dimensionality of a real flow at that Reynolds number, but this test
 538 case allows to assess the accuracy of outlet boundary conditions [17].

539 On figure 6 we show, through isocontours of z vorticity, the exit of several
 540 vortices through the outlet boundary. The top row of figures presents the
 541 result with TF, whereas the bottom row of figures presents the result using
 542 ET. On the top images, one can observe that the use of TF tends to flatten

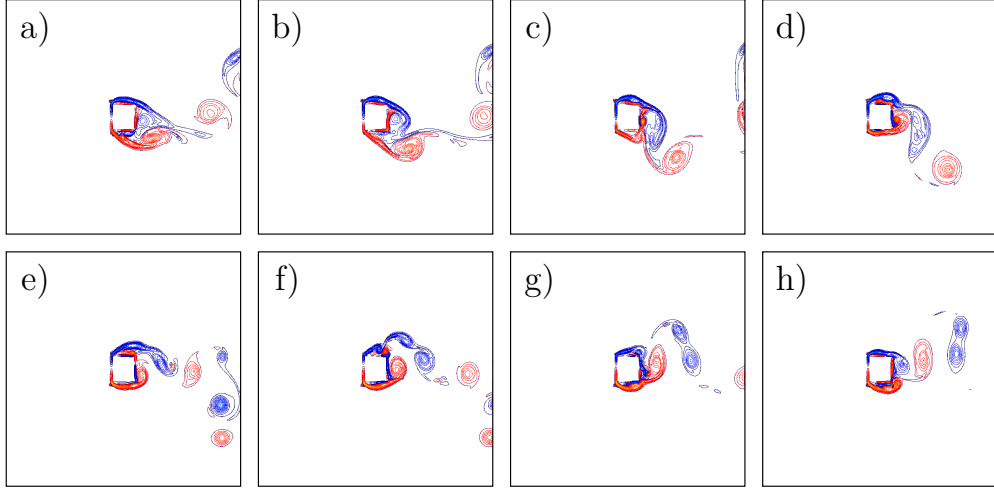


Figure 6: Isocontours of z vorticity. Top figures: TF; bottom figures: ET. From left to right, all figures are separated by a time interval of $0.5H/U$.

543 the vortices on the outlet and to delay their complete exit through the open
 544 boundary. This can simply be explained by a balance of pressure: the pres-
 545 sure at the vortex center is balanced by the imposed outlet pressure through
 546 imposed traction and by inertial effects. As inertial effects are not strong
 547 enough to push out the vortex, it sticks to the boundary and is only slighty
 548 – and slowly – pulled out of the domain by the backflow stabilization term.
 549 We observed that if no backflow stabilization is taken into account, vortices
 550 were gathering on the artificial boundary, finally leading to the blow-up of
 551 the simulation due to the backflow instability. Note that, although the vor-
 552 tices exit seems unnatural, once the stabilization term is included the code
 553 remains perfectly stable to backflow at the outlet boundary. On the other
 554 hand, with ET, no vortex sticking is observed and vortices simply cross the
 555 boundary with barely any deformation.

556 We now propose a more quantitative comparison between different OBCs
 557 through the study of the aerodynamic quantities. To avoid any confinement
 558 effect and any impact of the inflow position, the domain is this time of size
 559 $-10H \leq x \leq L$ and $-10H \leq y \leq 10H$, with L the position of the outlet
 560 boundary and H the size of the square located at $(0,0)$. The Reynolds
 561 number $Re = \rho UH/\mu$ is now equal to 100. The domain is discretized with
 562 a uniform cell size $\Delta = H/40$ in the sub-domain $-10H \leq x \leq L$ and

563 $-4H \leq y \leq 4H$, to avoid any loss of resolution of the vortices in the wake of
 564 the obstacle, and is then progressively stretched up to the top and bottom
 565 boundaries with a constant stretching ratio of 1.05. The time step is chosen
 566 such that the CFL number stays equal to 1. The aerodynamic forces are
 567 directly integrated on the surface of the obstacle.

568 Figure 7 presents the evolution of different aerodynamic quantities as a
 569 function of the position and the type of open boundary. We also included the
 570 results of two recent publications using the stabilized traction-free condition
 571 [17] and the traction-free condition [35]. In order to simplify comparison with
 572 other publications, the evolution of the aerodynamic quantities is presented
 573 in terms of error relative to the value obtained on the longest domain. Figure
 574 7a) shows the evolution of the mean drag coefficient, figure 7b) shows the
 575 evolution of the r.m.s lift coefficient and figure 7c) shows the evolution of the
 576 Strouhal number associated with the vortex shedding frequency. The results
 577 obtained with ET keep a correct behavior even on the smaller domains by
 578 exhibiting the lowest variation of aerodynamic quantities as a function of the
 579 outflow position. This improvement is largely explained by the fact that the
 580 underlying assumption of well-developed flow associated with the traction-
 581 free condition, stabilized or not, is no longer required with ET.

582 4.4. *Turbulent plane jet*

583 To finally assess the stability and the accuracy of the proposed boundary
 584 condition we study the spatial evolution of a turbulent plane jet. The config-
 585 uration, the expression of the analytical inlet velocity profile and the choice
 586 of parameters are the same as in Da Silva & Metais [42] (case referred to as
 587 “DNS2” in their original paper). The numerical domain is a 3D domain of
 588 size $0 \leq x \leq 12.4h$, $-6h \leq y \leq 6h$ and $-1.6h \leq z \leq 1.6h$, where h is the jet
 589 width. The inlet boundary is located at $x = 0$ and the outflow at $x = 12.4h$.
 590 The other boundaries are periodic. The domain is discretized with a uniform
 591 cell size $\Delta x = \Delta y = \Delta z = 0.04h$. The constant time step is $\Delta t = 0.02$.

592 In a first study the Reynolds number based on the jet width, $Re = (U_i -$
 593 $U_{ff})h/\nu$, is taken equal to 3000, with U_i the jet centerline inlet velocity and
 594 U_{ff} the inlet far-field velocity. The isocontours of positive Q-criterion [43]
 595 are shown on figure 8, using TF (a) and ET (b). On both figures one can see
 596 the spatial development of the jet, initiated by the apparition of successive
 597 Kelvin-Helmholtz rolls that are then connected by the apparition of vortices
 598 in the streamwise direction. When reaching the outlet boundary the flow
 599 is fully tridimensional. On figure 8a) one can see the dramatic effect of TF

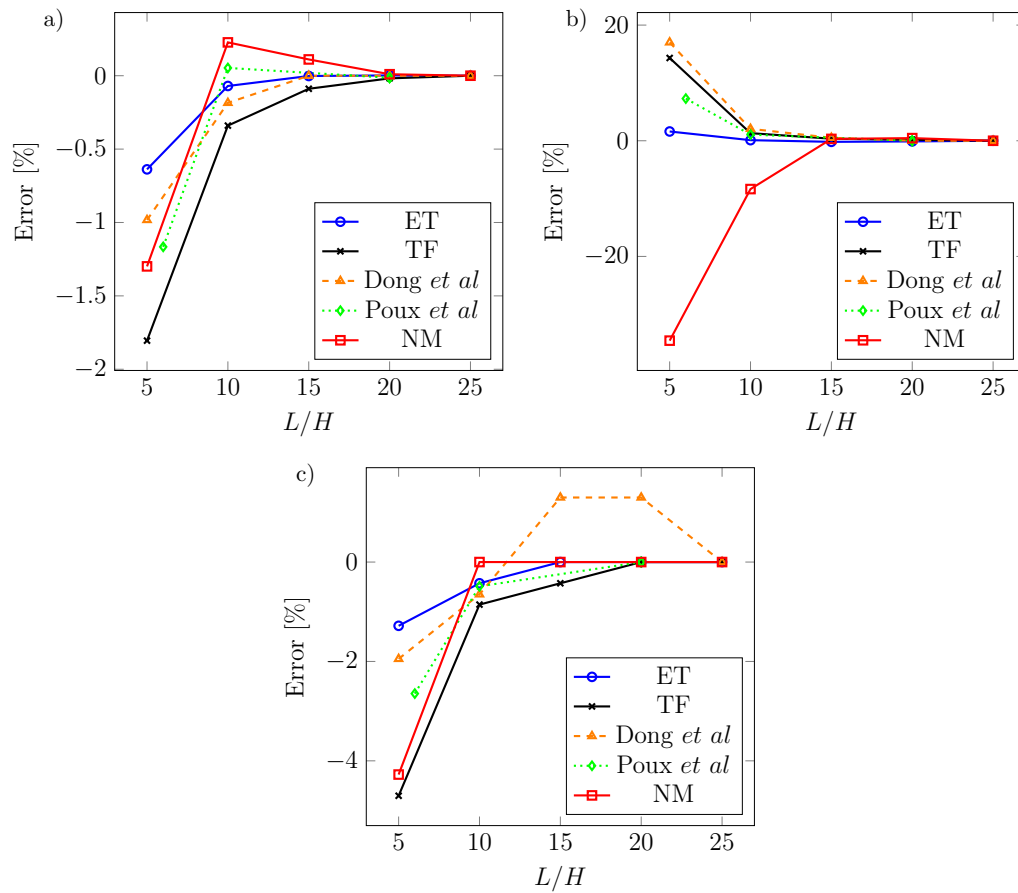


Figure 7: Impact of the outflow position and type on the aerodynamic quantities: a) mean drag coefficient, b) r.m.s lift coefficient, c) Strouhal number. On all plots, the vertical axis is the error compared to the value obtained on the longest domain, whereas the horizontal axis is the distance between the square and the outflow position L normalized by the size of the square H . The reference results included are the results from Dong *et al* [17] and Poux *et al* [35].

600 on the exit of the vortices. A part of them sticks to the boundary and is
601 prevented to leave the domain. On the other hand, using ET, no vortex
602 sticking is observed and the vortices are crossing the boundary with barely
603 any deformations, see figure 8b). With CV, the vortices exit looks very
604 similar to the one seen using ET (results not shown). Note that using TF
605 we had to reduce the time step size in order to obtain a stable simulation.
606 This may be due to the vortex sticking phenomena coupled to the delayed
607 backflow correction of one time step. Considering the poor qualitative result
608 seen on figure 8a) and the need to decrease the time step size, we therefore
609 exclude TF from the following analysis.

610 The jet exhibits a self-similar behaviour in its downstream region [42]. In
611 this region, several quantities computed from the time averaged velocity field
612 are evolving linearly with the downstream distance. We choose here to use the
613 centerline velocity, $U_c = \langle u(x, y = 0) \rangle$, and the jet half-width, $\delta_{1/2}$, defined as
614 the y -location where the velocity is equal to half of the centerline velocity,
615 i.e., $\langle u(x, y = \delta_{1/2}) \rangle - U_{x,\infty} = 0.5 (U_c - U_{x,\infty})$, with $U_{x,\infty} = \langle u(x, y = \infty) \rangle$,
616 the far-field velocity. Those quantities follow the following relationships [44]:

$$\frac{\delta_{1/2}}{h} = K_{u1} \left[\frac{x}{h} + K_{u2} \right], \quad (49)$$

617 and

$$\left[\frac{U_i - U_{ff}}{U_c - U_{x,\infty}} \right]^2 = C_{u1} \left[\frac{x}{h} + C_{u2} \right]. \quad (50)$$

618

619 We plot those quantities, along with their linear relations, on figure 8c)
620 and 8d) using ET and CV. Using ET, in addition to provide a natural exit of
621 the vortices as well as the stability of the simulation, the self-similar region
622 is barely disturbed by the presence of the open boundary. With CV both of
623 the self-similar quantities are strongly affected by the presence of the outflow.
624 Note that the slopes of the linear relations are the same as in Da Silva &
625 Metais [42].

626 To demonstrate that the proposed boundary treatment is stable for highly
627 turbulent flows, we study the large eddy simulation of the turbulent plane
628 jet at $Re = 30000$. The sub-grid stresses are estimated with a dynamic
629 Smagorinsky eddy viscosity model using Lagrangian averaging to compute
630 the dynamic coefficient [45]. The computational domain is now larger in
631 the vertical direction to account for the entrainment induced by the jet,
632 i.e., $-8h \leq y \leq 8h$. The isocontours of positive Q-criterion are shown on

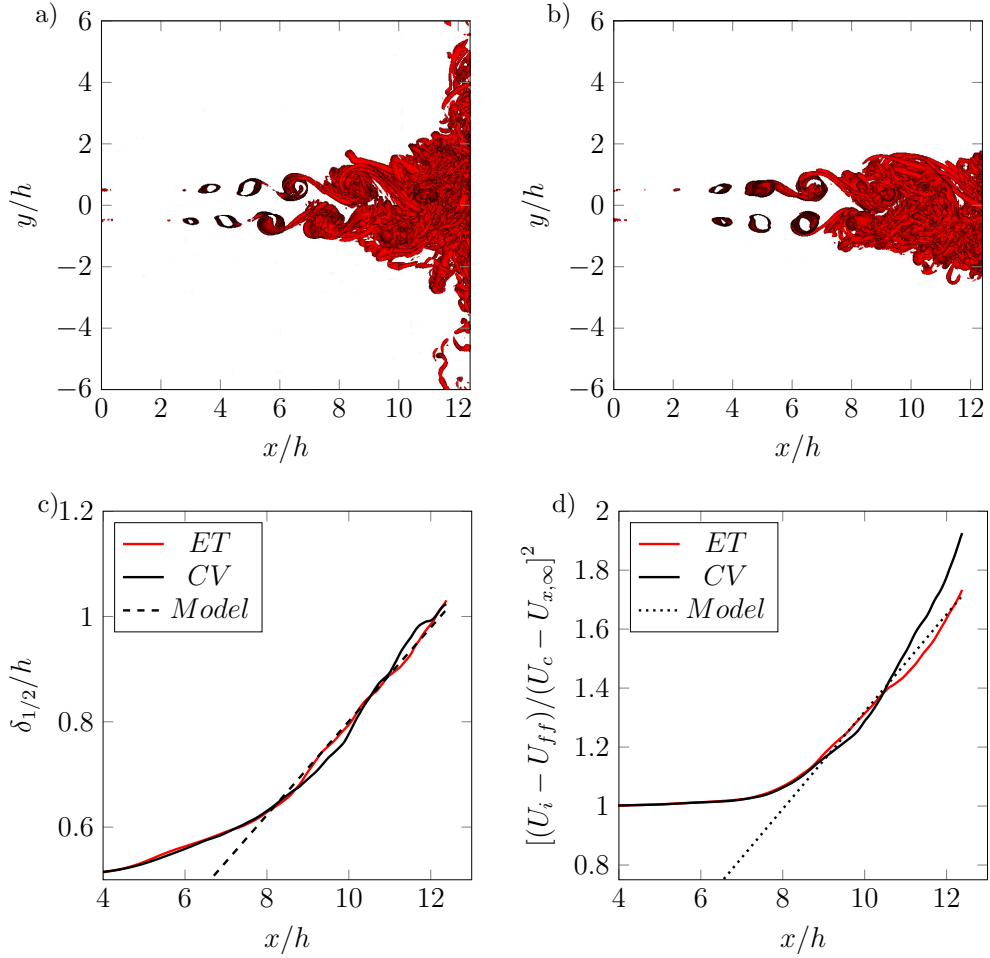


Figure 8: (Color online) Turbulent plane jet at $Re = 3000$. Positive Q-criterion isocontours (20 isocontours from $Q = 0.25$ to $Q = 100$) at $t(U_i - U_{ff})/h = 166$, using TF (a) and ET (b). c) Evolution of the jet half-width with downstream distance using ET and CV. Model computed using Eq. (49) with $K_{u1} = 0.089$ and $K_{u2} = -1$. d) Evolution of the centerline jet velocity with downstream distance using ET and CV. Model computed using Eq. (50) with $C_{u1} = 0.165$ and $C_{u2} = -2$.

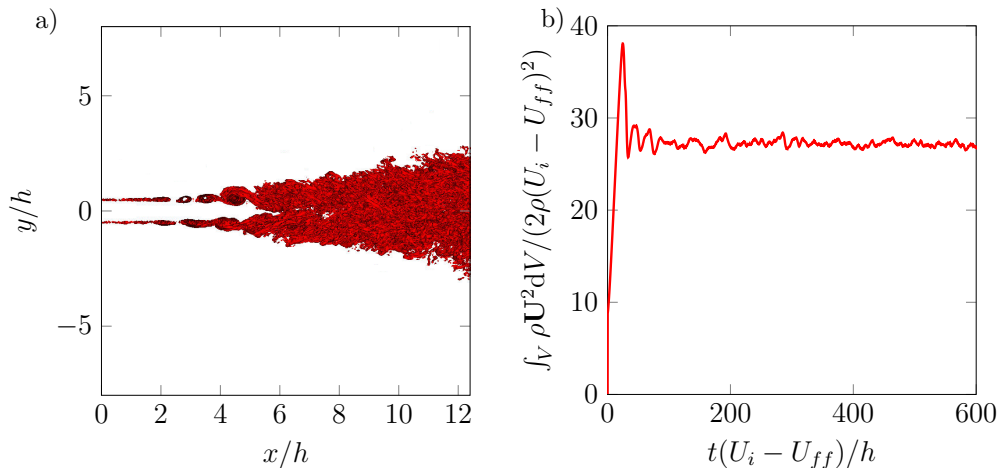


Figure 9: Large eddy simulation of a turbulent plane jet at $Re = 30000$. a) Positive Q-criterion isocontours (10 isocontours from $Q = 0.25$ to $Q = 100$) at $t(U_i - U_{ff})/h = 400$ using ET. b) Temporal evolution of the normalized kinetic energy integrated over the domain using ET.

633 figure 9a). One can see that there is no accumulation of vortices on the open
 634 boundary although the turbulence is fully developed when reaching the open
 635 boundary. To show the long-term stability of the proposed method even in
 636 the presence of a strong turbulent flow, we show the temporal evolution of
 637 the kinetic energy integrated over the computational domain on figure 9b).
 638 After an initial transient, the flow reaches a statistically stationary state
 639 that is not perturbed by the presence of backflow at the open boundary. As
 640 stated before, this result strongly suggests that a zero energy flux at the
 641 open boundary is not needed to ensure the stability of the simulation. The
 642 accuracy of the proposed boundary treatment could even be improved using
 643 a better estimation of the traction at the open boundary, for example with
 644 CT.

645 5. Multiphase test cases

646 We now turn our attention to multiphase flows. In this section, the
 647 importance of backflow stabilization is demonstrated using first a single drop
 648 advection test case, then a turbulent swirling jet flow simulation. Finally, we
 649 demonstrate the improvements obtained using CT on a problem of surface
 650 waves reflection.

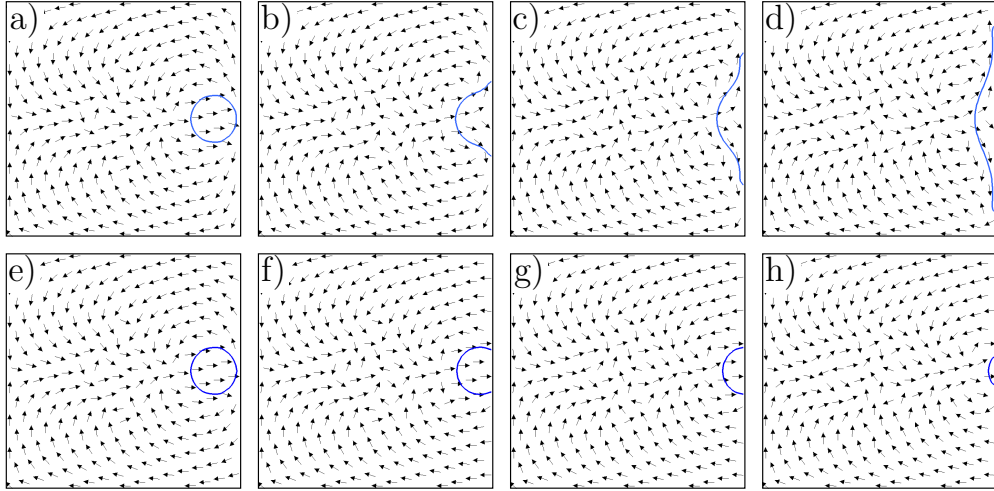


Figure 10: Water drop advection in a domain without inlet. a)-d) : CV ; e)-h) : ET. From left to right, all figures are separated by a time interval of $0.6D/U_l$.

651 *5.1. Drop convection*

652 A water droplet of size $D = 0.1$ with initial velocity $U_l = 3$ is placed
 653 at the center a domain of size $-10D \leq x \leq 10D$ and $-10D \leq y \leq 10D$
 654 and surrounded by quiescent air. The outflow is located at $x = 10D$, with
 655 periodic boundary conditions at $y = \pm 10D$. At $x = -10D$, a slip wall
 656 condition is used. The simulation is run on a 64×64 mesh with a timestep
 657 $\Delta t = 0.001$.

658 Figure 10 shows velocity vectors along with the liquid-gas interface dur-
 659 ing the advection of the drop towards the outlet for two types of boundary
 660 conditions. On the top row of images the result are obtain with the CV, and
 661 on the bottom row of images the result are obtained with ET. Note that,
 662 on this test case, one can replace CV by NM and ET by TF, for the same
 663 qualitative result.

664 On the top pictures of figure 10, one can observe that with CV OBC the
 665 drop is flattening on the boundary and no liquid is exiting the domain. On
 666 the other hand, using ET, the drop is completely going out with minimal
 667 deformation. The reason for these completely different behaviors lies in the
 668 fact that the incompressibility condition requires the outlet flow rate to be
 669 equal to the inlet flow rate, in this case zero. Thus, the only way for the drop
 670 to exit is to allow backflow. We see here one strong limitation of the clipping

671 strategy, which severely affects the flow by preventing the drop from going
672 out, though it provides unconditional stability. On the other hand, once the
673 stabilization term is included, ET and TF are perfectly stable to backflow as
674 can be seen in figures 10f-g-h).

675 5.2. Turbulent swirling jet

676 To show the importance of backflow stabilization in a more realistic case,
677 we present a simulation of turbulent swirling jet. As shown in figure 11, a
678 turbulent liquid jet exits from a nozzle located on the left of the domain.
679 The jet then develops into a conical shape and becomes subject to different
680 interfacial instabilities leading to its atomization. The outflow is located
681 on the right of the domain (colored in pink), whereas all lateral boundary
682 conditions are periodic. All physical properties, injection parameters and
683 geometric characteristics are the same as in [46]. The domain is discretized
684 with a $200 \times 400 \times 400$ cartesian grid and the simulation is advanced with a
685 CFL number of 0.8.

686 On figures 11a) and 11b), the liquid-gas interface colored by the axial
687 velocity is shown after a simulation time $tU/D = 11$, where U is the bulk
688 injection velocity, and D the external diameter of the injector. On figure
689 11a), the result with CV is shown, with the phase velocity computed using
690 Eq. (27). One can see that since this outflow treatment does not allow
691 backflow, some of the liquid is prevented from going out and “splashes” on
692 the exit plane. Figure 11b) shows the result using the ET OBC, and in this
693 case the liquid is not blocked on the exit plane. This obviously has a large
694 impact on the capability to reach long term simulations of such atomizing
695 liquid jets. With a boundary condition that does not allow backflow, the
696 simulation time is obviously limited by the length of the domain, which is
697 not the case with a stabilized traction boundary condition. It should be
698 noted here that CV may be replaced by NM and ET by TF for the same
699 results on the liquid exit. The difference between TF and ET will lie in the
700 speed of the droplets in the vicinity of the outlet and in the behavior of the
701 vortices exiting the domain, as already discussed using the test case of the
702 flow around a square.

703 Although here traction conditions are used only as exit conditions, it
704 should be noted that they may also be used as lateral boundary condition [21,
705 47]. One can also imagine replacing the wall used around the liquid injector
706 by an open traction boundary condition in order to get a more realistic

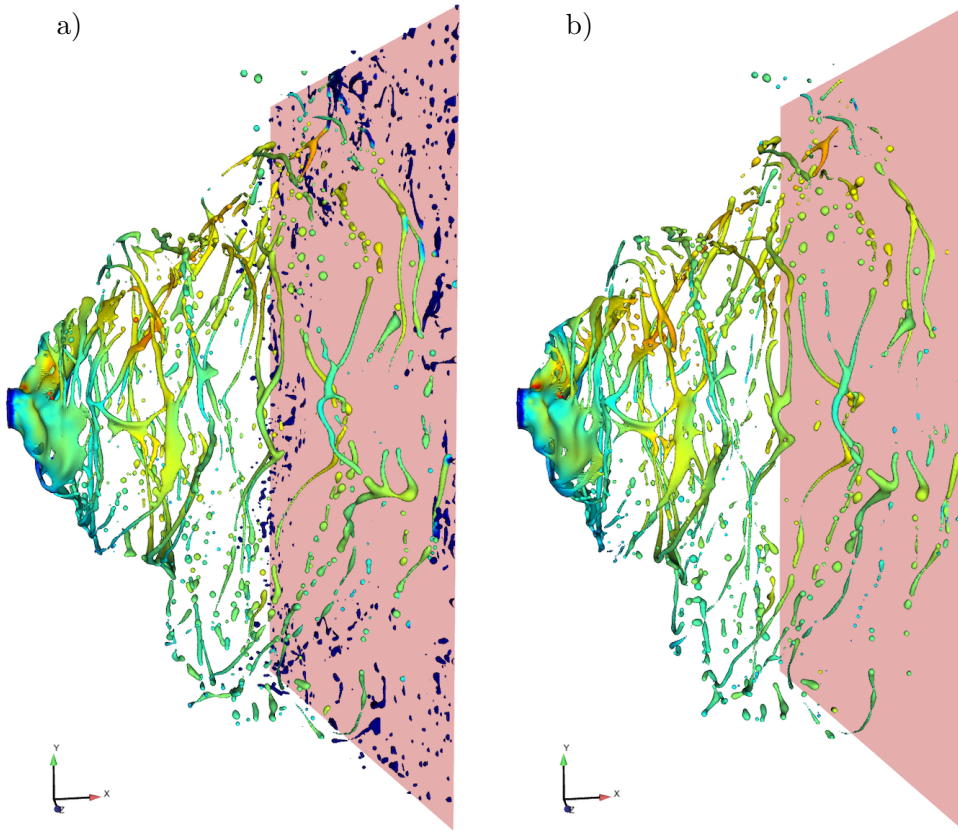


Figure 11: (Color online) Turbulent swirling jet test case. Liquid-gas interface colored by axial velocity shown at a time $tU/D = 11$ (dark blue: $u = 0$, dark red: $u = 3U$, with U the bulk injection velocity). a) result using CV, b) result using ET.

707 representation of such jets by allowing the development of a “natural” gas
 708 co-flow. We will investigate that point in future works.

709 5.3. Surface gravity waves

710 We finally evaluate the ability of the different OBCs to evacuate a surface
 711 wave without reflection. As said in the introduction, wave reflection is a prob-
 712 lem of critical importance in ocean modeling as it prevents the convergence
 713 of flow statistics and may create unrealistic flows [4].

714 The test case is set up using solitary wave theory [48]. The interface

715 height is defined as

$$\eta(x) = A_0 \operatorname{sech}^2 \left(\sqrt{\frac{3A_0}{4h_0^3}} x \right), \quad (51)$$

716 with A_0 the initial height of the wave and h_0 the water depth. The initial
717 velocity is defined as $\mathbf{u} = (u(x), 0, 0)$ where

$$u(x) = \eta(x) \frac{\sqrt{|g|(h_0 + A_0)}}{h_0 + \eta(x)} + U_{in}, \quad (52)$$

718 and U_{in} is the inflow velocity. The computational domain is two-dimensional,
719 of size $-60h_0 \leq x \leq 20h_0$ and $-h_0 \leq y \leq 4h_0$ with symmetry boundary
720 conditions along y , a constant velocity inflow $u = U_{in}$ at $x = -60h_0$ and the
721 OBC at $x = 20h_0$. Air/water conditions are used for the choice of physical
722 properties. This setup results in the transport of a soliton from the position
723 $x = 0$ to the OBC at a constant phase velocity $c_{th} = \sqrt{|g|(h_0 + A_0)} + U_{in}$.
724 For all cases presented below parameters are chosen as $A_0 = 0.005$, $h_0 = 0.01$,
725 $U_{in} = 0.07$. The domain is discretized using a uniform Cartesian mesh with
726 $\Delta x = \Delta y = 5 \times 10^{-4}$. The solution is advanced using a time step size
727 $\Delta t = 1 \times 10^{-3}$.

728 On figure 12 are presented the space-time plots of the interface height
729 for 4 different OBCs along with, on figure 13, the interface height signals
730 at a position $x = 10h_0$. On figure 12a), the result with CV is shown. As
731 in previous tests, the wave speed is taken as $c = c_{max}$. One can first see
732 a transient phenomenon at the initialization which causes the emission of
733 perturbations towards the left of the domain and the height of the wave to
734 slightly decrease. Since the inflow is located at $x = -60h_0$, none of the results
735 presented herein are affected by the reflexion of these initial perturbations
736 on the inflow. The reason for these perturbations is an initial adjustment
737 due to the discrete approximations of the continuous solution [4]. Following
738 this initial transient, the soliton travels towards the OBC at a constant speed
739 c_{th} . Once the wave reaches the artificial boundary, it completely crashes on
740 the boundary and a large part is reflected in the domain in a succession of
741 smaller waves, forming a reflection cone. This result is not a surprise given
742 the inappropriate choice of the convective velocity.

743 In figure 12c), we use the theoretical wave speed as the convective velocity
744 in CV. One can see that the reflection is much lower in amplitude but creates

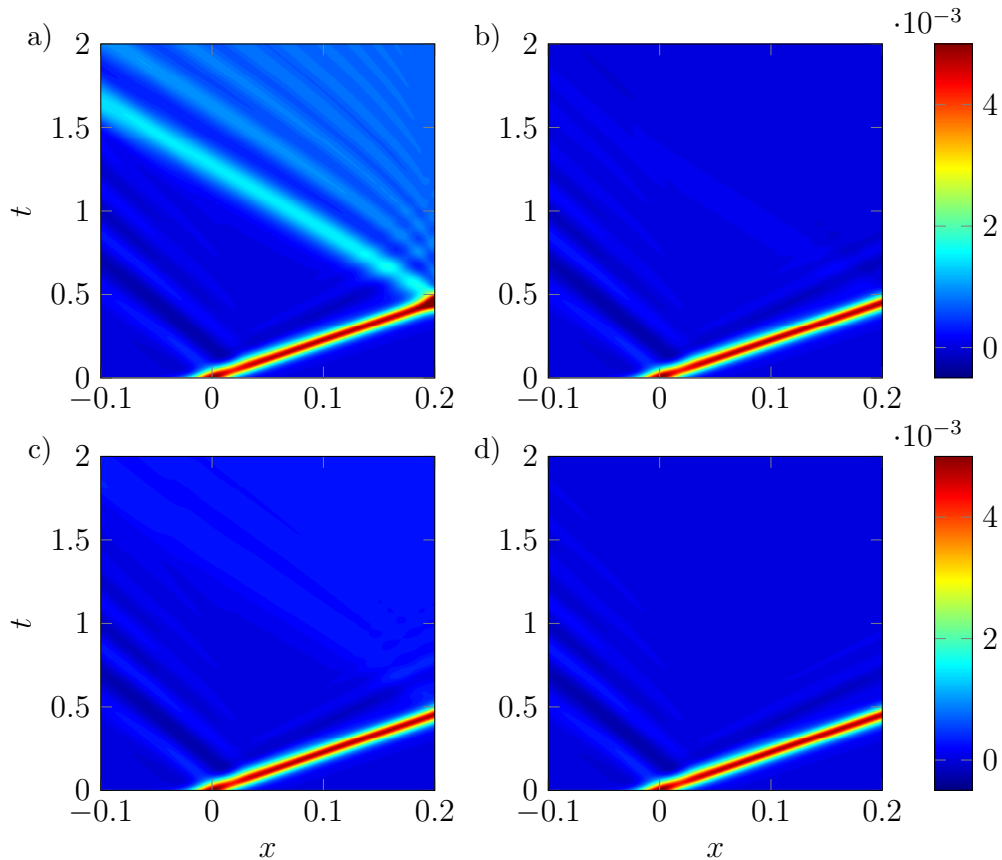


Figure 12: (Color online) Transport of a surface gravity waves through an OBC. a) CV with $c = c_{max}$, b) ET, c) CV with $c = c_{th}$, d) CT with $c = c_{th}$. The color indicates the liquid height.

745 an increase of the mean liquid level, seen also in figure 13. Thus, even with the
 746 best choice of the wave speed, a convective condition is not able to evacuate
 747 a soliton out of the domain without reflection.

748 We now focus our study on the use of a traction condition. First, it should
 749 be noted that the use of TF is impractical for such simulations. The pressure
 750 being hydrostatic in the domain, using a traction-free condition will impose
 751 a pressure close to zero at the outlet (velocity gradients being small far from
 752 the soliton), thus resulting in a strong suction of the flow which rapidly
 753 propagates up to the inlet. On figure 12b), we show the result using the
 754 ET. One can observe that the reflection is almost suppressed but that small

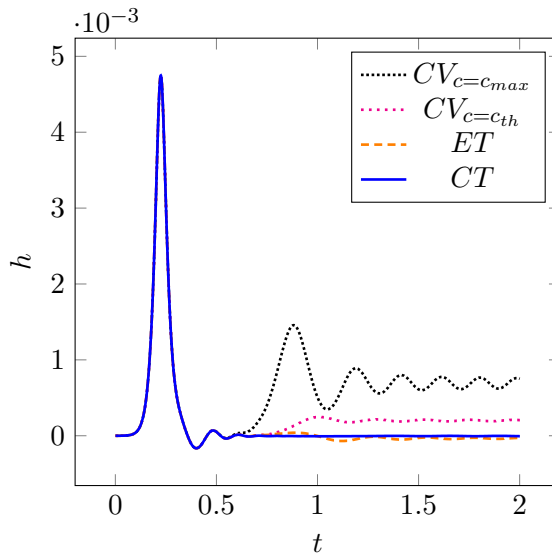


Figure 13: Interface height signals at a fixed position $x = 10h_0$ for 4 different OBCs.

755 waves propagate upstream. Thus, such an arbitrary choice of the estimated
756 traction (computed at the point just before the boundary at the previous
757 time step) is in fact even better than the best choice of a convective OBC.
758 However, two points have to be emphasized. Firstly, ET is not perfectly
759 non-reflective. Secondly, we have observed a dependence of its performance
760 to numerical parameters such as the time step or cell sizes.

761 The reason for the last two points has in fact already been explained in
762 section 2. Considering the estimated traction as a Lagrangian quantity, the
763 present choice is not optimal. Indeed, taking the estimation of the traction
764 at the point before the boundary and at the previous time step is not always
765 a good choice depending on numerical parameters. A more accurate choice
766 can be found considering the convected traction boundary condition (CT).
767 The theoretical wave speed, c_{th} , is taken as the advection velocity. The
768 interpolation coefficient used in Eq. (14) is therefore $\phi = c_{th}\Delta t/\Delta x$. The
769 result using this approach is shown on figures 12d) and 13).

770 One can see that CT, our new OBC, is now perfectly non-reflective. It
771 must be emphasized that this result is now independent of the time step, the
772 mesh size, and is also independent of the OBC position.

773 *5.4. Additional remark*

774 In most of the present paper, we use an estimation of the traction at
775 the point just before the boundary, which is easy to define on a structured
776 mesh. The extension to fully unstructured meshes is possible thanks to
777 the Lagrangian estimation of the traction introduced previously, as done in
778 Eq. (14). On such meshes, one has to define an advection velocity and then
779 perform a semi-Lagrangian interpolation of the traction field at the location
780 of interest to obtain the traction estimate. In case of curved boundaries, one
781 has to use differential geometry to complete the pressure boundary condition,
782 Eq. (37), as done in [38].

783 **6. Conclusion**

784 We have presented a comparison between several outlet boundary treat-
785 ments on single and multiphase test cases along with their numerical imple-
786 mentation in the context of fractional step methods. One major difference
787 between these open boundary conditions lies in the backflow treatment. The
788 implementation of backflow clipping associated with Neumann or convective
789 open boundary conditions, while providing unconditional stability, can have
790 a strong effect in the simulation of multiphase flows. On the other hand, sta-
791 bilized traction conditions are perfectly suited to resolve this issue. The main
792 drawback of the traction-free condition lies in its underlying assumption of
793 well-developed flow that is not suited for severely truncated domains or high
794 Reynolds number flows. To overcome this issue, an open boundary condition
795 combining stabilization to backflow and space and time varying estimated
796 traction is proposed, allowing stable and accurate simulations for turbulent
797 and multiphase flows. This estimated traction is considered as a Lagrangian
798 quantity, which allows to use it as a non-reflective artificial boundary for sur-
799 face waves simulations. This work shows that traction conditions have the
800 potential to resolve most of issues related to outflow treatment. They might
801 also be used as lateral or inlet boundary conditions and allow a consider-
802 able reduction in the cost of numerical simulations, as we will explore in
803 future work. The very general form under which the estimated traction is
804 introduced also opens the way to a study of the effect of different advection
805 methods on the accuracy of traction boundary conditions.

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