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Eco-design approaches for developping sustainable processes: New opportunities for the dairy sector

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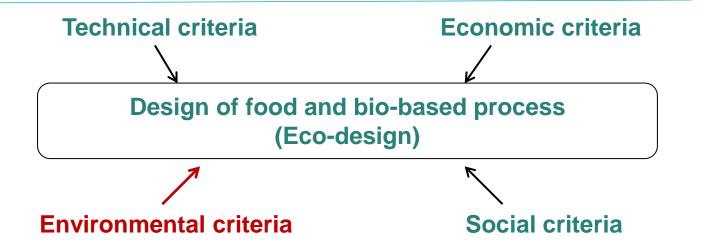






Rennes

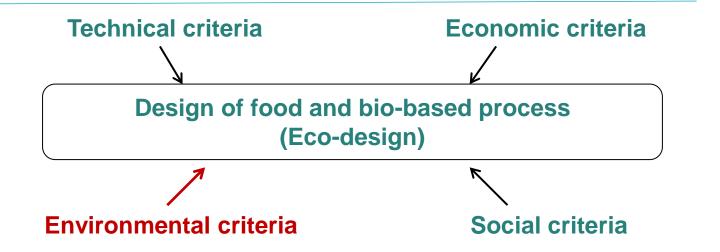
Definition



Eco-design: Integration of "environmental impacts" from the early design or re-design stage of the process



Definition



Eco-design: Integration of "environmental impacts" from the early design or re-design stage of the process

Eco-efficiency is the equation between the value of a product/ service/process and its impact on the environment



> Why eco-design food processing?

- 1/ The food processes face evolving economic situation: increase in price of energy & water; depletion of water supply; increase in environmental taxes ...
- 2/ The transformation processes use raw materials with high environmental impacts. They should avoid losses and wastes.
- 3/ The transformation processes should meet demands / regulations in terms of eco-designed products
 - evolving regulatory framework : e.g. Ecological labelling
 - increase in consumer awareness

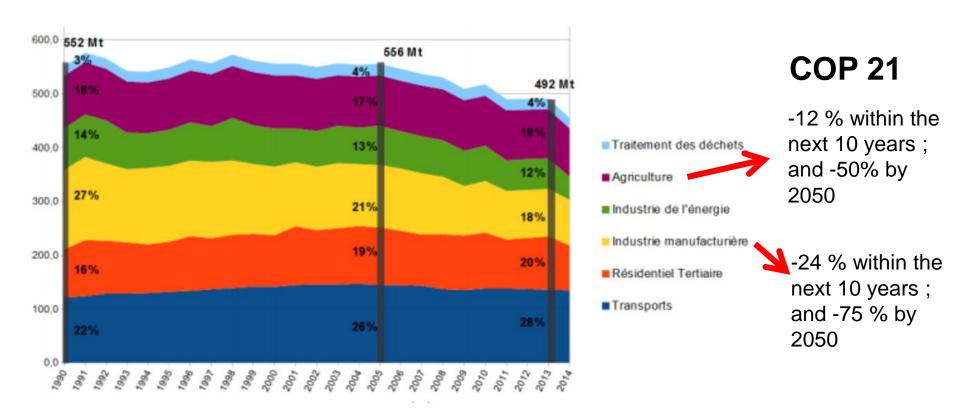
Encouragement by COP 21 in Paris, 7 years ago



> Why eco-design food processing?

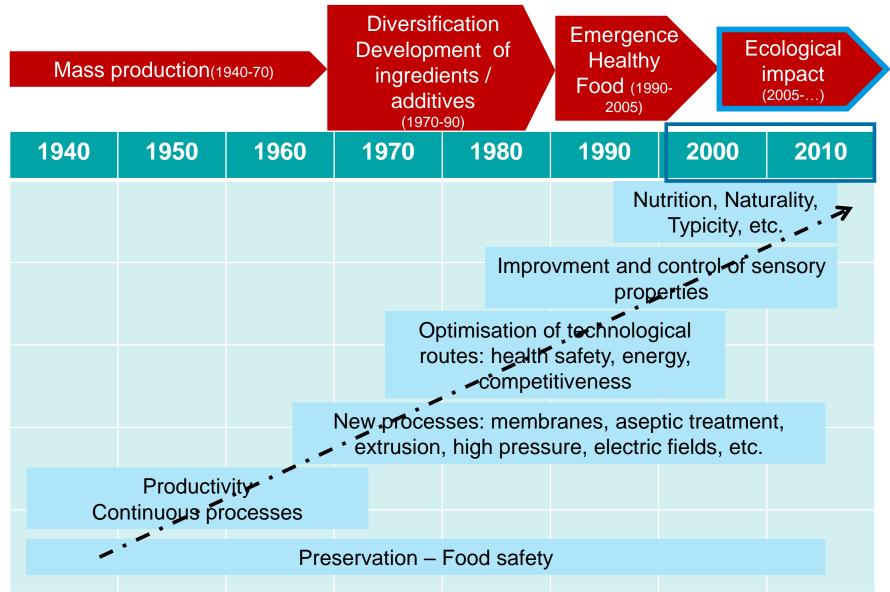
Much effort has to be made on manufacturing industries in the next years (COP 21)

Evolution of Greenhouse gas emissions in France from 1990 and 2013

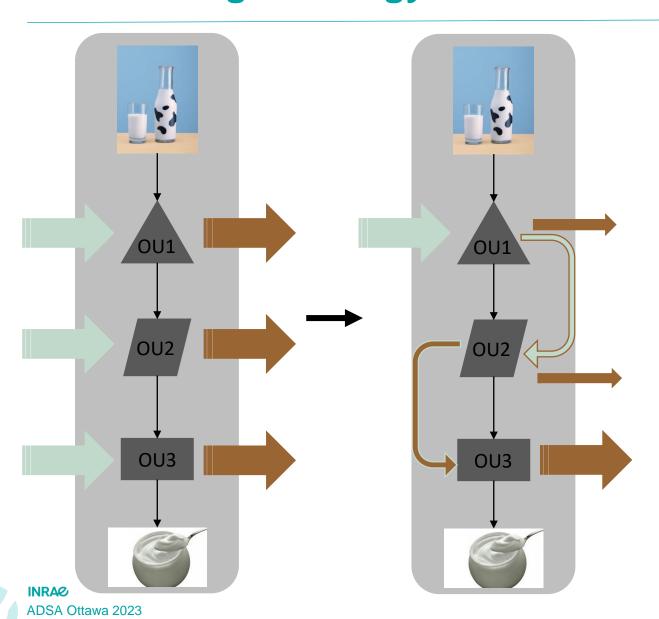




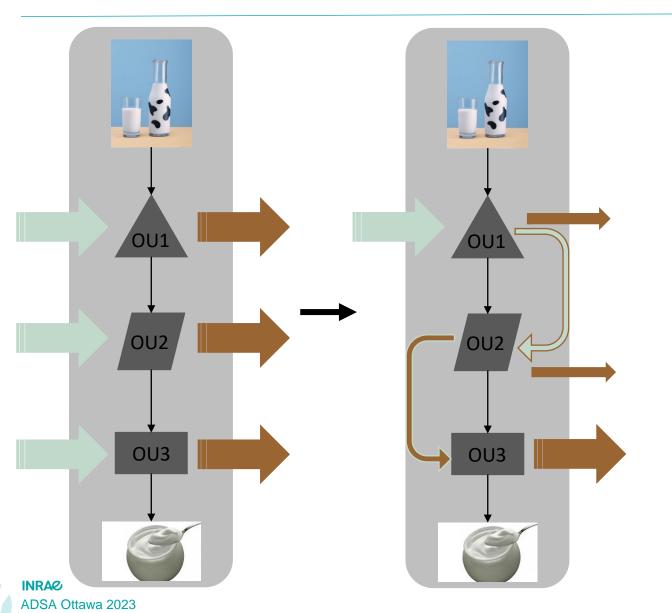
> Evolution in food processing

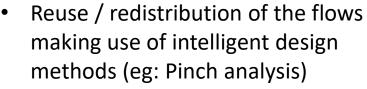






- Reuse / redistribution of the flows making use of intelligent design methods (eg: Pinch analysis)
- Modifications of operating conditions (temperature, flux < critical flux, ...)
- → Reduction of costs (driver = economy)







→ Reduction of costs (driver = economy)

- Single action on water or energy consumptions
- Does not consider modifications of food product
- Does not allow search for a global optimum
- Low potential of innovation, but significant economic and environmental benefits



- Reduction of energy consumption in ripening chambers

EuropeanTruefood (2006-2010), Picque et al., IDJ, 2009

<u>Context</u>: The ripening cheese rooms are constantly ventilated, and the energy cost for this ventilation is high (50% of the cost linked to ripening)

- 1- A sequential ventilation procedure based on the control of temperature was adopted
- 2- Electrical energy savings =~ 50-60 % of the consumption linked to ventilation with no significant impact on the quality of the cheeses (microbiology, biochemistry)



Cellar volume ~ 1300 m³ Ripened cheeses ~ 20 000

- Recommendations for rationalizing cleaning-in-place in dairies

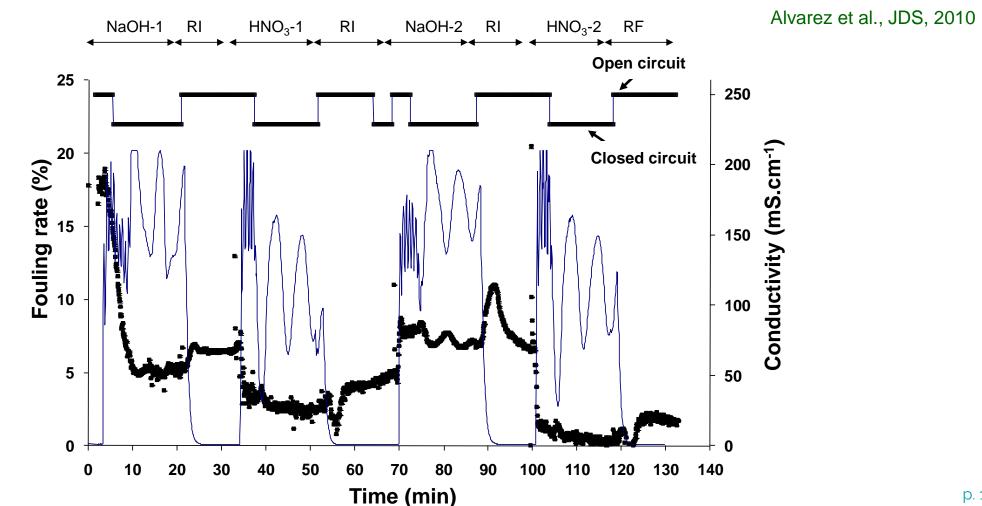
Industrial project, Alvarez et al. JDS, 2010

- 1- A new strategy based on the on-line and off-line use of sensors and tracers was implemented (case study of an ultra-high temperature heat exchanger)
- 2- The CIP operating time and the volume and load of effluents was reduced by half.



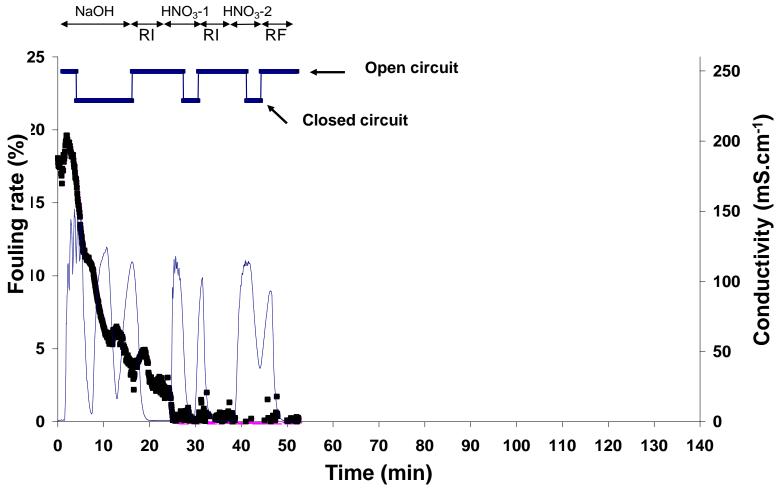


Example of an ultra-high temperature heat exchanger - chocolate cream Initial situation



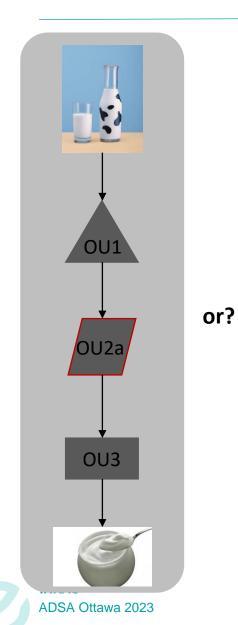
Example of an ultra-high temperature heat exchanger - chocolate cream Improved situation

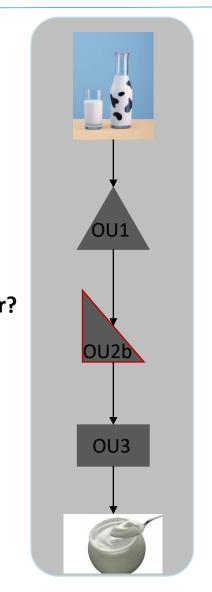
Alvarez et al., JDS, 2010



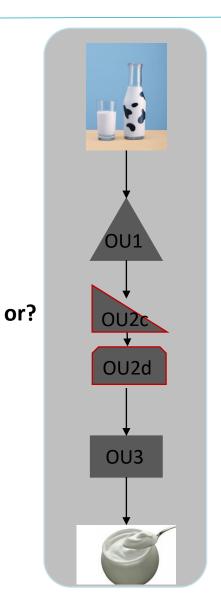
Eco-design strategy n°2: Comparative assessment of processes

Life Cycle Analysis, LCA





OU: unit operation





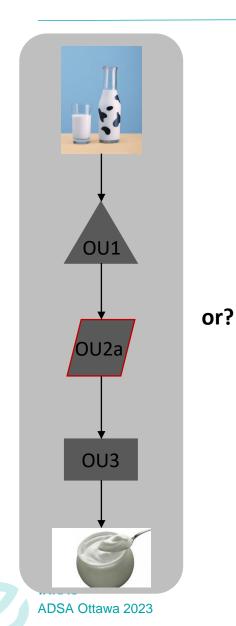


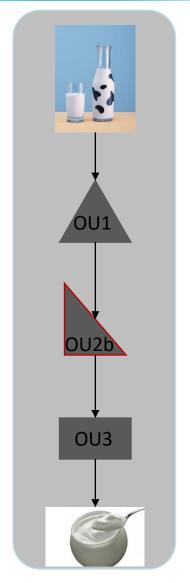


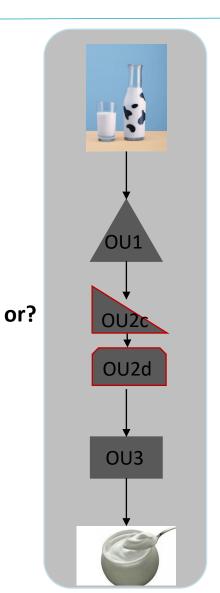
- Simple and readily applicable
- Easy when product is not affected (constant Functional Unit)
- Identification of « hot spots »
- Comparison of scenarios and technologies

Eco-design strategy n°2: Comparative assessment of processes















- Simple and readily applicable
- Easy when product is not affected (constant Functional Unit)
- Identification of « hot spots »
- Comparison of scenarios and technologies

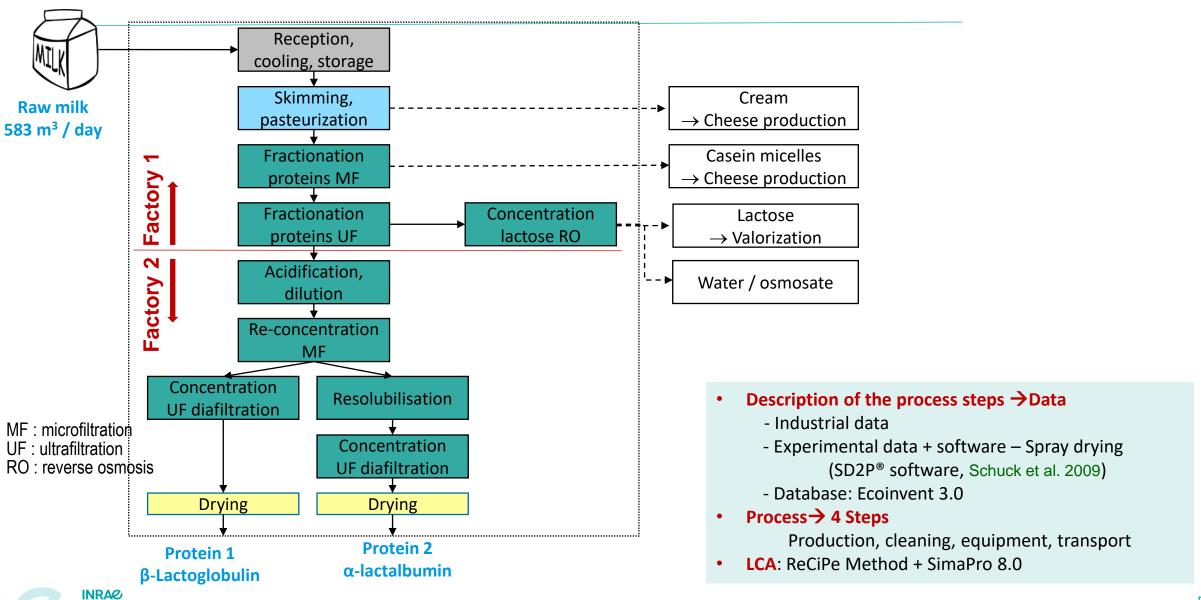


- Tricky when product (and Functional Unit) is affected
- Collection of data difficult
- Does not offer solutions for improvement
- Does not allow search for a global optimum



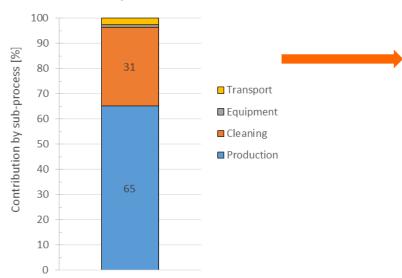
> Industrial milk protein fractionation process

ADSA Ottawa 2023



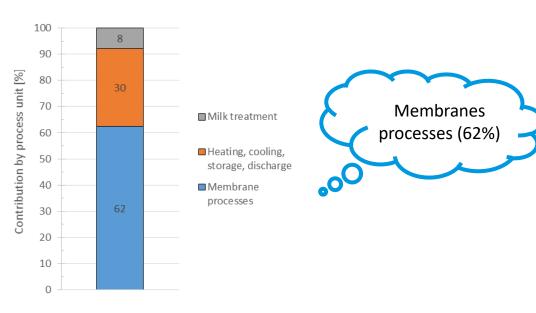
Industrial milk protein fractionation process Examples of results

Contribution of sub-process to the environmental impact according to Impact2002+



Production (65 %) and cleaning (31 %) phases are the main contributors to the overall environmental impact

Cleaning



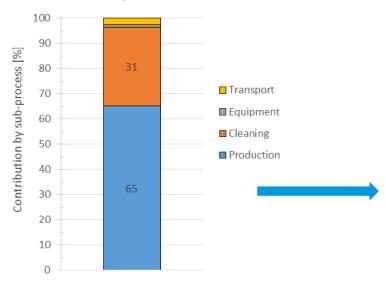
Cleaning of the membranes is the main contributor to the environmental impact of the entire cleaning phase (multiple single passage steps requiring high amounts of freshwater and detergents)

Underestimation of the impact stemming from cleaning the membranes due to missing data for certain cleaning agents that are contained in the complex cleaning solutions



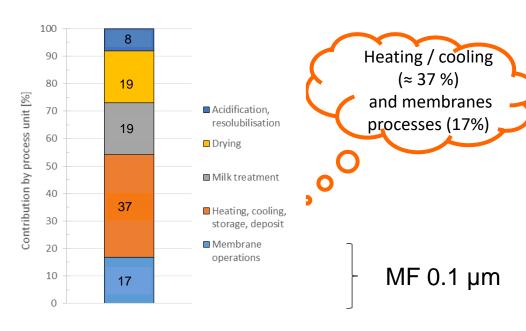
Industrial milk protein fractionation process Examples of results

Contribution of sub-process to the environmental impact according to Impact2002+



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Production



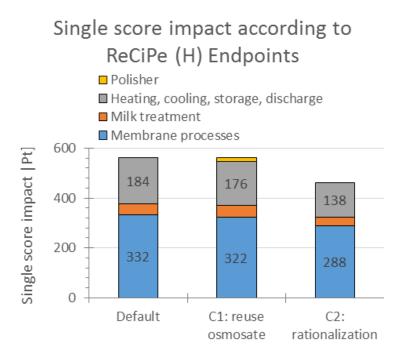
Membranes operations (17%) and heating / cooling / storage (37 %) operations are the main contributors to the overall environmental impact of the production phase



Industrial milk protein fractionation process

Examples of results

Impacts of 2 novel cleaning strategies / alternatives



C1: Reutilization of the water from the lactose concentration process → reduction of the freshwater consumption but requirement of a polisher

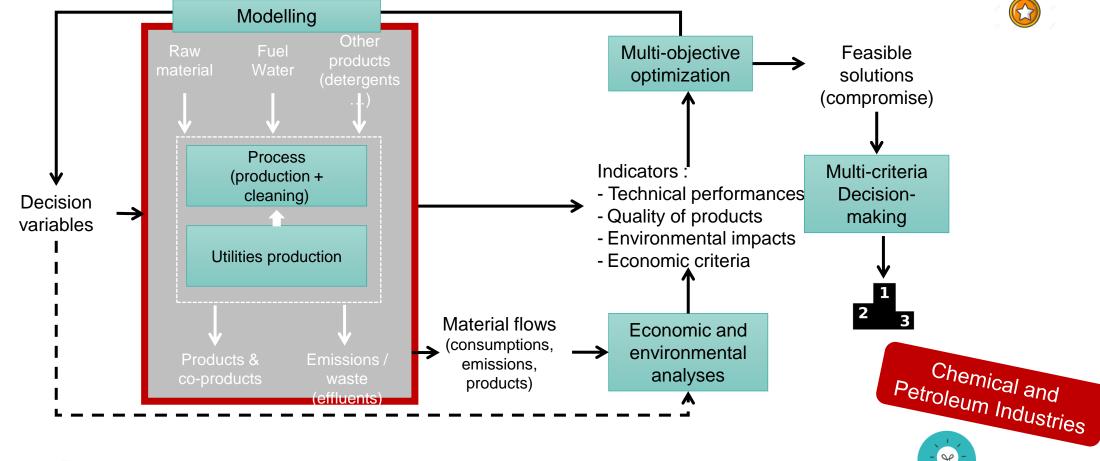
C2: Rationalization of the cleaning solutions (less frequent caustic soda CIP renewal, reduction of cleaning time, etc.) → reduced consumption of resources

If regarded in detail, the optimization strategies show an improvement for certain categories: ReCiPe: in 12/18



Eco-design strategy n°3: Multi-objective optimization

Azzaro-Pantel et al, FBP, 2022 Moulton Junior Medals 2023, awarded by IChemE



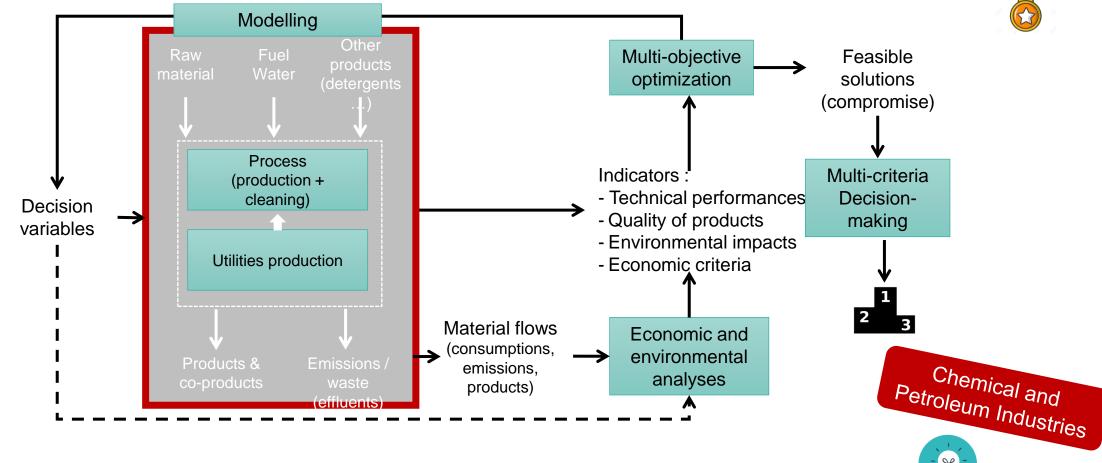


Simultaneous optimization of conflicting objectives



Eco-design strategy n°3: Multi-objective optimization

Azzaro-Pantel et al, FBP, 2022 Moulton Junior Medals 2023, awarded by IChemE





Simultaneous optimization of conflicting objectives



Lack of process models

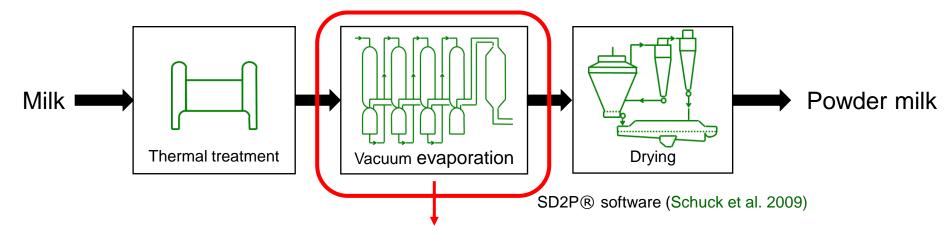
- Food properties difficult to predict
- Lack of knowledge on the impact of decision variables
- Scarce use of process simulators

Eco-design strategy n° 3: Multi-objective optimization

Case study: evaporation of milk / process simulator

Concentration and drying of dairy products

☐ Highly energy-intensive process: 25% of the total energy used in the dairy industry (Agreste, 2011)

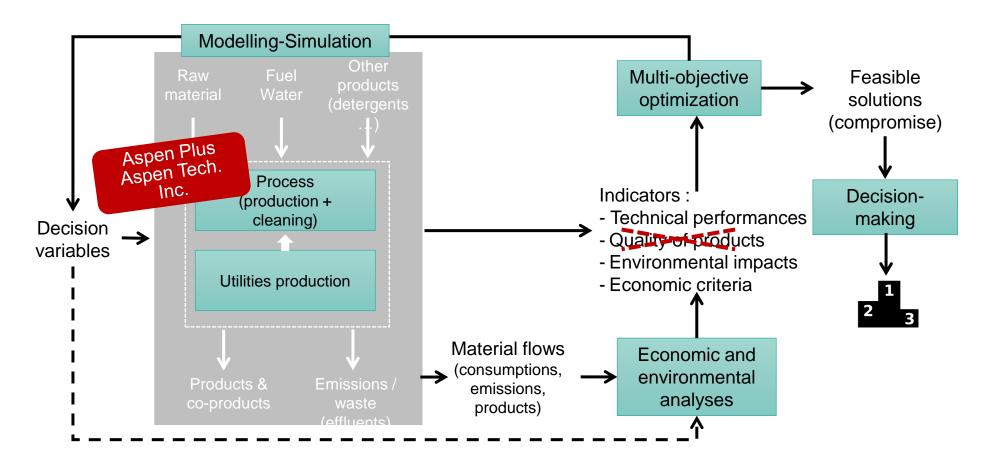


- □ > 50% of the energy consumption of the overall concentration and drying process (Jebson, 1991)
- □ Various options for evaporator design
- Use of a Process simulator
 - > to design evaporator
 - to choose the primary source of energy needed for the steam production



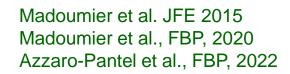
Eco-design strategy n° 3: Multi-objective optimization

Case study: evaporation of milk / process simulator



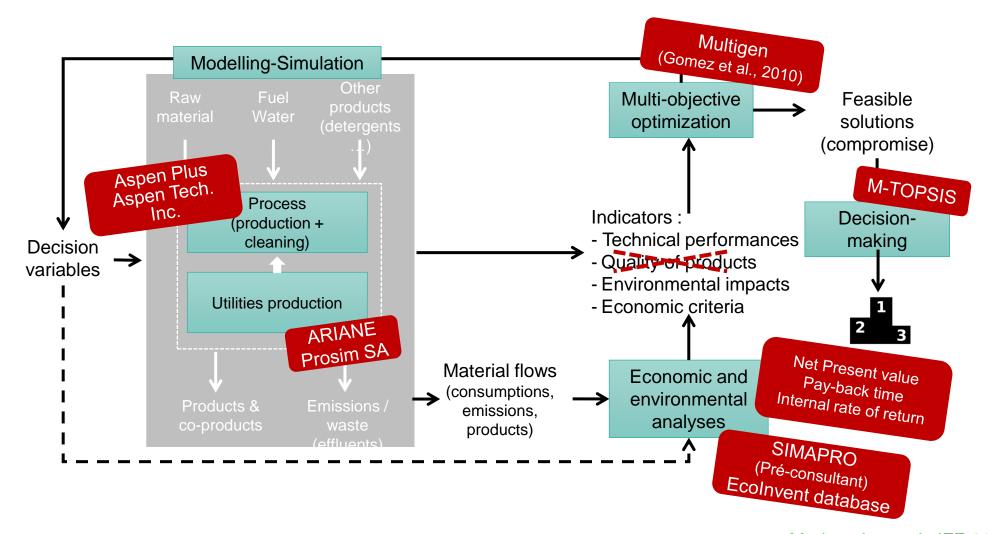
Choice of Aspen Plus

- Coupling with optimization algorithms
- Integration of data/correlations/ models in the software by users



Eco-design strategy n° 3: Multi-objective optimization

Case study: evaporation of milk / process simulator

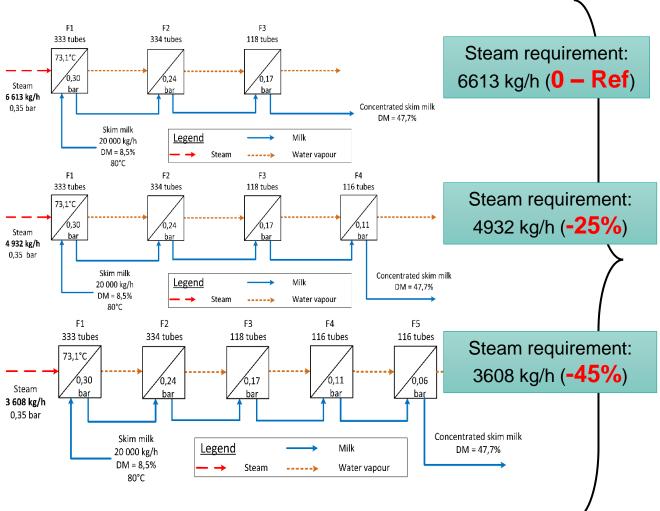




Eco-design strategy n° 3: Multi-objective optimization

Case study: evaporation of milk / process simulator

→ Choice of the number of effects



Parameters of the Process

Falling-film evaporator

20 t/h of treated skimmed milk 50 % DM of the concentrate

Constant CIP sequences

Primary source of energy = natural gas

Variables in design

Number of effects ([3;4;5])

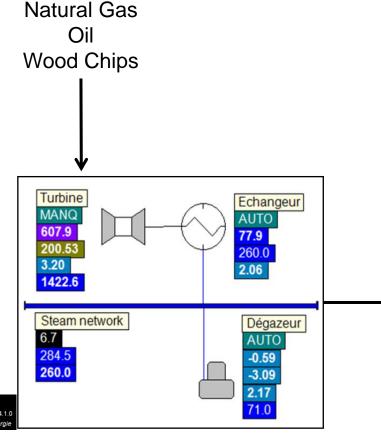


Madoumier et al. JFE 2015 Madoumier et al., FBP, 2020 Azzaro-Pantel et al., FBP, 2022

Eco-design strategy n° 3: Multi-objective optimization

Case study: evaporation of milk / process simulator

→ Choice of the primary source of energy



Parameters of the Process

Constant evaporation process

20 t/h of treated skimmed milk 50 % DM of the concentrate

Constant CIP sequences

Variables in design

Fuel: natural gas, oil, wood chips

Calculation of utility consumption (water, fuel, etc., electricity) combustion emissions (carbon dioxide, nitrogen oxides, etc.) according to energy demand of the evaporator

environmental and economic impacts



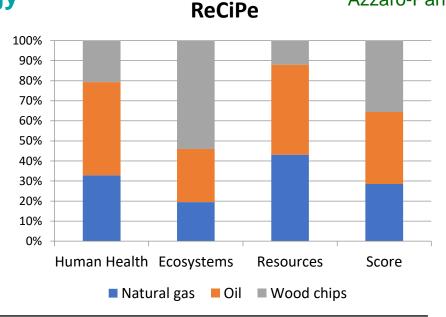
Eco-design strategy n° 3: Multi-objective optimization

Case study: evaporation of milk / process simulator

→ Choice of the primary source of energy

Madoumier et al. JFE 2015 Madoumier et al., FBP, 2020 Azzaro-Pantel et al., FBP, 2022

Environmental criteria



Economic criteria

	Net Present value (+) (M€)	Pay-back time (-) (year)	Internal Rate of Return (+) (%)
Natural Gas (reference)	8.26	3.6	47
Oil	9.34 (+13%)	3.4 (-7%)	51 (+9%)
Wood chips	9.54 (+16%)	4.0 (+9%)	42 (-10%)



Eco-design strategy n° 3 : Multi-objective optimization

Case study: evaporation of milk / process simulator

→ Choice of the primary source of energy

Multicriteria analysis (M-TOPSIS)

	Combustible		
	Natural gas	Oil	Wood chips
Net Present Value, Single score ReCiPe	1	3	2
3 economic criteria,3 Endpoint scores ReCiPe	2	3	1





Eco-design strategy n° 3: Multi-objective optimization

Belna et al. JFE, 2020 Belna et al, ESWA, 2022 Baudrit et al., IJAEIS, 2022

Case study: microfiltration of milk / knowledge integration

Microfiltration 0.1 µm of milk

☐ Fractionation of the two major groups of dairy proteins
 → (cheese manufacture, production of ingredients)



UTP, Uniform Transmembrane Pressure System (Sandblöm, 1974)

Membrane with permeability gradient



Spiral wound

- □ Various options for microfiltration design→ conflicting objectives
- ☐ No optimization of MF design integrating conflicting objectives
- ☐ Lack of predictive MF performance models

Input of Artificial Intelligence

> Use of « Expert knowledge integration » to design microfiltration



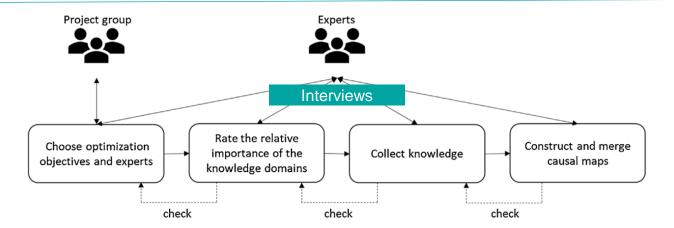




Eco-design strategy n° 3: Multi-objective optimization

Belna et al. JFE, 2020 Belna et al, ESWA, 2022 Baudrit et al., IJAEIS, 2022

Case study: microfiltration of milk / knowledge integration

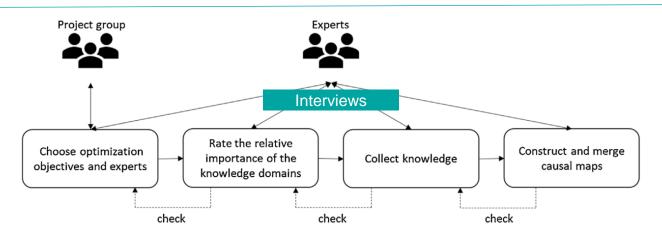




Eco-design strategy n° 3 : Multi-objective optimization

Case study: microfiltration of milk / knowledge integration

Belna et al. JFE, 2020 Belna et al, ESWA, 2022 Baudrit et al., IJAEIS, 2022



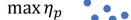
- 5 optimisation objectives
- 5 decision variables
- 31 intermediate variables

 $\max CD_{CN,r}$



Casein concentration in retentate on dry basis

 $\max CD_{SP,p}$ Serum protein concentration in permeate on dry basis





Serum protein protein recovery rate

min Cl



Investment cost

min CPR



Productionc cost

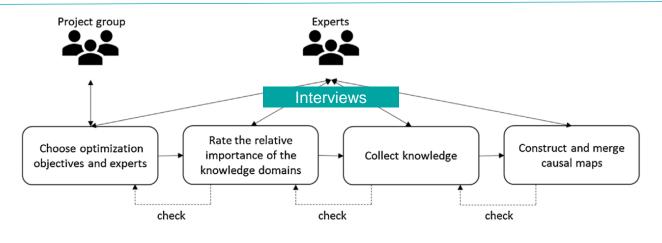
- Casein micelles
- Serum proteins

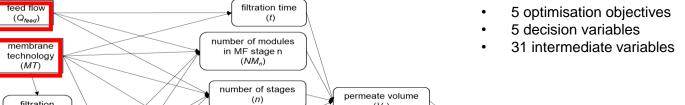


Eco-design strategy n° 3 : Multi-objective optimization

Case study: microfiltration of milk / knowledge integration

Belna et al. JFE, 2020 Belna et al, ESWA, 2022 Baudrit et al., IJAEIS, 2022





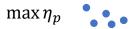
filtration temperature (T)serum protein serum protein quantity in recovery yield permeate in permeate $(q_{SP,p})$ (VRRn) serum protein serum protein concentration in transmembrane transmission permeate pressure (Tr_{SP}) (TMP) Decision variable Intermediate variable recirculation flow n

 $\max CD_{CN,r}$



Casein concentration in retentate on dry basis

 $\max CD_{SP,p}$ Serum protein concentration in permeate on dry basis



Serum protein protein recovery rate

min Cl



Investment cost

min CPR

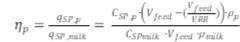


Productionc cost

- Casein micelles
- Serum proteins

INRAE ADSA Ottawa 2023

 $(Q_{rec,n})$



Hobballah et al. Expert Syst. (2018)

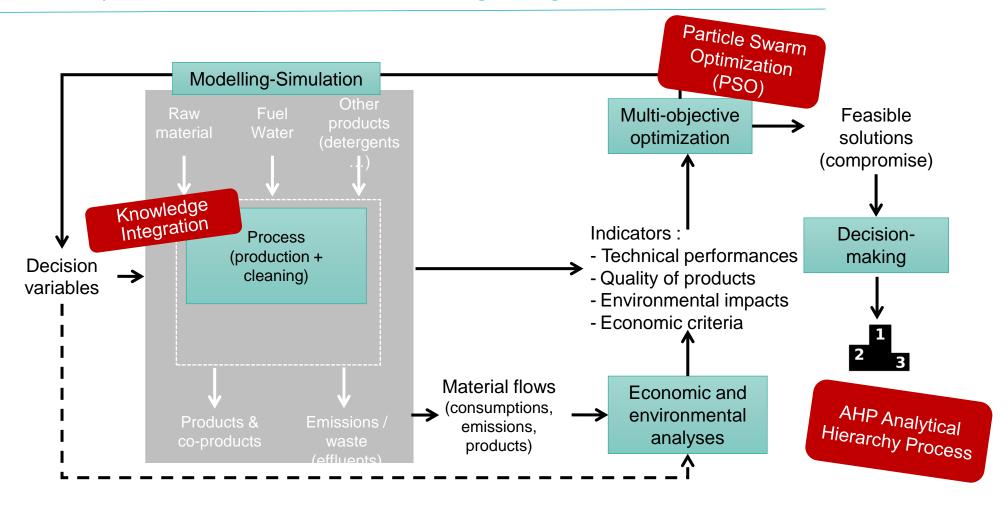
Optimization objective



Eco-design strategy n° 3: Multi-objective optimization

Belna et al. JFE, 2020 Belna et al, ESWA, 2022 Baudrit et al., IJAEIS, 2022

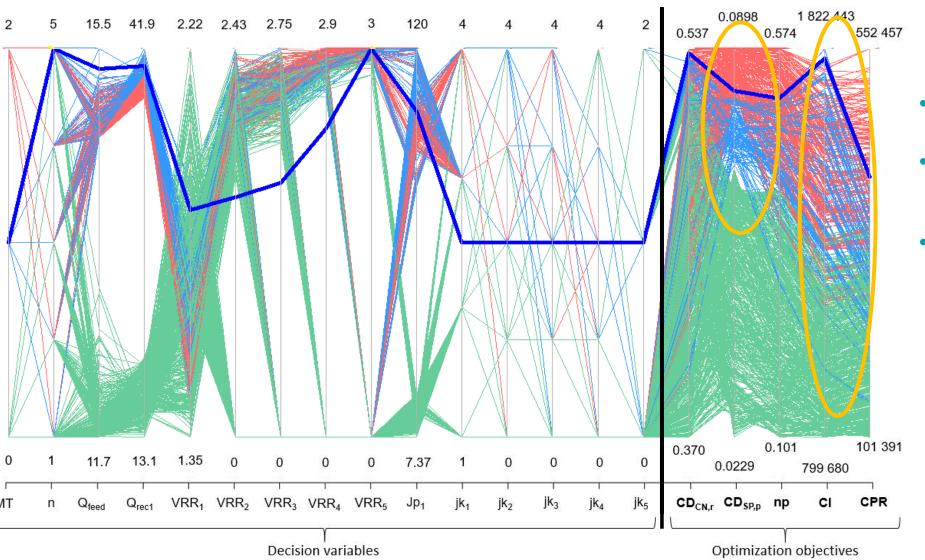
Case study: microfiltration of milk / knowledge integration





Belna et al, ESWA, 2022



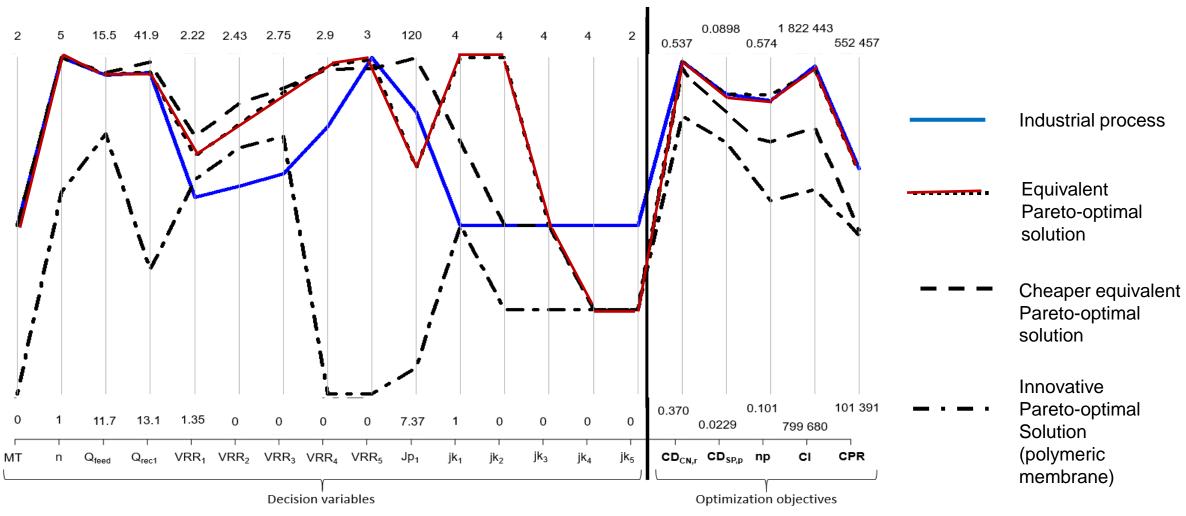


- Over 1000 Paretooptimal solutions
- Consistent with literature and industrial practices
- Trade-off in the choice of MT:
 Ceramic membranes compared to polymeric:

Technical objectives more efficient
BUT
More expensive

 $Q_{\text{feed}} \ (m^3.h^{\text{-}1}) \ ; \ Q_{\text{rec}1} \ (m^3.h^{\text{-}1}) \ ; \ Jp_1 \ (L.h^{\text{-}1}.m^{\text{-}2}) \ ; \ CD_{CNr} \ (g.kg^{\text{-}1} \ DM) \ ; \ CD_{SPp} \ (g.kg^{\text{-}1} \ DM) \ ; \ CI \ (\ree) \ ; \ CPR \ (\ree)$

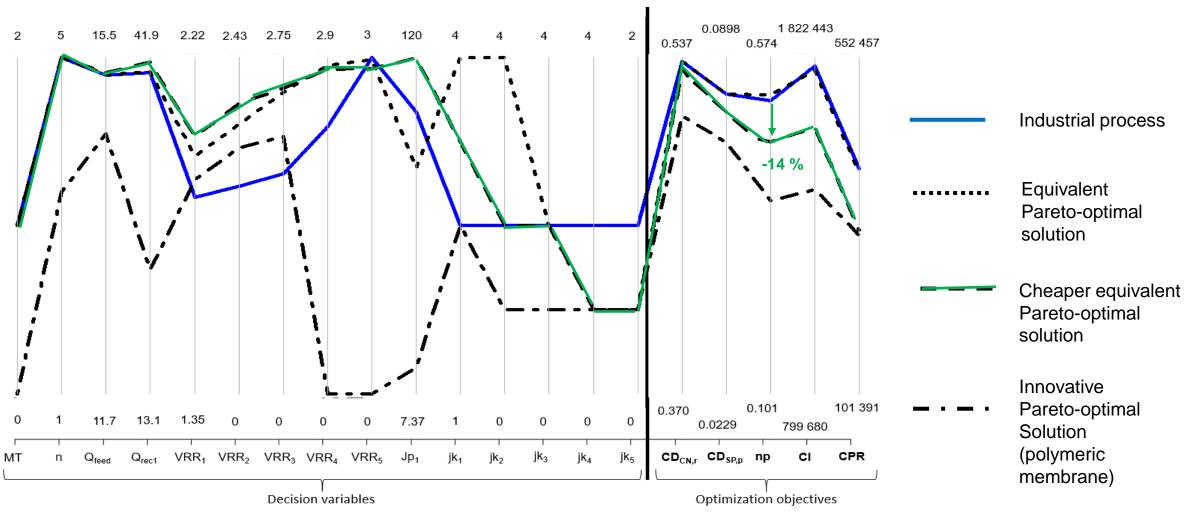
> Particular Pareto-optimal solutions analysis



 $Q_{\text{feed}} \ (m^3.h^{-1}) \ ; \ Q_{\text{rec}1} \ (m^3.h^{-1}) \ ; \ Jp_1 \ (L.h^{-1}.m^{-2}) \ ; \ CD_{CNr} \ (g.kg^{-1} \ DM) \ ; \ CD_{SPp} \ (g.kg^{-1} \ DM) \ ; \ CI \ (\ree) \ ; \ CPR \ (\ree)$



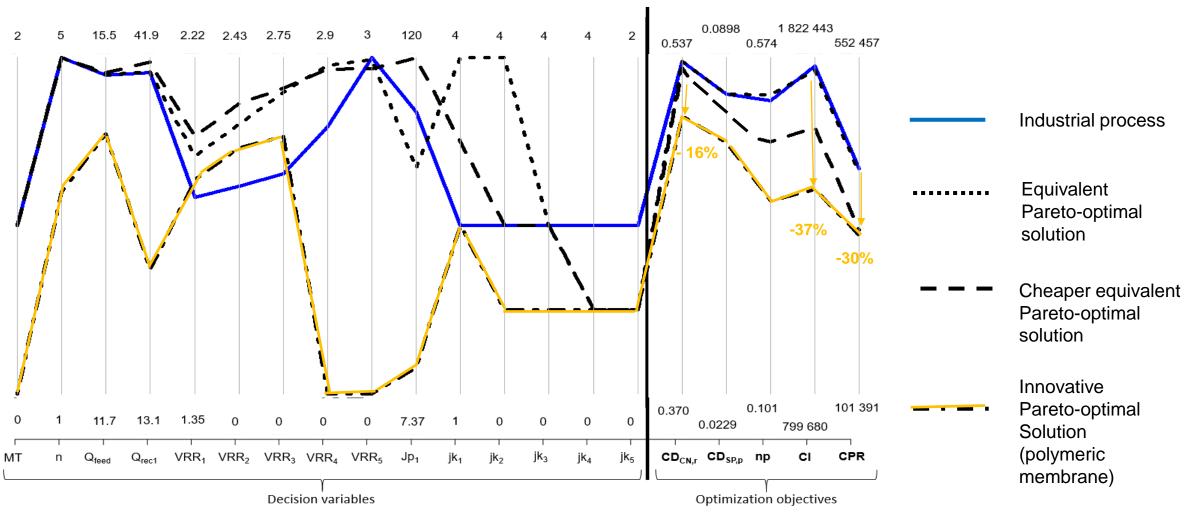
> Particular Pareto-optimal solutions analysis



 $Q_{\text{feed}} \ (m^3.h^{-1}) \ ; \ Q_{\text{rec}1} \ (m^3.h^{-1}) \ ; \ Jp_1 \ (L.h^{-1}.m^{-2}) \ ; \ CD_{CNr} \ (g.kg^{-1} \ DM) \ ; \ CD_{SPp} \ (g.kg^{-1} \ DM) \ ; \ CI \ (\ree) \ ; \ CPR \ (\ree)$



> Particular Pareto-optimal solutions analysis



 $Q_{\text{feed}} \ (m^3.h^{-1}) \ ; \ Q_{\text{rec}1} \ (m^3.h^{-1}) \ ; \ Jp_1 \ (L.h^{-1}.m^{-2}) \ ; \ CD_{CNr} \ (g.kg^{-1} \ DM) \ ; \ CD_{SPp} \ (g.kg^{-1} \ DM) \ ; \ CI \ (\ree) \ ; \ CPR \ (\ree)$



> Take-home messages

- 1/ Strategies of eco-design of food processing have emerged for < 20 years
- → Different levels of strategies are possible
- → Inspiration can be taken from other industrial sectors and disciplines
- 2/ Holistic multi-objective optimization methods are relevant and can be used to improve the design of food process taking into account sustainability criteria
- 3/ Efforts are still needed
- To improve the methodologies, the collection, storage and update of data, and user-friendly tools
- To improve the models and predictive approaches which could help develop multi-objective optimisation methods for processes
- To better implement these approaches in the food supply chain



https://www.fairchain-h2020.eu/



Thank you for your attention!

And to all contributors ...

Maëllis Belna, Martial Madoumier, Nicolas AlvarezAmadou Ndiaye, Franck Taillandier,
Patrice Buche, Cédric Baudrit, Christophe Fernandez
Nadine Leconte, Fabienne Lambrouin, Maksym Loginov
Gaëlle Tanguy, Pierre Schuck



















































