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1	Performance study of two serial
2	interconnected chemostats with mortality
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Abstract

12

The present work considers the model of two chemostats in series when a 13 biomass mortality is considered in each vessel. We study the performance 14 of the serial configuration for two different criteria which are the output 15 substrate concentration and the biogas flow rate production, at steady 16 state. A comparison is made with a single chemostat with the same total 17 volume. Our techniques apply for a large class of growth functions and 18 allow us to retrieve known results obtained when the mortality is not 19 included in the model and the results obtained for specific growth func-20 tions in both the mathematical literature and the biological literature. 21 In particular, we provide a complete characterization of operating condi-22 tions under which the serial configuration is more efficient than the single 23 chemostat, i.e. the output substrate concentration of the serial configu-24 ration is smaller than that of the single chemostat or, equivalently, the 25 biogas flow rate of the serial configuration is larger than that of the single 26 chemostat. The study shows that the maximum biogas flow rate, relative 27 to the dilution rate, of the series device is higher than that of the single 28 chemostat provided that the volume of the first tank is large enough. This 29 non-intuitive property does not occur for the model without mortality. 30

Keywords: chemostat, gradostat, mortality, bifurcations, global stability,
 operating diagram, biogas production

MSC Classification: 34D20, 34H20, 65K10, 92C75

³⁴ 1 Introduction

33

The mathematical model of the chemostat has received a great attention in the literature for many years (see for instance [16] and literature cited inside). This is probably due to its relative simplicity that can explain and predict quite faithfully the dynamics of real bioprocesses exploiting microbial ecosystems. It is today an important tool for decision making in industrial world, such as for dimensioning bioreactors or designing efficient operating conditions [13, 20].

Several extensions of the original model of the chemostat, considering spa-41 tial heterogeneity, have been proposed to better cope reality (see for instance 42 [19]). Lovitt and Wimpenny has proposed the "gradostat" experimental device 43 as a collection of chemostats of same volume interconnected in series [22, 23], 44 which has led to the so-called "gradostat model" representing in a more gen-45 eral framework a gradient of concentrations [37, 40]. The gradostat model has 46 been further generalized as the "general gradostat model" representing more 47 general interconnection graphs with tanks of different volumes [38, 39]. 48

Efficient use of a chemostat in practice relies on the analysis of its per-49 formance. The performance is considered for different criteria studied in the 50 literature [31], among which the most common are: the output substrate 51 concentration, the residence time, the biogas flow rate and the biomass pro-52 ductivity. Particular interconnection structures have been investigated and 53 compared for the properties in terms of input-output performances (see for 54 instance [5, 7, 15, 28]). It has been notably shown that a series of reactors 55 instead of a single perfectly mixed one can significantly improve the perfor-56 mances of the bioprocess (in terms of matter conversion) while preserving 57 the same residence time, or equivalently that the same performance can be 58 obtained with a smaller residence time considering several tanks in series 59 instead of a single one [14, 17, 24, 25, 47]. 60

On another hand, it is known that in real processes, various growth con-61 ditions can be met and that it could be difficult to setup exactly the same 62 perfect conditions in different reactors. These conditions include toxicity lev-63 els of culture media, which means more concretely that the consideration of 64 a bacterial mortality, although often neglected compared to the removal rate, 65 might be non avoidable and could also be variable. To the best of our knowl-66 edge, the possible impacts of mortality in the design of series of chemostats 67 has not been yet studied in the literature, which is the purpose of the present 68 work. Its contributions also cover interests in theoretical ecology for a better 69 grasp of the interplay between spatial heterogeneity and mortality in resource-70 consumers models. Indeed, considering different removal rates in the classical 71 chemostat model or more general ones allows to consider additional mortal-72 ity terms [21, 29, 34, 44]. However, these mathematical studies have mainly 73

⁷⁴ concern analyses of equilibria and stability and not the performances of the ⁷⁵ system in presence of mortality.

In view of providing clear messages to the practitioners, we investigate 76 how the operating diagram of a series of two interconnected chemostats in 77 series is modified when considering different or identical mortality rates in 78 both tanks. Operating diagrams have proven to be a good synthetic tool to 70 summarize the possible operating modes, emphasized in [26] for its importance 80 for bioreactors. Indeed, such diagrams are more and more often constructed 81 both in the biological literature [26, 36, 41, 45] and the mathematical literature 82 [1, 2, 4, 9-12, 18, 31-33, 35, 42, 43].83

Then, we study the performances in terms of conversion ratio and byproduct production (such as biogas). As we shall see, several aspects are not intuitive, which show that the consideration of mortality can significantly modify the favorable operating conditions.

Along the paper, we use the abbreviations LES for locally exponentially stable and GAS for globally asymptotically stable in the positive orthant.

The paper is organized as follows. Section 2 includes the introduction 90 of the mathematical model corresponding to the serial configuration of two 91 chemostats with mortality rate. Afterwards, Section 3 focuses on the study of 92 performances of the serial configuration with respect of the output substrate 93 concentration. Then, Section 4 considers the performances of the serial con-94 figuration with respect of the biogas production. Next, Section 5 is devoted to 95 illustrations and numerical simulations and a conclusion is given in Section 6. 96 Moreover, we set up the single chemostat with mortality in Appendix A, while 97 Appendix B is devoted to the existence and stability analysis of the steady 98 states of the serial chemostat and Appendix C to its operating diagram. These 99 results are extension of former results, in the case without mortality [7], but 100 that have required to revisit significantly the mathematical proofs. Finally, 101 Appendix D contains technical proofs. 102

¹⁰³ 2 Presentation of the model

We consider two serial interconnected chemostats where the total volume V is divided into $V_1 = rV$ and $V_2 = (1 - r)V$, with $r \in (0, 1)$, as shown in Fig. 1. The substrate and the biomass concentrations in the tank *i* are respectively denoted S_i and x_i , i = 1, 2. The input substrate concentration in the first chemostat is designated S^{in} , the flow rate is constant and is designated by Q. The output substrate concentration is the concentration of substrate in the second tank $S^{out} = S_2$.

¹¹¹ The mathematical model is given by the following equations:



Fig. 1 The serial configuration of two chemostats respectively of volumes rV and (1-r)V.

$$\dot{S}_{1} = \frac{D}{r}(S^{in} - S_{1}) - f(S_{1})x_{1}
\dot{x}_{1} = -\frac{D}{r}x_{1} + f(S_{1})x_{1} - ax_{1}
\dot{S}_{2} = \frac{D}{1-r}(S_{1} - S_{2}) - f(S_{2})x_{2}
\dot{x}_{2} = \frac{D}{1-r}(x_{1} - x_{2}) + f(S_{2})x_{2} - ax_{2},$$
(1)

where $\dot{S}_i = \frac{dS_i}{dt}$, $\dot{x}_i = \frac{dx_i}{dt}$, i = 1, 2, f is the growth function such that $f(S_i)$ is the growth function of the substrate in the tank i = 1, 2, a is the mortality rate of the biomass and D = Q/V is the dilution rate of the whole structure. The dilution rate of the first tank is $Q/V_1 = D/r$. The dilution rate of the second tank is $Q/V_2 = D/(1-r)$.

Note that these equations are not valid for r = 0 and r = 1, which correspond to a single chemostat. For sake of completeness, the useful results on the single chemostat are given in Appendix A. The considered growth function satisfies the following properties.

Assumption 1 The function f is \mathcal{C}^1 , with f(0) = 0 and f'(S) > 0 for all S > 0.

We define

$$m := \sup_{S>0} f(S), \quad (m \text{ may be } +\infty).$$
(2)

As f is increasing then the break-even concentration is defined by

$$\lambda(D) := f^{-1}(D) \quad \text{when} \quad 0 \le D < m.$$
(3)

The particular case without mortality of the biomass (a = 0) is studied in [7]. The results on the existence and stability of steady states of system (1) are very similar to the case without mortality. The details are given in Appendix B. The system can have up to three steady states:

- The washout steady state $E_0 = (S^{in}, 0, S^{in}, 0)$.
- The steady state $E_1 = (S^{in}, 0, \overline{S}_2, \overline{x}_2)$ of washout in the first chemostat but not in the second one.
- The steady state $E_2 = (S_1^*, x_1^*, S_2^*, x_2^*)$ of persistence of the species in both chemostats.

As in the case without mortality, see Table C2 in the Appendix, for any operating condition (S^{in}, D) , one and only one of the steady-states E_0 , E_1 and E_2 , is stable. It is then globally asymptotically stable (GAS).

The operating diagram of the system is described in Appendix C. The operating diagram has as coordinates the input substrate concentration S^{in} and the dilution rate D, and shows how the solutions of the system behave for different values of these two parameters. The regions constituting the operating diagram correspond to different qualitative asymptotic behaviors. The operating diagram of system (1) is depicted in Fig. 2.

The aim of this work is to establish a comparison of the performance of the serial configuration with ones of the single chemostat. In the following, we compare both structures according to two different criteria; the output substrate concentration and the biogas flow rate.

¹⁴⁵ **3** Output substrate concentration

The output substrate concentration measures the biodegradation of the input substrate by the overall device. The reduction of the output substrate concentration is one of the main objectives of the biological wastewater treatment, and its minimization is often addressed in the literature, see for example [46]. We assume that the serial configuration is functioning at a stable steady state. The output substrate concentration at steady state depends on the parameters D, S^{in} and r, and will be denoted $S_r^{out}(S^{in}, D)$.

Proposition 1 Assume that Assumption 1 is satisfied. The output substrate concentration at steady state of system (1) is given by

$$S_r^{out}(S^{in}, D) = \begin{cases} S^{in} & \text{if } S^{in} \le \min\left(\lambda\left(\frac{D}{1-r}+a\right), \lambda\left(\frac{D}{r}+a\right)\right) \\ \overline{S}_2 & \text{if } \lambda\left(\frac{D}{1-r}+a\right) \le S^{in} \le \lambda\left(\frac{D}{r}+a\right) \\ S_2^* & \text{if } S^{in} > \lambda\left(\frac{D}{r}+a\right) \end{cases}$$
(4)

where $\overline{S}_2 = \lambda \left(\frac{D}{1-r} + a\right)$ and S_2^* is the unique solution of equation $h(S_2) = f(S_2)$. In this equation, the function h is defined by:

$$h(S_2) = \frac{D + (1-r)a}{1-r} \frac{S_1^* - S_2}{b - S_2},$$
(5)
where $S_1^* = \lambda \left(\frac{D}{r} + a\right)$ and $b = \frac{D(S^{in} - S_1^*)}{D + ra} + S_1^*.$

¹⁵⁸ Proof The output substrate concentration at steady state of system (1) is equal to ¹⁵⁹ S^{in} , if E_0 is the GAS steady state. It is equal to \overline{S}_2 if E_1 is the GAS steady state ¹⁶⁰ and to S_2^* if E_2 is GAS. According to Theorem 3 in the Appendix, E_0 is GAS if and ¹⁶¹ only if

$$D \ge \max(r, 1-r)(f(S^{in}) - a),$$

¹⁶² which is equivalent to

$$S^{in} \le \min\left(\lambda\left(\frac{D}{1-r}+a\right),\lambda\left(\frac{D}{r}+a\right)\right).$$

On the other hand, using Theorem 3, \overline{S}_2 depends on D and r and we have $\overline{S}_2 = \lambda \left(\frac{D}{1-r} + a\right)$. E_1 is GAS if and only if

$$r(f(S^{in}) - a) \le D \le (1 - r)(f(S^{in}) - a),$$

¹⁶⁵ which is equivalent to

$$\lambda\left(\frac{D}{1-r}+a\right) \leq S^{in} \leq \lambda\left(\frac{D}{r}+a\right).$$

Finally, using Theorem 3, we know that S_2^* depends on parameters S^{in} , D, r. It is the unique solution of equation $h(S_2) = f(S_2)$, where h is defined by (5). On the other hand E_2 is GAS if and only if the condition $D < r(f(S^{in}) - a)$ is satisfied, which is equivalent to the condition $S^{in} > \lambda \left(\frac{D}{r} + a\right)$.

Although $S_r^{out}(S^{in}, D)$ is defined only for 0 < r < 1, we can extend it, by continuity, for r = 0 and r = 1 by

$$S_0^{out}(S^{in}, D) = S_1^{out}(S^{in}, D) = S^{out}(S^{in}, D).$$
 (6)

where $S^{out}(S^{in}, D)$, which is the output substrate concentration of the single chemostat, is given by

$$S^{out}(S^{in}, D) = \begin{cases} S^{in} & \text{if } S^{in} \le \lambda(D+a), \\ \lambda(D+a) & \text{if } S^{in} > \lambda(D+a). \end{cases}$$
(7)

For more information on $S^{out}(S^{in}, D)$, see Appendix A.

The proof of (6), comes from the following remarks. First, we have $\overline{S}_2(D,0) = \lambda(D+a)$ and second, according to Lemma 9 in the Appendix, we can extend $S_2^*(S^{in}, D, r)$, by continuity, to r = 1, by

$$S_2^*(S^{in}, D, 1) = \lambda(D+a)$$

Our aim in this section is to compare S_r^{out} defined by (4) and (6) and S^{out} defined by (7).

3.1 The serial configuration can be more efficient than the single chemostat

We fix r and we describe the set of operating conditions (S^{in}, D) for which

$$S_r^{out}(S^{in}, D) < S^{out}(S^{in}, D), \tag{8}$$

that is to say, the serial configuration with volumes rV and (1-r)V, is more efficient than the single chemostat of volume V. For $r \in (0,1)$, let $g_r : [0, r(m-1)) \mapsto \mathbb{R}$ defined by

$$g_r(D) := \lambda \left(\frac{D}{r} + a\right) + \frac{r(D+ar)}{(1-r)(D+a)} \left(\lambda \left(\frac{D}{r} + a\right) - \lambda(D+a)\right).$$
(9)

186 **Lemma 1** For $r \in (0,1)$ we have $g_r(D) > \lambda\left(\frac{D}{r} + a\right)$.

¹⁸⁷ Proof As 0 < r < 1 and λ is an increasing function then, we have $\lambda(D/r + a) > \lambda(D + a)$. Using (9), we have $g_r(D) > \lambda(D/r + a)$.



Fig. 2 The operating diagram of of system (1) and the curve Γ_r defined by (14) under which the serial configuration is more efficient than the single chemostat.

Theorem 1 Assume that Assumption 1 is satisfied. For any $r \in (0, 1)$, we have

$$S_r^{out}(S^{in}, D) = S^{out}(S^{in}, D) \Longleftrightarrow S^{in} = g_r(D).$$

190 Moreover,

$$S_r^{out}(S^{in}, D) < S^{out}(S^{in}, D) \iff S^{in} > g_r(D).$$

Proof Recall that $S_2^*(S^{in}, D, r)$ is the unique solution of equation $f(S_2) = h(S_2)$ with h defined by (5). Let us first prove that

$$S_2^*(S^{in}, D, r) < \lambda(D+a) \Longleftrightarrow S^{in} > g_r(D).$$
⁽¹⁰⁾

Since f is increasing, see Assumption 1, and h is decreasing, see Lemma 8 in the Appendix, then the condition $S_2^*(S^{in}, D, r) < \lambda(D+a)$ is equivalent to the condition $h(\lambda(D+a)) < f(\lambda(D+a)) = D+a$. Using (5), a straightforward computation shows that the condition $h(\lambda(D+a)) < D+a$ is equivalent to $S^{in} > g_r(D)$, where g_r is defined by (9). This proves (10).

Let us go now to the proof of the theorem. Assume that $S^{in} > g_r(D)$. Using Lemma 199 1, we have

$$S^{in} > \lambda(D/r+a) > \lambda(D+a).$$

 $_{200}$ Using (4) and (7), we have

$$S_{r}^{out}(S^{in}, D) = S_{2}^{*}(S^{in}, D, r),$$

$$S^{out}(S^{in}, D) = \lambda(D + a).$$
(11)

From (10), we have $S_r^{out}(S^{in}, D) < S^{out}(S^{in}, D)$. Hence, we proved the following implication

$$S^{in} > g_r(D) \Longrightarrow S^{out}_r(S^{in}, D) < S^{out}(S^{in}, D).$$
(12)

Assume now that $S^{in} \leq g_r(D)$. When r < 1/2, three cases must be distinguished. First, if

$$\lambda(D+a) < \lambda\left(\frac{D}{r}+a\right) < S^{in} \le g_r(D),$$

then, by (4) and (7), we obtain (11). Hence, using (10), we have $S_r^{out}(S^{in}, D) \geq S_r^{out}(S^{in}, D)$. Secondly, if

$$\lambda(D+a) < \lambda\left(\frac{D}{1-r}+a\right) \le S^{in} \le \lambda\left(\frac{D}{r}+a\right),$$

 $_{207}$ then, by (4) and (7), we have

$$S_r^{out}(S^{in}, D) = \lambda \left(\frac{D}{1-r} + a\right),$$

$$S^{out}(S^{in}, D) = \lambda (D+a).$$

Therefore, we have $S_r^{out}(S^{in}, D) > S^{out}(S^{in}, D)$. Finally, if $S^{in} \leq \lambda(D+a)$, then

$$S_r^{out}(S^{in}, D) = S^{out}(S^{in}, D) = S^{in}.$$

When $r \ge 1/2$, the proof is similar, excepted that we must distinguish only two cases, $\lambda(D+a) < S^{in} \le \lambda(D/r+a)$ and $S^{in} \le \lambda(D+a)$. Hence, we have proved the reciprocal implication of (12). This completes the proof of second equivalence in the theorem.

The same calculations show the equivalence if inequalities are replaced by equalities. $\hfill\square$

Theorem 1 asserts that the serial configuration is more efficient than the single chemostat if and only if $S^{in} > g_r(D)$. Let us illustrate this result in the operating diagram of system (1). Consider the curve of equation

$$\Phi_r = \{ (S^{in}, D) : S^{in} = \lambda (D/r + a) \}.$$
(13)

According to the results given in Appendix C, the curves Φ_r and Φ_{1-r} defined by (13) separate the operating plane (S^{in}, D) in four regions in which the system has different asymptotic behaviour, see Table C2. To put it simply, in the $I_0(r)$ region, E_0 is GAS, in $I_1(r)$, E_1 is GAS, and in $I_2(r) \cap I_3(r)$, E_3 is GAS, see Fig. 2. This figure also shows the plot of the curve Γ_r , defined by

$$\Gamma_r := \left\{ (S^{in}, D) : S^{in} = g_r(D) \right\}.$$
(14)

Using Lemma 1, we see that for all $r \in (0, 1)$, the curve Γ_r is always at right of the curve Φ_r . According to Theorem 1, the output substrate concentration of the serial configuration is smaller than the one of the single chemostat, if and only if (S^{in}, D) is at right of the curve Γ_r depicted in Fig. 2.

3.2 The output substrate concentration as a function of 227 the volume fraction r228

In this section we assume that (S^{in}, D) is fixed and we look at the values of r for which (8) holds. More precisely we are going to describe the function

$$r \mapsto S_r^{out}(S^{in}, D). \tag{15}$$

Proposition 2 Assume that Assumption 1 is satisfied. Let D > 0. $S^{in} > \lambda(a)$. We 229 denote $r_0 = D/(f(S^{in}) - a)$. 230

1. If $S^{in} \leq \lambda(D+a)$, then for any $r \in [0,1]$, one has $S_r^{out}(S^{in}, D) = S^{out}(S^{in}, D) = S^{in}$. 231 232

2. If $\lambda(D+a) < S^{in} < \lambda(2D+a)$, then $1/2 < r_0 < 1$ and one has

$$S_r^{out}(S^{in}, D) = \begin{cases} \overline{S}_2 & \text{if } 0 \le r \le 1 - r_0 \\ S^{in} & \text{if } 1 - r_0 \le r \le r_0 \\ S_2^* & \text{if } r_0 \le r \le 1. \end{cases}$$
(16)

3. If $\lambda(2D+a) \leq S^{in}$, then $0 < r_0 \leq 1/2$ and one has 233

$$S_r^{out}(S^{in}, D) = \begin{cases} \overline{S}_2 & \text{if } 0 \le r \le r_0 \\ S_2^* & \text{if } r_0 \le r \le 1. \end{cases}$$
(17)

Here $\overline{S}_2 = \lambda \left(\frac{D}{1-r} + a \right)$ and $S_2^* = S_2^*(S^{in}, D, r)$ is the unique solution of equation 234 $f(S_2) = h(S_2)$, where h is defined by (5). 235

Proof If $S^{in} \leq \lambda(D+a)$, then, for all $r \in (0,1)$, one has 236

$$S^{in} \le \lambda(D+a) \le \min\left\{\lambda\left(\frac{D}{1-r}+a\right), \lambda\left(\frac{D}{r}+a\right)\right\}.$$

Then, according to (4), one has $S_r^{out}(S^{in}, D) = S^{in}$. This proves item 1 of the 237 proposition. 238

Let $r_0 = D/(f(S^{in}) - a)$, i.e. $S^{in} = \lambda(D/r_0 + a)$. 239

If $\lambda(D+a) < S^{in} < \lambda(2D+a)$, then $r_0 \in (1/2, 1)$, so that $1 - r_0 < r_0$. The 240 interval [0, 1] is subdivided into three sub-intervals. Firstly, if $0 \le r \le 1 - r_0 < r_0$, 241 then $r < r_0 \leq 1 - r$, so that 242

$$\lambda\left(\frac{D}{1-r}+a\right) \le S^{in} = \lambda\left(\frac{D}{r_0}+a\right) < \lambda\left(\frac{D}{r}+a\right).$$

Hence, according to (4), one has 243

$$S_r^{out}(S^{in}, D) = \lambda \left(\frac{D}{1-r} + a\right).$$

Secondly, if $1 - r_0 \le r \le r_0$, then $r_0 \ge \max\{r, 1 - r\}$, so that 244

$$S^{in} = \lambda \left(\frac{D}{r_0} + a \right) \le \min \left\{ \lambda \left(\frac{D}{1-r} + a \right), \lambda \left(\frac{D}{r} + a \right) \right\}.$$

9

Hence, according to (4), one has $S_r^{out}(S^{in}, D) = S^{in}$. Finally, if $r_0 < r \le 1$, then one has

$$S^{in} = \lambda \left(\frac{D}{r_0} + a\right) > \lambda \left(\frac{D}{r} + a\right)$$

²⁴⁷ Hence, according to (4), one has

$$S_r^{out}(S^{in}, D) = S_2^*(S^{in}, D, r).$$

²⁴⁸ This proves item 2 of the proposition.

If $\lambda(2D+a) \leq S^{in}$, then $r_0 \in (0, 1/2]$. Therefore, $r_0 \leq 1-r_0$. The proof of item 3 of the proposition is the same as the proof of item 2 excepted that now, the interval [0, 1] is subdivided now into two sub-intervals $[0, r_0]$ and $[r_0, 1]$, so that the interval for which $S_r^{out}(S^{in}, D) = S^{in}$ is empty.



Fig. 3 In each region J_i , i = 0, ..., 4, the map $r \mapsto S_r^{out}(S^{in}, D)$ for fixed (S^{in}, D) has a different behavior.

We want to determine the values $r \in (0, 1)$ for which the condition (8) is satisfied. We need the following Assumption that is satisfied by any concave growth function but also by non concave growth functions, satisfying additional conditions, see Section 3.4.

Assumption 2 For every $D \in [0, m-a)$, the function $r \in (D/(m-a), 1) \mapsto g_r(D) \in \mathbb{R}$ is decreasing.

Let
$$D < m-a$$
. Using $g_r(D) > \lambda(D/r+a)$, we have

$$\lim_{r \to D/(m-a)} g_r(D) > \lim_{r \to D/(m-a)} \lambda(D/r+a) = +\infty.$$

260 On the other hand, using L'Hôpital's rule, we have

$$\lim_{t \to 0} g_r(D) = g(D). \tag{18}$$

where $g: [0, m-a) \to \mathbb{R}^+$ is defined by

$$g(D) = \lambda(D+a) + D\lambda'(D+a).$$
⁽¹⁹⁾

Therefore, from Assumption 2, the function $r \mapsto g_r(D)$ is decreasing from (D/(m-a), 1) to $(g(D), +\infty)$. Hence, it admits an inverse function

$$S^{in} \in (g(D), +\infty) \mapsto r_1(S^{in}, D) \in (D/(m-a), 1).$$

We use the notation $r_1(\cdot, D)$ to recall the dependence of the inverse function in D. For all $D \in (0, m-a), r \in (D/(m-a), 1)$ and $S^{in} > g(D)$, we have

$$r = r_1(S^{in}, D) \Longleftrightarrow S^{in} = g_r(D), \tag{20}$$

$$r > r_1(S^{in}, D) \iff S^{in} > g_r(D).$$
 (21)

Theorem 2 Assume that Assumptions 1 and 2 are satisfied. Let g defined by (19).

- If $S^{in} \leq g(D)$ then for any $r \in (0,1)$, we have $S_r^{out}(S^{in}, D) > S^{out}(S^{in}, D)$. In addition, for r = 0 and r = 1 we have $S_r^{out}(S^{in}, D) = S^{out}(S^{in}, D)$.
- If $S^{in} > g(D)$ then $S_r^{out}(S^{in}, D) < S^{out}(S^{in}, D)$ if and only if $r_1(S^{in}, D) < r < 1$, with $r_1(S^{in}, D)$, defined by (20). In addition, for r = 0, $r = r_1(S^{in}, D)$ and r = 1, we have $S_r^{out}(S^{in}, D) = S^{out}(S^{in}, D)$.

Proof The function $r \mapsto g_r(D)$ is decreasing and tends to g(D) as r tends to 1, as shown by (18). Thus, for all $r \in (0,1)$, we have $g(D) < g_r(D)$. If $S^{in} \leq g(D)$, then $S^{in} < g_r(D)$. According to Theorem 1, for all $r \in (0,1)$, we have $S_r^{out}(S^{in}, D) > S^{out}(S^{in}, D)$.

Let $S^{in} > g(D)$. Let $r_1 = r_1(S^{in}, D)$. According to (21), for all $r > r_1$, we have $S^{in} > g_r(D)$. Thus, according to Theorem 1, we have $S^{out}_r(S^{in}, D) < S^{out}(S^{in}, D)$. The equality $S^{out}_r(S^{in}, D) = S^{out}(S^{in}, D)$ is verified for the r = 0 and r = 1, see (6). In addition, we have $S^{in} = g_{r_1}(D)$, see (20). Hence, according to Theorem 1, we have $S^{out}_{r_1}(S^{in}, D) = S^{out}(S^{in}, D)$.

Let us now describe the subsets of the operational space (S^{in}, D) for which the behaviour described in the three cases of Proposition 2 occurs. For a complete description we will also distinguish the sub-cases for which there exists $r_1 = r_1(S^{in}, D)$ such that, for $r_1 < r < 1$, (8) is satisfied, as shown in Theorem 2. Consider the curves Φ_1 and $\Phi_{1/2}$, defined by (13), and the curve Γ defined by

$$\Gamma := \{ (S^{in}, D) : S^{in} = g(D) \},$$
(22)

²⁸⁷ These three curves intersect at $(\lambda(a), 0)$ and, using the inequality $g(D) > \lambda(D+a)$, which is satisfied for all D > 0, one deduces that Γ is at the right



Fig. 4 For S^{in} and D fixed, the output substrate concentration of the serial configuration, in red, compared to that of the single chemostat, in blue; $r_1(S^{in}, D)$ is defined by (20), $r_0 = D/(f(S^{in}) - a)$ and J_1, J_2, J_3, J_4 are depicted in Fig. 3.

of Φ_1 . Therefore, the curves Φ_1 , $\Phi_{1/2}$ and Γ separate the set of operating parameters (S^{in}, D) into the following four subsets, see Fig. 3.

$$J_{0} = \left\{ (S^{in}, D) : S^{in} \leq \lambda(D+a) \right\}, J_{1} = \left\{ (S^{in}, D) : \lambda(D+a) < S^{in} \leq \min\{g(D), \lambda(2D+a)\} \right\}, J_{2} = \left\{ (S^{in}, D) : g(D) < S^{in} < \lambda(2D+a) \right\}, J_{3} = \left\{ (S^{in}, D) : \max\{g(D), \lambda(2D+a)\} \leq S^{in} \right\}, J_{4} = \left\{ (S^{in}, D) : \lambda(2D+a) < S^{in} < g(D) \right\}.$$
(23)

²⁹¹ Combining the results of Proposition 2 and Theorem 2, we find that the ²⁹² function $r \mapsto S_r^{out}(S^{in}, D)$ is as in Fig. 4. In the following we will comment on ²⁹³ this figure.

• If $(S^{in}, D) \in J_1$, then when $S^{in} < \lambda(2D+a)$, $S_r^{out}(S^{in}, D)$ is given by (16) and when $S^{in} = \lambda(2D+a)$, $S_r^{out}(S^{in}, D)$ is given by (17). In addition, for all $r \in (0, 1)$, $S_r^{out}(S^{in}, D) > S^{out}(S^{in}, D)$. The equality is fulfilled for r = 0and r = 1, see Fig. 4(a).

• If
$$(S^{in}, D) \in J_2$$
, then $S_r^{out}(S^{in}, D)$ is given by (16) and $S_r^{out}(S^{in}, D) < S^{out}(S^{in}, D)$ if and only if $r \in (r_1(S^{in}, D), 1)$, where $r_1(S^{in}, D)$ is defined

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by (20). The equality is fulfilled for r = 0, $r = r_1(S^{in}, D)$ and r = 1, see 300 Fig. 4(b). 301

• If $(S^{in}, D) \in J_3$ then $S_r^{out}(S^{in}, D)$ is given by (17) and $S_r^{out}(S^{in}, D) <$ 302 $S^{out}(S^{in}, D)$ if and only if $S^{in} > g(D)$ and $r \in (r_1(S^{in}, D), 1)$ where 303 $r = r_1(S^{in}, D)$ is defined by (20). The equality is fulfilled for r = 0, 304 $r = r_1(S^{in}, D)$ and r = 1, see Fig. 4(c). 305

• If $(S^{in}, D) \in J_4$ then $S_r^{out}(S^{in}, D)$ is given by (17) and for all $r \in (0, 1)$, 306 $S_r^{out}(S^{in}, D) > S^{out}(S^{in}, D)$. The equality is fulfilled for r = 0 and r = 1, 307 see Fig. 4(d). 308

Note that if $(S^{in}, D) \in J_0$, then case 1 of Proposition 2 occurs. One remarks 309 that the lowest value of the red curve, corresponding to the lowest output 310 substrate concentration of the serial configuration, is obtained for $(S^{in}, D) \in$ 311 $J_2 \cap J_3$ and $r > r_1(S^{in}, D)$. This lowest concentration is obtained with the 312 best possible serial configuration. 313

Figures 2, 3 and 4 are made without graduations on the axes because they 314 represent general situations where the growth function is only assumed to 315 verify our hypotheses. It should be noticed that regions J_0 , J_1 and J_3 always 316 exist and are connected. However, regions the J_2 and J_4 do not always exist or 317 are necessarily connected. This depends on the number of points of intersection 318 between curves $\Phi_{1/2}$ and Γ . For a linear growth rate, $\Phi_{1/2} = \Gamma$ and hence, 319 regions J_2 and J_4 do not exist, see Fig. 7(a). For a Monod growth function, 320 curves $\Phi_{1/2}$ and Γ intersect only at point $(\lambda(a), 0)$ and hence, region J_3 always 321 exist and is connected but region J_3 does not exist, see Fig. 8(a). For a Hill 322 growth function, curves $\Phi_{1/2}$ and Γ always intersect at $(\lambda(a), 0)$ and also at a 323 unique positive point, Lemma 6. Hence, regions J_2 and J_4 both exist and are 324 connected, see Fig. 9(a,b,c). 325

3.3 The output substrate concentration as a function of 326 the dilution rate 327

In this section we assume that S^{in} and r are fixed and we look at the values 328 of the dilution rate D for which (8) holds, i.e. the serial configuration, is more 329 efficient than the single chemostat. More precisely we are going to describe the 330 function 331

$$D \mapsto S_r^{out}(S^{in}, D). \tag{24}$$

We want to determine the subset of values of D for which the condition 332 (8) is satisfied. We need the following Assumption that is satisfied by any 333 concave growth function, but also by non concave growth functions, satisfying 334 additional conditions, see Section 3.4. 335

Assumption 3 For every $r \in (0, 1)$, the function $D \in [0, r(m-a)) \mapsto g_r(D) \in \mathbb{R}$ is 336 increasing. 337

13

Using $g_r(D) > \lambda(D/r + a)$, we have

$$\lim_{D \to r(m-a)} g_r(D) > \lim_{D \to r(m-a)} \lambda(D/r + a) = +\infty.$$

From Assumption 3, the function $D \mapsto g_r(D)$ is increasing from [0, r(m-a)) to $[g_r(0) = \lambda(a), +\infty)$. Hence, its admits an inverse function

$$S^{in} \in (\lambda(a), +\infty) \mapsto D_r(S^{in}) \in [0, r(m-a)).$$

For all $r \in (0, 1)$, $S^{in} \ge \lambda(a)$ and $D \in [0, r(m-a))$, we have

$$D = D_r(S^{in}) \iff S^{in} = g_r(D), \tag{25}$$

$$D < D_r(S^{in}) \Longleftrightarrow S^{in} > g_r(D).$$
⁽²⁶⁾

Proposition 3 Assume that Assumptions 1 and 3 are satisfied. We have

$$S_r^{out}(S^{in}, D) < S^{out}(S^{in}, D) \Longleftrightarrow 0 < D < D_r(S^{in}),$$

³³⁸ where $D_r(S^{in})$ is defined by (25).

Proof Let $r \in (0,1)$. According to (26), if $D < D_r(S^{in})$, then $S^{in} > g_r(D)$. Consequently, according to Theorem 1, we have $S_r^{out}(S^{in}, D) < S^{out}(S^{in}, D)$.

³⁴¹ 3.4 How to check Assumptions 2 and 3

³⁴² In this section we give sufficient conditions for Assumption 2 and 3 to be ³⁴³ satisfied. These conditions will be useful for the applications given in Section ³⁴⁴ 5. For this purpose we consider the function γ defined by

$$\gamma(r, D) = g_r(D), \tag{27}$$

defined on

$$dom(\gamma) = \{ (r, D) : 0 < r < 1, 0 < D/r + a < m \},\$$

which consists simply in considering $g_r(D)$, given by (9), as a function of both variables r and D. If

 $\frac{\partial \gamma}{\partial r}(r,D) < 0$ for all $(r,D) \in \operatorname{dom}(\gamma)$,

347 then Assumption 2 is satisfied. Similarly, if

$$\frac{\partial \gamma}{\partial D}(r, D) > 0$$
 for all $(r, D) \in \operatorname{dom}(\gamma)$,

 $_{\rm 348}$ then Assumption 3 is satisfied. The following Lemmas give sufficient condi-

 $_{\rm 349}$ $\,$ tions, for partial derivatives of γ to have their signs as indicated above.

³⁵⁰ Lemma 2 For $D \in (0, m - a)$, let l_D be defined on dom $(l_D) = (D/(m - a), 1]$ by ³⁵¹ $l_D(r) = \lambda(D/r + a)$.

a) Assume that for $D \in (0, m - a)$ and $r \in dom(l_D)$ we have

$$l_D(1) > l_D(r) + (1-r)l'_D(r)$$
(28)

then, for all $(r, D) \in \operatorname{dom}(\gamma)$, we have $\frac{\partial \gamma}{\partial r}(r, D) < 0$.

b) If, for $D \in (0, m - a)$, l_D is strictly convex on dom (l_D) , then the condition (28) is satisfied.

 $_{355}$ c) If f is twice derivable, then l_D is twice derivable and the following conditions are $_{356}$ equivalent

³⁵⁷ 1. For $D \in (0, m - a)$ and $r \in \text{dom}(l_D)$, $l''_D(r) > 0$. ³⁵⁸ 2. For $S > \lambda(a)$, $(f(S) - a) f''(S) < 2 (f'(S))^2$.

Proof Notice first that $\gamma(r, D)$ can be written as follows

$$\gamma(r,D) = g_r(D) = \lambda \left(D+a\right) + \left(\frac{1}{1-r} - \frac{ra}{D+a}\right) \left(\lambda \left(\frac{D}{r} + a\right) - \lambda(D+a)\right).$$
⁽²⁹⁾

Using the definition of l_D , $\gamma(r, D)$ is given then by

$$\gamma(r,D) = l_D(1) + \left(\frac{1}{1-r} - \frac{ra}{D+a}\right) \left(l_D(r) - l_D(1)\right).$$

The partial derivative, with respect to r of γ is given then by

$$\frac{\partial \gamma}{\partial r}(r,D) = \frac{a(1-2r)}{D+a} l'_D(r) +
\left(\frac{1}{(1-r)^2} - \frac{a}{D+a}\right) \left(l_D(r) - l_D(1) + (1-r)l'_D(r)\right).$$
(30)

Notice that $\frac{1}{(1-r)^2} - \frac{a}{D+a} > 0$ for all $r \in (0,1)$. From $l'_D(r) = -\frac{D}{r^2}\lambda'\left(\frac{D}{r} + a\right)$, it is deduced that $l'_D(r) < 0$. Therefore, if the condition (28) is satisfied, and, in addition $0 < r \le 1/2$, then, from (30), it is deduced that $\frac{\partial \gamma}{\partial r}(r, D) < 0$.

In the case $r \in (1/2, 1)$, we use the following expression of $\gamma(r, D)$ which is deduced from (29):

$$\gamma(r, D) = l_D(1) + B(r) \frac{l_D(r) - l_D(1)}{1 - r}$$

where $B(r) = \frac{D+a-ar(1-r)}{D+a}$. Straightforward computation show that

$$\frac{\partial \gamma}{\partial r}(r,D) = \\
\frac{D + ar(2-r)}{(D+a)(1-r)^2} \left(l_D(r) - l_D(1) + (1-r)C(r)l'_D(r) \right),$$
(31)

where $C(r) = \frac{D+a-ar(1-r)}{D+ar(2-r)}$. We have

$$C'(r) = \frac{a}{(D+ar(2-r))^2} \left(ar^2 + 2(a+2D)r - 3D - 2a \right).$$

360 Thus C'(r) = 0 for

$$r = r^* := \frac{1}{a} \left(\sqrt{3a^2 + 7aD + 4D^2} - a - 2D \right) \in (1/2, 1)$$

and $(r - r^*)C'(r) > 0$ for $r \in (1/2, 1)$, $r \neq r^*$. Hence, from C(1/2) = C(1) = 1, we have 0 < C(r) < 1 for all $r \in (1/2, 1)$. Now, if we assume that (28) is satisfied, for 1/2 < r < 1 we have

$$l_D(1) > l_D(r) + (1-r)l'_D(r) > l_D(r) + (1-r)C(r)l'_D(r).$$

Hence, from (31), it is deduced that $\frac{\partial \gamma}{\partial r}(r, D) < 0$. This proves part *a* of the lemma. Moreover, if l_D is strictly convex on dom (l_D) then for all *s* and *r* in (D/(m-a), 1], if $s \neq r$, then

$$l_D(s) > l_D(r) + (s - r)l'_D(r)$$

Taking s = 1 and $r \in \text{dom}(l_D)$ one obtains the condition (28). This proves part b of the lemma. Assume now that f, and hence l_D , are twice derivable. Using

$$\lambda'(D) = \frac{1}{f'(\lambda(D))}, \quad \lambda''(D) = -\frac{f''(\lambda(D))}{(f'(\lambda(D)))^3}, \tag{32}$$

we can write

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$$l_D''(r) = \frac{2D}{r^3} \lambda' \left(\frac{D}{r} + a\right) + \frac{D^2}{r^4} \lambda'' \left(\frac{D}{r} + a\right)$$
$$= \frac{D\left(2(f'(\lambda(\frac{D}{r} + a)))^2 - \frac{D}{r}f''(\lambda(\frac{D}{r} + a))\right)}{r^3(f'(\lambda(\frac{D}{r} + a)))^3}.$$

Therefore, the condition 1 in item c in the lemma is equivalent to the following condition: For all $D \in (0, m - a)$ and $r \in (D/(m - a), 1]$, we have

$$\frac{D}{r}f''\left(\lambda\left(\frac{D}{r}+a\right)\right) < 2f'\left(\lambda\left(\frac{D}{r}+a\right)\right)^2.$$
(33)

Using the notation $S = \lambda \left(\frac{D}{r} + a\right)$, which is the same as D/r = f(S) - a, the condition (33) is equivalent to : For all S > 0, $(f(S) - a)f''(S) < 2(f'(S))^2$, which is the condition 2 in c in the lemma.

367 Lemma 3 Assume that

$$f'\left(\lambda\left(\frac{D}{r}+a\right)\right) \le \frac{1}{r}f'\left(\lambda\left(D+a\right)\right).$$
(34)

Then, $\frac{\partial \gamma}{\partial D}(r, D) > 0$. Hence Assumption 3 is satisfied. If f' is decreasing, then the condition (34) is satisfied.

 $_{370}$ Proof From (29) we deduce that

$$\frac{\partial \gamma}{\partial D}(r,D) = \lambda'(D+a) + \frac{ra}{(D+a)^2} \left(\lambda\left(\frac{D}{r}+a\right) - \lambda(D+a)\right) \\ + \left(\frac{1}{1-r} - \frac{ra}{D+a}\right) \left(\frac{1}{r}\lambda'\left(\frac{D}{r}+a\right) - \lambda'(D+a)\right).$$

Notice that $\frac{1}{1-r} - \frac{ra}{D+a} > 0$, $\lambda'(D+a) > 0$ and $\lambda\left(\frac{D}{r} + a\right) > \lambda(D+a)$. Therefore the condition

$$\frac{1}{r}\lambda'\left(\frac{D}{r}+a\right) - \lambda'(D+a) \ge 0$$

is sufficient to have $\frac{\partial \gamma}{\partial D}(r, D) > 0$. Using (32), this condition is equivalent to (34). Note that if f' is decreasing, then this condition is satisfied. Indeed, we have

$$f'\left(\lambda\left(\frac{D}{r}+a\right)\right) \le f'\left(\lambda\left(D+a\right)\right) \le \frac{1}{r}f'\left(\lambda\left(D+a\right)\right),$$
edition (34)

which is the condition (34).

Remark 1 Notice that: 376

i) The condition 2 in part c of Lemma 2 is equivalent to the condition i377

For all
$$S > \lambda(a), \frac{d^2}{dS^2} \left(\frac{1}{f(S)-a}\right) > 0.$$
 (35)

Therefore, if f satisfies the condition (35), then it verifies Assumption 2. 378

ii) If the increasing growth function f is twice derivable and satisfies $f''(S) \leq 0$ for 379 all S > 0, then the condition b in Lemma 2 and the condition (34) in Lemma 3 380 are satisfied. Thus, Assumptions 2 and 3 are satisfied and our results apply for any 381 concave growth function. 382

iii) Assume that the increasing growth function f is twice derivable and there exists 383 $\hat{S} \in (0, +\infty)$ such that f'' is nonnegative on $(0, \hat{S})$ and nonpositive on $(\hat{S}, +\infty)$. 384 If moreover the condition 2 in part c of Lemma 2 is verified for a = 0, then this 385 condition is also verified for any a > 0 and $S \in (\lambda(a), \hat{S})$. Therefore, if (1/f)'' > 0386 on $(0, \hat{S})$ then Assumption 2 is satisfied. 387

We will see in Section 5, how to use Remark 1 and Lemmas 2 and 3 to show 388 that a linear growth function, a Monod function and a Hill function satisfy 389 Assumptions 2 and 3. 390

4 Biogas flow rate 301

Microbial activity often produces by-products such as biogas, which can be 392 a valuable source of energy in certain contexts. For instance, the anaerobic 393 digestion of organic matter by microbial species produces methane and carbon 394 dioxide. Valorizing biogas production while treating wastewater has received 395 recently great attention, as a way of producing valuable energy and limiting 396 the carbon footprint of the process [30]. 307

We recall that the biogas flow rate is proportional to the microbial activity, 398 as defined for instance in [3, 27]. We consider here the biogas flow rate as a 300 function of the input substrate concentration S^{in} , the dilution rate D and the 400 parameter r. 401

For $r(f(S^{in}) - a) \leq D < (1 - r)(f(S^{in}) - a)$, the biogas flow rate 402 corresponding to the steady state E_1 is given by the expression 403

$$G_1(S^{in}, D, r) = V_2 \overline{x}_2 f(\overline{S}_2), \tag{36}$$

with $V_2 = (1 - r)V$, \overline{x}_2 and \overline{S}_2 defined in (B15). 404

For $D < r(f(S^{in}) - a)$, the biogas flow rate corresponding to the positive 405 steady state E_2 is given by the expression 406

$$G_2(S^{in}, D, r) = V_1 x_1^* f(S_1^*) + V_2 x_2^* f(S_2^*),$$
(37)

with $V_1 = rV$, $V_2 = (1 - r)V$, x_1^* and S_1^* defined in (B17), x_2^* defined by (B18) 407 and S_2^* the unique solution of $h(S_2) = f(S_2)$. 408

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Proposition 4 1. When $r(f(S^{in}) - a) \le D$ and $D < (1 - r)(f(S^{in}) - a)$ then $G_1(S^{in}, D, r) = VD(S^{in} - \overline{S}_2).$ (38)

2. When
$$D < r(f(S^{in}) - a)$$
 then
 $G_2(S^{in}, D, r) = VD(S^{in} - S_2^*).$
(39)

Proof From system (B10), considering equation $\dot{S}_2 = 0$, one obtains $\overline{x}_2 f(\overline{S}_2) = D(S^{in} - \overline{S}_2)/(1-r)$. Thus,

$$G_1(S^{in}, D, r) = V_1 \frac{D}{r} (S^{in} - \overline{S}_2) = V D(S^{in} - \overline{S}_2).$$

From system (B10), considering $\dot{S}_1 = 0$ and $\dot{S}_2 = 0$ gives respectively $x_1^* f(S_1^*) = D(S^{in} - S_1^*)/r$ and $x_2^* f(S_2^*) = D(S_1^* - S_2^*)/(1 - r)$. Thus, one has

$$G_2(S^{in}, D, r) = V_1 \frac{D}{r} (S^{in} - S_1^*) + V_2 \frac{D}{1-r} (S_1^* - S_2^*)$$

= $VD(S^{in} - S_2^*).$

409 This ends the proof of the proposition.

Although $G_1(S^{in}, D, r)$ and $G_2(S^{in}, D, r)$, given by (36) and (37), respectively, are not defined for r = 0 or r = 1, the formulas (38) and (39) allow them to be extended to r = 0 and r = 1, as was done for S_r^{out} in (6). We can write

$$G_1(S^{in}, D, 0) = G_2(S^{in}, D, 1) = G_{chem}(S^{in}, D),$$

where

$$G_{chem}(S^{in}, D) = VD(S^{in} - \lambda(D+a),$$
(40)

⁴¹³ represents the biogas flow rate of the single chemostat when $0 < D < f(S^{in}) - a$. ⁴¹⁴ a. For more information on $G_{chem}(S^{in}, D)$, see (A7) in Appendix A.



Fig. 5 For r and S^{in} fixed, the curves of the maps $D \mapsto G_1(S^{in}, D, r)$, in green, $D \mapsto G_2(S^{in}, D, r)$, in orange, and $D \mapsto G_{chem}(S^{in}, D)$, in black, where G_1, G_2 and G_{chem} are given by (38), (39) and (40) respectively.



Fig. 6 The map $r \mapsto \overline{G}(r)$ with \overline{G} defined by (42). (a) f(S) = 4S, a = 0.6 and $S^{in} = 1.5$. (b) f(S) = 4S/(5+S), a = 0.3 and $S^{in} = 1.5$. (c) $f(S) = 4S^2/(25+S^2)$, a = 0.3 and $S^{in} = 10$.

415 4.1 The serial configuration can be more efficient than 416 the single chemostat

⁴¹⁷ In this section, we prove that the biogas flow rate G_1 corresponding to the ⁴¹⁸ steady state E_1 is always smaller than the biogas flow rate of the single chemo-⁴¹⁹ stat. However, the biogas flow rate G_2 corresponding to the steady state E_2 ⁴²⁰ can be larger than the biogas flow rate of the single chemostat. More precisely, ⁴²¹ we have the following result.

Proposition 5 Assume that Assumption 1 is satisfied. Let $r \in (0,1)$, $0 \le D < (423 \quad f(S^{in}) - a \text{ and } G_{chem}$ defined by (40).

424 1. If $r(f(S^{in}) - a) \leq D$ and $D < (1 - r)(f(S^{in}) - a)$, then $G_1(S^{in}, D, r) < G_{chem}(S^{in}, D)$, where G_1 is given by (38). 2. If $D < r(f(S^{in}) - a)$, then

2. If $D < r(f(S^{in}) - a)$, then

$$G_2(S^{in}, D, r) > G_{chem}(S^{in}, D) \iff S^{in} > g_r(D),$$

where G_2 is given by (39) and g_r is defined by (9).

• If, in addition, Assumption 2 is satisfied, and $S^{in} > g(D)$, then $G_2(S^{in}, D, r) > G_{chem}(S^{in}, D)$, if and only if $r > r_1(S^{in}, D)$, where $r_1(S^{in}, D)$ is defined by (20).

• If, in addition, Assumption 3 is satisfied, then $G_2(S^{in}, D, r) > G_{chem}(S^{in}, D)$, if and only if $D < D_r(S^{in})$, where $D_r(S^{in})$ is defined by (25).

⁴³³ Proof 1. Since D/(1-r) > D and λ is increasing, we have $\lambda(D/(1-r)+a) > \lambda(D+a)$. Then, using the formula for G_1 given in Proposition 4, this induces ⁴³⁵ the inequality $G_1(S^{in}, D, r) < G_{chem}(S^{in}, D)$.

2. According to Theorem 1, for any $r \in (0,1)$ and $D < r(f(S^{in}) - a)$ one 436 has $S_2^*(S^{in}, D, r) < \lambda(D+a)$ if and only if $S^{in} > g_r(D)$. Consequently, 437 using the formula for G_2 given in Proposition 4, one has $G_2(S^{in}, D, r) >$ 438 $G_{chem}(S^{in}, D)$ if and only if $S^{in} > g_r(D)$. If Assumption 2 is satisfied, 439 then, using (21), we see that $G_2(S^{in}, D, r) > G_{chem}(S^{in}, D)$ if and only if 440 $r > r_1(S^{in}, D)$. If Assumption 3 is satisfied, then, using (26), we see that 441 $G_2(S^{in}, D, r) > G_{chem}(S^{in}, D)$ if and only if $D < D_r(S^{in})$. 442 This ends the proof of the proposition. 443

Let S^{in} and D be fixed. The graphs of the biogas flow rates functions

$$r \mapsto G_1(S^{in}, D, r)$$
, and $r \mapsto G_2(S^{in}, D, r)$,

are easily obtained from the graph of the output substrate concentration, $r \mapsto S_r^{out}(S^{in}, D)$, see Fig. 4. Indeed, the formulas given in Proposition 4 show that, whenever these functions are defined, we have

$$G_1(S^{in}, D, r) = VD \left(S^{in} - S_r^{out}(S^{in}, D)\right)$$

$$G_2(S^{in}, D, r) = VD \left(S^{in} - S_r^{out}(S^{in}, D)\right)$$

We will see in Section 5, some illustrative plots of the biogas flow rates G_1 and G_2 as functions of the parameter $r \in [0, 1]$, for linear growth, see Fig. 7, Monod growth, see Fig. 8 and Hill growth, see Fig. 9.

Let us illustrate the result of Proposition 5 by plotting the graphs of the biogas flow rates

$$D \mapsto G_1(S^{in}, D, r)$$
 and $D \mapsto G_2(S^{in}, D, r)$,

when r and S^{in} are fixed, see Fig. 5. This figure is made without graduations on the axes because its represents a general situation where the growth function is only assumed to verify our hypotheses. Indeed the behaviors of the functions, depicted in this figure, follow from our results and are not simply numerical illustrations.

Notice that for any $r \in (0, 1)$, the graph of G_1 (plotted in green in the figure) is always below the graph G_{chem} (plotted in black). This illustrates item 1 of Proposition 5. Assuming that Assumption 3 is satisfied, then for all $0 < D < D_r(S^{in})$, the graph of G_2 (plotted in orange) is above the graph of G_{chem} (plotted in black). This illustrates item 2 of Proposition 5.

463 4.2 The maximal biogas of the serial configuration can 464 exceed that of the single chemostat

In Figure 5(c) the plot shows that the maximum of G_2 (the red curve) is larger than the maximum of G_{chem} , as we want to emphasize that the following inequality is possible

$$\max_{D} G_2(S^{in}, D, r) > \max_{D} G_{chem}(S^{in}, D).$$
(41)

Indeed we will show that there is a value $r^* \in (0, 1)$ such that this inequality is true for all $r \in (r^*, 1)$. The threshold r^* obviously depends on S^{in} and the rate of mortality a. It will be noted $r^*(S^{in}, a)$ when we want to highlight this dependence. This phenomenon never occurs in the case of no mortality, since we have $r^*(S^{in}, 0) = 1$. Indeed, in the case without mortality, we proved, see Proposition 6 of [7], that for all $S^{in} > 0$, and all $r \in (0, 1)$ we have

$$\max_{D} G_2(S^{in}, D, r) < \max_{D} G_{chem}(S^{in}, D),$$

that is to say, the maximal biogas flow rate of the serial configuration never exceed the maximal biogas flow rate of the single chemostat.

Let us prove that, when a > 0, the inequality (41) is always true for rsufficiently close to 1. Observe that for any fixed $S^{in} > \lambda(a)$ and $r \in (0, 1]$, the continuous function $D \mapsto G_2(S^{in}, D, r)$ is defined on the closed interval $[0, r(f(S^{in}) - a)]$. It is null at the extremities of this interval and positive on the open interval $(0, r(f(S^{in}) - a))$. Therefore, it reaches it maximum. For a given $S^{in} > \lambda(a)$, we then consider the function

$$\overline{G}(r) := \max_{D \in [0, r(f(S^{in}) - a)]} G_2(S^{in}, D, r).$$
(42)

⁴⁷³ We want to ensure that this maximum is reached at a single value, denoted ⁴⁷⁴ $\overline{D}(r)$. Note that $\overline{D}(1)$ represents the value, which we will assume to be unique, ⁴⁷⁵ at which the function $D \mapsto G_{chem}(S^{in}, D)$ reaches its maximum. We need the ⁴⁷⁶ following assumption.

Assumption 4 The function f is C^2 and increasing and, for $S^{in} > \lambda(a)$, there exists $\overline{D}(1) \in (0, f(S^{in}) - a)$ such that $D \mapsto G_{chem}(S^{in}, D)$ is

- strictly concave at $\overline{D}(1)$,
- increasing on $(0, \overline{D}(1))$,
- decreasing on $(\overline{D}(1), f(S^{in}) a),$

These conditions are related to the single chemostat model. They are verified for linear, Monod, or Hill growth functions, see Remark 3 in Appendix A.

If Assumption 4 is satisfied, then the maximum of the function $D \mapsto G_{chem}(S^{in}, D)$ is unique. The following lemma shows that the function $D \mapsto G_2(S^{in}, D, r)$ satisfies the same property for r sufficiently close to 1.

Lemma 4 Assume that Assumption 4 is satisfied, then for any $S^{in} > \lambda(a)$, there exists a neighborhood \mathcal{V}_1 of 1, such that for any $r \in \mathcal{V}_1 \cap \{r \leq 1\}$, the maximum of the function $D \mapsto G_2(S^{in}, D, r)$ is unique. We denote it by $\overline{D}(r)$. Moreover, \overline{D} is differentiable on $\mathcal{V}_1 \cap \{r < 1\}$ with bounded derivative.

⁴⁹² *Proof* The proof is given in in Appendix D.2.

Proposition 6 Under Assumption 4, the function \overline{G} admits left limits of its first and second derivatives at r = 1, which are

$$\overline{G}'(1^{-}) = 0, \quad \overline{G}''(1^{-}) = \frac{2aD(1)}{\overline{D}(1) + a} \left(S^{in} - \lambda(\overline{D}(1) + a)\right). \tag{43}$$

⁴⁹³ *Proof* The proof is given in Appendix D.3.

Proposition 7 Under Assumption 4, there exists r^* in (0,1) such that (41) is true for any $r \in (r^*, 1)$ and

$$\max_{D} G_2(S^{in}, D, r^*) = \max_{D} G_{chem}(S^{in}, D)$$

Proof From Proposition 6, there exist $\varepsilon > 0$ such that for all $r \in (1 - \varepsilon, 1)$, we have $\overline{G}(r) > \overline{G}(1)$. Therefore, the subset I of (0, 1) defined by

$$I = \{ \rho \in (0,1) : \forall r \in (\rho,1), \overline{G}(r) > \overline{G}(1) \},\$$

is non empty. Let r^* be the lower bound of I. We have $\overline{G}(r^*) = \overline{G}(1)$ and $\overline{G}(r) > \overline{G}(1)$ for $r \in (r^*, 1)$. Using (42), we deduce that the equality in the proposition is true and (41) is true for any $r \in (r^*, 1)$.

The function $r \mapsto \overline{G}(r)$ reaches its maximum at some $r^{max} \in (r^*, 1)$. Let $D^{max} = \overline{D}(r^{max})$ be the maximum of the function $D \mapsto G_2(S^{in}, D, r^{max})$. Therefore the maximal biogas flow rate of the serial chemostat is given by $G_2(S^{in}, D^{max}, r^{max})$. It satisfies

$$G_2(S^{in}, D^{max}, r^{max}) > G_{chem}\left(S^{in}, \overline{D}(1)\right).$$

We have plotted the function $r \mapsto \overline{G}(r)$ for the linear, Monod, and Hill 497 growth functions considered in Fig. 6. It is seen in this figure that the tangent 498 at r = 1 is horizontal which corresponds to $\overline{G}'(1) = 0$. In addition, one remarks 499 that $\overline{G}(r) > \overline{G}(1)$ for r in some interval $(r^*, 1)$ and $\overline{G}(r^*) = \overline{G}(1)$. Thus, 500 with presence of mortality rate, if practitioners are able to choose the dilution 501 rate D, the good strategy consists in working with a serial configuration and 502 choose r in the interval $(r^*, 1)$. The serial configuration should be operated at 503 $D = \overline{D}(r)$, where $\overline{D}(r)$ is defined in Lemma 4. 504

Remark 2 • If one is interested in increasing the flow of biogas, the best choice is $r = r^{max}$, $D = D^{max}$.

• If one is interested in reducing the dilution rate, the best choice is $r = r^*$ and $D = D^*$, where $D^* = \overline{D}(r^*)$.

Indeed, for the choice $r = r^*$ and $D = D^*$, we have

$$G_2(S^{in}, D^*, r^*) = G_{chem}\left(S^{in}, \overline{D}(1)\right),$$

⁵⁰⁹ but D^* is expected to be significantly smaller than $\overline{D}(1)$, the dilution rate that ⁵¹⁰ maximises biogas for the simple chemostat. In fact, reducing D means that the ⁵¹¹ flow rate Q has been reduced, and therefore energy has been saved to obtain ⁵¹² the same result as with a simple chemostat

This result has an important message for practitioners: the serial configuration is worth considering when mortality is not negligible. To the best of our knowledge, this result is new in the literature. On the other hand, it is not intuitive. For more information on this issue, see Section 5.4. For biological comments on the heuristic underlying this non-intuitive behaviour, the reader is referred to [6].

519 5 Illustrations and numerical simulations

This section illustrates of results using three different growth functions. As concave functions, we choose the linear growth function and the Monod function. As a non concave function, we choose the Hill function.



Fig. 7 (a) The regions J_0 , J_1 and J_3 of the operating plane with f(S) = 4S and a = 0.3. The biogas flow rates corresponding to points $\eta_1 = (0.27, 0.6) \in J_1$ and $\eta_3 = (0.5, 0.6) \in J_3$ are depicted in panels (b) and (c) respectively. In these panels, the numbered curves (1) (in black), and (1), (2) (in orange) are respectively defined by $y = G_{chem}(S^{in}, D), y = G_1(S^{in}, D, r)$ and $y = G_2(S^{in}, D, r); r_0(S^{in}, D) = D/(f(S^{in}) - a)$ and $r_1(S^{in}, D)$ is defined by (20). (b) $r_0 \approx 0.77$. (c) $r_0 \approx 0.35$ and $r_1 = 0.5$.

523 5.1 Linear growth function

Let consider a linear function $f(S) = \alpha S$, $\alpha > 0$. As it is concave, according to item *ii* in Remark 1, the linear function verifies Assumptions 2 and 3. Therefore, our results apply for a linear function.

⁵²⁷ One has $\lambda(2D+a) = g(D) = (2D+a)/\alpha$ then, the curves $\Phi_{1/2}$, defined by ⁵²⁸ (13), and Γ , defined by (22), are identical. Consequently, the operating plane



Fig. 8 (a) The regions J_0 , J_1 J_2 and J_3 in the operating plane with f(S) = 4S/(5+S) and a = 0.3. The biogas flow rates corresponding to points $\eta_1 = (3, 0.7) \in J_1$, $\eta_2 = (3.45, 0.7) \in J_2$ and $\eta_3 = (5, 0.7) \in J_3$ are depicted in panels (b), (c) and (d) respectively. In these panels the curves are coloured and numbered as in Fig. 7, $r_0(S^{in}, D) = D/(f(S^{in}) - a)$, and $r_1(S^{in}, D)$ is defined by (20) (b) $r_0 \approx 0.58$. (c) $r_0 \approx 0.53$ and $r_1 \approx 0.87$. (d) $r_0 \approx 0.41$ and $r_1 \approx 0.54$.

⁵²⁹ (S^{in}, D) is divided in three regions J_i , i = 0, 1, 3 defined in (23) that describe ⁵³⁰ the behavior of the output substrate concentration and the biogas flow rate, ⁵³¹ see Figure 7(a).

Consider the operating points η_1 and η_3 , fixed respectively in regions J_1 532 and J_3 , as shown in Figure 7(a). The behavior of the biogas flow rate for 533 these operating points is depicted in Figure 7(b,c). It should be noticed that 534 for any other point $(S^{in}, D) \in J_1$, the curve representing the biogas flow rate 535 with respect to r should be similar to the curve shown in Figure 7(a), and 536 corresponding to $(S^{in}, D) = \eta_1$. Similarly, for any other point $(S^{in}, D) \in J_3$, 537 it should be similar to the curve shown in Figure 7(b), and corresponding to 538 $(S^{in}, D) = \eta_3.$ 539

In the linear case, the equation $S^{in} = g_r(D)$ is a second degree algebraic equation in r that gives two solutions, one corresponds to $r_1(S^{in}, D)$ defined by (20) and the other one is not considered as it does not belong to (0, 1).

Since the point $\eta_3 = (0.5, 0.6)$ satisfies the condition $S^{in} > g(D)$, as stated in item 2 of Proposition 5, the serial configuration has a higher biogas flow rate production than a single chemostat if and only if $r \in (r_1, 1)$, where $r_1(0.5, 0.6) \approx 0.5$, see Figure 7 (b).

547 5.2 Monod function

The Monod function is f(S) = mS/(K+S). As it is concave, according to item *ii* in Remark 1, the Monod function verifies Assumptions 2 and 3. Therefore, our results apply for Monod function.

Lemma 5 For any D > 0, the curve Γ, defined by (22), is at left of the curve $\Phi_{1/2}$, defined by (13).

⁵⁵³ Proof The curves $\Phi_{1/2}$ and Γ are respectively defined by equations $S^{in} = \lambda(2D+a)$ ⁵⁵⁴ and $S^{in} = g(D)$. Let the function $H : [0, (m-a)/2) \mapsto \mathbb{R}$ be defined by

$$H(D) = \lambda(2D+a) - g(D) = \frac{KmD^2}{(m-D-a)^2(m-a-2D)}.$$

Note that H(0) = 0 and, for any $D \in (0, (m-a)/2)$, one has H(D) > 0 i.e. $\lambda(2D + 1)$ 555 a) > g(D).556

Hence, the curve Γ is at left of the curve $\Phi_{1/2}$. 557

As a consequence of Lemma 5, the operating plane (S^{in}, D) is divided in 558 four regions J_i , i = 0, 1, 2, 3 defined in (23) that describe the behavior of the 559 output substrate concentration and the biogas flow rate, see Fig. 8(a). 560

Consider the operating points η_1 , η_2 and η_3 , fixed respectively in regions J_1 , 561 J_2 and J_3 , as shown in Fig. 8(a). The behavior of the biogas flow rate for these 562 points is depicted in Fig. 8(b,c,d). It should be noticed that for any other point 563 $(S^{in}, D) \in J_1$ (resp. $(S^{in}, D) \in J_2$ and $(S^{in}, D) \in J_3$), the curve representing 564 the biogas flow rate with respect to r should be similar to the curve shown 565 in Fig. 8(b) (resp. 8(c) and 8(d)), and corresponding to $(S^{in}, D) = \eta_1$ (resp. 566 $(S^{in}, D) = \eta_2$ and $(S^{in}, D) = \eta_3)$. 567

In the Monod case, the equation $S^{in} = g_r(D)$ is a second degree algebraic 568 equation in r that gives two solutions, one corresponds to $r_1(S^{in}, D)$ defined 569 by (20) and the other one is not considered as it does not belong to (0, 1). 570

Since the point η_2 (resp. η_3) satisfies the condition $S^{in} > g(D)$, as stated 571 in item 2 of Proposition 5, the serial configuration has a higher biogas flow 572 rate production than a single chemostat if and only if $r \in (r_1, 1)$, with 573 $r_1(3.45, 0.7) \approx 0.87$ in Fig.8(c) and $r_1(5, 0.7) \approx 0.54$ in Fig.8(c). 574

5.3 Hill function 575

The Hill function is $f(S) = mS^p/(K^p + S^p)$. Note that if p = 1 this function 576 reduces to the Monod function. For p > 1 it is non-concave. We have 577

$$\lambda(a) = \left(\frac{a}{m-a}\right)^{1/p} K.$$

Proposition 8 The Hill function satisfies the conditions (34) and (35). Therefore, 578 according to item iii in Remark 1, it verifies Assumption 2 and according to Lemma 579 3. it satisfies Assumption 3. 580

Proof Let us first prove that the Hill function satisfies the condition (35). Straight-581 forward computation give 582

$$\frac{d^2}{dS^2} \left(\frac{1}{f(S)-a}\right) = mpK^p \frac{(p+1)(m-a)S^{2p-2} + (p-1)aK^p S^{p-2}}{((m-a)S^p - aK^p)^3}$$

Therefore, $\frac{d^2}{dS^2}\left(\frac{1}{f(S)-a}\right) > 0$ for all $S > \lambda(a)$, that is to say, (35) is satisfied. This result can also be obtained without laborious calculations by using item *iii* of Remark 583 584 1. Let $\hat{S} \in (0, +\infty)$ be the inflexion point of the Hill function f. It is sufficient to 585 show that (1/f)'' > 0 for all $S \in (0, \hat{S})$. One easily see that 586



26 Performance study of two serial interconnected chemostats

Fig. 9 (a) The regions J_0 , J_1 J_2 , J_3 and J_4 in the operating plane with $f(S) = 4S^2/(25 + S^2)$ and a = 0.1. The curves Γ and $\Phi_{1/2}$ intersects for $D_1 = 0.69$ (see Lemma 6). (b,c) Zooms of (a) showing the region J_4 . The biogas flow rates corresponding to points $\eta_1 = (7, 1.6) \in J_1$, $\eta_2 = (9, 1.6) \in J_2$, $\eta_3 = (12, 1.6) \in J_3$ and $\eta_4 = (2.33, 0.3) \in J_4$ are depicted in panels (d) to (g), respectively. In these panels curves are coloured and numbered as in Fig. 7, $r_0(S^{in}, D) = D/(f(S^{in}) - a)$, and $r_1(S^{in}, D)$ is defined by (20). (d) $r_0 \approx 0.63$. (e) $r_0 \approx 0.54$ and $r_1 \approx 0.81$. (f) $r_0 \approx 0.48$ and $r_1 \approx 0.61$. (g) $r_0 \approx 0.49$.

$$\left(\frac{1}{f}\right)''(S) = \frac{p(p+1)K^p}{mS^{p+2}} > 0,$$

for any S > 0. Consequently, for all p > 1, the Hill function verifies Assumption 2. Let us now prove that the Hill function verifies the condition (34). Straightforward computations give

$$f'(\lambda(D+a)) = \frac{p}{Km}(D+a)^{\frac{p-1}{p}}(m-a-D)^{\frac{p+1}{p}}.$$
(44)

590 Therefore,

$$f'\left(\lambda\left(\frac{D}{r}+a\right)\right) = \frac{p}{Km}\left(\frac{D}{r}+a\right)^{\frac{p-1}{p}}\left(m-a-\frac{D}{r}\right)^{\frac{p+1}{p}}$$
Since $p > 1, D+ra < D+a$ and

0 < rm - ra - D < m - a - D,

one has 592

591

$$(D+ra)^{\frac{p-1}{p}} < (D+a)^{\frac{p-1}{p}}$$
(45)

$$(rm - ra - D)^{\frac{1}{p}} < (m - a - D)^{\frac{1}{p}}.$$
 (46)

From (45) one has 593

$$\left(\frac{D}{r}+a\right)^{\frac{p-1}{p}} = \left(\frac{1}{r}\right)^{\frac{p-1}{p}} \left(D+ra\right)^{\frac{p-1}{p}} < \left(\frac{1}{r}\right)^{\frac{p-1}{p}} \left(D+a\right)^{\frac{p-1}{p}}.$$
(47)

On the other hand, we have 594

$$\left(m-a-\frac{D}{r}\right)^{\frac{p+1}{p}} = \left(\frac{1}{r}\right)^{\frac{1}{p}} \left(m-a-\frac{D}{r}\right)A$$

where $A = (rm - ra - D)^{\frac{1}{p}}$. From (46), and using 595

$$0 < m - a - D/r < m - a - D,$$

we then deduce 596

$$\left(m - a - \frac{D}{r}\right)^{\frac{p+1}{p}} < \left(\frac{1}{r}\right)^{\frac{1}{p}} \left(m - a - D\right)^{\frac{p+1}{p}}.$$
(48)

Therefore, using (44), (47) and (48) one obtains 597

$$f'\left(\lambda\left(\frac{D}{r}+a\right)\right) = \frac{p}{Km}\left(\frac{D}{r}+a\right)^{\frac{p-1}{p}}\left(m-a-\frac{D}{r}\right)^{\frac{p+1}{p}} < \frac{p}{Km}\frac{1}{r}(D+a)^{\frac{p-1}{p}}(m-a-D)^{\frac{p+1}{p}} = \frac{1}{r}f'(\lambda(D+a)).$$

This ends the proof of (34). Consequently, according to Lemma 3, any Hill function 598 satisfies Assumption 3. 599

Let now consider the case p = 2 of the Hill function: $f(S) = mS^2/(K^2+S^2)$. 600

Lemma 6 Let $D_1 = (3m - 4a - \sqrt{m(5m - 4a)})/4$. If $0 < D < D_1$ then the curve 601 $\Phi_{1/2}$, defined by (13), at left of the curve Γ , defined by (22). In contrast, if $D_1 < 1$ 602 D < (m-a)/2 then the curve $\Phi_{1/2}$ is at right of the curve Γ . 603

Proof Let the function $H: [0, (m-a)/2) \mapsto \mathbb{R}$ be defined by $H(D) := \lambda(2D+a) - \lambda(2D+a)$ 604 q(D). We have 605

$$H(D) = K\left(\sqrt{\frac{2D+a}{m-a-D}} - \frac{(2D+a)(m-a-D)+(D+a)(m-a)}{2(m-a-D)^{3/2}\sqrt{D+a}}\right).$$

606 Straightforward computation shows that this function is positive if and only if the polynomial 607

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Fig. 10 (a) The map $r \mapsto \overline{G}(r)$ defined by (42), with f(S) = 4S/(5+S), a = 0.1 and $S^{in} = 1.5$, showing the values r^* and r^{max} . (b) The corresponding maps $D \mapsto G_{chem}(S^{in}, D)$, in black, $D \mapsto G_2(S^{in}, D, r^*)$, in blue and $D \mapsto G_2(S^{in}, D, r^{max})$, in red, show the values $D^* < D^{max}_{chem}$. (c) The biogas flow rates for a = 0, 0.1, 0.2, 0.3 showing the effects of mortality.

$$Q(D) := 4D^2 - 2(3m - 4a)D + 4a^2 - 5am + m^2$$

is negative. The solution of equation Q(D) = 0 are

$$D_1 = \frac{3m - 4a - \sqrt{\Delta}}{4}$$
 and $D_2 = \frac{3m - 4a + \sqrt{\Delta}}{4}$,

where $\Delta = 4m(5m-4a) > 0$, as a < m. Notice that we have $0 < D_1 < (m-a)/2$ and $(m-a)/2 < D_2$. Thus, for any $D \in (D_1, (m-a)/2)$, we have H(D) > 0 and then the curve $\Phi_{1/2}$ at right of the curve Γ .

As a consequence of Lemma 6, the operating plane is divided in five regions $J_i i = 0, 1, 2, 3, 4$ defined in (23), see Figure 9(a,b,c).

Consider the operating points η_1 , η_2 , η_3 and η_4 fixed respectively in regions J_1 , J_2 , J_3 and J_4 , as shown in Figure 9(a,b,c). It should be noticed that for any other point $(S^{in}, D) \in J_1$ (resp. $(S^{in}, D) \in J_2$, $(S^{in}, D) \in J_3$ and $(S^{in}, D) \in J_4$), the curve representing the biogas flow rate with respect to r should be similar to the curve shown in Fig. 9(a) (resp. (b), (c) and (d)), and corresponding to $(S^{in}, D) = \eta_1$ (resp. $(S^{in}, D) = \eta_2$, $(S^{in}, D) = \eta_3$ and $(S^{in}, D) = \eta_4$).

Recall that $r_1(S^{in}, D)$ is defined by (20). It is obtained by solving numerically the equation $S^{in} = g_r(D)$. Since the point η_2 (resp. η_3) satisfies the condition $S^{in} > g(D)$, as stated in item 2 of Proposition 5, the serial configuration has a higher biogas flow rate production than a single chemostat if and only if $r \in (r_1, 1)$, with $r_1(9, 1.6) \approx 0.81$ in Fig. 9(e) and $r_1(12, 1.6) \approx 0.61$, in Fig. 9(f).

5.4 The serial configuration is worth considering when mortality is not negligible

⁶²⁹ In this section we numerically illustrate Remark 2. We fix S^{in} and we adopt ⁶³⁰ the following notations.

$$D_{chem}^{max} = \overline{D}(1), \quad G_{chem}^{max} = \overline{G}(1) = G_{chem}\left(S^{in}, D_{chem}^{max}\right)$$

where $\overline{G}(r)$ is defined by (42) and $\overline{D}(r)$ is as in Lemma 4. Recall that $r^* \in (0, 1)$ satisfies

$$\overline{G}(r^*) = \overline{G}(1) = G_{chem}^{max},\tag{49}$$

and $\overline{G}(r) > \overline{G}(1)$ for $r \in (r^*, 1)$, so that $\overline{G}(r)$ attains its maximum for $r = r^{max} \in (r^*, 1)$, see Fig. 10(a), obtained with a Monod function and $S^{in} = 1.5$. We adopt the following notations.

$$D^{max} = \overline{D}(r^{max}), \ G^{max} = G_2\left(S^{in}, D^{max}, r^{max}\right)$$
$$D^* = \overline{D}(r^*), \qquad G^* = G_2\left(S^{in}, D^*, r^*\right) = G^{max}_{chem}$$

	a = 0	a = 0.1	a = 0.2	a = 0.3
D_{chem}^{max}	0.4918	0.4359	0.3806	0.3259
$G^* = G^{max}_{chem}$	0.3930	0.3167	0.2478	0.1866
r^*	1	0.839	0.717	0.631
D^*	0.4918	0.3758	0.2969	0.2369
r^{max}	1	0.889	0.808	0.751
D^{max}	0.4918	0.3925	0.3190	0.2591
G^{max}	0.3930	0.3169	0.2490	0.1890
$\frac{G^{max}-G^{max}_{chem}}{G^{max}_{chem}}$	0	0.06%	0.5%	1.3%
$\frac{\frac{D_{chem}^{max} - D^{max}}{D_{chem}^{max}}$	0	10%	16.2%	20.5%
$\frac{\frac{D_{chem}^{max} - D^*}{D_{chem}^{max}}}{D_{chem}^{max}}$	0	13.6%	22%	27.3%

These notations are illustrated in Figs. 10(a,b). The zoom in Fig. 10(b) shows that G^{max} exceeds $G^* = G^{max}_{chem}$ only slightly, but D^* is significantly smaller than D^{max} , which is itself smaller than D^{max}_{chem} . We give in Table 1 the numerical values of r^* , r^{max} , D^* , D^{max} , G^{max} and $G^* = G^{max}_{chem}$, for various values of the mortality rate a. The table also gives the relative gains

$$\frac{G^{max}-G^{max}_{chem}}{G^{max}_{chem}}, \quad \frac{D^{max}_{chem}-D^{max}}{D^{max}_{chem}}, \quad \frac{D^{max}_{chem}-D^*}{D^{max}_{chem}},$$

when replacing the single chemostat with the serial device using the ratios r^* and r^{max} . The gain in biogas production is almost negligible, but the gain in bioreactor flow rate is significant.

The biogas flow rates $G_{chem}(S^{in}, D)$, $G_2(S^{in}, D, r^*)$ and $G_2(S^{in}, D, r^{max})$, for the various considered values of the mortality rate a, are depicted in Fig. 10(c), in black, blue and red, respectively. This figure shows that mortality is a real problem as it considerably reduces biogas production. Where mortality cannot be avoided or reduced, instead of using the single chemostat, by using a serial device, biogas production can be slightly improved while significantly reducing the bioreactor flow rate.

651 6 Conclusion

In this work, an in-depth study is carried out on the mathematical model of 652 two interconnected chemostats in serial with mortality. Equations contain a 653 term representing the mortality rate of the species. Due to this added term 654 characterizing the mathematical model, this paper is considered as an exten-655 sion of the work done in [7], where the model does not consider the mortality 656 rate. However, the mathematical analysis revealed that the proofs have had to 657 be significantly revisited and reveal several new non intuitive differences com-658 pared to the case without mortality. Let us recall that without mortality, the 659 dynamics admits a forward attractive invariant hyperplane related to the total 660 mass conservation, which is no longer verified under mortality consideration. 661 This at the core of the differences in the mathematical analysis. The study 662 of the model is based on the analysis of the asymptotic behavior of its solu-663 tions, and is supported by an operating diagram which describes the number 664 and stability of steady states. In a first step, we considered different mortality 665 rates a_1, a_2 in each tank. Then, in view of comparing with the single config-666 uration, we considered identical mortality rate $a = a_1 = a_2$. We analyzed the 667 performances of the model at steady state for two different criteria: the out-668 put substrate concentration and the biogas flow rate (and compared them for 669 the single chemostat with the same mortality rate a). Explicit expressions of 670 criteria, depending on the dilution rate D and the input substrate concentra-671 tion S^{in} , are provided. These new results provide conditions that insure the 672 existence of a serial configuration more efficient than a single chemostat, in 673 the sense of minimizing the output substrate concentration or maximizing the 674 biogas flow rate. 675

Along the paper, the similarities, specificities and differences of our model 676 compared to the model without mortality (i.e. for a = 0) studied in [7] are 677 highlighted. Among the differences that attract attention, on the one hand, 678 we have the operating diagram with different mortality which presents many 679 more cases than the diagram without mortality where it is reduced to only two 680 cases. Thus, the presence of the four regions of stability on the same diagram 681 is now possible. On the other hand, we have the biogas production of the 682 serial device in its maximum state which can be significantly larger than the 683 largest biogas production of the single chemostat. This never happens in the 684 case without mortality. Finally, unlike the case without mortality, the biomass 685 productivity and the biogas flow rate at steady state are not given by the 686 same formulas. Therefore, if biomass productivity is taken into account as a 687 performance criterion, the comparison between the serial chemostat and the 688 single chemostat does not lead to the same conclusions. For more details on 689 this issue the reader can refer to [8]. 690

⁶⁹¹ Appendix A The single chemostat

⁶⁹² In this section, we give a brief presentation of the mathematical model of the ⁶⁹³ single chemostat with mortality rate. The mathematical equations are given by



Fig. A1 (a) The map $D \mapsto S^{out}(S^{in}, D)$ is increasing on $[0, \delta]$, where $\delta = f(S^{in}) - a$. (b) The map $D \mapsto x^{out}(S^{in}, D)$ with f(S) = 4S/(5+S), $S^{in} = 10$ and a = 0.6. (c) The curve Γ in the operating plane (S^{in}, D) of the single chemostat.

$$\dot{S} = D(S^{in} - S) - f(S)x,$$

$$\dot{x} = -Dx + f(S)x - ax,$$
(A1)

where S and x denote respectively the substrate and the biomass concentra-694 tion, S^{in} the input substrate concentration, a the mortality rate and D = Q/V695 the dilution rate, with Q the input flow rate and V the volume of the tank. 696 The specific growth rate f of the microorganisms satisfies Assumption 1. It is 697 well known (see [16, 39]) that, besides the washout $F_0 = (S^{in}, 0)$, this system 698 can have a positive steady state 699

$$F_1 = (S^*(D), x^*(S^{in}, D))$$

where 700

$$S^* = \lambda(D+a)$$
 and $x^* = \frac{D}{D+a}(S^{in} - \lambda(D+a)).$

See Fig. A1(a) for the plot of the function $D \mapsto S^*(D)$ and Fig. A1(b) for the 701 plot of the function $D \mapsto x^*(S^{in}, D)$ for $0 < D < \delta$, where $\delta = f(S^{in}) - a$. 702

The washout steady state F_0 always exists. It is GAS if and only if $D \ge \delta$. 703 It is LES if and only if $D > \delta$. The positive steady state F_1 exists if and only if 704 $D < \delta$. It is GAS and LES whenever it exists. Therefore, the curve Φ defined 705 by 706

$$\Phi := \{ (S^{in}, D) : D = f(S^{in}) - a \}$$
(A2)

splits the set of operating parameters (S^{in}, D) into two regions, denoted I_0 707 and I_1 , as depicted in A1(c). These regions are defined by 708

$$I_0 := \{ (S^{in}, D) : D \ge f(S^{in}) - a \}, I_1 := \{ (S^{in}, D) : D < f(S^{in}) - a \}.$$
(A3)

The behavior of the system in each region is given in Table A1. Figure A1(c), 709 together with A1 is called the operating diagram of the single chemostat. 710

The particularity of this operating diagram is that the curve limiting both 711 regions I_0 and I_1 is translated from zero, unlike the case with mortality, as 712 shown in Figure 2.5 of [16]. Thus, with presence of mortality rate, the region 713 where the washout is GAS, is larger. 714

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Table A1 Stability of steady states in the various regions of the operating diagram.

	I_0	I_1
F_0	GAS	U
F_1		GAS

The output substrate concentration of the single chemostat, at its stable steady state is given by

$$S^{out}(S^{in}, D) = \begin{cases} S^{in} & \text{if } D \ge \delta\\ \lambda (D+a) & \text{if } D < \delta. \end{cases}$$
(A4)

717 Its output biomass concentration at steady state is then given by

$$x^{out}(S^{in}, D) = \frac{D}{D+a}(S^{in} - S^{out}(D, a))$$
(A5)

⁷¹⁸ For all $S^{in} > \lambda(a)$, one has

$$\frac{\partial S^{out}}{\partial D}(S^{in},D) = \begin{cases} 0 & \text{if } D > \delta \\ \lambda'(D+a) & \text{if } D < \delta, \end{cases}$$

Thus, for any growth function satisfying Assumption 1 the function $D \mapsto S^{out}(S^{in}, D)$ is increasing on $[0, \delta]$, as shown in Figure A1(a). The function $D \mapsto x^{out}(S^{in}, D)$ is illustrated in Figure A1(b) for a Monod function.

The biogas flow rate of the single chemostat is defined, up to a multiplicative yield coefficient, by

$$G_{chem}(S^{in}, D) := V x^{out} f(S^{out}).$$
(A6)

Using the expressions (A4) and (A5) respectively of S^{out} and x^{out} , the biogas flow rate of the single chemostat is given by:

$$G_{chem}(S^{in}, D) = \begin{cases} 0 & \text{if } D \ge \delta\\ VD(S^{in} - \lambda(D+a)) & \text{if } D < \delta. \end{cases}$$
(A7)

For a given $S^{in} > \lambda(a)$, the function $D \mapsto G_{chem}(S^{in}, D)$ is null for D = 0 or $D \ge \delta$, and is positive for $D \in (0, \delta)$. Therefore it admits a maximum in $(0, \delta)$, which is assumed to be unique. A characterization of the growth functions for which this uniqueness is satisfied can be found in [31].

Proposition 9 Assume that for any $S^{in} > \lambda(a)$, the maximum of $D \mapsto G_{chem}(S^{in}, D)$ is unique, and define $\overline{D}(S^{in}) \in (0, \delta)$, such that

$$G_{chem}\left(S^{in}, \overline{D}\left(S^{in}\right)\right) = \max_{D \ge 0} G_{chem}\left(S^{in}, D\right)$$

Then, the dilution rate $D = \overline{D}(S^{in})$ is the solution of the equation $S^{in} = g(D)$, where the function $g: [0, m-a) \mapsto \mathbb{R}$ is given by

$$g(D) := \lambda(D+a) + D\lambda'(D+a)).$$
(A8)

734

⁷³⁵ Proof For any $S^{in} > \lambda(a)$ and $D \in (0, \delta)$, we have

$$\frac{\partial G_{chem}}{\partial D}(S^{in}, D) = V\left(S^{in} - \lambda(D+a) - D\lambda'(D+a)\right) \tag{A9}$$

Therefore, $\frac{\partial G_{chem}}{\partial D}(S^{in}, D) = 0$ if and only if $S^{in} = g(D)$, where g is defined by (A8).

Notice that the function q defined by (A8) is the same as the function 738 g, defined by (19), which was obtained as the limit, when r tends to 1, to 739 the function g_r , defined by (9). Recall that Γ is the curve of equation $S^{in} =$ 740 q(D), see (22). This curve is depicted in Fig. A1(c). It is the set of operating 741 conditions given the higher biogas of the single chemostat. More precisely, for 742 any $S^{in} > \lambda(a)$, the maximum $D = \overline{D}(S^{in})$ of the biogas satisfies the condition 743 $(S^{in}, D) \in \Gamma$. Therefore, a sufficient condition for the uniqueness of $\overline{D}(S^{in})$ is 744 that the mapping g is increasing. If, in addition, f is \mathcal{C}^2 , then, deriving (A9) 745 with respect of D, we have 746

$$\frac{\partial^2 G_{chem}}{\partial D^2}(S^{in}, D) = -Vg'(D).$$

Hence, a sufficient condition for Assumption 4 to be satisfied is that g'(D) > 0 for $D \in [0, m - a)$. This last condition if satisfied whenever $f'' \leq 0$ on $(\lambda(a), +\infty)$, or $(\frac{1}{f-a})'' > 0$ on $(\lambda(a), +\infty)$, see Lemma 1 in [31]. Therefore we can make the following remark.

Remark 3 Linear and Monod growth functions satisfy Assumption 4, since they satisfy $f'' \leq 0$ on $(0, +\infty)$. On the other hand the Hill function satisfy Assumption 4, since it satisfies $\left(\frac{1}{f-a}\right)'' > 0$ on $(\lambda(a), +\infty)$, as shown in Proposition 8.

⁷⁵⁴ Appendix B The serial configuration

We consider a slight extension of system (1) with different mortality rates in the two tanks. Indeed, we assume that the growth environment differs from one tank to another one. This can lead to two different mortality rates in the tanks. We denote by a_1 and a_2 the mortality rates. The mathematical model is given by the following equations.

$$\dot{S}_{1} = \frac{D}{r}(S^{in} - S_{1}) - f(S_{1})x_{1}$$

$$\dot{x}_{1} = -\frac{D}{r}x_{1} + f(S_{1})x_{1} - a_{1}x_{1}$$

$$\dot{S}_{2} = \frac{D}{1-r}(S_{1} - S_{2}) - f(S_{2})x_{2}$$

$$\dot{x}_{2} = \frac{D}{1-r}(x_{1} - x_{2}) + f(S_{2})x_{2} - a_{2}x_{2}.$$
(B10)

The following result is classical in the mathematical theory of the chemoresult is classical in the mathematical theory of the chemo-

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TE2 Lemma 7 For any nonnegative initial condition, the solution of system (B10) TE3 $(S_1(t), x_1(t), S_2(t), x_2(t))$ is nonnegative for any t > 0 and positively bounded.

Proof Since the vector field defined by (B10) is C^1 , the uniqueness of the solution to an initial value problem holds. From (B10) and using f(0) = 0, we have:

$$\begin{array}{ll} \text{for } i=1,2, \quad S_i=0 \Longrightarrow \dot{S}_i > 0, \\ x_1=0 \Longrightarrow \dot{x}_1=0 \\ x_1 \ge 0 \text{ and } x_2=0 \Longrightarrow \dot{x}_2 \ge 0 \end{array}$$

Therefore, for i = 1, 2, $S_i(t) \ge 0$ and $x_i(t) \ge 0$, for all $t \ge 0$, for which they are defined, provided $S_i(0) \ge 0$ and $x_i(0) \ge 0$, for i = 1, 2, see Prop. B.7 in [39]. This proves that the solutions of nonnegative initial conditions are always nonnegative. Let $z_i = S_i + x_i$, i = 1, 2. From system (B10), we have

$$\dot{z_1} = \frac{D}{r}(S^{in} - z_1) - a_1x_1, \quad \dot{z_2} = \frac{D}{1-r}(z_1 - z_2) - a_2x_2.$$

770 Consequently, we have the differential inequality

$$\dot{z_1} \le \frac{D}{r}(S^{in} - z_1)$$

171 It follows by comparison of solutions of ordinary differential equations (see for172 instance [48]) that one has

$$z_1(t) \le S^{in} + (z_1(0) - S^{in})e^{-\frac{D}{r}t}$$

TT3 Therefore, $z_1(t) \leq Z_1$, where $Z_1 = \max(S^{in}, z_1(0))$. Then, we also have the differential inequality

$$\dot{z_2} \le \frac{D}{1-r}(Z_1 - z_2)$$

It follows again by comparison of solutions of ordinary differential equations that onehas also

$$z_2(t) \le Z_1 + (z_2(0) - Z_1)e^{-\frac{D}{1-r}t}$$

Therefore, $z_2(t) \leq Z_2$, where $Z_2 = \max(Z_1, z_2(0))$. Hence, the solutions of (B10) are positively bounded. Therefore, they are defined for all $t \geq 0$.

For the description of the steady states, we shall consider the following function h that will play a key role

$$h(S_2) = \frac{D + (1-r)a_2}{1-r} \frac{S_1^* - S_2}{b - S_2}, \quad S_2 \in (0, b)$$

where $S_1^* = \lambda \left(\frac{D}{r} + a_1\right), \ b = \frac{D(S^{in} - S_1^*)}{D + ra_1} + S_1^*.$ (B11)

⁷⁸¹ This function satisfies the following property.

Lemma 8 Assume that $D/r + a_1 < f(S^{in})$. The function h is decreasing from h(0) > 0 to $h(S_1^*) = 0$, where h(0) is given by

$$h(0) = \frac{D + (1 - r)a_2}{1 - r} \frac{(D + ra_1)S_1^*}{DS^{in} + ra_1S_1^*}.$$
 (B12)

Proof From the condition $D/r + a_1 < f(S^{in})$ it is deduced that $S_1^* < S^{in}$. Note that 784

$$b = \frac{DS^{in} + ra_1S_1^*}{D + ra_1}.$$

Hence, b is a convex combination of S^{in} and S_1^* , and we have $S_1^* < b < S^{in}$. 785 Therefore, the vertical asymptote $S_2 = b$ of h is at right of S_1^* . The derivative of h is 786

$$h'(S_2) = \frac{D + (1 - r)a_2}{1 - r} \frac{S_1^* - b}{(b - S_2)^2}.$$

Hence, we have $h'(S_2) < 0$ for all $S_2 < b$. Therefore, h is defined on the interval 787 $(0, S_1^*)$ and is decreasing from h(0), given by (B12) to $h(S_1^*) = 0$. 788

Therefore, if $D/r + a_1 < f(S^{in})$, equation $f(S_2) = h(S_2)$ admits a unique 789 solution, denoted by $S_2^*(S^{in}, D, r)$, as shown in Fig. B2(a). This solution satisfy 790 the following property. 791

Lemma 9 Considering $a_1 = a_2 = a$, for all $0 \le D < f(S^{in}) - a$, one has 792

$$\lim_{r \to 1} S_2^*(S^{in}, D, r) = \lambda(D+a).$$

793

Proof Let $0 \le D < f(S^{in}) - a$. Using (5), the condition $h(S_2) = f(S_2)$ is equivalent 794 $_{\mathrm{to}}$ 795

$$(D + (1 - r)a)(S_1^* - S_2^*) = (1 - r)\left(\frac{D}{D + ra}(S^{in} - S_1^*) + S_1^* - S_2^*\right)f(S_2^*).$$
(B13)

For r = 1, we have $S_1^* = \lambda(D + a)$. As $\lim_{r \to 1} f(S_2^*) < +\infty$ then, (B13) gives 796

$$D(\lambda(D+a) - \lim_{r \to 1} S_2^*(S^{in}, D, r)) = 0.$$

Consequently, one has $\lim_{r\to 1} S_2^*(S^{in}, D, r) = \lambda(D+a).$ 797



Fig. B2 (a) Existence and uniqueness of the solution S_2^* of equation $f(S_2) = h(S_2)$. (b) Graphical illustration of Proposition 10: S_2^* decreases when S^{in} increases.

The existence and stability of steady states of (B10) are given by the 798 following result. 799

- **Theorem 3** Assume that Assumption 1 is satisfied. The steady states of (B10) are:
 - The washout steady state $E_0 = (S^{in}, 0, S^{in}, 0)$ which always exists. It is GAS if and only if

$$D \ge \max\{r(f(S^{in}) - a_1), (1 - r)(f(S^{in}) - a_2)\}.$$
 (B14)

It is LES if and only if

$$D > \max\{r(f(S^{in}) - a_1), (1 - r)(f(S^{in}) - a_2)\}$$

• The steady state $E_1 = (S^{in}, 0, \overline{S}_2, \overline{x}_2)$ of washout in the first chemostat but not in the second one with

$$\overline{S}_2 = \lambda \left(\frac{D}{1-r} + a_2 \right), \ \overline{x}_2 = \frac{D}{D + (1-r)a_2} \left(S^{in} - \overline{S}_2 \right).$$
(B15)

It exists if and only if $D < (1-r)(f(S^{in}) - a_2)$. It is GAS if and only if

$$r(f(S^{in}) - a_1) \le D \text{ and } D < (1 - r)(f(S^{in}) - a_2).$$
 (B16)

It is LES if and only if

$$r(f(S^{in}) - a_1) < D < (1 - r)(f(S^{in}) - a_2).$$

• The steady state $E_2 = (S_1^*, x_1^*, S_2^*, x_2^*)$ of persistence of the species in both chemostats with

$$S_1^* = \lambda \left(\frac{D}{r} + a_1\right), \quad x_1^* = \frac{D}{D + ra_1} (S^{in} - S_1^*),$$
 (B17)

$$x_2^* = \frac{D}{D + (1 - r)a_2} \left(\frac{D}{D + ra_1} (S^{in} - S_1^*) + S_1^* - S_2^* \right)$$
(B18)

and $S_2^* = S_2^*(S^{in}, D, r)$ is the unique solution of the equation $h(S_2) = f(S_2)$ with h defined by (B11). This steady state exists and is positive if and only if $D < r(f(S^{in}) - a_1)$. It is GAS and LES whenever it exists and is positive.

Proof The 4-dimensional system of ODEs (B10) has a cascade structure of two planar systems of ODEs, whose mathematical analysis is easy and well known in the mathematical theory of the chemostat [16, 39]. Using this cascade structure, the global behavior of the system is deduced from the global behaviour of planar systems and Thieme's theory of asymptotically autonomous systems.

For the convenience of the reader the details of the proof are given in Appendix D.1.

Proposition 10 The function $S^{in} \mapsto S_2^*(S^{in}, D, r)$ is decreasing.

Proof D and r are fixed. Let $S^{in,1} > S^{in,2}$ and h_i defined by (B11), with $S^{in} = S^{in,i}$, i = 1, 2. Let S_2^{*i} , the solution of equation $f(S_2) = h_i(S_2)$, i = 1, 2. Using Lemma 8, h_i is a decreasing hyperbola from $h_i(0)$ defined by (B12), with $S^{in} = S^{in,i}$, to $h_i(S_1^*) = 0$. Since $h_1(0) < h_2(0)$, we have $h_1(S_2) < h_2(S_2)$ for all $S_2 \in (0, S_1^*)$. Therefore, $S_2^{*1} < S_2^{*2}$, see Fig. B2(b).

This result means that the effluent steady state concentration of substrate decreases when the influent concentration of substrate increases. This behavior is very different from the single chemostat, where the effluent steady state substrate concentration is independent of the influent substrate concentration.

⁸²¹ Appendix C Operating diagram

For the chemostat model, the operating diagram has as coordinates the input 822 substrate concentration S^{in} and the dilution rate D, and shows how the solu-823 tions of the system behave for different values of these two parameters. The 824 regions constituting the operating diagram correspond to different qualitative 825 asymptotic behaviors. Indeed, the main interest of an operating diagram is 826 to highlight the number and stability of the steady states for a given pair of 827 parameters (S^{in}, D) . The input substrate concentration S^{in} and the dilution 828 rate D are the usual parameters manipulated by the experimenter of a chemo-829 stat. Apart from these parameters, and the parameter r that can be also chosen 830 by the experimenter but not easily changed as S^{in} and D, all other parame-831 ters have biological meaning and are fitted using experimental data from real 832 measurements of concentrations of micro-organisms and substrates. Therefore 833 the operating diagram is a bifurcation diagram, quite useful to understand the 834 possible behaviors of the solutions of the system from both the mathematical 835 and biological points of view. 836

Here, we fix $r \in (0,1)$ and we depict in the plane (S^{in}, D) the regions in which the solution of system (B10) globally converges towards one of the steady state E_0 , E_1 or E_2 . From the results given in Theorem 3, it is seen that these regions are delimited by the curves Φ_1^r and Φ_{1-r}^2 defined by:

$$\Phi_r^1 := \left\{ (S^{in}, D) \in \mathbb{R}^2_+ : D = r(f(S^{in}) - a_1) \right\},\tag{C19}$$

$$\Phi_{1-r}^2 := \left\{ (S^{in}, D) \in \mathbb{R}^2_+ : D = (1-r)(f(S^{in}) - a_2) \right\}.$$
 (C20)

When $a_1 = a_2 = 0$, as we have shown in [7], these curves meet only at one 841 point (the origin) and merge when r = 1/2. Therefore, in this case the curves 842 Φ_r^1 and Φ_{1-r}^2 separate the operating plane (S^{in}, D) , in only three regions, see 843 [7, Figure 5]. This property continue to hold when $a_1 = a_2$, that is to say, 844 the curves intersect only at $(\lambda(a_1), 0)$ and merge when r = 1/2. In this case 845 the curves Φ_r^1 and Φ_{1-r}^2 separate the operating plane (S^{in}, D) , in only three 846 regions, see Figure B3 (c) and (d). The novelty when a_1 and a_2 are different 847 and non null, is that the intersection of the curves Φ_r^1 and Φ_{1-r}^2 can lie outside 848 the S^{in} axis. Therefore there can be four regions in the operating plane, as 849 depicted in Figure B3 (a) and (f). For the description of the intersection of 850



Fig. B3 The operating diagram of (B10). The asymptotic behaviour in each region is depicted in Table C2.

the curves Φ_r^1 and Φ_{1-r}^2 , we need some definitions and notations. Let $\overline{r} \in (0, 1)$ be defined by

$$\overline{r} := \frac{m-a_2}{2m-a_1-a_2}.\tag{C21}$$

Note that if $a_1 < a_2$ then $\overline{r} < 1/2$, and if $a_1 > a_2$ then $\overline{r} > 1/2$. For $a_1 < a_2$ and $0 < r < \overline{r}$ (or $a_1 > a_2$ and $\overline{r} < r < 1$), we define the point $P = (S_P^{in}, D_P)$ of the operating plane by:

Table C2 The regions $I_k(r)$, k = 0, 1, 2, 3 of the operating diagram of (B10) and asymptotic behaviour in these various regions.

Regions									
$I_0(r) = \left\{ (S^{in}, D) : \max\{r(f(S^{in}) - a_1), (1 - r)(f(S^{in}) - a_2)\} \le D \right\}$									
$I_1(r) = \left\{ (S^{in}, D) : r(f(S^{in}) - a_1) \le D \text{ and } D < (1 - r)(f(S^{in}) - a_2) \right\},\$									
$I_2(r) = \{ (S^{in}, D) : 0 < D < \min\{r(f(S^{in}) - a_1), (1 - r)(f(S^{in}) - a_2)\} \},\$									
$I_3(r) = \{ (S^{in}, D) : (1 - r)(f(S^{in}) - a_2) \le D \text{ and } D < r(f(S^{in}) - a_1) \}.$									
		$I_0(r)$	$I_1(r)$	$I_2(r)$	$I_3(r)$				
	E_0	GAS	U	U	U				
	E_1		GAS	U					

$$S_P^{in} := \lambda \left(\frac{ra_1 - (1 - r)a_2}{2r - 1} \right), \quad D_P := \frac{r(1 - r)(a_2 - a_1)}{1 - 2r}.$$
 (C22)

GAS

GAS

Note that $S_P^{in} > 0$ and $D_P > 0$. With these notations we can state the following 856 result: 857

 E_1 E_2

Proposition 11 1. If $a_1 < a_2$ then for all $r \in (0, \overline{r})$, the curves Φ_r^1 and Φ_{1-r}^2 858 intersect at the point P and Φ_r^1 is strictly below [resp. above] Φ_{1-r}^2 for 859 $S^{in} > S^{in}_{P}$ [resp. $S^{in} < S^{in}_{P}$], see Figure B3 (a). For all $r \in (\overline{r}, 1)$, Φ^{1}_{r} is 860 strictly above Φ_{1-r}^2 , see Figure B3 (b). 861

2. If $a_1 > a_2$ then for all $r \in (\overline{r}, 1)$, the curves Φ^1_r and Φ^2_{1-r} intersect at the 862 point P and Φ_r^1 is strictly above [resp. below] Φ_{1-r}^2 for $S^{in} > S_P^{in}$ [resp. $S^{in} < S_P^{in}$], see Figure B3 (f). For all $r \in (0, \overline{r}), \Phi_r^1$ is below Φ_{1-r}^2 , see 863 864 Figure B3 (e). 865

3. If $a_1 = a_2$ then, for r = 1/2, $\Phi_r^1 = \Phi_{1-r}^2$. Moreover, if r < 1/2 then Φ_r^1 is 866 strictly below Φ_{1-r}^2 , see Figure B3 (c) and, if r > 1/2 then Φ_r^1 is strictly 867 above Φ_{1-r}^2 , see Figure B3 (d). 868

Proof For 0 < r < 1 and $S^{in} > \lambda(a_i)$ we define the function φ_i , i = 1, 2, by 869

$$\varphi_1(S^{in}, r) = r(f(S^{in}) - a_1),
\varphi_2(S^{in}, r) = (1 - r)(f(S^{in}) - a_2).$$
(C23)

The curves Φ_r^1 and Φ_{1-r}^2 , defined respectively by (C19) and (C20), intersect if and 870 only if there exists $r \in (0,1)$ and $S^{in} > \max(\lambda(a_1), \lambda(a_2))$ such that $\varphi_1(S^{in}, r) =$ 871 $\varphi_2(S^{in}, r)$, that is to say 872

$$f(S^{in}) = A(r), \quad \text{with} \quad A(r) := \frac{ra_1 - (1-r)a_2}{2r-1}.$$
 (C24)

This equation has a solution $S^{in} > \max(\lambda(a_1), \lambda(a_2))$ if and only if 873

$$\max\left(a_1, a_2\right) < A(r) < m,\tag{C25}$$

where $m = \sup(f)$, as in (2). When these conditions are satisfied, the solution of (C24) is given by $S^{in} = \lambda(A(r))$, where λ is the inverse function pf f, i.e. the break-even concentration defined by (3). Hence, $S^{in} = S_P^{in}$, given in (C22). The corresponding intersection point of Φ_1^1 and Φ_{1-r}^2 is given by $D_P = r\left(f(S_P^{in}) - a_1\right)$, which is the value given in (C22).

Let us determine now for which value of r, the conditions (C25) are satisfied. The function A is a homographic function. Its graphical representation is a hyperbola, whose vertical asymptote is r = 1/2. Its derivative is given by

$$A'(r) = \frac{a_2 - a_1}{(2r - 1)^2}.$$
 (C26)

Note that A(r) = m if and only if $r = \overline{r}$, where \overline{r} is defined by (C21). Therefore if $a_1 < a_2$ then, according to (C26), A is increasing. Since $A(0) = a_2$, $A(\overline{r}) = m$, and $\overline{r} < 1/2$, the condition (C25) is satisfied if and only if $0 < r < \overline{r}$. Similarly, if $a_1 > a_2$, then, according to (C26), A is decreasing. Since $A(1) = a_1$, $A(\overline{r}) = m$ and $\overline{r} > 1/2$, the condition (C25) is satisfied if and only if $\overline{r} < r < 1$. Finally, if $a_1 = a_2$ then $A(r) = a_1$ and the condition (C25) cannot be satisfied.

Suppose that $a_1 < a_2$. Note that for 0 < r < 1/2, the condition $f(S^{in}) > A(r)$ (resp. $f(S^{in}) < A(r)$) is equivalent to $\varphi_1(S^{in}, r) < \varphi_2(S^{in}, r)$ [resp. $\varphi_1(S^{in}, r) > \varphi_2(S^{in}, r)$]. Thus:

- If $r \in (0, \overline{r})$, then $f(S^{in}) < A(r)$ if and only if $S^{in} < S_P^{in}$, where S_P^{in} is defined by (C22). Hence, the curves Φ_r^1 and Φ_{1-r}^2 intersect at $P = (S_P^{in}, D_P)$ and the curve Φ_r^1 is strictly below [resp. above] the curve Φ_{1-r}^2 , for all $S^{in} > S_P^{in}$ [resp. $S^{in} < S_P^{in}$].
- If $r \in [\overline{r}, 1/2)$ then $f(S^{in}) < A(r)$ for all $S^{in} > 0$, so that the curve Φ_r^1 is strictly above the curve Φ_{1-r}^2 .
- If $r \in [1/2, 1)$, then, using $r \ge 1 r$ and $a_1 < a_2$, one has $\varphi_1(S^{in}, r) > \varphi_2(S^{in}, r)$. Therefore, the curve Φ_r^1 is strictly above the curve Φ_{1-r}^2 .

If $a_1 > a_2$, the proof is similar to the case $a_1 < a_2$.

If $a_1 = a_2$ then $\varphi_1(S^{in}, r) = \varphi_2(S^{in}, r)$ is equivalent to $r(f(S^{in}) - a_1) = (1 - r)(f(S^{in}) - a_1)$. Therefore, r = 1 - r, that is r = 1/2. In this case the curves Φ_r^1 and Φ_{1-r}^2 merge. In addition, if r < 1/2 [resp. r > 1/2] then r < 1 - r [resp. r > 1 - r] and the curve Φ_r^1 is strictly below [resp. above] the curve Φ_{1-r}^2 . This ends the proof of the proposition.

For any $r \in (0, 1)$, the curves Φ_r^1 and Φ_{1-r}^2 , defined by (C19) and (C20), respectively split the plane (S^{in}, D) in the regions denoted $I_0(r)$, $I_1(r)$, $I_2(r)$ and $I_3(r)$ and defined in Table C2. These regions are depicted in Fig. B3 in the cases $a_1 < a_2$, $a_1 = a_2$ and $a_1 > a_2$.

The behavior of the system in each region, when it is not empty, is given in Table C2. Notice that E_1 exists in both regions $I_1(r)$ and $I_2(r)$, but is stable only when (S^{in}, D) is fixed in $I_1(r)$.

When $a_1 = a_2 = 0$ then $\lambda(a_1) = \lambda(a_2) = 0$ and the curves Φ_1^r and Φ_{1-r}^2 of the operating diagram start from the origin of the plane (S^{in}, D) and merge for r = 1/2. Therefore, the diagrams shown in panels (a), (b), (c), (d), (e) and (f) of Fig. B3 are reduced to only two different cases characterized by 0 < r < 1/2 and 1/2 < r < 1, as shown in Figure 5 of [7]. There is no changes

in the stability of the steady states and in the number of the regions depicted 917 in the operating diagram. 918

This result reveals an interplay between spatial heterogeneity (the ratio r of 919 volume distribution between tanks) and the mortality heterogeneity (difference 920 between a_1 and a_2). Indeed, panels (a) and (f) of Fig. B3 bring a particular 921 feature when mortality rates are different: domains $I_1(r)$ and $I_3(r)$ can appear 022 or disappear playing only with the spatial distribution r, a phenomenon which 923 does not happens when mortality is identical in each tank. This shows that 924 the existence of domains $I_1(r)$ and $I_3(r)$ is controlled by a relative toxicity in 925 the tanks, and not only the spatial distribution as it is the case for identical 926 mortality. This feature can have interest when practitioners can adjust pH or 927 other abiotic parameters having impacts on the mortality rate, independently 928 in each tank. Given operating parameters S^{in} , D and r, panels (a) and (f) of 929 Fig. B3 show that it is theoretically possible to pass from domain $I_3(r)$ to $I_2(r)$ 930 when mortality parameter is diminished only in the second tank. In practice, 931 being in domain $I_2(r)$ might be more desirable than $I_3(r)$ with respect to some 932 dysfunctioning of the first tank that can drop suddenly its biomass to zero. 933 Indeed, in $I_2(r)$, the second tank is no conducted to the wash-out differently 934 to the $I_3(r)$ case. 935

When $a_1 = a_2 = a$, which is the case corresponding to the system (1) 936 considered in Section 2, only panels (c,d) of Fig. B3 are encountered, as shown 937 in Fig. 2. We describe hereafter the bifurcations that occur in this particular 938 case. The general case i.e. when $a_1 \neq a_2$ is similar. 939

Remark 4 Transcritical bifurcations occur in the limit cases $D = r(f(S^{in}) - a)$ and 940 $D = (1 - r)(f(S^{in}) - a)$, for system (1). If 0 < r < 1/2 then, we have a transcritical 941 bifurcation of E_0 and E_1 when $D = (1-r)(f(S^{in})-a)$ and a transcritical bifurcation 942 of E_1 and E_2 when $D = r(f(S^{in}) - a)$. If 1/2 < r < 1 then, we have a transcritical 943 bifurcation of E_0 and E_1 when $D = (1-r)(f(S^{in})-a)$ and a transcritical bifurcation 944 of E_0 and E_2 when $D = r(f(S^{in}) - a)$. If r = 1/2 and $D = (f(S^{in}) - a)/2$ then, we 945 have transcritical bifurcations of E_0 and E_1 , and E_0 and E_2 , simultaneously. 946

Appendix D Proofs 947

D.1Proof of Theorem 3 948

We begin by the existence of steady states. The steady states are the solutions 949 of the set of equations $\dot{S}_1 = 0$, $\dot{x}_1 = 0$, $\dot{S}_2 = 0$, $\dot{x}_2 = 0$. From equation $\dot{x}_1 = 0$, 950 it is deduced that $x_1 = 0$ or $f(S_1) = D/r + a_1$. Suppose first that $x_1 = 0$. 951 Then, from equation $\dot{S}_1 = 0$ it is deduced that $S_1 = S^{in}$ and from equation 952 $\dot{x}_2 = 0$ it is deduced that $x_2 = 0$ or $f(S_2) = D/(1-r) + a_2$. If $x_2 = 0$, 953 then from equation $S_2 = 0$ it is deduced that $S_2 = S^{in}$. Hence we obtain the 954 steady state $E_0 = (S^{in}, 0, S^{in}, 0)$, which always exist. On the other hand, if 955 $f(S_2) = D/(1-r) + a_2$, then $S_2 = \overline{S}_2$, defined in (B15). From equation $\dot{S}_2 = 0$, 956 it is deduced that $x_2 = \overline{x}_2$, defined in (B15). Hence we obtain the steady state 957

 $E_1 = (S^{in}, 0, \overline{S}_2, \overline{x}_2)$. This steady state exists if and only if $S^{in} > \overline{S}_2$, that is 058 $D < (1-r)(f(S^{in}) - a_2).$ 959

Suppose now that $f(S_1) = D/r + a_1$. Then $S_1 = S_1^*$, defined in (B17). From 960 equation $\dot{S}_1 = 0$, it is deduced that $x_1 = x_1^*$, defined in (B17). From equation 961 $\dot{S}_2 + \dot{x}_2 = 0$, it is deduced that 962

$$x_2 = \frac{D}{D + (1 - r)a_2} (S_1^* + x_1^* - S_2).$$
 (D27)

Replacing x_2 by this expression in the equation $\dot{S}_2 = 0$, it is deduced that 963 $f(S_2) = h(S_2)$, where h is defined by (B11). Hence $S_2 = S_2^*$, which is the 964 unique solution of the equation $f(S_2) = h(S_2)$, as shown in Figure B2 (a). 965 Replacing S_2 by S_2^* in (D27) gives $x_2 = x_2^*$, defined by (B18). Consequently, 966 we obtain the steady state $E_2 = (S_1^*, x_1^*, S_2^*, x_2^*)$. This steady state is positive 967 if and only if $S^{in} > S_1^*$, which is equivalent to $D < r(f(S^{in}) - a_1)$. 968

Let us now study the local stability. Since the system has a cascade struc-969 ture, the stability analysis reduces to the study of square 2×2 matrices. Indeed, 970 the Jacobian matrix associated to system (B10) is the lower triangular matrix 971 by blocs, $J = \begin{pmatrix} A & 0 \\ B & C \end{pmatrix}$ where B is the diagonal matrix whose diagonal elements

972 are D/(1-r), and A and C are given by: 973

$$A = \begin{pmatrix} -\frac{D}{r} - f'(S_1)x_1 & -f(S_1) \\ f'(S_1)x_1 & -\frac{D}{r} + f(S_1) - a_1 \end{pmatrix},$$

$$C = \begin{pmatrix} -\frac{D}{1-r} - f'(S_2)x_2 & -f(S_2) \\ f'(S_2)x_2 & -\frac{D}{1-r} + f(S_2) - a_2 \end{pmatrix},$$

Hence, the eigenvalues of J are the ones of A and C. 974

For E_0 , the eigenvalues are -D/r, $-D/r + f(S^{in}) - a_1$, -D/(1-r) and 975 $-D/(1-r) + f(S^{in}) - a_2$. They are negative if and only if $D > r(f(S^{in}) - a_1)$ 976 and $D > (1-r)(f(S^{in}) - a_2)$. Therefore, E_0 is LES if and only if the condition 977 in the theorem is satisfied. 978

For E_1 , the eigenvalues of A are $-D/r + f(S^{in}) - a_1$ and -D/r. The first 979 eigenvalue is negative if and only if $D > r(f(S^{in}) - a_1)$. On the other hand, 980 since the determinant of C is positive, and its trace is negative, the eigenvalues 981 of C are of negative real parts. Therefore, E_1 is LES if and only if the condition 982 in the theorem is satisfied. 983

For E_2 , the determinant of A is positive and its trace is negative. On the 984 other hand, using the notation C_{E_2} for the matrix C evaluated at E_2 , we have 985

$$\det(C_{E_2}) = \left(-\frac{D}{1-r} - f'(S_2^*)x_2^*\right) \left(-\frac{D}{1-r} - a_2 + f(S_2^*)\right) + f(S_2^*)f'(S_2^*)x_2^*,$$

$$\operatorname{tr}(C_{E_2}) = -2\frac{D}{1-r} - a_2 - f'(S_2^*)x_2^* + f(S_2^*).$$

Note that $h(S_2) < D/(1-r) + a_2$ for all $S_2 \in (0, S_1^*)$. Therefore, from (B11), 986 we have $f(S_2^*) = h(S_2^*) < D/(1-r) + a_2$. Consequently, $\det(C_{E_2})$ and $\operatorname{tr}(C_{E_2})$ 987

are respectively positive and negative. Therefore, E_2 is LES whenever it exists, that is $D < r(f(S^{in}) - a_1)$.

For the study of the global stability we use the cascade structure of the system (B10) and Thieme's Theorem (see Theorem A1.9 of [16]). In the rest of the proof, we denote by $(S_1(t), x_1(t), S_2(t), x_2(t))$ the solution of (B10) with the initial condition $(S_1^0, x_1^0, S_2^0, x_2^0)$. Then, $(S_1(t), x_1(t))$ is the solution of system

$$\dot{S}_{1} = \frac{D}{r}(S^{in} - S_{1}) - f(S_{1})x_{1}$$

$$\dot{x}_{1} = -\frac{D}{r}x_{1} + f(S_{1})x_{1} - a_{1}x_{1}$$
(D28)

with initial condition (S_1^0, x_1^0) and $(S_2(t), x_2(t))$ is the solution of the nonautonomous system of differential equations

$$\dot{S}_{2} = \frac{D}{1-r} (S_{1}(t) - S_{2}) - f(S_{2}) x_{2}$$

$$\dot{x}_{2} = \frac{D}{1-r} (x_{1}(t) - x_{2}) + f(S_{2}) x_{2} - a_{2} x_{2}$$
(D29)

with the initial condition (S_2^0, x_2^0) . The system (D28) is the classical model of a single chemostat. Its asymptotic behaviour is well known (see, for instance, Proposition 2.2 of [16]). This system admits the steady states:

$$e_0^1 = (S^{in}, 0)$$
 and $e_1^1 = (S_1^*, x_1^*)$ (D30)

where S_1^* and x_1^* are defined by (B17). Two cases must be distinguished.

Firstly, if $\lambda (D/r + a_1) \geq S^{in}$, that is $D \geq r(f(S^{in}) - a_1)$ then, e_0^1 , defined in (D30), is GAS for (D28) in the nonnegative quadrant. Hence, for any nonnegative initial condition (S_1^0, x_1^0) ,

$$\lim_{t \to +\infty} (S_1(t), x_1(t)) = (S^{in}, 0).$$
 (D31)

¹⁰⁰³ Therefore, the system (D29) is asymptotically autonomous with the limiting ¹⁰⁰⁴ system

$$\dot{S}_{2} = \frac{D}{1-r}(S^{in} - S_{2}) - f(S_{2})x_{2}$$

$$\dot{x}_{2} = -\frac{D}{1-r}x_{2} + f(S_{2})x_{2} - a_{2}x_{2}.$$
 (D32)

Recall that the solutions of (D29) are positively bounded. Therefore, we shall use Thieme's results which apply for bounded solutions.

The system (D32) represents the classical model of a single chemostat. It admits the two steady states $e_0^2 = (S^{in}, 0)$ and $e_1^2 = (\overline{S}_2, \overline{x}_2)$, with $(\overline{S}_2, \overline{x}_2)$ defined by (B15). Two subcases must be distinguished.

• If $\lambda (D/(1-r) + a_2) \geq S^{in}$, that is $D \geq (1-r)(f(S^{in}) - a_2)$ then, e_0^2 is GAS in the nonnegative quadrant. Using Thieme's Theorem, we deduce that for any nonnegative (S_2^0, x_2^0) , the solution $(S_2(t), x_2(t))$ of (D29) converges towards $e_0^2 = (S^{in}, 0)$. Using (D31) we deduce that, when $D \geq \max(r(f(S^{in}) - a_1), (1-r)(f(S^{in}) - a_2))$, the solution $(S_1(t), x_1(t), S_2(t), x_2(t))$ of (B10) converges towards $E_0 = (S^{in}, 0, S^{in}, 0)$, which proves (B14).

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• In contrast, if $\lambda(D/(1-r) + a_2) < S^{in}$, that is $D < (1-r)(f(S^{in}) - a_2)$ 1017 then, both steady states e_0^2 and e_1^2 exist and e_1^2 is GAS in the positive quad-1018 rant. Although system (D29) has the saddle point e_0^2 , no polycyle can exist. 1019 Using Thieme's Theorem, for any positive (S_2^0, x_2^0) , the solution $(S_2(t), x_2(t))$ 1020 of (D29) converges towards $e_1^2 = (\overline{S}_2, \overline{x}_2)$. Using (D31) we deduce that, 1021 if $r(f(S^{in}) - a_1) \leq D$ and $D < (1 - r)(f(S^{in}) - a_2)$, then the solution 1022 $(S_1(t), x_1(t), S_2(t), x_2(t))$ of (B10) converges towards $E_1 = (S^{in}, 0, \overline{S}_2, \overline{x}_2),$ 1023 which proves (B16). 1024

Secondly, if $\lambda (D/r + a_1) < S^{in}$, that is $D < r(f(S^{in}) - a_1)$ then, e_1^1 , defined in (D30), is GAS for (D28) in the positive quadrant. Hence, for any positive initial condition (S_1^0, x_1^0)

$$\lim_{t \to +\infty} (S_1(t), x_1(t)) = (S_1^*, x_1^*).$$
(D33)

Therefore, the system (D29) is asymptotically autonomous with the limiting system

$$\dot{S}_{2} = \frac{D}{1-r}(S_{1}^{*} - S_{2}) - f(S_{2})x_{2}
\dot{x}_{2} = \frac{D}{1-r}(x_{1}^{*} - x_{2}) + f(S_{2})x_{2} - a_{2}x_{2}.$$
(D34)

The system (D34) represents the classical model of a single chemostat with an input biomass. In this case, there is no washout and the system (D34) always admits one LES steady state $e_2 = (S_2^*, x_2^*)$ with positive biomass defined by (B18) and S_2^* the unique solution of $h(S_2) = f(S_2)$.

Let us show that this steady state is GAS for (D34). Assume that $x_2 > 0$. Consider the change of variable $\xi = \ln(x_2)$. The system (D34) becomes as

$$\dot{S}_{2} = \frac{D}{1-r}(S_{1}^{*} - S_{2}) - f(S_{2})e^{\xi}
\dot{\xi} = \frac{D}{1-r}(x_{1}^{*}e^{-\xi} - 1) + f(S_{2}) - a_{2}.$$
(D35)

The divergence of the vector field

$$\psi(S_2,\xi) = \begin{bmatrix} \frac{D}{1-r}(S_1^* - S_2) - f(S_2)e^{\xi} \\ \frac{D}{1-r}(x_1^*e^{-\xi} - 1) + f(S_2) - a_2 \end{bmatrix}$$

associated to (D35) is $\operatorname{div}\psi(S_2,\xi) = -\frac{D}{1-r}(1+x_1^*e^{\xi}) - f'(S_2)e^{\xi}$. It is negative. 1036 Thus, using Bendixon-Dulac criterion, system (D35) cannot have a periodic 1037 solution. Hence, system (D34) has no cycle in the positive quadrant. For any 1038 non negative initial condition (S_2^0, x_2^0) , the solution of (D34) is bounded. Hence, 1039 the ω -limit set of (S_2^0, x_2^0) , denoted $\omega(S_2^0, x_2^0)$, is non-empty and included in the 1040 positive quadrant. If $e_2 \notin \omega(S_2^0, x_2^0)$ then, using Poincaré-Bendixon Theorem, 1041 $\omega(S_2^0, x_2^0)$ is a limit cycle, but the system does not present any, due to the 1042 divergence property. One then deduces $e_2 \in \omega(S_2^0, x_2^0)$ and, as e_2 is LES, then 1043 $\omega(S_2^0, x_2^0) = \{e_2\}$. Consequently, e_2 is GAS for (D34) in the positive quadrant. 1044 Using again Thieme's Theorem, for any positive (S_2^0, x_2^0) , the solution 1045 $(S_2(t), x_2(t))$ of (D29) converges towards $e_2 = (S_2^*, x_2^*)$. Using (D33) we deduce 1046

that, if $D < r(f(S^{in}) - a_1)$, then the solution $(S_1(t), x_1(t), S_2(t), x_2(t))$ of (B10) converges towards $E_2 = (S_1^*, x_1^*, S_2^*, x_2^*)$. This ends the proof of the theorem.

1049 D.2 Proof of Lemma 4

Let us fix S^{in} such that $\delta := f(S^{in}) - a > 0$. The proof consists in showing that the function $(D, r) \mapsto G_2(S^{in}, D, r)$ can be formally extended as a C^2 function for values of r larger than 1 (although such values have no physical meaning). Recall first that for any $D \in (0, \delta)$, one has $G_2(S^{in}, D, 1) = G_{chem}(S^{in}, D)$. As $G_2(S^{in}, \overline{D}(1), 1) > 0$ and $G_2(S^{in}, 0, 1) = 0$, there exists by continuity of the function G_2 , numbers $\underline{D} \in (0, \overline{D}(1)), \underline{r} \in (0, 1)$ such that

$$G_2(S^{in}, D, r) < \max_{d \in (0, r\delta)} G_2(S^{in}, d, r), \ (D, r) \in [0, \underline{D}] \times [\underline{r}, 1].$$
(D36)

1056

Let $\varepsilon > 0$ be such that

$$D_{\varepsilon} := \epsilon \left(a + \max_{s \in [0, S^{in}]} f'(s)(S^{in} - s) \right) < \underline{D}$$
 (D37)

1057 and consider the domain

$$\mathcal{D}_{\varepsilon} := \left\{ (D, r); \ D \in (D_{\varepsilon}, \delta), \ r \in \left(\max\left(\underline{r}, \frac{D}{\delta}\right), 1 + \varepsilon \right) \right\}.$$

Note that for any $(D, r) \in \mathcal{D}_{\varepsilon}$, the number $\lambda(D/r + a) = f^{-1}(D/r + a)$ is well defined. Posit the function

$$\varphi(S_2, D, r) = (D + (1 - r)a) \left(\lambda(D/r + a) - S_2\right) - (1 - r)f(S_2) \left(\frac{DS^{in} + ra\lambda(D/r + a)}{D + ra} - S_2\right),$$

where $(S_2, D, r) \in (0, S^{in}) \times \mathcal{D}_{\varepsilon}$. As f is C^2 , φ is C^2 on $(0, S^{in}) \times \mathcal{D}_{\varepsilon}$. For r < 1 and $(D, r) \in \mathcal{D}_{\varepsilon}$, one has

$$\varphi(S_2, D, r) = (1 - r) \left(\frac{DS^{in} + ra\lambda(D/r + a)}{D + ra} - S_2 \right) \left(h(S_2) - f(S_2) \right)$$

where h is the function defined in (5). According to Lemma 8, h is positive decreasing on $(0, \lambda(D/r + a))$, and h - f admits an unique zero $S_2^{\star} = S_2^{\star}(S^{in}, D, r)$ on $(0, \lambda(D/r + a))$. Then, one can write

$$\partial_{S_2}\varphi\Big|_{S_2=S_2^{\star}} = (1-r)\left(\frac{DS^{in} + ra\lambda(D/r + a)}{D + ra} - S_2\right)(\partial_{S_2}h - f')\Big|_{S_2=S_2^{\star}} < 0.$$

For $r \in [1, 1 + \varepsilon)$ and $(D, r) \in \mathcal{D}_{\varepsilon}$, on has

$$\partial_{S_2}\varphi = -(D + (1 - r)a) - (1 - r)f'(S_2) \Big(\frac{DS^{in} + ra\lambda(D/r + a)}{D + ra} - S_2\Big) + (1 - r)f(S_2),$$

which is negative for any $S_2 \in (0, S^{in})$ thanks to condition (D37). As $\varphi(0, D, r) > 0$ and $\varphi(S^{in}, D, r) < 0$, we deduce the existence of a unique $S_2^{\star} = S_2^{\star}(S^{in}, D, r)$ in $(0, S^{in})$ such that $\varphi(S_2^{\star}, D, r) = 0$, which also verifies $\partial_{S_2} \varphi < 0$ at $S_2 = S_2^{\star}$.

Then, by the Implicit Function Theorem, the function $(D, r) \mapsto$ 1070 $S_2^{\star}(S^{in}, D, r)$ is C^2 on $\mathcal{D}_{\varepsilon}$. Recall that for r < 1 and $D < r\delta$, on has the 1071 expression $G_2(S^{in}, D, r) = VD(S^{in} - S_2^{\star}(S^{in}, D, r))$ (see Proposition 4). We 1072 extend now the function $(D,r) \mapsto G_2(S^{in}, D, r)$ with this last C^2 expression 1073 on $\mathcal{D}_{\varepsilon}$. As $G_2(S^{in}, D, 1) = G_{chem}(S^{in}, D)$ for any $D \in (0, \delta)$, one deduces, 1074 by continuity of the partial derivatives of G_2 with respect to D and property 1075 (D36), the existence of \mathcal{V}_D , \mathcal{V}_r as neighborhoods respectively of D(1) and 1 1076 with $\mathcal{V}_D \times \mathcal{V}_r \subset \mathcal{D}_{\varepsilon}$ such that for any $r \in \mathcal{V}_r$, the function $D \mapsto G_2(S^{in}, D, r)$ 1077 possesses the following properties 1078

1079 1. it is strictly concave on \mathcal{V}_D ,

- ¹⁰⁸⁰ 2. it is increasing on $(D_{\varepsilon}, \overline{D}(1)) \setminus \mathcal{V}_D$ and decreasing on $(\overline{D}(1), r\delta) \setminus \mathcal{V}_D$,
- 1081 3. its maximum over $(0, r\delta)$ is not reached for $D \leq D_{\varepsilon}$.

We thus deduce that $D \mapsto G_2(S^{in}, D, r)$ admits a unique maximum $\overline{D}(r)$ on (0, $r\delta$), for any $r \in \mathcal{V}_r$.

Finally, for any $r \in \mathcal{V}_r$, $\overline{D}(r)$ is characterized as the zero of the map $D \mapsto F(D,r)$ where F is the C^1 function

$$F(D,r) := \partial_D G_2(S^{in}, D, r)$$

¹⁰⁸⁶ From property 1. above, one obtains

$$\partial_D F(\overline{D}(r), r) = \partial_{DD}^2 G_2(S^{in}, \overline{D}(r), r) < 0, \quad r \in \mathcal{V}_r$$

and by the Implicit Function Theorem, there exists a neighborhood $\mathcal{V}_1 \subset \mathcal{V}_r$ of 1 such that \overline{D} is C^1 on \mathcal{V}_1 , which ends the proof of the lemma.

1089 D.3 Proof of Proposition 6

 S^{in} being fixed, we shall drop the S^{in} dependency in the expressions of S_i^*, x_i^* (i = 1, 2) and G_2 . Thus, let us define

$$G(D,r) := G_2(S^{in}, D, r),$$

$$F_i(D,r) := f(S_i^*(D, r))x_i^*(D, r), \quad i = 1, 2,$$

as functions of $D \ge 0$ and $r \in \mathcal{V}_1 \cap \{r < 1\}$. Remark from the expression of F_1 , that it is well defined as well as its partial derivatives at r = 1. In addition, for the limiting case r = 1, using Lemma 9, for all $D \ge 0$, one has

$$S_2^*(D,1) = S_1^*(D,1) = \lambda(D+a)$$

$$x_2^*(D,1) = x_1^*(D,1) = \frac{D}{D+a}(S^{in} - \lambda(D+a)).$$
(D38)

1095 Thus, for all $D \ge 0$, one has

$$F_1(D,1) = F_2(D,1),$$
 (D39)

and F_2 is also well defined for r = 1. Thus, according to (37), for all $D \ge 0$ and $r \in \mathcal{V}_1 \cap \{r \le 1\}$, one has

$$G(D,r) = rF_1(D,r) + (1-r)F_2(D,r)$$

and from Lemma 4, for $r \in \mathcal{V}_1 \cap \{r < 1\}$, one has

$$\overline{G}(r) = G(\overline{D}(r), r), \tag{D40}$$

with \overline{G} defined by (42). For convenience, for a function E of (D, r) that is differentiable, we shall define the three following functions: $\overline{E}(r) := E(\overline{D}(r), r)$ and

$$\partial_r E(r) := \frac{\partial E}{\partial r}(\overline{D}(r), r), \quad \partial_D E(r) := \frac{\partial E}{\partial D}(\overline{D}(r), r)$$

1102 Therefore, the function \overline{G} writes

and ∂

1105

$$\overline{G}(r) = r\overline{F}_1(r) + (1-r)\overline{F}_2(r), \text{ for } \underline{r} \in \mathcal{V}_1 \cap \{r < 1\}.$$
(D41)

As the functions F_i are differentiable and as $\overline{D}(r)$ is a maximizer of $D \mapsto rF_1(D,r) + (1-r)F_2(D,r)$ on the interior of the interval $[0, f(S^{in}) - a]$, one has

$$r\partial_D F_1(r) + (1-r)\partial_D F_2(r) = 0, \text{ for } r \in \mathcal{V}_1 \cap \{r < 1\}, \qquad (D42)$$

$${}_DF_1(1) = 0. \text{ As } f \text{ is } \mathcal{C}^2 \text{ and } \overline{D} \text{ is assumed to be differentiable on } \mathcal{V}_1 \cap \{r < 1\}, \qquad (D42)$$

1106 1}, \overline{G} is differentiable and from (D41), for all $r \in \mathcal{V}_1 \cap \{r < 1\}$, one has

$$\overline{G}'(r) = \overline{F}_1(r) - \overline{F}_2(r) + r\partial_r F_1(r) + (1-r)\partial_r F_2(r) + (r\partial_D F_1(r) + (1-r)\partial_D F_2(r))\overline{D}'(r),$$

and with (D42), for all $r \in \mathcal{V}_1 \cap \{r < 1\}$, one has simply

$$\overline{G}'(r) = \overline{F}_1(r) - \overline{F}_2(r) + r\partial_r F_1(r) + (1-r)\partial_r F_2(r).$$
(D43)

Let us now determine the limits of the terms of the right side of this last equality when r tends to 1. Firstly, according to (D39), one has in particular

$$\overline{F}_1(1) = \overline{F}_2(1). \tag{D44}$$

Secondly, remark that the dynamics of the first tank is parameterized by the single dilution rate $D_1 = D/r$, the other parameters being fixed (see the expression (B17)). The function F_1 takes then the form $F_1(D,r) = \tilde{F}_1(D/r)$ where \tilde{F}_1 is a smooth function. Therefore, one has

$$\partial_D F_1(r) = -\frac{r}{\overline{D}(r)} \partial_r F_1(r). \tag{D45}$$

1114 As $\partial_D F_1(1) = 0$ then one deduces

$$\partial_r F_1(1) = 0. \tag{D46}$$

Finally, from $\dot{S}_2 = 0$, for all $r \in \mathcal{V}_1 \cap \{r < 1\}$, one gets

$$F_2(D,r) = \frac{D}{1-r} (S_1^*(D,r) - S_2^*(D,r)).$$
(D47)

Differentiating (D47) with respect to r gives

$$\frac{\partial F_2}{\partial r}(D,r) = \frac{D}{1-r} \left(\frac{\partial S_1^*}{\partial r}(D,r) - \frac{\partial S_2^*}{\partial r}(D,r) \right) + \frac{D}{(1-r)^2} (S_1^*(D,r) - S_2^*(D,r))$$

¹¹¹⁷ which can be written equivalently as

$$(1-r)\frac{\partial F_2}{\partial r}(D,r) = D\left(\frac{\partial S_1^*}{\partial r}(D,r) - \frac{\partial S_2^*}{\partial r}(D,r)\right) + F_2(D,r).$$

Thus, for $D = \overline{D}(r)$, one has

$$(1-r)\partial_r F_2(r) = \overline{D}(r)(\partial_r S_1^*(r) - \partial_r S_2^*(r)) + \overline{F}_2(r)$$

Notice that for $D = \overline{D}(r)$, (D47) gives

$$\overline{F}_2(r) = \frac{\overline{D}(r)}{1-r} (\overline{S}_1^*(r) - \overline{S}_2^*(r)), \quad \text{for all } r \in \mathcal{V}_1 \cup \{r < 1\}.$$
(D48)

Using L'Hôpital's rule in (D48) when r tends to 1, one gets

$$\overline{F}_2(1) = \lim_{r \to 1^-} \frac{\overline{D}'(r)(\overline{S}_1^*(r) - \overline{S}_2^*(r)) + \overline{D}(r)(\partial_r S_1^*(r) - \partial_r S_2^*(r))}{-1}$$

and using (D38) and (D44), one obtains

$$\overline{F}_1(1) = \lim_{r \to 1^-} -\overline{D}(r)(\partial_r S_1^*(r) - \partial_r S_2^*(r)).$$

¹¹²² Consequently, one has

$$\lim_{r \to 1^{-}} (1 - r)\partial_r F_2(r) = 0.$$
 (D49)

With (D44), (D46) and (D49), expression (D43) gives the existence of the limit of \overline{G}' when r tends to 1 with r < 1, which is

$$\overline{G}'(1^-) = 0.$$
 (D50)

Note that $\overline{G}''(1^-)$ exists if and only if $\lim_{r\to 1^-} \frac{\overline{G}'(r) - \overline{G}'(1)}{r-1}$ exists. Using (D50) and (D43), one has

$$\frac{\overline{G}'(r) - \overline{G}'(1^-)}{r-1} = -\frac{\overline{G}'(r)}{1-r} = -\frac{\overline{F}_1(r) - \overline{F}_2(r) + r\partial_r F_1(r) + (1-r)\partial_r F_2(r)}{1-r}$$
(D51)

1127 On the one hand, using L'Hôpital's rule, one has

$$\lim_{r \to 1^{-}} \frac{\overline{F}_{1}(r) - \overline{F}_{2}(r)}{1 - r} = \lim_{r \to 1^{-}} \frac{\overline{F}_{1}'(r) - \overline{F}_{2}'(r)}{-1}$$

Recall that $\partial_r F_1(1) = 0$ and thus one has $\overline{F}'_1(1) = 0$. Consequently, one has

$$\lim_{r \to 1^{-}} frac\overline{F}_1(r) - \overline{F}_2(r)1 - r = \lim_{r \to 1^{-}} \overline{F}_2'(r) = \lim_{r \to 1^{-}} \partial_r F_2(r) + \partial_D F_2(r)\overline{D}'(r).$$
(D52)

1129 On the other hand, using (D42) and (D45), one has

$$\frac{r}{1-r}\partial_r F_1(r) = \frac{\overline{D}(r)}{r}\partial_D F_2(r).$$
(D53)

Thus, according to (D51), (D52) and (D53), one gets

$$\lim_{r \to 1^{-}} \frac{\overline{G}'(r) - \overline{G}'(1^{-})}{r - 1} = \lim_{r \to 1^{-}}$$
(D54)

Let us show now that the limit of $\partial_D F_2(r)$ is 0 when r tends to 1. One has

$$\frac{\partial F_2}{\partial D} = f'(S_2^*) \frac{\partial S_2^*}{\partial D} x_2^* + f(S_2^*) \frac{\partial x_2^*}{\partial D}.$$

Let use the expression $G(D,r) = D(S^{in} - S_2^*(D,r))$ given by Proposition 4. As $\overline{D}(r)$ is a maximizer then one has

$$\partial_D G(r) = S^{in} - \overline{S}_2^*(r) - \overline{D}(r)\partial_D S_2^*(r) = 0.$$

1134 Using (D38), one then deduces

$$\partial_D S_2^*(1^-) = \frac{S^{in} - \lambda \left(\overline{D}(1) + a\right)}{\overline{D}(1)}$$

¹¹³⁵ In addition, using expressions (B18) and (D38), one gets

$$\partial_D x_2^*(1^-) = -\frac{\overline{D}(1)}{\left(\overline{D}(1)+a\right)^2} \left(S^{in} - \lambda \left(\overline{D}(1)+a\right)\right),\,$$

and hence the limit of $\partial_D F_2$ when r tends to 1 exists:

$$\partial_D F_2(1^-) = \frac{S^{in} - \lambda \left(\overline{D}(1) + a\right)}{\overline{D}(1) + a} f' \left(\lambda \left(\overline{D}(1) + a\right)\right) A_i$$

where $A = S^{in} - \lambda \left(\overline{D}(1) + a\right) - \frac{\overline{D}(1)}{f'(\lambda(\overline{D}(1) + a))}$. Thus, one has

$$\partial_D F_2(1^-) = \frac{S^{in} - \lambda \left(\overline{D}(1) + a\right)}{\overline{D}(1) + a} f' \left(\lambda \left(\overline{D}(r) + a\right)\right) \left(S^{in} - g\left(\overline{D}(1)\right)\right),$$

with g defined by (A8). According to Proposition 9, one has $S^{in} - g(\overline{D}(1)) = 0$. Consequently, one has $\partial_D F_2(1^-) = 0$.

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Finally, it remains to calculate the limit of $\partial_r F_2(r)$ when r tends to 1. One has

$$\frac{\partial F_2}{\partial r} = f'(S_2^*) \frac{\partial S_2^*}{\partial r} x_2^* + f(S_2^*) \frac{\partial x_2^*}{\partial r}$$

Let use again the expression $G(D,r) = D(S^{in} - S_2^*(D,r))$. According to (D41), one has

$$\overline{G}'(r) = \partial_r G(r) + \partial_D G(r) \overline{D}'(r)$$

where $\partial_D G(r) = 0$. According to (D50), we have $\partial_r G(1^-) = 0$, and thus $\partial_r S_2^*(1^-) = 0$. Using expression (B18), one gets

$$\partial_r x_2^*(1^-) = -a\overline{D}(1) \frac{S^{in} - \lambda \left(\overline{D}(1) + a\right)}{\left(\overline{D}(1) + a\right)^2},$$

and then the limit of $\partial_r F_2$ when r tends to 1 exists:

$$\partial_r F_2(1^-) = -a\overline{D}(1) \frac{S^{in} - \lambda \left(\overline{D}(1) + a\right)}{\overline{D}(1) + a}.$$

As \overline{D}' is assumed to be bounded on $\mathcal{V}_1 \cup \{r < 1\}$, we thus obtain from (D54) the existence of $\overline{G}''(1^-)$ with

$$\overline{G}''(1^-) = -2\partial_r F_2(1^-)$$

which is given by expression (43).

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Author Contributions

All authors contributed to the study conception, methodology and mathematical analysis. The first draft of the manuscript was written by Manel
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1164 Data Availability

Data sharing not applicable to this article as no datasets were generated or analysed during the current study.

1167 References

- [1] N. Abdellatif, R. Fekih-Salem and T. Sari, Competition for a single
 resource and coexistence of several species in the chemostat, Math. Biosci.
 Eng., 13 (2016), 631–652.
- [2] B. Bar and T. Sari, The operating diagram for a model of competition
 in a chemostat with an external lethal inhibitor, Discrete & Continuous
 Dyn. Syst. B, 25 (2020), 2093–2120.
- [3] G. Bastin and D. Dochain, On-line estimation and adaptive control of
 bioreactors: Elsevier, Amsterdam, 1991.
- [4] A. Bornhöft, R. Hanke-Rauschenbach and K. Sundmacher: steady state
 analysis of the anaerobic digestion model no. 1 (adm1). Nonlinear
 Dynamics 73 (2013), 535–549.
- [5] M. Crespo and A. Rapaport, About the chemostat model with a lateral diffusive compartment, Journal of Optimization, Theory and Applications, Vol. 185 (2020), 597—621.
- [6] M. Dali-Youcef, J. Harmand, A. Rapaport, T. Sari. Some non-intuitive properties of serial chemostats with and without mortality. 2021. https://hal.archives-ouvertes.fr/03404740
- [7] M. Dali-Youcef, A. Rapaport and T. Sari, Study of performance criteria of
 serial configuration of two chemostats, Math. Biosci. Eng., 17(6) (2020),
 6278-6309.
- [8] M. Dali-Youcef and T. Sari. The productivity of two serial chemostats
 (2021). https://hal.inrae.fr/hal-03445797
- [9] Y. Daoud, N. Abdellatif, T. Sari and J. Harmand: Steady-state analysis
 of a syntrophic model: The effect of a new input substrate concentration.
 Math. Model. Nat. Phenom. 13 (2018), 31.
- [10] M. Dellal, M. Lakrib and T. Sari, The operating diagram of a model of
 two competitors in a chemostat with an external inhibitor, Math. Biosci.,
 302 (2018), 27–45.

Springer Nature 2021 LATEX template

52 Performance study of two serial interconnected chemostats

- [11] R. Fekih-Salem, Y. Daoud, N. Abdellatif and T. Sari. A mathematical model of anaerobic digestion with syntrophic relationship, substrate inhibition and distinct removal rates. *SIAM Journal on Applied Dynamical Systems* 20 (2021), 621–1654.
- [12] R. Fekih-Salem, C. Lobry and T. Sari, A density-dependent model of competition for one resource in the chemostat, Math. Biosci., 286 (2017), 104–122.
- [13] S. Fogler: Elements of Chemical Reaction Engineering, 4th edition.
 Prentice Hall, New-York (2008).
- [14] C. de Gooijer, W. Bakker, H. Beeftink and J. Tramper, Bioreactors
 in series: an overview of design procedures and practical applications.
 Enzyme Microb. Technol. 18 (1996), 202–219.
- [15] I. Haidar, A. Rapaport, A. and F. Gérard, Effects of spatial structure and diffusion on the performances of the chemostat. Mathematical Bioscience and Engineering. 8(4) (2011), 953–971.
- [16] J. Harmand, C. Lobry, A. Rapaport and T. Sari, The Chemostat: Mathematical Theory of Microorganism Cultures, John Wiley & Sons, Chemical Engineering Series, 2017.
- I214 [17] J. Harmand, A. Rapaport and A. Trofino, Optimal design of two
 interconnected bioreactors-some new results. AIChE J. 49(6) (1999),
 I433-1450.
- [18] Z. Khedim, B. Benyahia, B. Cherki, T. Sari and J. Harmand: Effect of control parameters on biogas production during the anaerobic digestion of protein-rich substrates. Applied Mathematical Modelling 61 (2018), 351–376.
- [19] C.M. Kung and B.C. Baltzis: The growth of pure and simple microbial competitors in a moving and distributed medium. Math. Biosci. 111
 (1992), 295–313.
- ¹²²⁴ [20] 0. Levenspiel, Chemical reaction engineering, 3^{rd} edition. Wiley, New York ¹²²⁵ (1999).
- [21] B. Li, Global asymptotic behavior of the chemostat : general response
 functions and differential removal rates. SIAM Journal on Applied
 Mathematics 59 (1998), 411–4.
- [22] R. W. Lovitt and J.W.T. Wimpenny, The gradostat: a tool for investigating microbial growth and interactions in solute gradients. Soc. Gen.
 Microbial Quart. 6 (1979), 80 .

- R. W. Lovitt and J.W.T. Wimpenny, The gradostat: a bidirectional compound chemostat and its applications in microbiological research, J. Gen. Microbiol. 127 (1981), 261—268
- [24] K. Luyben and J. Tramper, Optimal design for continuously stirred tank
 reactors in series using Michaelis-Menten kinetics. Biotechnol. Bioeng. 24
 (1982), 1217–1220.
- [25] M. Nelson and H. Sidhu, Evaluating the performance of a cascade of two
 bioreactors. Chem. Eng. Sci. 61 (2006), 3159–3166.
- [26] S. Pavlou, Computing operating diagrams of bioreactors, J. Biotechnol.,
 71 (1999), 7–16.
- [27] M. Polihronakis, L. Petrou and A. Deligiannis, Parameter adaptive control techniques for anaerobic digesters—real-life experiments, Elsevier, Computers & chemical engineering, 17(12) (1993), 1167-1179.
- [28] A. Rapaport, I. Haidar and J. Harmand, Global dynamics of the buffered
 chemostat for a general class of growth functions, J. Mathematical
 Biology, 71(1) (2015), 69–98.
- [29] A. Rapaport and J. Harmand, Biological control of the chemostat
 with nonmonotonic response and different removal rates. Mathematical
 Biosciences and Engineering 5, no. 3 (2008), 539–547.
- [30] T. Reh and J. Muller, CO2 abatement costs of greenhouse gas (GHG)
 mitigation by different biogas conversion pathways. J. Environ. Manag.
 114, no. 15 (2013), 13–25.
- [31] T. Sari. Best Operating Conditions for Biogas Production in Some Simple
 Anaerobic Digestion Models. *Processes* 2022, 10, 258.
- [32] T. Sari and B. Benyahia. The operating diagram for a two-step anaerobic digestion model. *Nonlinear Dynamics* 2021, **105**, 2711–2737.
- [33] T. Sari and J. Harmand, A model of a syntrophic relationship between two
 microbial species in a chemostat including maintenance, Math. Biosci.,
 275 (2016), 1–9.
- ¹²⁶¹ [34] T. Sari and F. Mazenc, Global dynamics of the chemostat with different removal rates and variable yields. Math Biosci Eng. 8(3) (2011), 827–40.
- [35] T. Sari and M.J. Wade, Generalised approach to modelling a three-tiered microbial food-web, Math. Biosci., 291 (2017), 21–37.

¹²⁶⁵ [36] M. Sbarciog, M. Loccufier and E. Noldus, Determination of appropriate ¹²⁶⁶ operating strategies for anaerobic digestion systems, Biochem. Eng. J., 51

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- 54 Performance study of two serial interconnected chemostats
- (2010), 180-188.
- ¹²⁶⁸ [37] H. Smith, The gradostat: A model of competition along a nutrient gradient. Microbial Ecology, 22(1) (1991), 207–26.
- [38] H. Smith, B. Tang and P. Waltman: Competition in a n-vessel gradostat.
 SIAM J. Appl. Math. 91(5) (1991), 1451–1471.
- [39] H. Smith and P. Waltman, The Theory of the Chemostat, Dynamics of
 Microbial Competition. Cambridge University Press, 1995.
- ¹²⁷⁴ [40] B. Tang, Mathematical investigations of growth of microorganisms in the ¹²⁷⁵ gradostat, J. Math. Biol., 23 (1986), 319–339.
- [41] M.J. Wade, R.W. Pattinson, N.G. Parker and J. Dolfing, Emergent
 behaviour in a chlorophenol-mineralising three-tiered microbial 'food
 web', J. Theor. Biol., 389 (2016), 171–186.
- [42] M. Weedermann, G. Seo and G.S.K Wolkowics: Mathematical model of
 anaerobic digestion in a chemostat: Effects of syntrophy and inhibition.
 Journal of Biological Dynamics 7 (2013), 59–85.
- [43] M. Weedermann, G.S.K Wolkowicz and J. Sasara: Optimal biogas production in a model for anaerobic digestion. Nonlinear Dynamics 81 (2015), 1097–1112.
- [44] G.S.K. Wolkowicz, Z. Lu,Global dynamics of a mathematical model of competition in the chemostat: general response functions and differential death rates. SIAM Journal on Applied Mathematics 52 (1992), 222–23.
- [45] A. Xu, J. Dolfing, T.P. Curtis, G. Montague and E. Martin, Maintenance affects the stability of a two-tiered microbial 'food chain'?, J. Theor. Biol., 276 (2011), 35–41.
- [46] J. Zambrano and B. Carlsson, Optimizing zone volumes in bioreactors
 described by Monod and Contois growth kinetics, Proceeding of the IWA
 World Water Congress & Exhibition, (2014).
- [47] J. Zambrano, B. Carlsson and S. Diehl, Optimal steady-state design of
 zone volumes of bioreactors with Monod growth kinetics. Biochem. Eng.
 J. 100 (2015), 59–66.
- [48] W. Walter, Ordinary Differential Equations. Springer Graduate Texts in
 Mathematics, 182 (1998).