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1	Populational and metabolic shifts induced by acetate, butyrate and
2	lactate in dark fermentation
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8	Abstract
9	Dark fermentation is subject to inhibition by end products. In this study, the effects of
10	acetate, butyrate and lactate on fermentation routes of glucose were investigated for
11	concentrations ranging from 25 to 400 mM. Whatever the acid considered, an
12	inhibition threshold of hydrogen production was observed at acid concentration as
13	low as 50 mM. 300 mM of acetate, 200 mM of butyrate and 400 mM of lactate were
14	critical concentrations resulting exclusively in lactate production. At these high
15	concentrations, bacterial communities shifted from Clostridiaceae to Lactobacillaceae
16	family after acetate or lactate addition, and to Bacillaceae after butyrate addition. At
17	lower acid concentrations, the nature and the concentration of the added acid shaped
18	metabolic and populational changes. Specifically, Clostridium butyricum was able to
19	grow up to 250 mM, 150 mM and 300 mM of acetate, butyrate and lactate
20	respectively, but was suspected to shift its metabolism towards lactate production.
21	Keywords: acid inhibition, biohydrogen, microbial diversity, undissociated acid

22

23 **1. Introduction**

Low carbon footprint hydrogen (H₂) could play a major role in the future to reduce 24 25 carbon dioxide emissions and prevent global warming. Among the existing green H_2 production technologies, biological production by dark fermentation (DF) presents 26 one of the lowest global warming potentials [1]. When performed with mixed cultures, 27 DF presents also the advantages of being light-independent, having high H₂ 28 production rates and using various low-cost raw materials and waste as feedstocks 29 [2]. This promising biological process relies on the degradation of carbohydrate-rich 30 organic matter by H₂-producing bacteria in anaerobic conditions. Efficient H₂ 31 production in DF is mostly associated to acetate and butyrate metabolic pathways 32 33 with the stoichiometry from Equation (1) [3],

$$4C_6H_{12}O_6 + 2H_2O \rightarrow 3CH_3CH_2CH_2COOH + 2CH_3COOH + 8CO_2 + 10H_2 (Equation 1)$$

together with the dominance of species belonging to the *Clostridiaceae* family. Although the microbial diversity in mixed cultures can provide robustness and function redundancies, it could also disfavour the H₂ production by introducing microorganisms engaged in substrate competition (*Lactobacillus sp.*), in the release of inhibitory co-products (bacteriocins, lactate) or in H₂ consumption (bacteria with homoacetogenic activities or hydrogenotrophic methanogens) [4].

The effects of end-products accumulation on H_2 production have been widely studied in mixed cultures [5]. Overall, acetate, butyrate, propionate and ethanol were found to have inhibitory effects on H_2 yields, hydrogen production rates (HPR) and substrate degradation [5]. Inhibitory threshold for H_2 yield (the lowest concentration that does not result in a significant reduction in H_2 yield) by butyrate varies from < 10 mM in batch at pH 7 using heat-treated digested sludge and glucose as substrate [6] to 38 mM in continuous reactor at pH 5.5 from glucose using baked agricultural soil

48 as inoculum [7]. Similarly, inhibition threshold for H_2 yield by acetate was reported to 49 vary from < 10 mM [6] to 98 mM [7].

Furthermore, the activity of lactic acid producing bacteria (LAB) was associated 50 51 with DF instability [8]. Regarding the specific effect of lactate, Baghchehsaraee et al. [9] showed that up to 55 mM of lactate did not inhibit H_2 production. Consistently, 52 Noblecourt et al. [10] did not observe a negative impact of 300 mM endogenously 53 produced lactate during the DF of pre-fermented food wastes. However, the latter 54 observed that 44 mM of exogenously added L-lactate induced a 35 % decrease in H₂ 55 production, highlighting that enantiomeric form of lactate plays a key role in its 56 inhibitory effect. In addition, Kim et al. [11] observed that 178 mM of lactate 57 (unknown enantiomeric form) induced a 40 % increase in lag phase. Therefore, the 58 different results and conclusions found in literature concerning inhibition by acetate, 59 butyrate and lactate are very dependent on the experimental conditions as well as 60 the reactor feeding modes applied, hindering efficient prevention of end-products 61 inhibition. 62

The cellular mechanisms of such end-products inhibition on the microbial activity 63 was deeply studied with pure cultures. Past experiments showed that organic acids 64 can affect the bacterial activity and thus inhibit H₂ production by various means. In 65 their undissociated form, the organic acids can freely cross the cytoplasmic 66 membranes and easily dissociate inside the cell, thus acidifying the cytoplasm and 67 dissipating the proton motive force [12]. Active proton extrusion by ATPases 68 counteracts this effect, but at the expense of the energy available for growth. In their 69 dissociated form, the organic acids can increase the ionic strength, triggering cell 70 lysis, and thus reducing the microbial activity [13,14]. Furthermore, depending on the 71

microorganism studied, the impact of the undissociated form compared to thedissociated form may vary, as well as the extent of the inhibition [15,16].

74 Therefore, in mixed cultures, it can be hypothesised that the variable resistance of the microorganisms to end-products would cause microbial communities shifts, but 75 the knowledge in the literature on this subject is rather poor. Recently, Chen et al. 76 [17] studied the impact of butyrate from 6 to 284 mM on microbial communities with 77 glucose as substrate and at pH 5.5, 6, 6.5 and 7. They showed that H₂ production 78 79 reduction was associated with a decrease in the proportion of H₂-producing microorganisms, such as Clostridium sp. (Clostridiaceae), and an increase in the 80 proportion of other bacteria, including Pseudomonas sp. (Pseudomonadaceae), 81 82 Klebsiella sp. (Enterobacteriaceae), Acinetobacter sp. (Moraxellaceae), and Bacillus sp. (Bacillaceae). However, the analysis of the microbial communities conducted by 83 the authors was limited, replicates of the trials are not presented and only the effect 84 of butyrate was studied. In contrast, under comparable conditions, i.e, at pH 6 with 85 glucose as substrate, Noblecourt et al. [18] observed that an endogenously produced 86 mixture of 191 mM butyrate and 80 mM acetate decreased H₂ production rate but 87 had no impact on the composition of the highly enriched microbial communities from 88 sewage sludge. These results show that H_2 production inhibition by end-products 89 90 could result from populational changes as well as from metabolic changes. However, the conditions that lead to either of these phenomena are unknown. 91

A deeper understanding of the mechanisms of end-product inhibition in mixed
 culture could then contribute to a more effective prevention of these inhibitions.

The objective of this work was to provide further insights on populational and metabolic mechanisms behind the impact of end-products on H₂ fermentation routes

in a mixed culture. More specifically, the novelty of this investigation is attributed to 96 the qualitative and quantitative comparison of bacterial communities through a beta 97 diversity analysis to distinguish between metabolic inhibition (i.e within the same 98 community, changes in metabolic activity are responsible for reduced H₂ production) 99 from populational inhibition (i.e changes in the bacterial community are responsible 100 for reduced H₂ production). For that, the impact of the addition of acetate (from 0 to 101 300 mM), butyrate (from 0 to 250 mM) and lactate (from 0 to 400 mM) on DF of 102 glucose was investigated. 103

104

2. Materials and Methods

105 **2.1. Seed sludge**

Activated sludge was used as inoculum. The sludge was collected from an aerobic 106 107 tank at the wastewater treatment plant (WWTP) of Narbonne (France). pH of the freshly collected sludge was 6.9. The sludge was first centrifuged 10 minutes at 108 109 16,800 g (20 °C), frozen, freeze-dried, mixed, aliquoted and stored at - 80 °C before 110 use. Freeze-drying storage was selected as it has recently been shown to be an effective strategy for preserving the H₂ production potential of WWTP sludge [19]. 111 After storage, the sludge was composed of 0.96 \pm 0.02 gTS.g⁻¹ and 0.75 \pm 0.04 112 gVS.g⁻¹. Prior to the experimental procedures, the sludge was rehydrated in 200 mL 113 of osmosed water and pre-treated by heating at 90°C for 15 min to select spore 114 forming organisms, as heat-treatment was reported as a great strategy to achieve 115 this purpose [20]. 116

117 **2.2. Experimental setup**

Experiments were performed in 600 mL bottles with a 200 mL working volume. The medium was composed of 9.34 \pm 0.26 g.L⁻¹ (i.e., 10.0 \pm 0.3 gDCO.L⁻¹) glucose, 100

mM 2-(N-morpholino)ethanesulfonic acid (MES buffer) (pKa = 6.15), 0.8 g.L⁻¹ NH₄Cl, 120 $0.5 \text{ g.L}^{-1} \text{ K}_2 \text{HPO}_4$ and 1 mL of a micronutrient solution (in mg.L⁻¹ : FeCl₂,4H₂O: 1500; 121 H₃BO₃ : 60; MnSO₄,H₂O: 117; CoCl₂,6H₂O: 25; ZnCl₂: 70; NiCl₂,6H₂O: 25; 122 CuCl₂,2H₂O: 15; NaMoO₄,2H₂O: 25; HCI: 1750). The glucose-to-inoculum ratio 123 (g/g_{VS}) was set at 10, by adjusting the amount of inoculum. The effects of acetate, 124 butyrate and lactate addition were separately evaluated, in three distinct experiments. 125 Sodium acetate (≥ 99 %, Sigma Aldrich) was added at 0, 50, 100, 150, 200, 250 and 126 300 mM; sodium butyrate (98 %, Sigma Aldrich) was added at 0, 25, 50, 100, 150, 127 200 and 250 mM and L (+) sodium lactate (> 99 %, PanReac AppliChem) was added 128 129 at 0, 50, 100, 150, 250, 300 and 400 mM. The concentration ranges evaluated for each acid were chosen based on their inhibitory effects reported in the literature 130 [6,21,22]. Temperature was maintained at 37 ± 1 °C by means of a water bath with 131 no stirring. As the H₂ yield in the present study were similar to the yield obtained 132 under similar conditions with stirring $(1.56 \pm 0.19 \text{ mol}_{H2}/\text{mol}_{dlucose added})$ in the present 133 study and $1.4 \pm 0.1 \text{ mol}_{H2}/\text{mol}_{\text{alucose}}$ with glucose as substrate, pH 6, 250 mL working 134 volume, 300 RPM [23]), it was considered that stirring was not essential in the 135 present study. 136

Each condition was carried out in quadruplicate. pH was initially adjusted at 6.0 ± 0.2 with 8M NaOH or 8M HCI. Finally, bottles were sealed with a rubber stopper, locked with an aluminium screw, and purged with N₂ to ensure anaerobic conditions. 2 mL samples were manually taken from each bottle at the beginning, after 2 days and after 4 days of fermentation. Samples were centrifuged at 13,000 g for 15 min. Supernatant and pellet were separated and stored at -20°C prior to metabolite, glucose and microbial analysis.

144 **2.3.** Analytical procedures

Composition of the headspace was analysed every two hours with an automatic 145 sampler coupled to a micro-gas chromatograph (SRA I-GC R3000) equipped with a 146 Molsieve 5A 10 m column running at 80 °C, 30 PSI with argon as carrier gas for H₂, 147 O₂, N₂, CH₄ analysis and a PoraPlot U (PPU) 8 m column running at 70 °C, 20 PSI 148 with helium as carrier gas for CO₂ analysis. Component detection was realised with a 149 micro-thermal conductivity detector (TCD) set at 90 °C. The volume of gas was 150 estimated every two hours by automatic measurement of the total pressure. The 151 pressure was automatically controlled in each bottle to not exceed 1.2 bar in order to 152 limit inhibition by gaseous products [24]. Data were automatically stored in dedicated 153 internal database. 154

Volatile fatty acids were measured by gas chromatography (GC) while glucose 155 and other metabolites (i.e., lactate, formate, ethanol, butanol) were analysed by high-156 performance liquid chromatography (HPLC). Samples were filtrated through 0.2 µm 157 prior to analysis. The Perkin Elmer Clarus 580 GC was equipped with an Alltech-158 FFAP EC[™]1000 column coupled to a flame ionization detector (FID) set at 280 °C. 159 N_2 was used as carrier gas with a flow of 6 mL.min⁻¹. The HPLC was equipped with a 160 protective precolumn (Microguard cation H refill catbridges, Biorad) and an HPX-87H 161 column (300 × 7.8 mm, Biorad) running at 45 °C, with a 4 mM H₂SO₄ solution as 162 eluent at a flow of 0.3 mL.min⁻¹. Component detection was carried out with a 163 refractive index detector (Waters 2414) running at 45 °C. 164

At the end of the experiment, the fermentation medium of each bottle was collected to assess the amount of biomass produced. Medium was centrifuged at 11,900 g for 20 minutes at 20 °C. Supernatant was removed and the pellet was resuspended in deionized water to eliminate liquid metabolic products and preserve biomass. Total dry mass and volatile solids analysis were performed according to the

APHA standard methods [25]. Biomass formula was considered to be $C_5H_7NO_2$ and 171 1.42g_{COD}/g_{biomass}. [26].

172 **2.4.** Microbial community analyses and sequencing

173 Microbial communities were analysed at start and at the end of the fermentation. At start, three samples were randomly selected for microbial community analyses, for 174 each of the three experiments (one per type of acid addition). At the end of the 175 fermentation, if significant H₂ production was observed, at least two samples were 176 analysed, for a total of 51 samples. More samples were analysed in case of 177 significant variability in H₂ production per replicate. DNA extraction was made with a 178 FastDNA[™] SPIN kit (MP biomedicals) following the manufacturer's instructions. 179 Bacterial members identification was carried out by amplification of the V3–V4 region 180 of the 16S rRNA gene as reported by Braga Nan et al. [27]. Sequences were 181 grouped in operational taxonomic units (OTUs) having 98 % similarity. Sequences 182 were submitted to GenBank, under the accession number PRJNA785481. 183

Beta diversity analysis was conducted after rarefying the samples at the smallest number of reads (21340). A multiple sequence alignment was performed using the Clustal Omega online tool from the European Bioinformatics Institute (EMBL-EBI) (https://www.ebi.ac.uk/).

188 **2.5.** Modelling and statistical data analysis

The most common Gompertz model did not fit the experimental data (Supplementary material 1). Therefore, H₂ production was modelled using a spline fit with the grofit() function of the grofit package in R [28]. The function returned the maximal H₂ production rate (HPR, mLH₂.g_{glucose added}⁻¹.day⁻¹), the maximal volume of cumulated H₂ per gram of glucose added (Hc, mLH₂/g_{glucose added}) and the lag time before H₂

194 production starts (λ , days). These three parameters were deducted from the fit as 195 follows: HPR was the maximal slope, Hc was the highest cumulated volume of H₂ per 196 gram of glucose added and λ corresponded to the x-intercept of the line of slope 197 HPR that passes through the inflection point (visual representation can be found in 198 Supplementary material 1).

199 Modelling of the inhibitory impact of acetate, lactate, butyrate on HPR was 200 performed with the following non-competitive inhibition equation (Equation 2) [22] :

$$HPR = \frac{HPR_{ctrl}}{1 + {(C/K_c)^n}}$$
(Equation 2)

202

where HPR_{ctrl} is HPR without acid addition, C is the concentration of the added acid (mM), n is the degree of inhibition and Kc is the inhibition constant (mM).

Statistical analysis of the data was performed with R software. Differences in bacterial community composition were assessed using average linkage cluster analysis (UPGMA) and the weighted UniFrac distance metric [29]. An edited version of *pvclust* was used [30] to assess the uncertainty in hierarchical cluster analysis through a multiscale bootstrap resampling (n= 10,000). The booststrap probability value (BP) and approximately unbiased probability values (AU) were also calculated. Nine clusters showing a AU > 95 % were considered as relevant.

Visual representation of bacterial relative abundance was done with phyloseq package [31]. Analysis of variance (ANOVA) and Kruskal wallis tests were performed using aov() and kruskal.test() function in R software, respectively. ANOVA was performed in case of validation of the assumptions associated with the test, otherwise a Kruskal wallis test was performed.

Table 1 – Kinetic constants describing H ₂ production: maximal hydrogen production Hc (mLH ₂ -g _{glucose added} -1), maximal hydrogen production rate									
HPR (mL·g _{glucose added} ⁻¹ ·day ⁻¹) and lag phase λ (days) at different concentrations of acetate, butyrate and lactate. The data are shown for the									
	d	ifferent groups of o	quadruplica	ite (mean value	es and standard dev	viation). NA	: not applicabl	e.	
Concentration		LACTATE			ACETATE		BUTYRATE		
of added acid	Hc	HPR	λ	Hc	HPR	λ	Hc	HPR	λ
(mNI)	(mL-g _{glucose}	(mL-g _{glucose added} -	(days)	(mL-g _{glucose}	(mL-g _{glucose added} -	(days)	(mL-g _{glucose}	(mL-g _{glucose added-}	(days)

217 **3. Results and Discussion**

3.1. Adverse effect of acid addition on biohydrogen production

219 Fermentation was monitored over a period of 4 days, after which a plateau in H₂ production was reached in all conditions (Supplementary material 2). No methane 220 production was observed in all experiments. H₂ production was modelled with a 221 spline fit used to estimate the volume of cumulated H₂ produced per gram of glucose 222 added (Hc, mL_{H2} · $g_{olucose added}^{-1}$), the maximal H₂ production rate (HPR, mL_{H2} · $g_{olucose}$ 223 $_{added}^{-1}$ day⁻¹) and the lag phase before H₂ production starts (λ , days) as reported in 224 Table 1. Without acid addition, Hc reached 193 \pm 23 mL_{H2} $g_{glucose added}^{-1}$ (1.56 \pm 0.19 225 $mol_{H2} \cdot mol_{glucose added}^{-1}$), HPR 248 ± 47 $mLH_2 \cdot g_{glucose added}^{-1} \cdot day^{-1}$ (2.0 ± 0.38) 226 $mol_{H2} \cdot mol_{glucose added}^{-1} \cdot day^{-1}$) and $\lambda 0.56 \pm 0.13$ day. Less than 20 % variability was 227 observed between the replicates for Hc, HPR and λ in each condition, exception 228 made 229

for 300 mM of lactate, 200 mM and 250 mM of acetate (Supplementary material 3).

	added- ¹)	¹ .day_ ¹)		added- ¹)	¹ .day ₋ ¹)		added- ¹)	¹ .day_ ¹)	
0	201 + 7	270 + 19	0.62 + 0.02	107 . 5	240 + 50	0.42 + 0.04	162 + 20	279 . 26	0.50 + 0.1
U	201 ± 7	279±10	0.62 ± 0.03	197 ± 5	240 ± 50	0.42 ± 0.04	102 ± 30	270 ± 30	0.50 ± 0.1
25	/	/	/	/	/	/	153 ± 27	242 ± 29	0.70 ± 0.14
50	203 ± 30	412 ± 19	0.69 ± 0.02	197 ± 17	327 ± 50	0.74 ± 0.1	164 ± 32	223 ± 11	0.70 ± 0.12
100	141 ± 18	336 ± 18	0.73 ± 0.05	161 ± 12	297 ± 27	0.88 ± 0.08	109 ± 30	136 ± 43	1.28 ± 0.39
150	134 ± 22	243 ± 46	0.88 ± 0.23	126 ± 13	219 ± 18	1.09 ± 0.17	75 ± 6	92 ± 4	1.78 ± 0.04
200	/	/	/	81 ± 49	137 ± 89	1.42 ± 0.11	0 ± 0	0 ± 0	NA
250	123 ± 23	172 ± 16	1.37 ± 0.17	37 ± 71	57 ± 95	2.24 ± 1.37	0 ± 0	0 ± 0	NA
300	63 ± 55	92 ± 70	2.31 ± 0.56	0 ± 0	0 ± 0	NA	/	/	/
400	0 ± 0	0 ± 0	NA	/	/	/	/	/	/

231 Cumulated hydrogen production - Hc

A significant inhibition threshold for Hc was observed at 50 mM when acetate (ANOVA, p = 0.0005), butyrate (ANOVA, p = 0.047) and lactate (Kruskal Wallis, p =0.0400) were individually added. From this threshold, Hc declined progressively until it reached 0 at different concentrations depending on the acid added: 400 mM for lactate addition, 300 mM for acetate addition and 200 mM for butyrate addition. This result shows that acetate, butyrate and lactate can inhibit the total volume of H2 produced and that this inhibitory effect is dose dependent.

Consistently, inhibitory threshold lower than 83 mM of acetate was observed at pH 5.5 with sucrose (25 gCOD·L⁻¹) [22]. Thresholds below 10 mM were found at pH 6 [32] and 7 [6] but in these study, pH was unregulated; and potentially insufficiently buffered (48 mM NaHCO₃ with 10 g·L⁻¹ glucose), respectively.

Concerning butyrate, the inhibitory threshold observed here is consistent with the 71 mM threshold found by Zheng and Yu [33] in similar conditions, i.e, at pH 6 with 10 g.L⁻¹ glucose. Again, lower thresholds of 17mM and < 10mM found by Chen et al. [17] at pH 6 and Wang et al. [6] at pH 7 were obtained with potentially insufficient buffering (48 mM NaHCO₃ with 10 g·L⁻¹ glucose again) and no buffering of the fermentation medium.

With regards to lactate, Noblecourt et al. [10] found a lower inhibitory threshold of < 44 mM of L-lactate at pH 6. In contrast, Kim et al. [11] found that lactate addition from 11 to 178 mM at pH 4.5 improved or did not affect the overall H_2 production. Finally, the 24h pre-treatment of the inoculum at pH 2 carried by Kim et al. [11] selected acid-resistant strains, which would explain the higher tolerance to lactic acid.

Interestingly, comparing the different studies, inhibitory thresholds for H₂ 254 production do not increase with an increase in pH. Also, in this study, inhibitory 255 threshold for H₂ production were 50 mM for acetate, butyrate and lactate, although 256 these acids present variable pka (4.76, 4.82 and 3.86, resp.). This may be surprising 257 as some authors have stated that the undissociated form of the acid was the main 258 cause of inhibition of H₂ production [7,17]. However, in Chen et al. [17] and Van 259 Ginkel and Logan [7] studies, the coefficient of determination associated with the 260 linear regression between H₂ yield and undissociated butyric acid concentration were 261 quite low, achieving 0.54 and 0.04 (calculated from the data shown in the article). 262 263 Furthermore, the inhibition thresholds found in the two studies were also different, reaching 6 mM [7] and less than 2 mM of undissociated butyric acid [17]. Considered 264 as a whole, this suggests that considering undissociated acid concentrations alone is 265 insufficient to explain inhibitions in mixed cultures. The extent of inhibition is probably 266 also related to the different operational parameters applied and the microbial 267 communities used as inoculum. 268

269 Hydrogen production rate - HPR

Inhibitory threshold values of HPR were estimated at 200 mM for acetate (ANOVA, p =0.007), 50 mM for butyrate (ANOVA, p = 0.00223), and 250 mM for lactate (ANOVA, p = 0.00011). Thus, acetate, butyrate and lactate exhibit an inhibitory activity on H₂ production rate, which could be related either to metabolic disruption or to changes in microbial communities. In addition, this result highlightsthat butyrate showed the strongest inhibitory effect on HPR, and lactate the lowest.

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In comparison, the threshold values for HPR inhibition for acetate and butyrate were 277 lower, < 83 mM in the experiment of Wang et al. [22] and < 48 mM in the experiment 278 of Zheng and Yu, respectively [33]. The higher HPR inhibitory threshold reported in 279 the present study could be interestingly attributed to the unstirred fermentation. 280 Indeed, flocculation was observed and extracellular polymeric substances 281 surrounding the cells in biofilms and flocs are known to protect them from toxic 282 283 substance [34]. Thus, flocculation may have been associated with a higher resistance of bacteria to organic acids. 284

In addition, 50 mM of acetate induced a significant 36 % improvement of HPR (ANOVA, p = 0.0367). Similarly, Colin and Moulin [35] observed that acetate addition up to 210 mM induced an increase in *Clostridium butyricum* growth rate. This effect and associated increase in the production of H₂ in presence of acetate was also observed by Heyndrickx et al. [36] with *C. butyricum* and *Clostridium pasteurianum*. These authors suggested that acetate was used as an indirect proton and electron acceptor, stimulating substrate fermentation by providing intermediate acetyl-CoA.

Interestingly, 50 mM and 100 mM of lactate induced in this study significant improvements of the HPR of 48 % and 20 % compared to HPR without lactate (ANOVA, p = 0.00005 and 0.004 respectively). This result could be attributed to the simultaneous consumption of glucose and lactate to produce H₂. Consistently, Kim et al. [11] also reported HPR increase after lactate addition from 11 to 178 mM.

297 **Lag phase -** λ

Inhibitory threshold of lag phase was < 50 mM for the three acids (ANOVA, p =
0.0003, 0.039, 0.0097 for acetate, butyrate and lactate addition, respectively).
Butyrate caused the highest lag phases, with a 3.5-fold increase from 0 to 250 mM,
compared to a 2.6- and a 1.4-fold increase with the addition of 250 mM of acetate
and lactate, respectively.

Consistently, Siqueira and Reginatto [32] found an inhibitory threshold value for lag phase of 42 mM of acetate and Wang et al. [22] reported a value lower than 83 mM. Concerning butyrate and lactate, inhibitory threshold of lag phase was estimated at 95 mM and 89 mM, respectively [11,33]. In conclusion, the present results are consistent with an inhibitory threshold of the lag phase below 100 mM in batch for acetate, butyrate and lactate.

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3.2. Hydrogen production rate inhibition modelling

Inhibition thresholds indicate the concentrations at which acids have an effect on 311 312 bacterial physiology. However, they do not provide information on the extent of the inhibitory effect as a function of acid concentration. To access this information, HPR 313 modelling was performed according to (Equation 2). Results of the inhibition 314 315 modelling from this study and from literature data in mixed cultures are presented in Table 2. Inhibition of HPR by 50 % (half maximal inhibitory concentration, Kc) was 316 achieved for 209 mM of acetate, 104 mM of butyrate and 273 mM of lactate. Again, 317 butyrate shows the highest inhibitory impact, and acetate the lowest. Total inhibition 318 of HPR and H₂ production was achieved at values named Cmax shown in Table 2 319 320 (i.e, at 300 mM of acetate, 200 mM of butyrate and 400 mM of lactate).

321 To the authors knowledge, Kc of 209 mM of acetate found in the present study 322 is the highest value found in the literature for mixed cultures. Siqueira and Reginatto ,

Wang et al. and Wang et al. [6,22,32] found Kc of 86, ~ 80 mM and 157 mM of acetate at pH 6, 7 and 5.5, respectively. Unfavourable pH conditions [6,32] and the use of sucrose as a substrate [22], a sugar which requires hydrolytic activities for its degradation and therefore a more diverse microbial community than for glucose degradation, could explain the differences observed.

The higher inhibitory impact of butyrate on HPR with regards to acetate found in this 328 329 study is consistent with the study of Van Ginkel and Logan and Zhang et al. [7,37]. In contrast, Kc of 104 mM of butyrate was 2-fold lower than the Kc of ~ 225 mM 330 estimated from Wang et al. [6]. The latter is close to the Kc of 220 mM estimated from 331 332 Zheng and Yu [33], although initial pH varied, set at 6 and 7, respectively. Chen et al. [17] observed a highly lower Kc of 17 mM of butyrate at pH 6, but, again, pH may 333 have been potentially insufficiently buffered (48 mM NaHCO3 with 10 g·L⁻¹ glucose). 334 Somehow, the microbial community composition may affect resistance to organic 335 acids, as suggested by Chen et al. [17] who investigated the impact of butyric acid in 336 337 two studies; indeed, under the same operating conditions, a distinct inhibition of the H_2 production is reported [6,17]. 338

Regarding lactate, 44 mM of L-Lactate addition by Noblecourt et al. [10] resulted in a reduction of 41 % of HPR, decreasing from 2.36 L.h⁻¹ to 1.39 L.h⁻¹. Such effect of lactate is much more detrimental than the effect reported in the present study, as 250 mM of lactate was needed to lower the HPR by 39%.

	Table 2 - Inhibit	ion parameters of m initial pH of fe	naximum rmentatio	hydrogen n in this s	produc study an	tion rate HPR by acids and d in the literature	d associated
Inhibitor	Inoculum	HPR max	Kc (mM)	Cmax (mM)	n	Initial pH - Regulation	Reference
	Freeze-dried activated sludge	93 mL∙h ⁻¹	209	300	7.56	6 – Buffered with 100mM MES	This study
Acetate	Sludge from UASB treating vinasse	8.7 ± 0.3 mL⋅h ⁻¹	86	167	/	6 - None	[32]
	Sludge from USAB treating citrate-producing wastewater	221.7 mL⋅gVSS⁻ ¹ ⋅h⁻¹	157	>833	1.52	5.5 - Regulated	[22]
	Clostridium bifermentans,	58 mL·L·h ⁻¹	/	502	0.52	7 - None	[37]

	cultivated with 30g/L NaCl, isolated from anaerobic digester of WWTP						
	Anaerobic sludge adapted for cultivation at 70°C	~ 70 mL·L·h ⁻¹	/	>200	/	7, Buffered with 20 mM MOPS	[38]
	Anaerobic sludge	12.9 mL∙h ⁻¹	~80	471	2.9	7 - 48mM NaHCO ₃	[6]
	Freeze-dried activated sludge	100 mL⋅h ⁻¹	104	200	3.07	6– Buffered with 100mM MES	This study
Buturata	Anaerobic sludge from WWTP	61.5 ml⋅gVSS ⁻¹ ⋅h ⁻¹	220	291	0.34	6 – Buffered with 59 mM H_2PO4^- and $HPO_4^{2^-}$	[33]
Битугате	Sludge from anaerobic digester	112 mLH₂·L ⁻¹ ·h ⁻¹	~225	306	0.6	7 - 48mM NaHCO₃	[6]
	Sludge from anaerobic digester	42 mLH ₂ ·L ⁻¹ ·h ⁻¹	~284	>284	/	7 - 48mM NaHCO ₃	[17]
	Clostridium bifermentans	60.1mL·L·h ⁻¹		334	2.35	7	[37]
	Sludge from anaerobic digester	$27mLH_2 \cdot L^{-1} \cdot h^{-1}$	~17	~34	/	6 - 48mM NaHCO ₃	[17]
Lactate	Freeze-dried activated sludge	102 mL∙h ⁻¹	273	400	7.58	6 – Buffered with 100mM MES	This study
	Derived mix of thermophilic sludge and sludge from WWTP, enriched with <i>Clostridium</i> <i>cellulolyticum</i>	2360mL·h ⁻¹	~50	>50	/	6 - Regulated	[10]

343

344 **3.3.** Glucose removal

Glucose removal, an indicator of microbial activity, was calculated as a ratio of glucose consumed to initial glucose, in percentage, and presented in Fig. 1 a. Without acid addition, glucose consumption was complete, as it reached 100 ± 0 348 %.



Fig. 1 - Effects of acetate, butyrate and lactate on metabolic activity. (a) mean glucose removal (%) \pm standard deviation. Mean yields of products \pm standard deviation as a function of acetate (b), butyrate (c) and lactate (d) concentrations. Yields were calculated in COD of products (H2, acetate, butyrate and lactate) per COD of consumed glucose and consumed exogenous added acid (viz. glucose + acetate consumed, glucose + butyrate consumed and glucose + lactate consumed for (b), (c) and (d) respectively).

349

Acetate concentrations from 50 to 250 mM did not influence glucose removal, which was only slightly affected at 300 mM ($89 \pm 2 \%$). This fact suggested that the global microbial activity was only slightly affected by acetate. In contrast, Wang et al. [22] reported a threshold value for the reduction of sucrose removal estimated at < 83 354 mM acetate. Wang et al. [6] found an inhibitory threshold of glucose removal at a 355 concentration of acetate lower than 10 mM.

Regarding butyrate, a concentration of 100 mM was estimated as the threshold value for inhibition of glucose removal (ANOVA, p = 0.02). Above this concentration, a linear dose-dependent inhibition of glucose removal was observed, reaching 16 ± 3 % at 250 mM. Consistently, Zhang et al. [37] showed that in presence of 250 mM butyrate, glucose removal was only 18 % while it was still 76 % in the presence of 250 mM acetate.

In contrast, Chen et al. [17] showed that at pH 6, the inhibitory threshold for glucose removal with butyrate was as low as 6 mM, but glucose removal was already low in control conditions, reaching ~ 45 %. Wang et al. [6] also found a low inhibitory threshold for glucose removal at a concentration of butyrate < 10 mM, pH 7, but the extent of the inhibition was far lower than in the present study, since more than 70 % of the substrate was still consumed in presence of 300 mM of butyrate. In contradiction, Zheng and Yu [33] assessed this threshold around 190 mM.

Finally, the threshold for glucose removal inhibition by lactate was 50 mM (ANOVA, p = 0.000747), with 79 \pm 6 % at 100 mM and 61 \pm 3 % at 400 mM. Similarly, the addition of 222 mM lactate also reduced glucose degradation by *Clostridium* saccharoperbutylacetonicum from 85 % to 47.5 % [39].

In comparison, Kim et al. [11] did not find any effect of lactate on glucose removalup to 178 mM.

Therefore, glucose removal was hence affected differently depending on the nature of the acid and its concentration. The reduction in H_2 production in the presence of butyrate and lactate can already be explained, at least in part, by a

378 reduction in glucose consumption, but the inhibitory effect of 100-200 mM acetate
379 must be explained by other mechanisms, such as alteration of metabolic pathways or
380 microbial communities.

381 **3.4.** Metabolic pathways

For each flask, a COD mass balance was performed at the end of the H_2 production phase, and varied between 78 and 112 %, with an average of 97 ± 6 % (Supplementary material 4). These results clearly show that all major metabolites were considered in the analysis.

386 Considering the concentrations of acetate, butyrate and lactate at the end of the experiment, it was observed that a partial consumption of the added acids occurred 387 during the fermentation. It was not surprising to observe lactate [8] and acetate 388 [32,35] consumption, but the decrease in butyrate concentration was more surprising, 389 although Chen et al. [17] also observed it. Metabolic pathways were investigated 390 taking into account the consumption of glucose and of the exogenously added acid 391 and calculating yields in gCOD gCOD⁻¹ (Fig. 1 b - d). Without acid addition (i.e., 392 glucose is the only source of substrate), H₂ yield reached 0.13 \pm 0.02 gCOD gCOD⁻¹ 393 $(1.6 \pm 0.2 \text{ mol} \cdot \text{mol}_{alucose}^{-1})$ and acetate and butyrate were the major products, with 394 $0.09 \pm 0.02 \text{ gCOD} \cdot \text{gCOD}^{-1} (14 \pm 3 \text{ mM}, 0.28 \pm 0.05 \text{ mol} \cdot \text{mol}_{\text{glucose}^{-1}}) \text{ and } 0.52 \pm 0.04$ 395 $gCOD \cdot gCOD^{-1}$ (30 ± 3 mM, 0.59 ± 0.06 mol·mol_{alucose}⁻¹), respectively. Other 396 metabolites were notably produced but in smaller quantities: lactate, formate, 397 propionate, succinate and butanol. 398

Metabolic pathways were greatly influenced by acid addition. A same trend was observed for increasing addition of acetate and butyrate, with a progressive decline of acetate and butyrate pathways in favour of lactate pathway, associated with a

decrease in H_2 yield. Ultimately, for the three acids, increasing concentration resulted in a total shift from acetate/butyrate to lactate fermentation, i.e, at 300 mM of acetate, 200 mM of butyrate and 400 mM of lactate, which coincides with the previously reported concentration associated with a total inhibition of H_2 production in this study.

406 Acetate addition induced a specific decrease of acetate production pathway. Indeed, butyrate-to-acetate (B/A, mol/mol) ratio was 2.1 ± 0.1 without acid addition, 407 408 and increased up to 21 at 100 mM. Above 100 mM acetate, endogenous acetate reached a maximum of 4.6 mM and was often consumed, while it was 15 ± 2 mM 409 without acid addition. This specific inhibition of acetate pathway and its consumption 410 411 was already observed elsewhere [6,32,35]. Such total inhibition of the acetate pathway (Fig. 1 - b) was not associated with a total inhibition of the butyrate 412 pathway. 413

Butyrate addition caused a reduction of the butyrate pathway, but less selective 414 415 as B/A decreased from 2.6 \pm 1.1 to 1.8 \pm 0.5 above 100 mM butyrate. Above 150 mM 416 butyrate, butyrate production was restricted to a maximum of 11 mM, while it was 31 ± 3 mM without acid addition. Interestingly, when butyrate pathway was totally 417 inhibited, acetate pathway was also totally suppressed. This observation is consistent 418 with the idea supported by Van Ginkel and Logan [7] suggesting that the reduction of 419 butyrate pathway is more deleterious for the cell due to the reduction of NAD+ 420 regenerating pathways. Indeed, butyrate production allows the regeneration of NAD+ 421 through Crotonyl coA reduction, Acetoacetyl coA reduction and H₂ production while 422 acetate production allow this regeneration only through H₂ producing pathways. To 423 ensure adequate regeneration of NAD+ when butyrate pathway is thermodynamically 424 restricted due to an excess of butyrate, electrons are likely redirected towards the 425

426 production of solvent, such as lactate or propionate [7]. Some of the lactate observed427 in presence of acids could be produced through this mechanism.

Conversely, Lactate from 0 to 250 mM had a low impact on metabolic spectrum as it reduced only slightly the butyrate yield from $0.53 \pm 0.03 \text{ gCOD} \cdot \text{gCOD}^{-1}$ to $0.43 \pm$ 0.08 gCOD · gCOD⁻¹ and the H₂ yield from 0.14 ± 0 gCOD · gCOD⁻¹ to 0.12 ± 0.0 gCOD · gCOD⁻¹. However, above 250 mM of lactate, H₂, butyrate and acetate yield decreased as lactate yield increased, as for acetate and butyrate addition.

In addition, endogenous lactate production and lactate yields at 200 mM of acetate and 100 mM of butyrate, i.e at concentrations close to the K_c of 209 mM of acetate and 104 mM of butyrate, were 50 ± 12 mM, 0.47 ± 0.1 gCOD·gCOD⁻¹ and 42 ± 20 mM, 0.41 ± 0.19 gCOD·gCOD⁻¹, respectively. In other words, 50 % inhibition of HPR in presence of acetate and butyrate was associated with a similar lactate production induction.

In conclusion, metabolic pathways were significantly affected by the addition of organic acids, and the inhibition was strongly related to the nature and concentration of the added acid. These results show that inhibition by organic acids in mixed culture cannot be explained solely by undissociated acid concentrations. Analyses of bacterial communities was then performed to distinguish cellular metabolic pathways alteration and microbial communities alteration caused by organic acids, which is currently poorly understood.

446 **3.5. Bacterial communities**

2714 OTUs were identified in all the experiments and grouped in 33 phyla, 70
classes, 153 orders, 310 families and 657 genera. Only three classes showed a
relative abundance higher than 1 %: Clostridia, Bacillii and Gammaproteobacteria.

Among them, 12 genera showed a relative abundance higher than 1 % and only 9
genera showed a relative abundance higher than 10 %. After rarefication, 477 OTUs
were kept, grouped in 12 phyla, 28 classes, 63 orders, 127 family and 198 genera.

Fig. 2 - Bacterial community analysis. Effects of acetate, butyrate and lactate on (a) pielou and (b) richness indexes. (c) Mean relative abundance of bacteria at family level depending on the concentration of acetate, butyrate and lactate.



Acid concentration had a significant negative effect on sample evenness (Kruskal 456 Wallis, p = 0.002 for pielou index) and an insignificant effect on sample richness (32) 457 \pm 11 species considering all samples, Kruskal Wallis, p = 0.27) (Fig. 2 a, b). This 458 result means that acid addition did not reduce the number of species in the microbial 459 community, but favoured an uneven growth of the species present. In comparison, 460 Chen et al. [17] found that inhibition of H₂ production by butyrate was associated with 461 an increase in microbial diversity but a decrease in richness. These differences can 462 be explained by the higher richness in Chen et al. [17] experiments, which they 463 estimated with the Chao1 index to be 132 ± 28 in the control conditions, whereas we 464 465 estimate Chao1 to be 32 ± 5 in the control experiments of this study. The lower richness in the present study might be due to the combination of inoculum storage 466 process (freeze-drying and storage at - 80 °C) and of the pretreatment (15 min at 90 467 468 °C) carried, while Chen et al. (2021a) only performed a 15 min pretreatment at 100 °C. 469

470 Microbial diversity at family level is presented in Fig. 2 c, depending on the nature and the concentration of added acid. With no acid addition, Clostridiaceae family 471 represented 78 ± 11 % of the microbial community. This is consistent with high 472 abundances of the Firmicutes phylum and *Clostridiaceae* family in high-yielding H₂ 473 producing reactor as reported by Etchebehere et al. [40]. In addition to the strong 474 dominance of Clostridiaceae family, bacteria from the Bacillaceae, Lactobacillaceae 475 and Aeromonadaceae families are also emerging in a variable extent, from 4 to 13 %, 476 0 to 17 % and 0 to 19 %, respectively. Such variability in minor OTUs is not unusual 477 478 in mixed culture [41] and is not associated in this study with significant differences in metabolic products. 479

At a concentration at which a total inhibition of H₂ production was observed, i.e., 300 mM, 200 mM and 400 mM for acetate, butyrate and lactate addition respectively, the microbial community analysis revealed a drastic shift in families relative abundances. 300 mM of acetate resulted in 87 \pm 3 % *Lactobacillaceae*. 200 mM of butyrate led to 98 % *Bacillaceae* while 250 mM of butyrate led to 71 % *Bacillaceae* and 27 % *Enterococcaceae*. 400mM of lactate induced the selection of 98.9 \pm 0.1 % *Lactobacillaceae* in 3 flasks and the growth of 89 % *Enterococcaceae* in one flask.

Below Cmax, trends at family level are not fully clear, as *Clostridiaceae* accounted in 487 average for more than 50 % of the bacterial community, in all conditions excepted at 488 200 mM of acetate. Therefore, the impact of acid addition was investigated at genus 489 level (Table 3). Addition of acetate, butyrate or lactate below Cmax inhibited 490 Clostridium sensu stricto 11 growth (OTU 4, Clostridium neuense / acetobutylicum / 491 hydrogeniproducens, 99.5 % identity), as its abundance decreased from 29 \pm 8 % in 492 control conditions to 2 ± 3 %. Also, Bacillus (OTU 10, Bacillus thuringiensis 99.3% 493 494 identity) was inhibited by the addition of acetate, butyrate or lactate as its abundance decreased from 8 ± 4 % to 0 % below Cmax. In contrast, Rumellibacillus (OTU 12, 495 Rummeliibacillus pycnus 99.8 % identity) abundance increased as acetate 496 497 concentration increased, from 0 % to 8 % below Cmax. Bacillus sp. and Lactobacillus sp. favoured in presence of high concentration of acids were identified as 498 Weizmannia coagulans (100 % identity) and Lactobacillus plantarum (97.9 % 499 identity), respectively. Interestingly, acetate, butyrate and lactate addition did not 500 inhibit the emergence of Clostridium_sensu_stricto_1 (OTU 1, C. butyricum, 98.5 % 501 identity) as its abundance reached 45 ± 8 % in control conditions and varied between 502 0.1 % and 83.4 % at 250 mM of acetate, 150 mM of butyrate and 300 mM of lactate. 503 Acid addition could even favour the growth of C. butyricum as its abundance reached 504

505 57 % for 150 mM of acetate, 66 % for 50 mM of butyrate and 91 % for 250 mM of 506 lactate.

From these results, it was hypothesised that the diminution in abundance of *Clostridium sp.* (OTU 4) and the emergence of *L. plantarum* and *W. coagulans* were responsible for the diminution of the H_2 yield at concentrations below Cmax. Globally, the emergence of *C. butyricum* instead of *Clostridium sp.* (OTU 4) below Cmax, did not permit to maintain H_2 yield although the abundance in *Clostridiaceae* was stable.

Interestingly, H_2 yield reached 0.11 gCOD gCOD⁻¹ when the community was 512 composed of 53 % C. butyricum and 26 % Clostridium sp. (OTU 4) (at 50 mM of 513 lactate) and when the community was composed of 84 % C. butyricum and 1 % 514 Clostridium sp. (OTU 4) (at 150 mM of lactate). This result show that the same H₂ 515 yield can be reached with and without Clostridium sp. (OTU 4), due to the growth of 516 C. butyricum. In addition, 25 mM of butyrate resulted in the selection of 21 % W. 517 coagulans and 53 % C. butyricum with a lactate yield of 0.07 gCOD gCOD⁻¹ 518 519 (producing 7 mM of lactate), while at 100 mM of butyrate 13% W. coagulans, 5 % L. plantarum and 55 % C. butyricum with a lactate yield of 0.44 gCOD gCOD⁻¹ 520

Condition	on, all replicates centration of ed acid (mM)	Clostridium butyricum (%)	Clostridium sp. (OTU 4) (%)	Clostridium sp. (%)	cted are present Weizmannia coagulans(%)	ed and separate Lactobacillus plantarum (%)	Enterococcus hirae (%)	ne. Bacillus thuringiensis (%)	Rummeliibacillus pycnus (%)	Others (%
	0	35 43	29 22	65 66	1 1	0 0	0 0	3 7	0 0	32 26
	50	39 59	7 9	49 73	0 11	0 3	49 12	0 0	0 0	2 1
cetate	100	49 63	7 4	58 67	29 17	9 14	3 0	0 0	1 1	1 1
	150	52 61	12 1	65 63	19 12	14 12	0 12	0 0	1 1	1 0
Ă	200	51 11 41	1 2 0	52 29 42	10 8 8	35 60 48	0 0 1	0 0 0	3 2 2	0 0 0
	250	68 0	8 1	76 1	8 20	10 67	1 0	0 0	5 11	0 1
	300	0 0	0 0	1 0	5 7	91 84	0 0	0 0	3 8	1 1
	0	37 53	17 35	74 88	4 1	17 0	0 0	4 9	0 0	0 2
	25	53 55	23 2	77 72	21 24	0 0	1 0	0 1	0 0	1 2
fe	50	61 71	14 21	76 92	23 6	0 0	0 0	0 0	0 0	1 2
tyra	100	70 40 56	16 3 19	86 53 75	1 35 13	6 8 5	1 3 0	0 0 0	0 0 0	5 1 6
Bu	150	0 65	0 3	0 69	98 31	0 0	0 0	0 0	0 0	2 0
	200	0	0	0	98	0	0	0	0	1
	250	0	0	0	71	0	27	0	0	2
	0	54 48	32 40	86 88	0 0	0 0	0 0	13 11	0 0	1 1
	50	38 52 55	29 28 25	97 95 89	0 0 0	0 0 0	0 2 10	0 1 1	0 0 0	2 2 1
e	100	77 77 61	3 0 6	84 78 67	0 0 0	14 18 29	0 0 0	1 3 2	0 0 0	1 1 2
Ictat	150	84 84	3 0	89 86	0 0	9 8	0 4	1 1	0 0	0 1
Ľ	250	86 86 99	0 0 0	87 86 99	1 1 0	12 13 0	0 0 0	0 0 0	0 0 0	1 1 0
	300	0 18 83 78	0 0 0 0	68 19 83 79	31 27 1 7	0 54 15 4	0 0 0 9	0 0 0 0	0 0 0 0	0 1 1 0
	400	0 0 0 0	0 0 0 0	0 0 0 0	0 0 0 0	99 99 9 99	0 0 89 0	0 0 0 0	0 0 0 0	1 1 1 1

(producing 44mM of lactate) was observed. As it is hardly possible that 5 % L. 521 plantarum would be responsible for the 6-fold improvement in lactate concentration 522 and yield, this result suggests that some lactate was produced by C. butyricum. 523 Considered all together, these results suggest that C. butyricum shifted its 524 metabolism from acetate/butyrate pathway to lactate pathway in presence of acids. 525 The comparison of spearman correlation coefficient between H₂ yield and *Clostridium* 526 sp. (OTU 4) abundance ($\rho = 0.59$, p-value = 6.53×10^{-5}) on one hand and between 527 H_2 yield and *C. butyricum* abundance ($\rho = 0.16$, p-value = 0.32) in another hand 528 reinforced this hypothesis. This metabolic shift could be explained by the perturbation 529 of the NADH/NAD+ ratio after acid addition [42]. This hypothesis is consistent with 530 the findings of Payot et al. [43], who showed that *Clostridium cellulolyticum* shifted its 531 532 metabolism from acetate-butyrate pathways to lactate in case of accumulation of intracellular NADH. 533

To decipher the impact of acid addition at populational or metabolic levels, 534 bacterial communities of each sample were compared qualitatively (i.e. considering 535 which species grew) and quantitatively (i.e. at what relative abundance). This beta 536 diversity analysis was performed by calculating the distance between microbial 537 communities at genus level in pairs (UniFrac distance metric) and then by applying a 538 hierarchical clustering method to the distance matrix (Unweighted pair group method 539 540 with arithmetic mean, UPGMA). The result is presented as a dendrogram in Fig. 3. Nine clusters were distinguished and bootstrapping (n=10,000) revealed that these 541 clusters were strongly supported by the data (approximately unbiased probability 542 543 value > 95 %). In this Figure, the distance between two microbial communities is represented by the height of the dendrogram. 544

All conditions for which no H₂ production was observed are grouped in the 545 cluster 8. This cluster 8 is subdivided in two clusters, with samples associated to 546 butyrate addition on one side, and samples associated to acetate or lactate addition 547 on the other side. This observation is consistent with the observations of populational 548 shifts above Cmax. In addition, samples with no acid addition or in presence of 50 549 mM butyrate and 50 mM lactate were grouped in cluster 2. The operating conditions 550 of the communities grouped in this cluster are those associated with the highest H_2 551 production performances, with 207 \pm 13 mLH₂/g_{alucose added}. Thus, for the extreme 552 conditions of high H_2 production and total inhibition of H_2 production, the 553 performances were clearly associated to populational shifts with clear and selection 554 of distinct microbial communities. 555



Fig. 3 - Bootstrapped dendrogram of Beta diversity. Booststrap probability value (BP) and approximately unbiased probability values (AU) appear in green and red respectively above each node. Clusters associated with an AU > 95 % circled in blue and numbered from 1 to 9. The maximal volume of cumulated H₂ per gram of glucose added (Hc, mLH₂/g_{glucose added}) measured in each condition are presented. For each sample, the added acid is abbreviated as "La", "Bu" and "Ac" for lactate, butyrate and acetate respectively. The initial concentration of the added acid is indicated between two underscores. The end number, from 1 to 4, is used to distinguish the replicates.

Interestingly, almost all samples with an exogenous addition of lactate at 100 557 to 300 mM and with H₂ yield between 110 mLH₂/g_{alucose added} and 158 mLH₂/g_{alucose} 558 added are grouped in cluster 3, with a low height between each sample (< 0.1). 559 Therefore, it was concluded that the inhibition of H₂ production by adding lactate from 560 100 mM to 300 mM was not related to population changes but to a lower substrate 561 degradation only. In addition, clusters 4, 5, 7 and 9 do not group samples sharing a 562 563 similar H₂ production performance. For example, cluster 7 groups three samples in presence of 100 and 150 mM of acetate, although H₂ production varies from 118 564 $mLH_2/g_{glucose added}$ to 161 $mLH_2/g_{glucose added}$ within these conditions. Thus, the 565 566 differences in H₂ yield within these conditions are not due to changes in populations, 567 but more probably to changes in metabolic pathways. These results support again the conclusion that below Cmax, a combination of metabolic shifts and to a lesser 568 569 extent populational changes explained the observed reduction in H₂ yield.

Inhibition by organic acids is one of the main causes of low H₂ production during DF in mixed cultures [5] and a deeper understanding of the mechanisms behind these inhibitions will contribute to select appropriate solutions to relieve this inhibition. Indeed, inhibition associated with metabolic shifts within a bacterial community could be addressed with acid tolerance response induction [44] or with organic acids extractions.

However, acid extraction, although often chosen, can be a major source of process failure due to the formation of cake layer or fouling and increase the energy and financial input [45]. Alternatively, inhibition associated with a populational shift could be mitigated at a lower cost and more easily through operational parameters modification (pH, temperature, organic loading rate) to disfavour the undesirable bacteria or with bioaugmentation with H₂-producing strains. Thus, the present study

highlights that above 250 mM of acetate, 150 mM of butyrate and 300 mM of lactate,
the strategies implemented to alleviate inhibition must address the finding that
populational change is the main factor responsible for a decrease in H₂ production.

585 **4.** Conclusions

In this study, the initial addition of acetate, butyrate and lactate in DF was 586 investigated. A significant reduction on H₂ production was shown. Butyrate and 587 lactate affected glucose removal, whereas 100 % glucose degradation efficiency was 588 observed at high acetate concentration of 250 mM. For all acids, significant 589 diminution of bacterial diversity was observed when increasing the concentration. 300 590 mM of acetate, 200 mM of butyrate and 400 mM of lactate resulted in total 591 community shift through the inhibition of Clostridiaceae growth in favour of 592 593 Lactobacillaceae and Bacillaceae. Below these concentrations, metabolic changes were mostly responsible of the decrease in H₂ production performances. More 594 595 specifically, C. butyricum was suspected to shift its metabolism towards lactate production. Overall, this work shows that both the nature and the concentration of the 596 inhibitors should be considered, as well as the microbial communities involved in the 597 process. These new insights on the mechanisms of inhibition by end-products in 598 mixed culture can be useful to efficiently select strategies for overcoming inhibition. 599

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- 605
- 6. CRediT authorship contribution statement

- 606 M. Noguer: Investigation, formal analysis, visualization, writing original draft.
- R. Escudie: Conceptualization, supervision, validation, writing review & editing
- 608 N.Bernet : Validation, writing review & editing.
- 609 E. Trably: Conceptualization, funding acquisition, supervision, validation, writing -
- 610 review & editing.
- 611 7. Declaration of Competing Interest
- The authors declare that they have no known competing financial interests or
- 613 personal relationships that could have appeared to influence the work reported in this
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615 8. References

- 616 [1] Dincer I, Acar C. Review and evaluation of hydrogen production methods for
 617 better sustainability. Int J Hydrogen Energy 2014;40:11094–111.
 618 https://doi.org/10.1016/j.ijhydene.2014.12.035.
- ⁶¹⁹ [2] Łukajtis R, Hołowacz I, Kucharska K, Glinka M, Rybarczyk P, Przyjazny A, et
 ⁶²⁰ al. Hydrogen production from biomass using dark fermentation. Renew Sustain
 ⁶²¹ Energy Rev 2018;91:665–94. https://doi.org/10.1016/j.rser.2018.04.043.
- [3] Hawkes FR, Hussy I, Kyazze G, Dinsdale R, Hawkes DL. Continuous dark
 fermentative hydrogen production by mesophilic microflora: Principles and
 progress. Int J Hydrogen Energy 2007;32:172–84.
 https://doi.org/10.1016/j.ijhydene.2006.08.014.
- [4] Castelló E, Nunes Ferraz-Junior AD, Andreani C, Anzola-Rojas M del P,
 Borzacconi L, Buitrón G, et al. Stability problems in the hydrogen production by
 dark fermentation: Possible causes and solutions. Renew Sustain Energy Rev
 2020;119:109602. https://doi.org/10.1016/j.rser.2019.109602.
- 630 [5] Chen Y, Yin Y, Wang J. Recent advance in inhibition of dark fermentative
 hydrogen production. Int J Hydrogen Energy 2021;46:5053–73.
 https://doi.org/10.1016/j.ijhydene.2020.11.096.
- [6] Wang B, Wan W, Wang J. Inhibitory effect of ethanol, acetic acid, propionic
 acid and butyric acid on fermentative hydrogen production. Int J Hydrogen
 Energy 2008;33:7013–9. https://doi.org/10.1016/j.ijhydene.2008.09.027.
- 636 [7] Van Ginkel S, Logan BE. Inhibition of biohydrogen production by undissociated
 637 acetic and butyric acids. Environ Sci Technol 2005;39:9351–6.
 638 https://doi.org/10.1021/es0510515.

- [8] García-Depraect O, Castro-Muñoz R, Muñoz R, Rene ER, León-Becerril E,
 Valdez-Vazquez I, et al. A review on the factors influencing biohydrogen
 production from lactate: The key to unlocking enhanced dark fermentative
 processes. Bioresour Technol 2021;324:124595.
 https://doi.org/10.1016/j.biortech.2020.124595.
- Baghchehsaraee B, Nakhla G, Karamanev D, Margaritis A. Effect of extrinsic
 lactic acid on fermentative hydrogen production. Int J Hydrogen Energy
 2009;34:2573–9. https://doi.org/10.1016/j.ijhydene.2009.01.010.
- [10] Noblecourt A, Christophe G, Larroche C, Fontanille P. Hydrogen production by
 dark fermentation from pre-fermented depackaging food wastes. Bioresour
 Technol 2018;247:864–70. https://doi.org/10.1016/j.biortech.2017.09.199.
- [11] Kim TH, Lee Y, Chang KH, Hwang SJ. Effects of initial lactic acid
 concentration, HRTs, and OLRs on bio-hydrogen production from lactate-type
 fermentation. Bioresour Technol 2012;103:136–41.
 https://doi.org/10.1016/j.biortech.2011.09.093.
- [12] Baronofsky JJ, Schreurs WJA, Kashket ER. Uncoupling by acetic acid limits
 growth and acetogenesis by *Clostridium thermoaceticum*. Appl Environ
 Microbiol 1984;48:1134–9. https://doi.org/10.1128/aem.48.6.1134-1139.1984.
- [13] Russell JB. Another explanation for the toxicity of fermentation acids at low pH:
 anion accumulation versus uncoupling. J Appl Bacteriol 1992;73:363–70.
 https://doi.org/10.1111/j.1365-2672.1992.tb04990.x.
- [14] van Niel EWJ, Claassen PAMM, Stams AJMM. Substrate and product inhibition
 of hydrogen production by the extreme thermophile, *Caldicellulosiruptor saccharolyticus*. Biotechnol Bioeng 2003;81:255–62.
 https://doi.org/10.1002/bit.10463.
- [15] Eklund T. The antimicrobial effect of dissociated and undissociated sorbic acid
 at different pH levels. J Appl Bacteriol 1983;54:383–9.
 https://doi.org/10.1111/j.1365-2672.1983.tb02632.x.
- [16] Kovanda L. In vitro antimicrobial activities of organic acids and their derivatives
 on several species of gram-negative and Gram-positive bacteria. Molecules
 2019;24:3770. https://doi.org/10.3390/molecules24203770.
- [17] Chen Y, Yin Y, Wang J. Influence of butyrate on fermentative hydrogen
 production and microbial community analysis. Int J Hydrogen Energy
 2021;46:26825–33. https://doi.org/10.1016/j.ijhydene.2021.05.185.
- [18] Noblecourt A, Christophe G, Larroche C, Santa-Catalina G, Trably E, Fontanille
 P. High hydrogen production rate in a submerged membrane anaerobic
 bioreactor. Int J Hydrogen Energy 2017;42:24656–66.
 https://doi.org/10.1016/j.ijhydene.2017.08.037.
- [19] Dauptain K, Schneider A, Noguer M, Fontanille P, Escudie R, Carrere H, et al.
 Impact of microbial inoculum storage on dark fermentative H₂ production.
 Bioresour Technol 2021;319:124234.
- 680 https://doi.org/10.1016/j.biortech.2020.124234.
- [20] Bundhoo MAZ, Mohee R, Hassan MA. Effects of pre-treatment technologies on

- 682dark fermentative biohydrogen production: A review. J Environ Manage6832015;157:20-48. https://doi.org/10.1016/j.jenvman.2015.04.006.
- Wang H, Fang M, Fang Z, Bu H. Effects of sludge pretreatments and organic
 acids on hydrogen production by anaerobic fermentation. Bioresour Technol
 2010;101:8731–5. https://doi.org/10.1016/j.biortech.2010.06.131.
- [22] Wang Y, Zhao QB, Mu Y, Yu HQ, Harada H, Li YY. Biohydrogen production
 with mixed anaerobic cultures in the presence of high-concentration acetate. Int
 J Hydrogen Energy 2008;33:1164–71.
 https://doi.org/10.1016/j.ijhydene.2007.12.018.
- [23] Park W, Hyun SH, Oh S-E, Logan BE, Kim IS. Removal of Headspace CO₂
 Increases Biological Hydrogen Production. Environ Sci Technol 2005;39:4416–
 20. https://doi.org/10.1021/es048569d.
- 694 [24] Chang S, Li J, Liu F, Yu Z. Effect of different gas releasing methods on
 695 anaerobic fermentative hydrogen production in batch cultures. Front Environ
 696 Sci Eng China 2012;6:901–6. https://doi.org/10.1007/s11783-012-0403-1.
- 697 [25] APHA. Standard Methods for the Examination of Water and Wastewater. vol.698 20th ed. 2017.
- 699 [26] Lakatos G. Biological wastewater treatment. 2018.700 https://doi.org/10.1201/b18368-4.
- [27] Braga Nan L, Trably E, Santa-Catalina G, Bernet N, Delgenès JP, Escudié R.
 Biomethanation processes: New insights on the effect of a high H₂ partial
 pressure on microbial communities. Biotechnol Biofuels 2020;13:1–17.
 https://doi.org/10.1186/s13068-020-01776-y.
- [28] Kahm M, Hasenbrink G, Lichtenberg-Fraté H, Ludwig J, Kschischo M. Grofit:
 Fitting biological growth curves with R. J Stat Softw 2010;33:1–21.
 https://doi.org/10.18637/jss.v033.i07.
- [29] Lozupone C, Knight R. UniFrac: A new phylogenetic method for comparing
 microbial communities. Appl Environ Microbiol 2005;71:8228–35.
 https://doi.org/10.1128/AEM.71.12.8228-8235.2005.
- [30] Cope EK, Goldberg AN, Pletcher SD, Lynch S V. Compositionally and
 functionally distinct sinus microbiota in chronic rhinosinusitis patients have
 immunological and clinically divergent consequences. Microbiome 2017;5:1–
 16. https://doi.org/10.1186/s40168-017-0266-6.
- [31] McMurdie PJ, Holmes S. Phyloseq: An R Package for Reproducible Interactive
 Analysis and Graphics of Microbiome Census Data. PLoS One 2013;8:e61217.
 https://doi.org/10.1371/journal.pone.0061217.
- [32] Siqueira MR, Reginatto V. Inhibition of fermentative H₂ production by hydrolysis
 byproducts oflignocellulosic substrates. Renew Energy 2015;80:109–16.
 https://doi.org/10.1016/j.renene.2015.01.070.
- [33] Zheng XJ, Yu HQ. Inhibitory effects of butyrate on biological hydrogen
 production with mixed anaerobic cultures. J Environ Manage 2005;74:65–70.
 https://doi.org/10.1016/j.jenvman.2004.08.015.

- [34] Suresh A, Grygolowicz-Pawlak E, Pathak S, Poh LS, Abdul Majid M bin,
 Dominiak D, et al. Understanding and optimization of the flocculation process in
 biological wastewater treatment processes: A review. Chemosphere
 2018;210:401–16. https://doi.org/10.1016/j.chemosphere.2018.07.021.
- [35] Colin T, Bories A, Lavigne C, Moulin G. Effects of acetate and butyrate during
 glycerol fermentation by *Clostridium butyricum*. Curr Microbiol 2001;43:238–43.
 https://doi.org/10.1007/s002840010294.
- [36] Heyndrickx M, De Vos P, Vancanneyt M, De Ley J. The fermentation of
 glycerol by *Clostridium butyricum* LMG 1212t2 and 1213t1 and *C. pasteurianum* LMG 3285. Appl Microbiol Biotechnol 1991;34:637–42.
 https://doi.org/10.1007/BF00167914.
- [37] Zhang S, Kim T-H, Lee Y, Hwang S-J. Effects of VFAs concentration on bio hydrogen production with *Clostridium Bifermentans* 3AT-ma. Energy Procedia
 2012;14:518–23. https://doi.org/10.1016/j.egypro.2011.12.968.
- [38] Liu D, Min B, Angelidaki I. Biohydrogen production from household solid waste
 (HSW) at extreme-thermophilic temperature (70 °C) Influence of pH and
 acetate concentration. Int J Hydrogen Energy 2008;33:6985–92.
 https://doi.org/10.1016/j.ijhydene.2008.059.
- [39] Oshiro M, Hanada K, Tashiro Y, Sonomoto K. Efficient conversion of lactic acid to butanol with pH-stat continuous lactic acid and glucose feeding method by *Clostridium saccharoperbutylacetonicum*. Appl Microbiol Biotechnol 2010;87:1177–85. https://doi.org/10.1007/s00253-010-2673-5.
- [40] Etchebehere C, Castelló E, Wenzel J, Del M, Anzola-Rojas P, Borzacconi L, et
 al. Microbial communities from 20 different hydrogen-producing reactors
 studied by 454 pyrosequencing. Appl Microbiol Biotechnol 2016;100:3371–84.
 https://doi.org/10.1007/s00253-016-7325-y.
- [41] Poirier S, Steyer JP, Bernet N, Trably E. Mitigating the variability of hydrogen production in mixed culture through bioaugmentation with exogenous pure strains. Int J Hydrogen Energy 2020;45:2617–26.
 https://doi.org/10.1016/j.ijhydene.2019.11.116.
- [42] Srikanth S, Venkata Mohan S. Regulating feedback inhibition caused by the
 accumulated acid intermediates during acidogenic hydrogen production
 through feed replacement. Int J Hydrogen Energy 2014;39:10028–40.
 https://doi.org/10.1016/j.ijhydene.2014.04.152.
- [43] Payot S, Guedon E, Gelhaye E, Petitdemange H. Induction of lactate
 production associated with a decrease in NADH cell content enables growth
 resumption of *Clostridium cellulolyticum* in batch cultures on cellobiose. Res
 Microbiol 1999;150:465–73. https://doi.org/10.1016/S0923-2508(99)00110-2.
- [44] Huang Z, Yu X, Miao H, Ren H, Zhao M, Ruan W. Enzymatic dynamics of
 microbial acid tolerance response (ATR) during the enhanced biohydrogen
 production process via anaerobic digestion. Int J Hydrogen Energy
 2012;37:10655–62. https://doi.org/10.1016/j.ijhydene.2012.04.116.
- [45] Tharani D, Ananthasubramanian M. Process intensification in separation and
 recovery of biogenic volatile fatty acid obtained through acidogenic

fermentation of organics-rich substrates. Hemical Eng Process Process Intensif
 2021;169:108592. https://doi.org/10.1016/j.cep.2021.108592.